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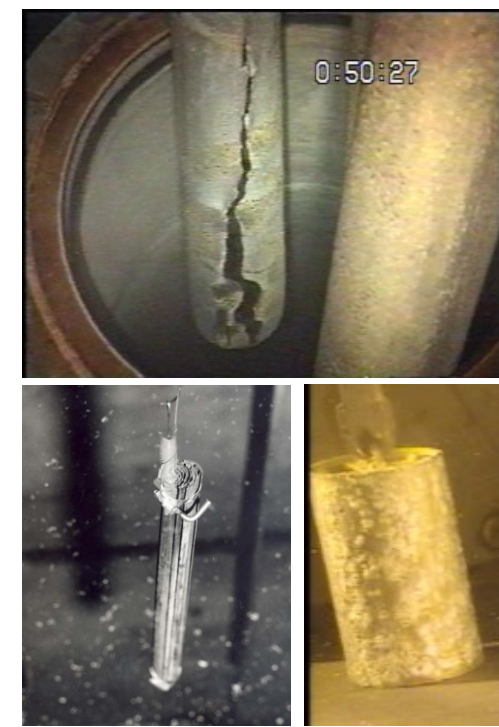
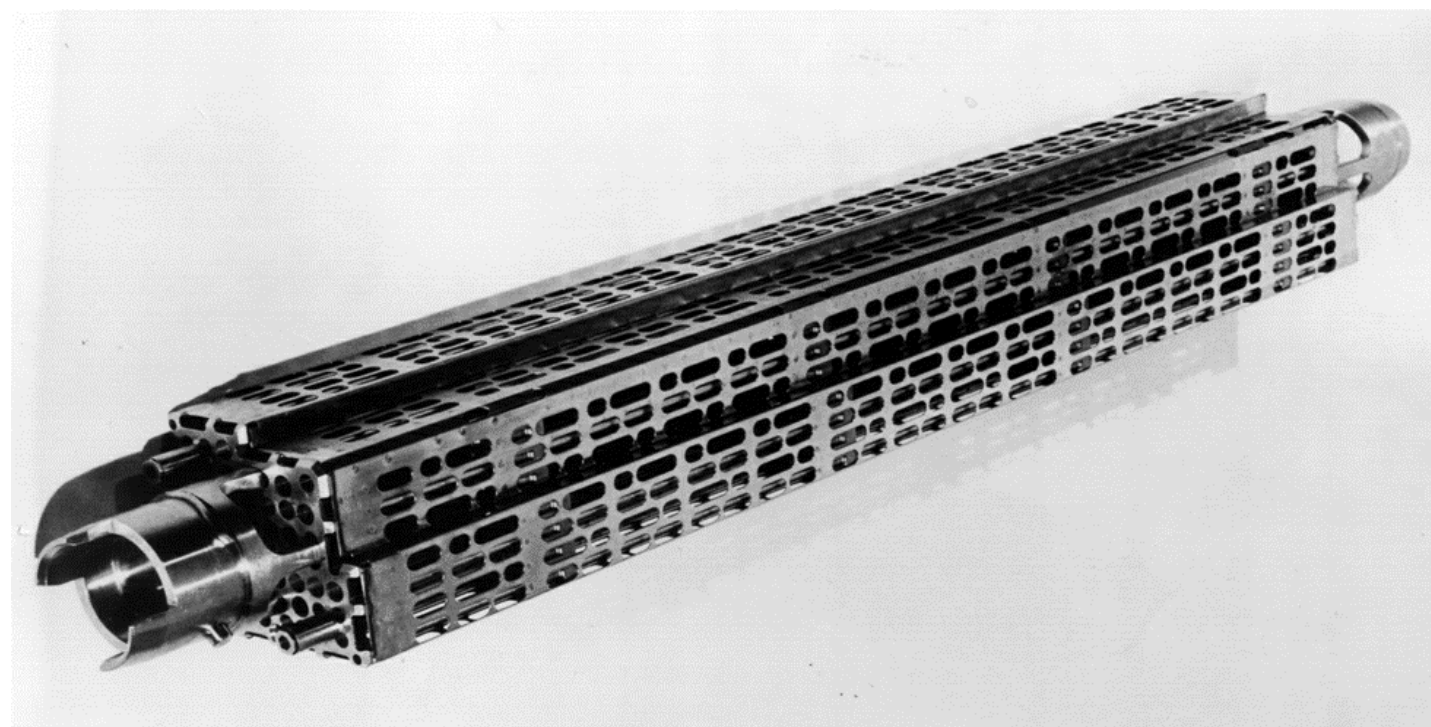
Demonstration of Chemical Decladding and Disposition Options of Non-Al Clad Fuels at the Savannah River Site

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Abstract

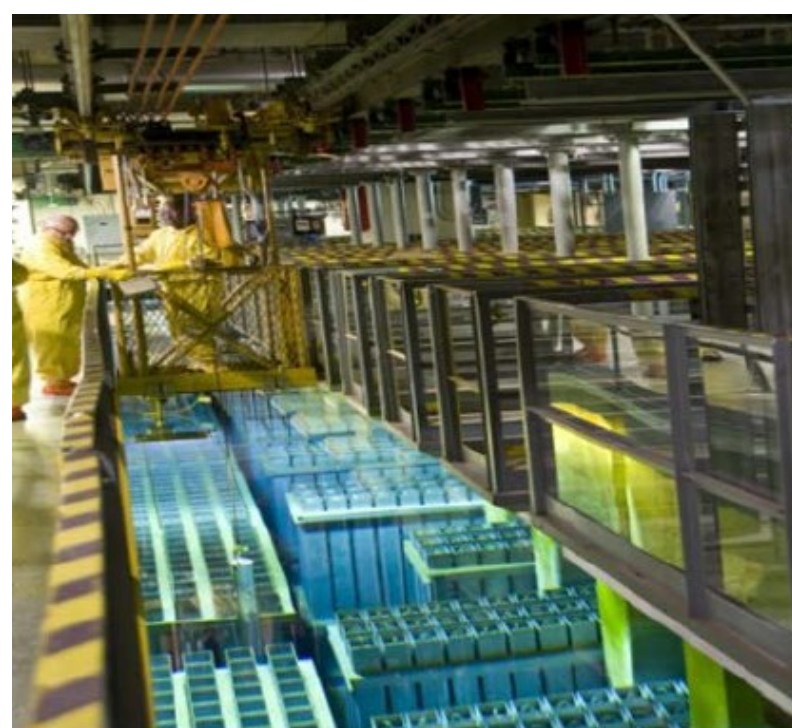
The Savannah River Site's H-Canyon processes aluminum-clad fuels from foreign and domestic research reactors to recover enriched uranium. However, there is an extensive inventory of non-Al-clad fuels currently in the storage basin, many of which are damaged or at risk of failure. Most of these are clad with stainless steel or Zircaloy, which are incompatible with H-Canyon's process chemistry. Development of decladding methods is therefore critical to the waste cleanup mission at SRS. Here we demonstrate the dissolution of stainless steel using the SULFEX process developed at Oak Ridge and the dissolution of Zircaloy using the ZIRFLEX process developed at the Hanford Site. Dissolution and offgassing rates are consistent with previous studies and show that these cladding materials can be processed even below reflux conditions. Waste streams have been treated and quantified, providing valuable information for potential future process development in H-Canyon. This study has demonstrated that the technology may be feasible in the near term for processing smaller damaged fuels in the SRS hot cells.



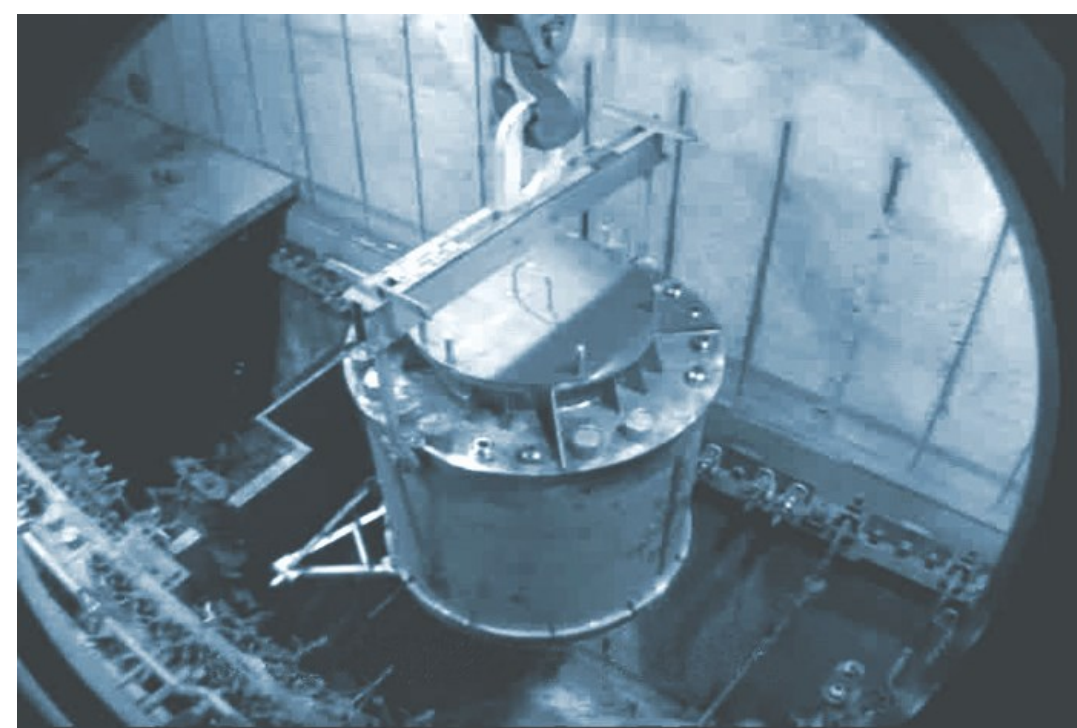
Saxton fuel (left) and various damaged fuels (right) are among the variety of fuels stored in SRS L-basin. Damaged or undamaged fuels can be processed by selective cladding dissolution.

Objectives

- Demonstrate processes for chemical decladding of non-Al clad fuels
 - DAREX – refluxing HCl/HNO₃ ← Stainless steels (e.g. 304L)
 - SULFEX – refluxing H₂SO₄
 - ZIRFLEX – refluxing NH₄F/NH₄NO₃ ← Zr alloys (e.g. Zircaloy-2)
- Determine suitability for H-Canyon implementation
 - Verify previous work done at ORNL and Hanford
 - Define waste streams and offgassing components/rates



L-basin storage pool



H-Canyon dissolver

Experimental Methods

Flowsheet down-selection based on literature review

DAREX: (M = Fe, Ni)
 $M + HNO_3 + 3HCl \rightarrow NOCl + MCl_2 + 2H_2O$
 $HNO_3 + 3HCl \rightarrow Cl_2 + 2H_2O + NOCl$
 $M + 2HNO_3 + 2HCl \rightarrow MCl_2 + 2H_2O + 2NO_2$
 $M + 6HNO_3 \rightarrow M(NO_3)_3 + 3NO_2 + 3H_2O$
 Analogous reactions for Cr

Chloride species are known to cause crevice corrosion and pinhole formation in stainless steels; therefore, DAREX is incompatible with process piping in H-Canyon and was not further explored in this project.

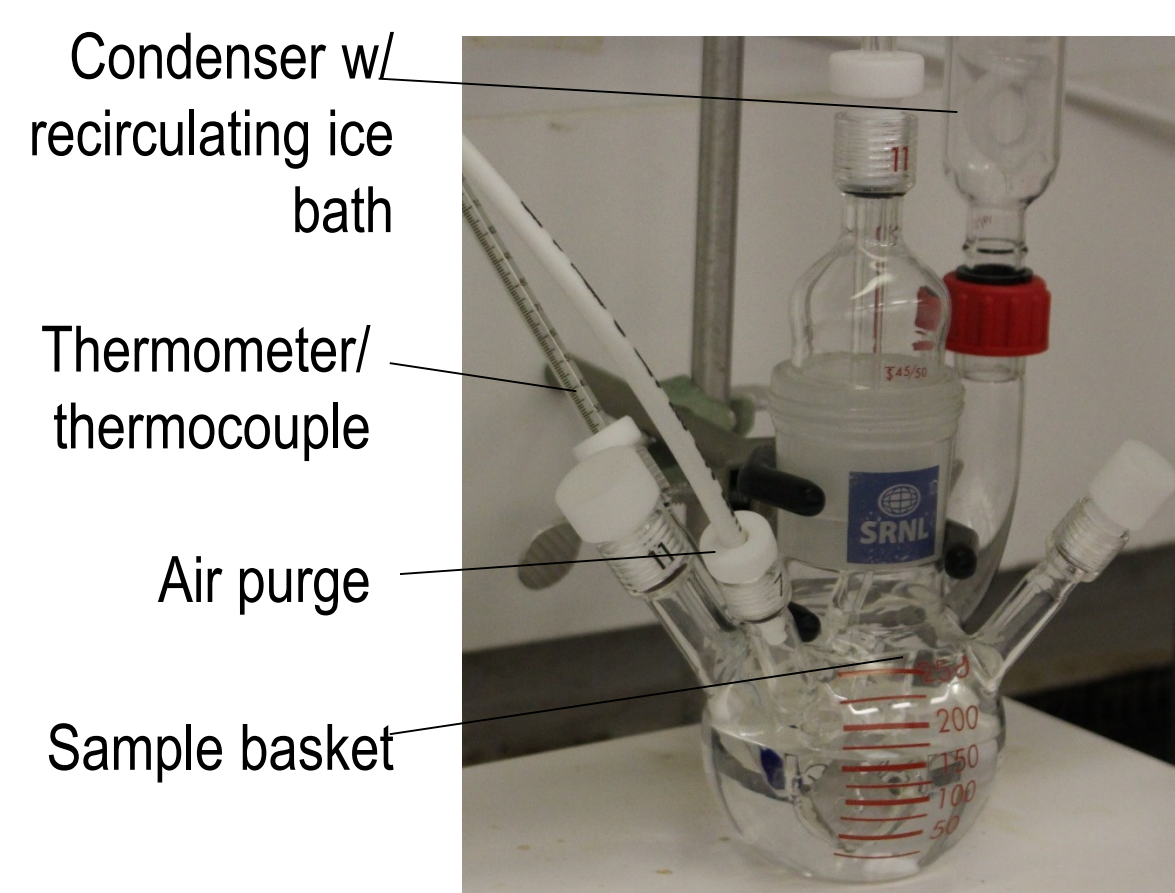
SULFEX: (M = Fe, Ni)
 $M + H_2SO_4 \rightarrow MSO_4 + H_2$
 $2Cr + 3H_2SO_4 \rightarrow Cr_2(SO_4)_3 + 3H_2$
 Potentially suitable with new dissolver

ZIRFLEX:
 $Zr + 6NH_4F + 0.5NH_4NO_3 \rightarrow (NH_4)_2ZrF_6 + 5NH_3 + 1.5H_2O$
 Potentially suitable (ensure offgas compatibility)

Small-scale testing to ensure safety

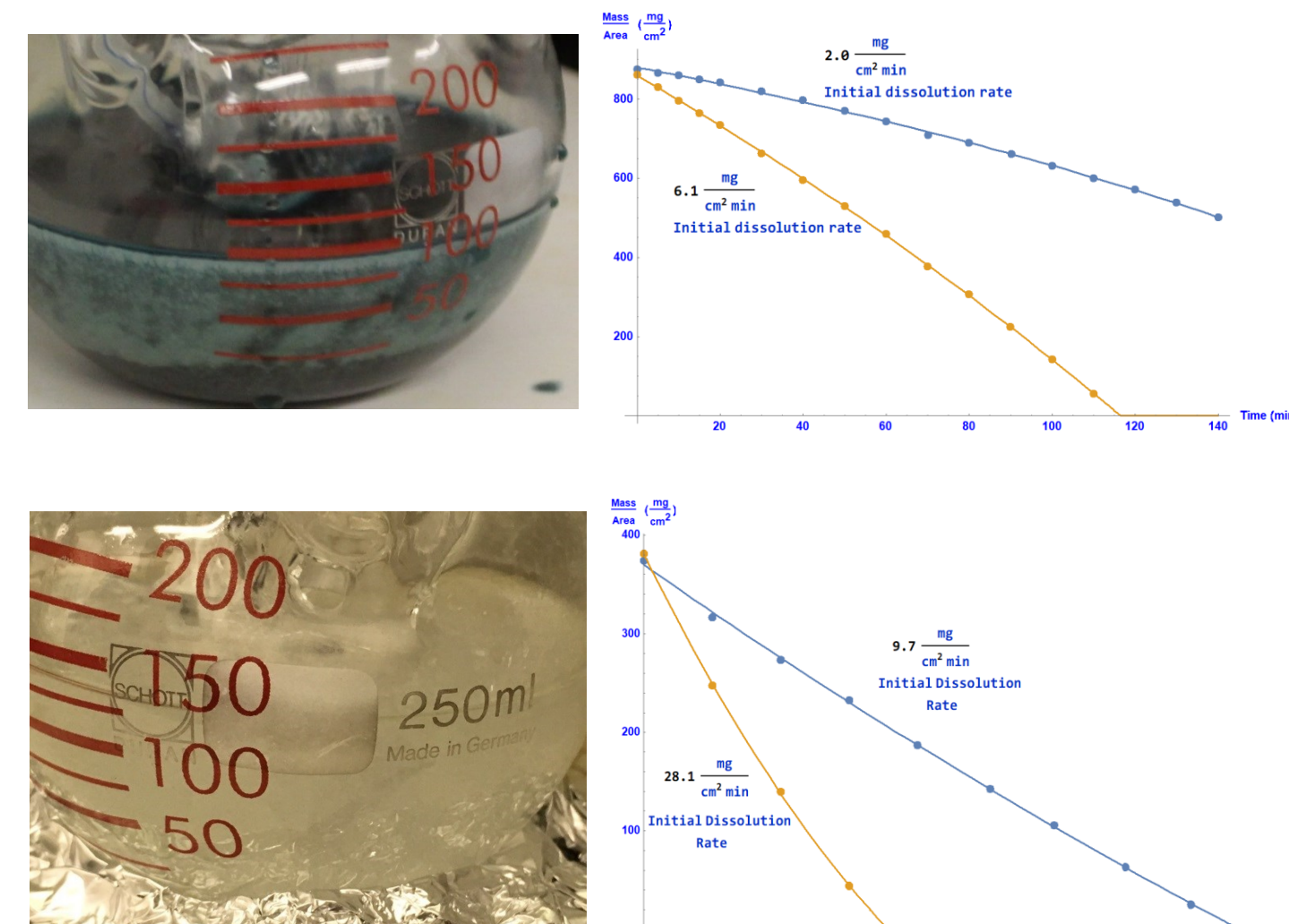


Design of glass dissolver



Results and Discussion

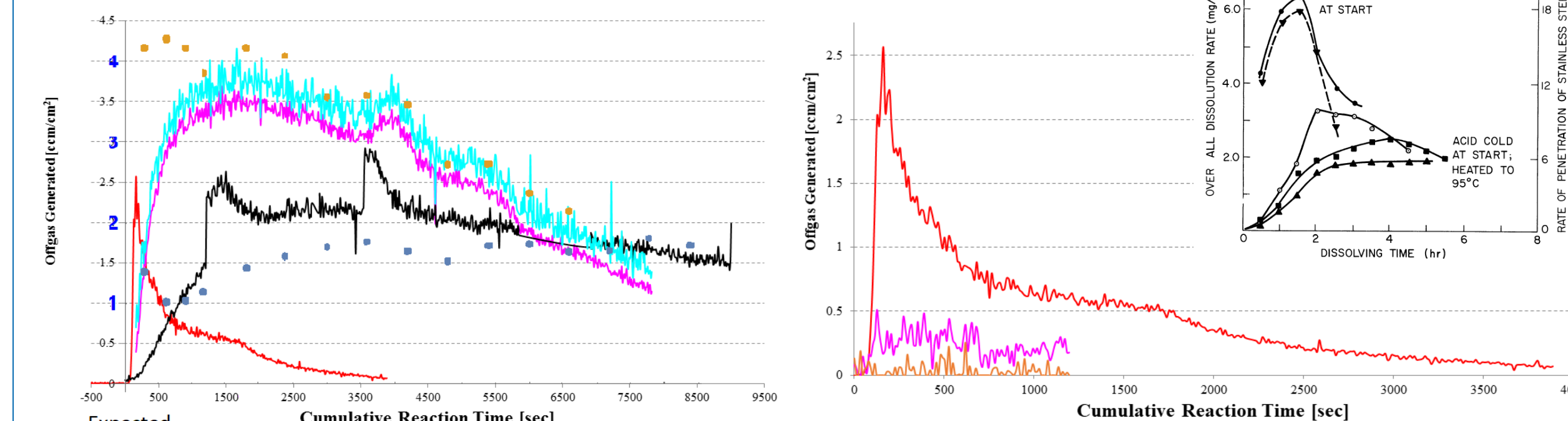
Dissolution rates at 100 °C (slightly below reflux)



SULFEX dissolution resulted in a deep blue solution of iron/metal sulfates. At 4M and 6M H₂SO₄, a 20-mil 304L cladding (e.g. Consolidated Edison fuel) would be fully dissolved in 2h10m and 45m, respectively.

Rapid dissolution and significant offgassing were observed in the ZIRFLEX dissolution. At 4M/0.5M and 6M/1M NH₄F/NH₄NO₃, a 27-mil Zr-2 cladding (e.g. PWR blanket fuel) would be fully dissolved in 40m and 17m, respectively.

Offgassing studies with Raman cell



SULFEX experiments (left) indicated nearly pure H₂ offgas that tracked with theoretical offgassing rates expected from the dissolution rate plots. ZIRFLEX experiments detected NH₃ at lower concentrations than expected, likely due to it condensing in the cold condenser before reaching the Raman cell. These results are quantitatively consistent with data from ORNL¹ (top right).

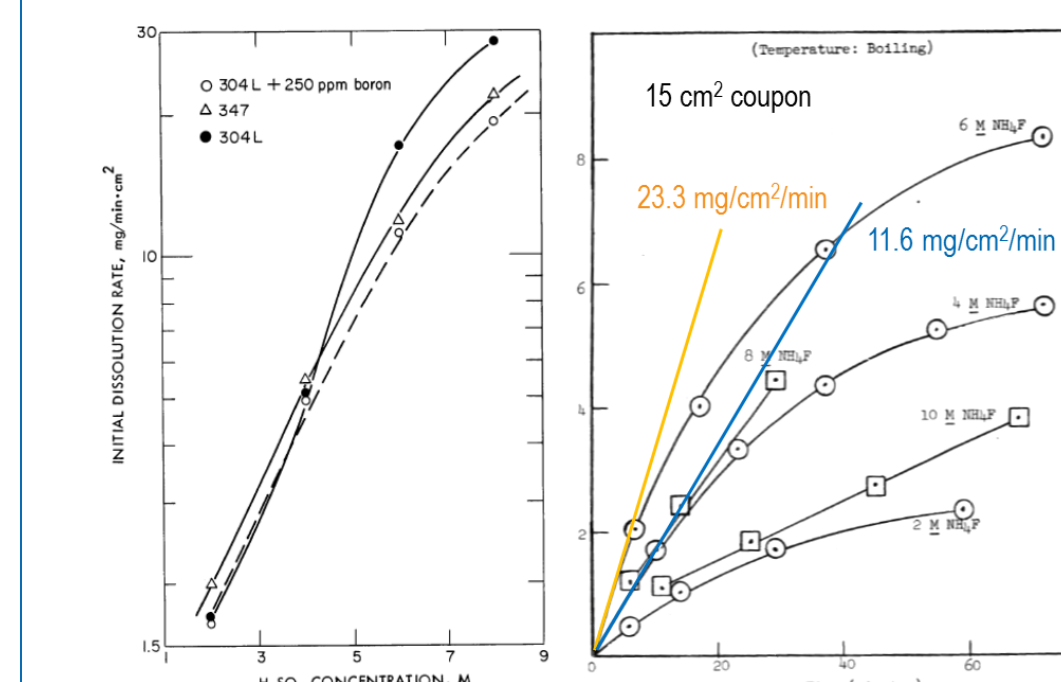
Waste generation

The SULFEX process resulted in a deep blue solution with a light blue deposit on the reactor walls. The solution produced large crystals of sodium sulfate upon neutralization.

The ZIRFLEX process resulted in a clear neutral solution to which Al(NO₃)₃ was added to complex the residual F⁻ in solution. The resulting slightly acidic solution was neutralized with caustic, producing a significant amount of white precipitate.



Comparison to existing data



Although SULFEX offgassing rates were consistent with ORNL data (see above), initial rates (left) were lower than those reported at ORNL.² ZIRFLEX initial dissolution rates (right) were consistent to within 20% of Hanford data.³ Initial rate of dissolution is known to depend strongly on the extent of surface oxidation, and temperature was slightly lower in these studies (100 °C vs. reflux).

Conclusions

- SULFEX and ZIRFLEX are feasible routes for processing non-Al clad fuels
 - Corrosion studies needed to select new dissolver materials for H-Canyon
 - Process development needed for handling waste streams in H-Canyon
- Data consistent with previous in-depth studies at ORNL and Hanford
- Could be suitable for processing small damaged non-Al clad fuels in hot cells

References:

- Flanary, J.R. *et al.*, Development of the SULFEX Process for Decladding Stainless-Steel-Clad Power Reactor Fuel Elements with Sulfuric Acid. ORNL-2461, Oak Ridge, TN, 1959.
- Ferris, L.M. and Kibbey, A.H. Laboratory Development of the SULFEX Process for the Dissolution of Consolidated Edison Power Reactor Fuel. ORNL-2714, Oak Ridge, TN, 1959.
- Swanson, J.L. The ZIRFLEX Process. Second United National Conference on the Peaceful Uses of Atomic Energy. A/CONF.15/P/2429, Richland, WA, 1958.