

**Contract No:**

This document was prepared in conjunction with work accomplished under Contract No. DE-AC09-08SR22470 with the U.S. Department of Energy (DOE) Office of Environmental Management (EM).

**Disclaimer:**

This work was prepared under an agreement with and funded by the U.S. Government. Neither the U. S. Government or its employees, nor any of its contractors, subcontractors or their employees, makes any express or implied:

- 1 ) warranty or assumes any legal liability for the accuracy, completeness, or for the use or results of such use of any information, product, or process disclosed; or
- 2 ) representation that such use or results of such use would not infringe privately owned rights; or
- 3) endorsement or recommendation of any specifically identified commercial product, process, or service.

Any views and opinions of authors expressed in this work do not necessarily state or reflect those of the United States Government, or its contractors, or subcontractors.





## Future Recovered Gas Dryer Development (SR19009)

Paul Beaumont, Luke Angelette, George Larsen, David James, and Steve Xiao

### Objectives:

Develop a method to remove strongly adsorbed tritium from 5A zeolite that require only slight modification in the future RGD process.

### Summary:

Recovered Gas Dryers (RGDs) remove tritiated moisture and ammonia from the recovered gas stream. As such, the RGD bed remained at elevated temperatures due to tritium decay heat. It is highly desired to remove or reduce the amount of tritium in the bed. Due to RGD limitations, a catalytic isotope exchange process with protium ( $H_2$ ) is proposed for next generation RGD. This concept builds on our recent and successfully developed water detritiation process and extends it to ammonia detritiation.

### Background:

Temperature-Programed-Desorption (TPD) analysis of 5A zeolites

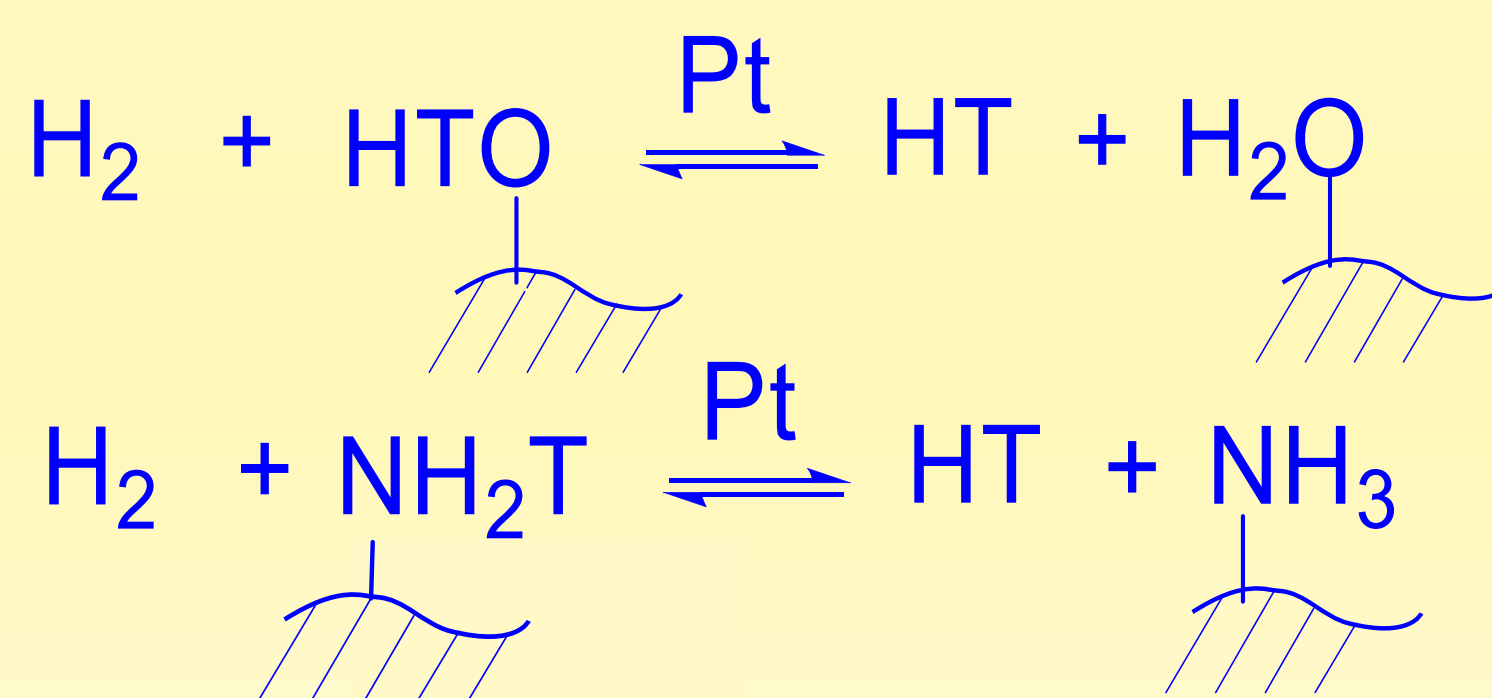
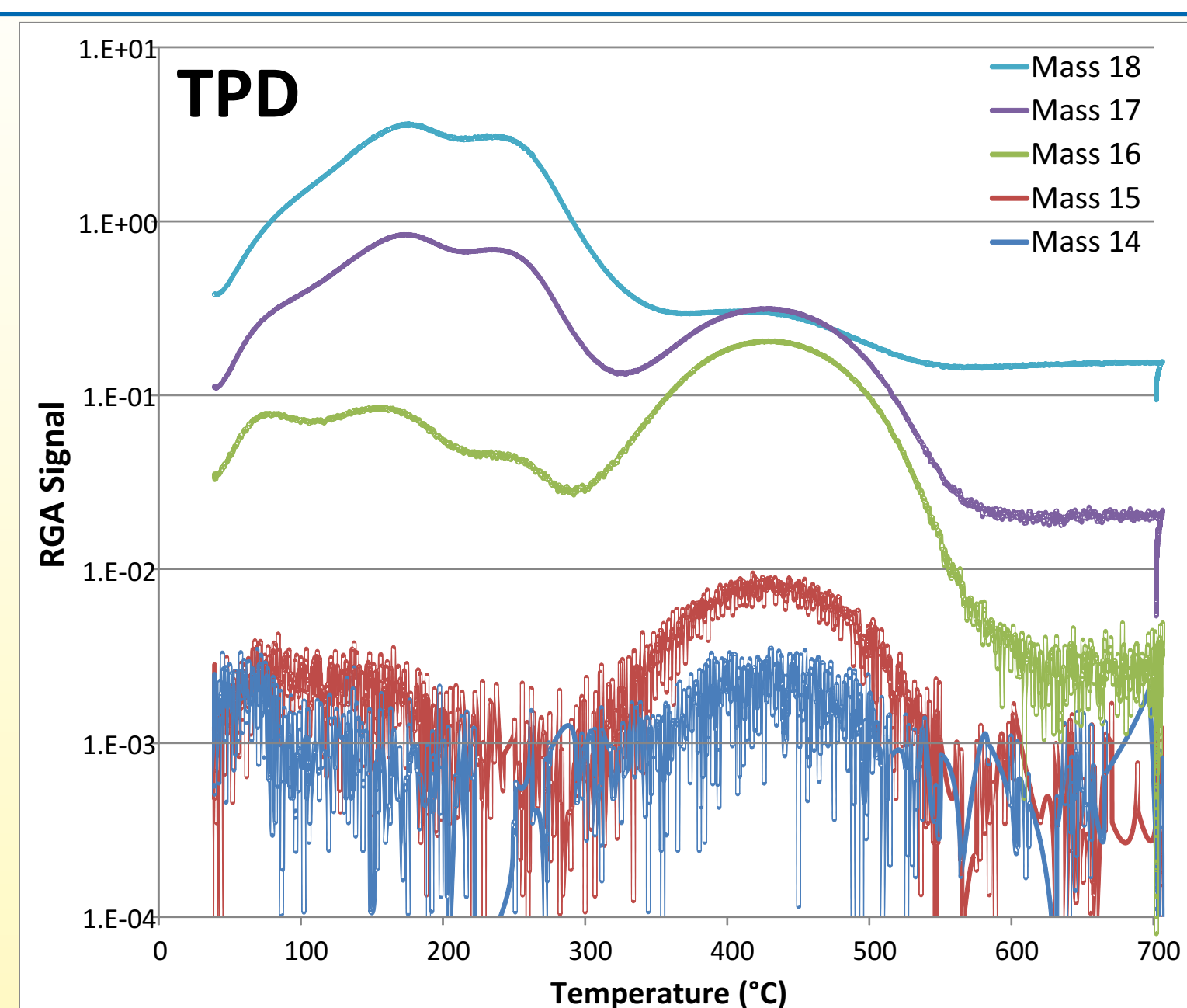
- Moisture desorbs by 350 °C
- Ammonia desorbs by 600 °C
- High temperature bake-outs is not an option due to RGD limitation

Moisture-Ammonia Isotope Exchange

- Does not require high temperature bake-outs
- SRTE RGD location does not have a moisture source to perform task

Catalytic Isotopic Exchange with  $H_2$

- $H_2$  exchanges with adsorbed water and ammonia, catalyzed by Pt



### FY19 Accomplishments:

#### Material Development

Material synthesis and screening for future RGD material with catalytic isotope exchange functionality.

Synthesis variables investigated:

- Incipient wetness impregnation
- Ion exchange
- Catalyst loading
- Type of catalyst support



### FY19 Accomplishments (continued):

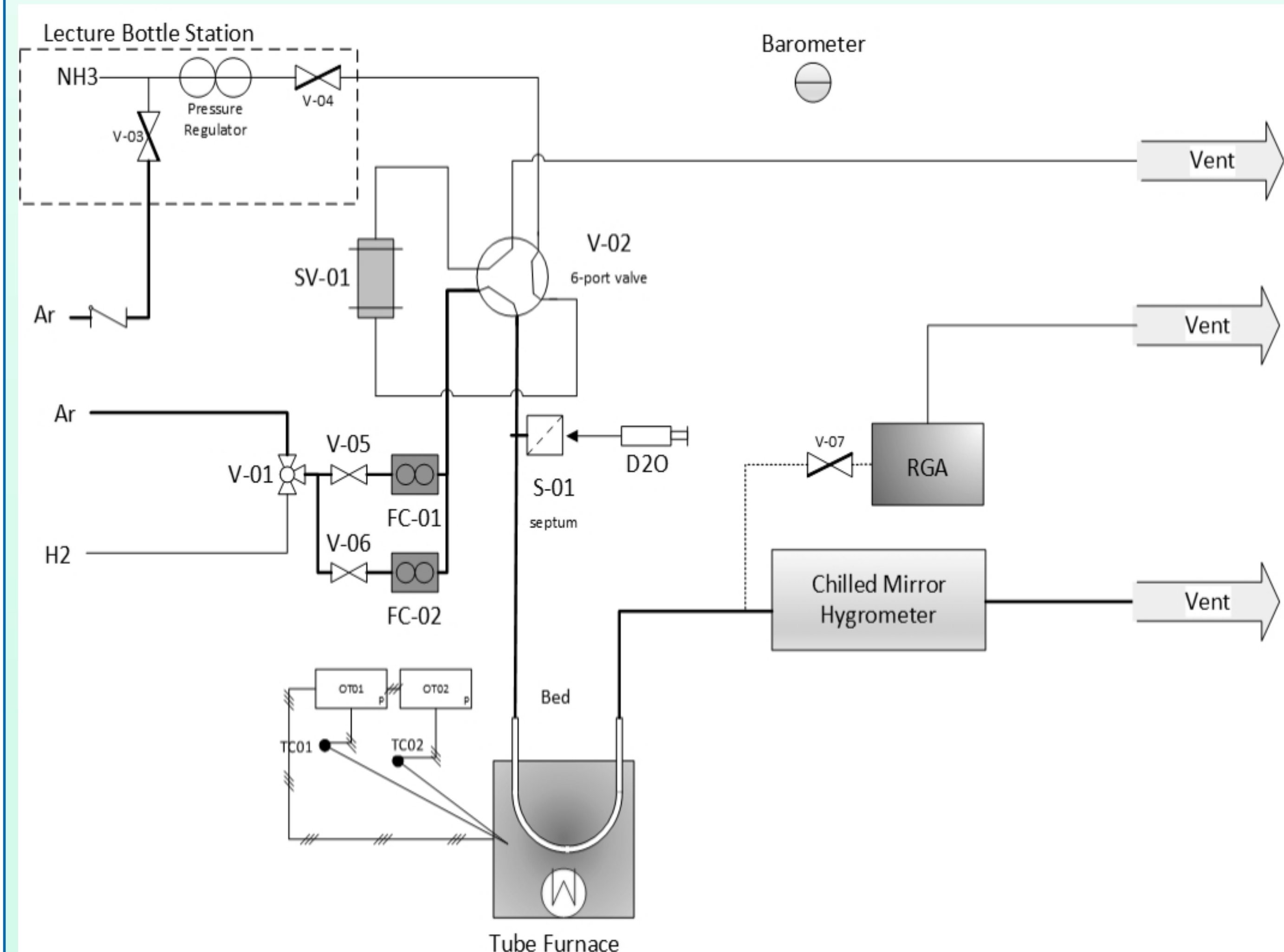
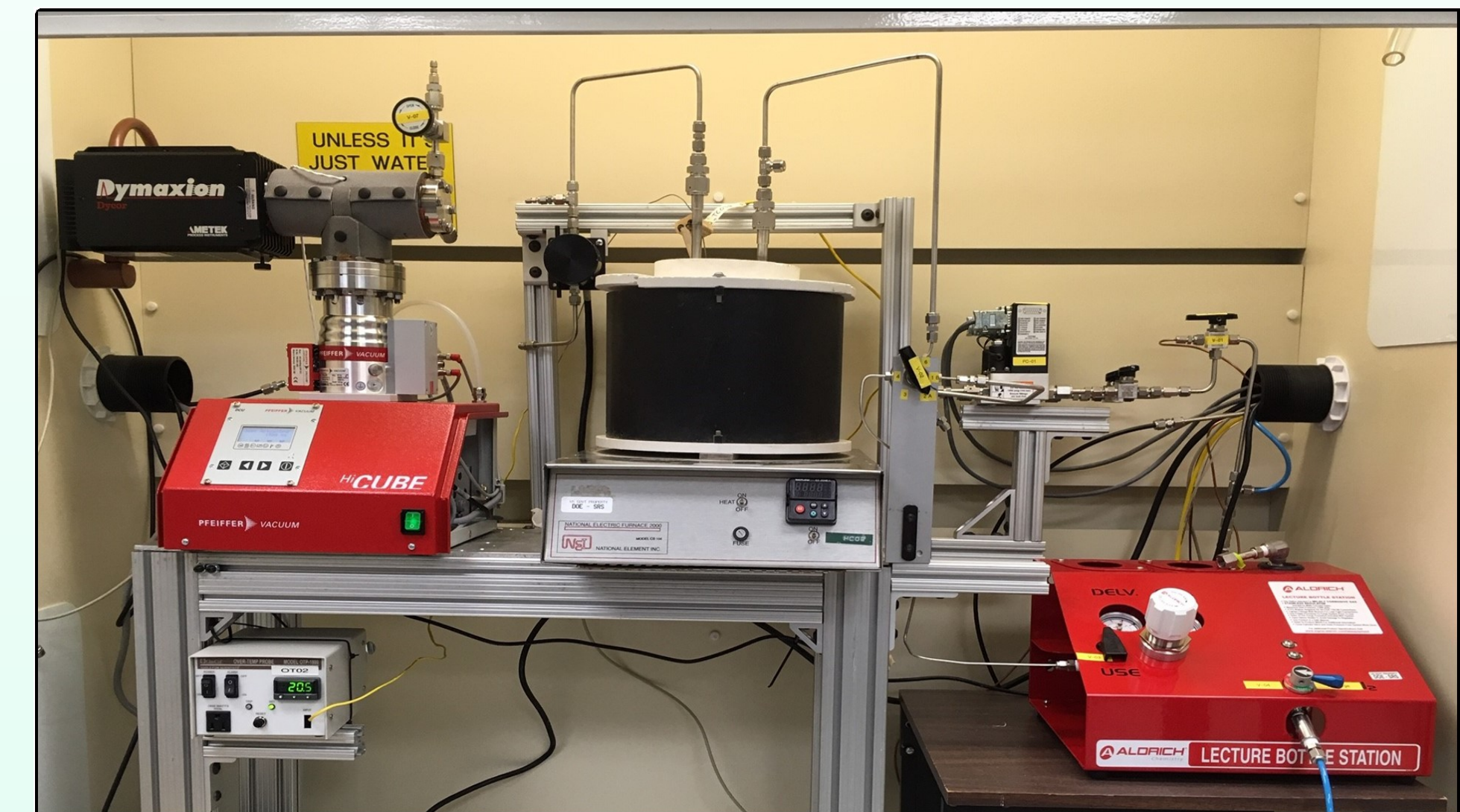
#### Separation Materials

Materials will be screened and evaluated for precious metal dispersions, surface area, isotopic exchange performance, and capacity.



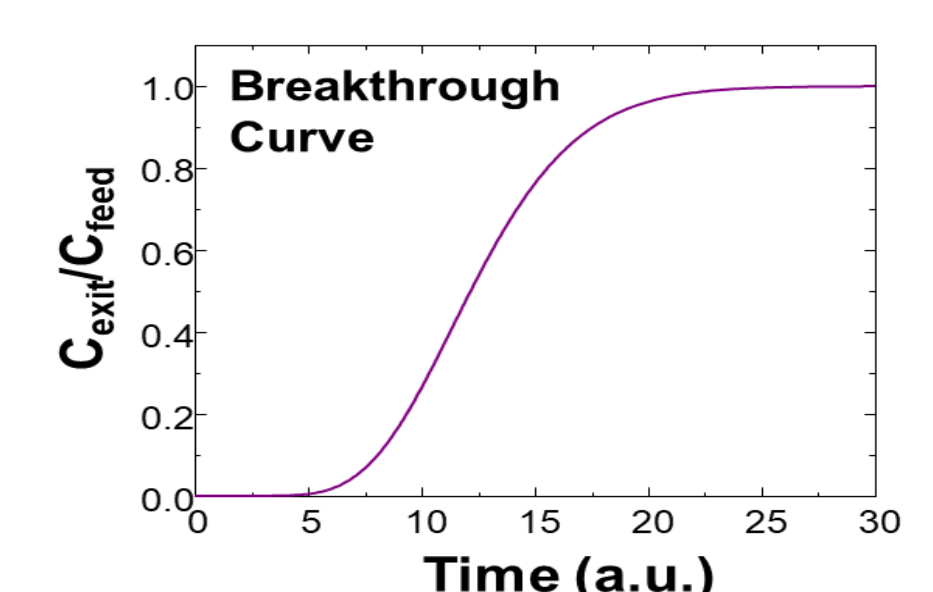
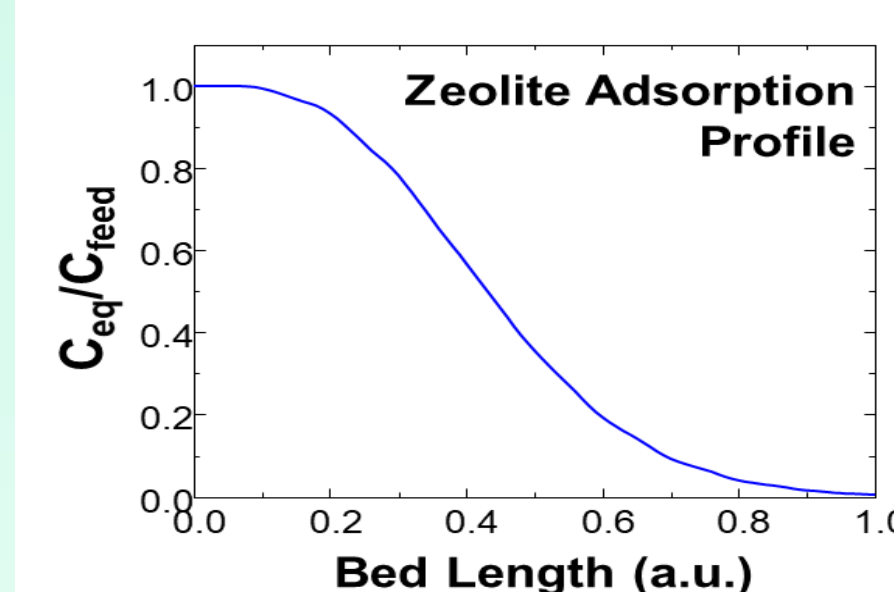
#### Manifold Design and Set up

Designed and assembled test manifold for catalytic isotope exchange performance evaluation.



#### Predictive Modeling

Expected outcome by Langmuir model.



### Acknowledgements:

The authors thank Robbie Allgood, Jared Clark, and Tritium Engineering Co-Lead Heather Mentzer for contributions to this work.

**Funding provided by:** Savannah River Tritium Enterprises (SRTE) Plant Directed Research and Development (PDRD) program.

### FY19 (year 1)



Manifold Design and Setup (Completed Mar)

Mar

Sample Preparation (objective accomplished Mar though work ongoing as discoveries are made)

Performance evaluation of  $H_2O$  and  $NH_3$  absorption (anticipated preliminary results Jun)

Jun

Scoping performance evaluation of catalytic isotope exchange (anticipated preliminary results Jun)

Future bed design (Anticipated execution Jun)

Sep

Issue year-end sample report (anticipated draft by Aug issued Sep)

### FY20 (Year 2) Proposed Activities



Predictive modeling tools expanded  
Additional catalyst impregnation

### FY21 (Year 3) Proposed Activities



Finalize conceptual designs and material specifications