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Bioprocessing-based approach for bitumen/water/fines separation and hydrocarbon recovery from oil sands tailings

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16 **ABSTRACT**

17   Oil sands are a major source of oil but their industrial processing generates tailings

18   ponds that are an environmental hazard. The main concerns are mature fine tailings

19   (MFT) composed of residual hydrocarbons, water and fine clay. Tailings ponds

20   include toxic contaminants such as heavy metals, and toxic organics including

21   naphthenics. Naphthenic acids and poly aromatic hydrocarbons (PAHs) degrade very

22   slowly and pose a long-term threat to surface and groundwater as they can be

23   transported in the MFT (Holowenko et al, 2001). Research into improved

24   technologies that would enable densification and settling of the suspended particles is

25   ongoing.   In batch tests, BioTiger™, a microbial consortium that can metabolize

26   PAHs, demonstrated improved oil sands tailings settling from a Canadian tailings

27   pond. Resulting also showed, depending on the timing of the measurements, lower

28   suspended solids and turbidity. Elevated total organic carbon was observed in the

29   first 48 hours in the BioTiger™ treated columns and then decreased in overlying

30   water.   Oil sands tailings mixed with BioTiger™ showed a two-fold reduction in

31   suspended solids within 24 hours as compared to abiotic controls. The tailings treated

32   with BioTiger™ increased in microbial densities three orders of magnitude from 8.5

33   X 105 CFU/mL to 1.2 X 108 CFU/mL without any other carbon or energy source

34   added indicating metabolism of hydrocarbons and other available nutrients. Results

35   demonstrated bioaugmentation of BioTiger™ increased separation of organic carbon

36   from particles in oil sands and enhanced settling with tailings with improved water

37   quality.

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40   1. **<u>Introduction</u>**

41   Recovering oil from the Athabasca Oil Sands has been a major technological challenge

42   (Masliyah et al., 2004). While many of the mining methods have been successful, the

43   fundamental mechanisms of hydrocarbon extraction from oil sands are cumbersome and

44   both the mining efforts and environmental impact have been costly (Thorley, 2012). The

45   heterogeneity of the oil sands including fines content, bitumen composition, clay

46   mineralogy, and other factors can influence the extraction process (Wallace et al., 2004).

47   Current methods employ multi-step systems of heating, aqueous phase separation,

48   mechanical mixing, aeration, and chemical additions to extract hydrocarbons from the oil

49   sands. These past and recent efforts have generated large tailings ponds that still contain

50   varying amounts of heavy molecular weight, highly viscous hydrocarbons, known as

51   bitumen, indicating the poor efficiency in that process (Siddique et al, 2007). Recently,

52   environmental concerns and regulations have grown for the processing water, energy cost

53   to operate the systems, runoff from the tailings ponds, wastewater from the facilities, as

54   well as chemical residues (e.g. paraffins) in the water effluent from the extraction process

55   (Alberta Energy Regulator, 2009).

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57   In the oil sands industry, the final product from bitumen extraction process is simply the

58   primary separation froth (Xu et al., 2012). Various flotation technologies can improve

59   froth and water recovery by generating higher-grade froth with less fine sand, thus

60   minimizing maintenance. More efficient processing may also increase water reclamation

61   by recycling within the system or as cleaner effluent to tailings ponds. The hot water

62   flotation process for oil sands is a separation process where the objective is to separate

63 bitumen from particulate matter by exploiting the differences in their physical properties.

64 The slurry conditioning process includes, ablation, mixing, mass and heat transfer, and

65 chemical reactions leading to separation of bitumen from sand and mineral particles

66 (Zhao et al., 2006). The phase separation is enhanced by the effects of mechanical mixing

67 and factors reducing silica-bitumen adhesion. However the process leaves 3-5 % of

68 bitumen resulting in contaminated tailings (Masliyah et al., 2004). The large scale of the

69 operations, estimates of water utilization by the oil sands industry are over 11 million

70 liters per day, have resulted in tailings ponds covering more than 130 square kilometers

71 in northern Alberta (Tenenbaum, 2009). Many of these operations and tailings ponds are

72 over 50 years old are expected to increase due to increasing oil production (Wells, 2011).

73 Characterization of microbial activity within the Athabasca oil sands formation has

74 indicated significant seasonal changes (Wyndham and Costerton, 1991). These changes

75 may be expected with the associated extreme climate changes of northern Canada.

76 However, hydrocarbon biodegradation of the oil sand-adapted mixed sediment population

77 has not correlated well with the concentrations of bituminous hydrocarbons in specific

78 site sediments. These results suggest that a general capability for hydrocarbon oxidation

79 exists in the Athabasca River system and that this capability is enhanced within the

80 natural bounds of the Athabasca oil sands. Select anaerobic bacteria within these oil

81 sands and tailings ponds can metabolize available hydrocarbons for growth and produce

82 methane (Siddique et al., 2011). The oil sands naturally contain high concentrations of

83 polyaromatic hydrocarbons (PAHs) and naphthenic acids that are a complex family of

84 cyclic and acyclic carboxylic acids present in oil sands that are a health concern

85 (Tenenbaum, 2009). These PAHs are of concern as they are acutely toxic to aquatic

86   organisms, some are carcinogenic, and the run-off and effluent from oil sands processing

87   sites is impacting aquatic systems (Kelly et al., 2009). Downstream wetland sediments

88   exposed to oil sands process water have distinct bacterial communities based on

89   naphthenic acids concentrations indicating adaptation and selection (Holowenko et al.,

90   2001).

91   A variety of microorganisms including sulfate-reducing, nitrate-reducing, methanogenic

92   bacteria and heterotrophic facultative anaerobic bacteria have been detected in tailings

93   pond water (TPW) (Holowenko et al., 2001; Bordenave et al., 2010). Microorganisms in

94   tailings ponds participate in biodegradation of the naphthenic acids, biosorption of heavy

95   metals, and sulfate reduction (Herman et al., 1993; Wolfaardy et al., 2008). In recent

96   years activity of the methanogenic and nitrate-reducing microbial communities have been

97   linked to increased densification/dewatering of tailings slurry (Bordenave et al., 2010).

98   This research project tested bioaugmentation, the addition of natural microorganisms, as

99   a means of improving oils sands processing including separation of hydrocarbons from

100 particles as well as improved settling of tailings. Bioremediation has proven successful

101 in numerous applications to petroleum contaminated soils and water both in active or

102 engineered applications (Brigmon et al., 2002). The toxicity of hydrocarbon

103 contaminated soil and water due to certain metal and PAH concentrations are a concern

104 in remediation efforts (Berry et al., 2006). Decreases in petroleum hydrocarbons, e.g.

105 PAHs, through microbiological or physical/chemical treatments, can result in production

106 of certain metabolites that remain toxic (Story et al., 2000). Under controlled conditions

107 the bioremediation of hydrocarbons can reduce toxicity as well as meet reclamation goals

108   (Płaza, et al., 2005). In this work, we tested BioTiger™, a patented consortium of natural

109   bacteria tested and isolated from a remediation project at a Polish Oil Refinery, with

110   Canadian oil sands and tailings (Brigmon et al., 2009; Brigmon and Berry, 2009). That

111   the BioTiger™ strains were isolated from Northern Europe with long winters and cooler

112   climate like Alberta, Canada, made this culture a choice for this application. Results

113   show that addition of BioTiger™ to oil sands and tailings respectively increased

114   separation of hydrocarbons from particles and enhanced tailings settling with improved

115   effluent process water quality.

116   **2. Materials and Methods**

117   *2.1 Microorganisms*

118   BioTiger^{TM} is a patented consortium of 12 natural aerobic bacteria (Table 1) isolated

119   from an acidic oil refinery sludge composed of asphaltics highly contaminated with

120   PAHs (Brigmon et al., 2009). The refinery source of the consortium originated was

121   located near Katowice, Poland, so the microorganisms were adapted to cold winter

122   temperatures similar to those found in Alberta, Canada. BioTiger^{TM} components are

123   grown separately on R2A liquid medium (Difco) and then combined when reaching 10^{7-8}

124   cells/ml. Prior to application, the combined BioTiger^{TM} was grown on 1% oil sands

125   (20% Bitumen, Athabasca Oil Sand, Alberta Research Council) in Bushnell Haas Broth

126   (Sigma–Aldrich, St. Louis, MO) to a density of 10^{7-8} cells/ml at room temperature.

127   Control bacteria used in this project including *Sphingomonas mobilis* EPA 505 (Story et

128   al., 2000), and *Eschericia coli K12* (American Type Culture Collection # 29425) were

129   prepared in the same manner on R2A broth and cultured to similar densities.

130   2.2 Phenanthrene Degradation by BioTiger™

131   Liquid cultures of *E. coli* k-12 and each the components in BioTiger™ were grown in

132   R2A broth. Each liquid culture was incubated at 30°C at 150 rpm for 24-48 hours. The

133   components were mixed together and washed 1X in Bushnell-Haas medium (Difco).

134   Appropriate controls were run in parallel to all experiments.

135   10% inoculations of both washed live and washed dead (autoclaved) cells into Bushnell-

136   Haas saturated with phenanthrene (Sigma) (1.6ppm), and were sampled at 0 and 24

137   hours. The samples were extracted in ethyl acetate (Fisher); 5ml of culture to 1ml of

138   solvent.

139   Phenanthrene was identified by an Agilent 6890 GC-MS in SIM mode (152, 176-179)

140   equipped with a Restek 13323 capillary column (30m x 250µm x 0.25 µm).   The

141   following oven program was used: initial temperature at 35°C hold for 30 min, initial

142   temperature gradient at 5°C/min from 35-200°C, final temperature gradient at 10°C/min

143   from 200-250°C, final temperature hold at 250°C for 1 min and 5ul was injected by

144   autosampler.

145   *2.3 Settling Experiment*

146   The BioTiger™ consortium and controls were tested with oilsands tailings (3% bitumen)

147   from Ft. McMurray, Canada, kindly supplied by Shell Canada. All columns treatments

148   were prepared in duplicate. Control columns included oil sands tailings with no bacteria

149   added, *E. coli* (ATCC#29425), and *S. mobilis* (EPA 505). The settling experiment was

150   performed at room temperature (25 °C) as environmental conditions at the oil sands

151   processing sited can vary from freezing to up to 65°C.   Oil sands process water has

152   increased temperatures to decrease the bitumen viscosity, increase surface charge of sand

153   grains and bitumen, and enhance bitumen separation and settling of sand particles (Zhao

154   et al., 2006). For the testing, 25 ml v/v of mixed tailings was added to 225 ml of sterile-

155   filtered phosphate buffered saline (PBS) in 250 ml autoclaved glass columns with air

156   stones at the bottom.   Eight columns were run simultaneously with treatments in

157   duplicate including BioTiger™, *E. coli* k-12, EPA 505, and an abiotic treatment (tailings

158   only). All microorganisms were added to an initial concentration of 10^{7-8} CFU/ml. Air

159   stones were operated for 1 hour and then all columns were allowed to settle.

160   Measurements were taken from a 10 cm depth at times 0, 24 h, 42 h, 48 h, 72 h, 144 h,

161   and 288 h of settling rates (cm), dissolved oxygen (D.O. %), turbidity, temperature, pH,

162   and conductivity. Air flow, 12 mL/min. per column, was turned off @ 24 h. Total organic

163   carbon (TOC) was measured with HACH kits (Cat# 28159-45 and 27604), settling rates

164   was measured in mLs, turbidity was determined with a Hach kit (Cat # 2660153) in

165   nephelometric turbidity units (NTU), chloride (Cl^-), pH, temperature (°C) and

166   conductivity (Cond. mS/cm) were measured with an Orion 5-Star (Thermo Scientific).

167   Heterotrophic colony forming units (CFU's) or aerobic microbial densities were

168   determined using plates made with R2A agar medium (Sigma Aldrich, St. Louis, MO.

169   Microbial densities, settling, and turbidity measurements were ceased after 24 hr. as

170   removal of any overlaying water disturbed the column settling process.

171   *2.4 Laser Confocal Microscopy*

172 Duplicate one gram samples of Athabasca oil sands were mixed with eight mLs of filter

173 sterilized PBS each in two separate 15 ml polypropylene tubes and vortexed for 2 min.

174 One ml BioTiger™ was added to one vial (treated) with a concentration of 10^{7-8} CFU/ml.

175 Then one ml of PBS was added to the second (untreated oil sands) vial. Both vials were

176 mixed another two min and then placed in a shaking incubator for 30 min @ 25° C.

177 After 30 min the tubes were removed from the shaker, and 10 µl aliquots aseptically

178 placed on microscope slides. Slides were air dried in a sterile hood, overlaid with 20 µl

179 sterile filtered 2% gelatin in PBS, heat fixed, stained with fluorescein isothiocyanate

180 (FITC) (Sigma Chemical Co.) for two minutes, and then washed three times with filter

181 sterilized (2 µm) deionized water. Samples were examined using a Zeiss Model 510

182 Laser Scanning Confocal Microscope (LSCM) excited at 488 nm with an argon laser.

183 Photographs were taken of the treated and untreated oil sands sample with a 1000 x 1.3

184 oil immersion objective.

185 **3. Results.**

186 3.1 Single Carbon Source Experiment

187 Over 24 hours (Fig 1) the live consortium of BioTiger™ decreased the phenanthrene

188 concentration below detection limits (4% relative to 100% saturated medium), and live

189 and dead *E. coli* k-12 decreased the phenanthrene concentration less than 12%, while the

190 autoclaved BioTiger™ was still modestly effective reducing the phenanthrene

191 concentration by 30%. Cell-free medium had no detectable change in phenanthrene

192 concentration.

193

194   *3.2 Settling Experiment*

195   Figure 2 shows the experimental set up of the eight columns for the settling experiment at

196   Time 0 and 24 h. Total organic carbon provides an indication of the amount of organic

197   matter and dissolved fraction of organic carbon found in the oil sands tailings, in which

198   PAHs can make up 40–60% of the organic carbon content (Small et al,. 2012). TOC

199   measurements in overlay water of sedimentation cylinders out to 144 hours are shown in

200   Fig. 3. Results at 24, 42, and 48 h indicate higher TOC concentrations in the BioTiger™

201   overlay samples as compared to controls with no bioaugmentation (indigenous

202   microorganisms only) or *E. coli* k-12. However, at 144 h the BioTiger™ overlay samples

203   TOC concentrations were lower than the other treatments, indicating biodegradation (Fig.

204   3).

205   The greatest rate of sedimentation was observed in the first 48 h by all treatments

206   measured (Fig. 4).   All figures from the column results represent the mean of two

207   columns for each reading with the bar being standard deviation. The columns with *S.*

208   *mobilis* EPA 505 developed floating flocs that made accurate determination of TOC,

209   settling rates, turbidity, pH, dissolved oxygen, overlay water conductivity, and chlorine

210   impossible. Oil sands tailings in the six columns demonstrated levels of sedimentation

211   ranging from 54-84 mL (v/v) in 24 h (Fig. 4).   Results demonstrated that BioTiger™ had

212   more increase in tailings settling as compared to controls with no bioaugmentation

213   (indigenous microorganisms only) or *E. coli* k-12. Initial (time 0). BioTiger™ treated

214   tailings solids settled slower initially, possibly due to observed small floc formation

215   observed in the these two columns.   The settling was most likely due to released

216   hydrocarbons from oil sands tailings particulates.   All figures from the column work

217   represent the mean of two columns for each reading with the bar being standard

218   deviation.

219   Turbidity measurements (NTU) could not be taken until 4h after enough settling had

220   occurred of the overlay water (Fig. 5).   Turbidity was highest at the initial 4 h and 6 h

221   sampling points for the uninoculated or abiotic columns and the lowest for BioTiger™

222   treatments.   However the abiotic columns had the lower turbidity at 24h although all the

223   treatment means were similar at that time (Fig. 5).   We did not attempt further turbidity

224   measurements after 24 hr. as sample removal caused disturbance of settled material as

225   well as a visible hydrocarbon layer on surface.

226   Dissolved oxygen (DO) was measured out to 288 h in the overlay water of the settling

227   experiment (Fig. 6).   The DO was observed to be variable by decreasing rapidly in all

228   treatments for the first few days and then rose most likely due to some stratification

229   observed, oxygen release from particles, and increase settling occurring in the water

230   columns.   However by 288 h variability was very low and BioTiger™ had the lowest DO

231   measured (Fig. 6).

232   The overlay water conductivity (mS/cm) was highly variable and increased the first 24 h

233   (Fig. 7).   It then generally increased out to 288 h in the settling experiment for the abiotic

234   and BioTiger™ treatments that did not seem to be significantly different. The *E. coli* k-

235   12 treated columns decreased slightly between the 148 h and 288 h measurements (Fig.

236   7).   Results represent the mean of two columns for each reading.   Bars are standard

237   deviation of two measurements.

238   The addition of the microorganisms as well as the sterile PBS for the abiotic control to

239   the columns appeared to cause an initial 0.10-0.55 decrease in pH (Fig. 8). Over lay water

240   pH measured out to 288 h demonstrated an overall decrease pH during the settling

241   experiment in the 7.2-7.3 range, ideal for microbial activity.

242   *3.2 Effect on microbial activity*

243   Indigenous microorganisms were observed in the untreated tailings as observed in Fig. 9.

244   There was as few as one bacterium observed per microscopic field. The active

245   heterotrophic microorganisms in the tailings were found to be 1.5×10^3 CFU/ gram (wet

246   weight). Table 2 lists the microbial concentrations in the column treatments at time 0

247   after immediate BioTiger™ or control addition and mixing and after 24 h. All values are

248   volume/volume (v/v) for the tailings/PBS slurry. The abiotic control is the untreated

249   tailings column with indigenous bacteria only. The abiotic control population varied less,

250   starting at 3.0×10^4 CFU/mL v/v, and then increasing slightly to 5.1×10^4 CFU/mL v/v

251   at 24 h. It was observed the indigenous culture plates had mostly small uniform white

252   colonies. Similarly the *E. coli* K-12 also varied from 5.6×10^7 CFU/mL to 8.6×10^7

253   CFU/mL. The bacteria in the BioTiger™ increased significantly three orders of

254   magnitude from 8.5×10^5 CFU/mL to 1.2×10^8 CFU/mL. A few fungi colonies were

255   noted on the plates as well. After BioTiger™ was added to tailings, cells were observed

256   attached to particulate material in the tailings within minutes of incubation (Fig. 9). Oil

257 sands tailing with no BioTiger™ added had some cells observed, as few as one per

258 microscopic field (Figure 9).

259 The microbial ecology of indigenous bacteria in oilsands and tailings, both aerobic and

260 anaerobic populations, has been well documented (Wyndham and Costerton, 1991;

261 Hadwin et al., 2006; Siddique et al., 2011). All though indigenous microorganisms, both

262 fungi and bacteria, were detected both microscopically and in culture here, the technique

263 used here to determine viable aerobic heterotrophic microbial populations (CFU) does

264 not allow identification of species.

265 **4. Discussion**

266 In this project we have demonstrated BioTiger™ could be potentially used in a

267 bioprocess to increase settling of oilsands tailings. BioTiger™ has a selective advantage

268 in this environment over certain indigenous bacteria from Athabasca watershed sediments

269 that have been shown to be inhibited by bituminous compounds (Yergeau et al., 2013).

270 Previous investigations have demonstrated the potential of anaerobic bioprocesses for

271 densification of oil sands tailings (Siddique et al., 2014; Bordenave et al., 2010).

272 Bioremediation of oil contamination, including biostimulation combined with

273 bioaugmentation, has proven effective for a wide range of conditions including Antarctic

274 soils, (Vázquez et al. 2009). Bioaugmentation of oil sands tailings with bacteriophages

275 has also been tested to enhance particle aggregation and sedimentation with some success

276 (Curtis et al., 2013). Hydrocarbons released from oilsands tailings could decrease

277 nutrient loading of sediments and associated methane and other greenhouse gas

278 formation. The released hydrocarbons could be recovered for processing.

279   Figure 1 demonstrates biodegradation of phenanthrene, a PAH, by BioTiger as a sole

280   carbon and energy source, in 24 h. Some slight decrease by the bacteria controls was

281   observed most likely due to sorption by the cells. The ability to degrade PAHs gives

282   BioTiger™ an ecological advantage in this environment. Improved water quality (e.g.

283   lower turbidity) could be managed in the bioprocess with BioTiger™.   TOC in overlay

284   water was greater in the BioTiger™ treated columns that the others up to 48 hours

285   indicating initial hydrocarbon release from tailings (Fig. 3). It would be possible to use

286   this action to recover hydrocarbons, e.g. through skimming, at this time if economically

287   feasible. However, at 144 hours the TOC concentrations were lowest in the BioTiger™

288   columns, indication potential remediation but crucial timing needed for any future

289   bioprocessing effort. It was observed that the BioTiger™ treatments had a lower

290   turbidity when sampled at 6 hours (Fig. 5).   However there was no difference between

291   the treatments at 24 hours. Again timing could be a factor in developing a BioTiger™-

292   based bioprocess that would take this timing into design considerations. Tailing

293   separation and densification is attributed to aggregation of bacterial cells with clay

294   particles and hydrocarbon release. It could have been after six hours materials were

295   being released from the sediments causing turbidity to go up in the water column of the

296   BioTiger™ treatments. The BioTiger™ columns had the lowest DO measured by day 12

297   (Fig. 6). This increase in oxygen consumption would be expected since the BioTiger™

298   treatments were also found to have significantly higher microbial activity (Table 2).

299   Increased DO consumption from the microbial activity could also result in increased CO_2

300   production from respiration. The associated CO_2 released from the sediments would

301   influence settling and turbidity.   In columns chloride was observed to increase slightly in

302   the overlay water where measurements were taken in all treatments (data not shown).

303   The fact that the bacteria densities in the BioTiger™ treated columns increased three

304   orders of magnitude could indicate synergistic activity with the indigenous tailings

305   microbial flora (Table 2). Similarly in Suncor's Northern Alberta oil sands tailings pond

306   chloride levels have been observed to be significantly lower in the MFT pore water

307   compared with those found in the overlaying water (Wells, 2011).

308

309   The described methodology could be employed on a larger scale to decrease the

310   transport of hazardous hydrocarbons from theses oils sands processing sites. Parameters

311   including mixing, temperature, and culture metabolism could be optimized for maximum

312   hydrocarbon recovery, settling efficiency, and improved effluent quality. One of the key

313   issues in densification and separation of hydrocarbons from particles and the MFTs is the

314   clay minerals (Hooshiar et al., 2012). The tailings can vary greatly in settling behavior

315   based on the initial oil sands ore quality (e.g. bitumen (4-20%), types of clay present, as

316   well as extraction efficiency (Hooshiar et al., 2012; Xu et al, 2012). Development of a

317   pilot-scale system would prove more flexible for industrial scale deployment than batch

318   treatments, and future work to improve MFT settling efficiency should include

319   continuous flow systems simulating pond conditions.

320   Organic carbons, including NAs have been identified as the largest component of MFTs

321   in the tailings waters from oils sands extraction processes (Small et al., 2012). They are

322   the major contributor to the acute toxicity of the fine tailings ponds and effluent

323   wastewater at the oil sands extraction plants in northeastern Alberta, Canada. In this

324   work, columns of oil sands tailings treated with microbial augmentation and abiotic

325   controls were studied, including BioTiger™, those organisms isolated from oil sludge

326   lagoon-affected waters, and the influence on overlay water chemistry and settling was

327   examined. Reducing the organic matter in tailings ponds with BioTiger™ would

328   minimize methanogenic activity and release of other greenhouse gases that can affect

329   these settling basins and impact environmental restoration.

330   Process water treatment has become of increasing concern for Canada's oil sands

331   industry. Increased water demand and ongoing recycling of tailings pond water has

332   contributed to a decline in water quality that has consequences for bitumen recovery,

333   water consumption, and reclamation efforts. From 1980 to 2001, the salinity of TPW

334   increased at a rate of 75 mg/L per year and while some biodegradation has been

335   documented naphthenic acids continues to be the primary biohazard of concern (Allen,

336   2008). Current increases in process effluent water hardness, sulfate, chloride, and

337   ammonia have raised concerns over scaling and corrosion. Naphthenic acids released

338   during bitumen extraction are the primary source of toxicity in TPW. While

339   biodegradation of naphthenic acids has been demonstrated in pond experiments,

340   remaining recalcitrant hydrocarbons may contribute to slow release or chronic toxicity in

341   reclaimed environments.

342   Active methanotrophic bacteria have been consistently detected in tailings pond surface

343   indicating constant methane production (Saidi-Mehrabad et al., 2012). Molecular

344   analysis demonstrated that the TPW methylotrophic community possessed capability for

345   formaldehyde oxidation, carbon fixation and detoxification of nitrogenous compounds as

346   well as methane monooxygenase. The fact that the TPW methane production is

347 increasing indicates the methanogenic bacterial activity in the sediments is responding to

348 the increase organic matter loading in the sediments (Holowenko et al., 2001).

349 Previous applications with bacteria from the BioTiger™ consortium in a bioreactor

350 resulted in degradation of over 20,000 mg/kg of hydrocarbon contaminated soils (Berry

351 et al., 2006). That project demonstrated that soils co-contaminated with radionuclides

352 and hydrocarbons could be successfully treated through bioventing and bioaugmentation

353 while protecting workers and the environment from radiological contamination.

354 From the results of this study, it can be concluded that BioTiger™ can be used to treat oil

355 sands tailings resulting in improved overlay water quality and increased settling of

356 sediments. This fact is critical as even microorganisms cultured from Athabasca sediment

357 have demonstrated inhibition by bituminous compounds (Yergeau et al., 2013). The

358 ability of the BioTiger™, a natural microbial consortium, to work with this hazardous

359 material with minimal handling demonstrates potential for pilot scale testing in larger

360 reactors with varying types of oil sands tailings. The fact that the BioTiger™ bacteria

361 increased three orders of magnitude in the oil sands tailings indicates this bioprocess

362 could be a sustainable and cost effective effort with limited added energy beyond mixing

363 and aeration. BioTiger™, a natural microbial consortium, worked effectively and

364 synergistically with indigenous microbial populations proving that it can be applied to

365 bioremediate hydrocarbons from oils sands processing tailings ponds. The target tailings

366 ponds and bioprocess described here has the potential to minimize the environmental

367 impact of oil sands processing while recovering bitumen and improving overlaying water

368 quality.

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488   **Tables**

489   **Table 1.** Components of the BioTiger Consortium and the American Type Culutre
490   Collection (ATCC) Accesssion number

491	**Isolate**	**Identification**	**ATCC Accession**
492			
493	CZOR-L1B	*Alcaligenes-Piechaudii SRS*	PTA-5580
494	BP-20 (KN-2)	*Ralstonia Pickettii SRS.*	PTA-5579
495	CZOR-L1Bsm	*Pseudomonas-Putida* BIOTYPE B *SRS*	PTA-5581
496	BPB	*Flexibacter CF. SANCTI SRS*	PTA-5570
497	BPC	*Pseudomonas Fredriksbergensis SRS*	PTA-5571
498	BPE	*Staphylococcus warneri. LMG 19417 SRS*	PTA-5572
499	BPF	*Sphingomonas SRS*	PTA-5573
500	BPH	*Sphingomonas SP. S37 SRS*	PTA-5574
501	BPI	*Phylobacterium SRS*	PTA-5575
502		(α Proteobacterium TA-A1)	
503	BPJ	*Serratia ficaria SRS*	PTA-5576
504		(α PROTEOBACTERIUM TA12-21)	
505	BPK	*Agrobacterium Tumefaciens SRS*	PTA-5577
506	BPL	*Rhizobium SP. SDW045 SRS*	PTA-5578
507			

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508

509 **Table 2.** Mean[*] CFU/mL (v/v) from columns (two per treatment) taken at time 0 (after 5
510 min mixing) and 24 hr.

511

Treatment	CFU/mL @ Time 0	CFU/mL @ 24 h
BioTiger™	8.5E+05	1.2E+08
E. coli K-12	5.6E+07	8.6E+07
Abiotic Control	3.0E+04	5.1E+04
S. mobilis EPA 505	1.9E+05	5.4E+04

512 [*]Mean from duplicate plates

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516   **Figures**

517   **Figure 1.**

518
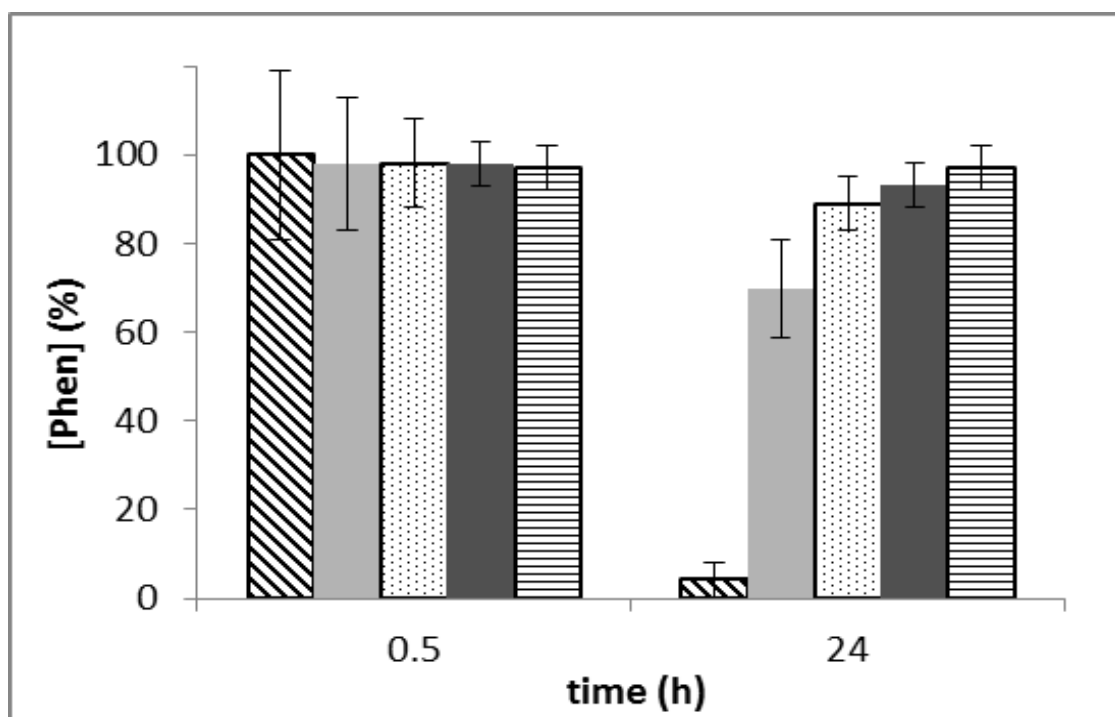
519

520   **Figure 1. Single carbon source experiment.   Cells inoculated in saturated**

521   **phenanthrene Bushnell-Haas medium.   Dotted bar is live *E. coli* (K12), Light gray**

522   **bar is dead BioTiger™, Diagonal lined bar is live BioTiger™, Dark gray bar is**

523   **killed *E. coli*, and horizontal lined bar is no cells added.**

524

525

526   **Figure 2.**

527

528

529

530   **Figure 2. Columns with oil sands tailings and treatments at time 0 (L) and after 24**

531   **hr   (R)**

532

533   **Figure 3.**
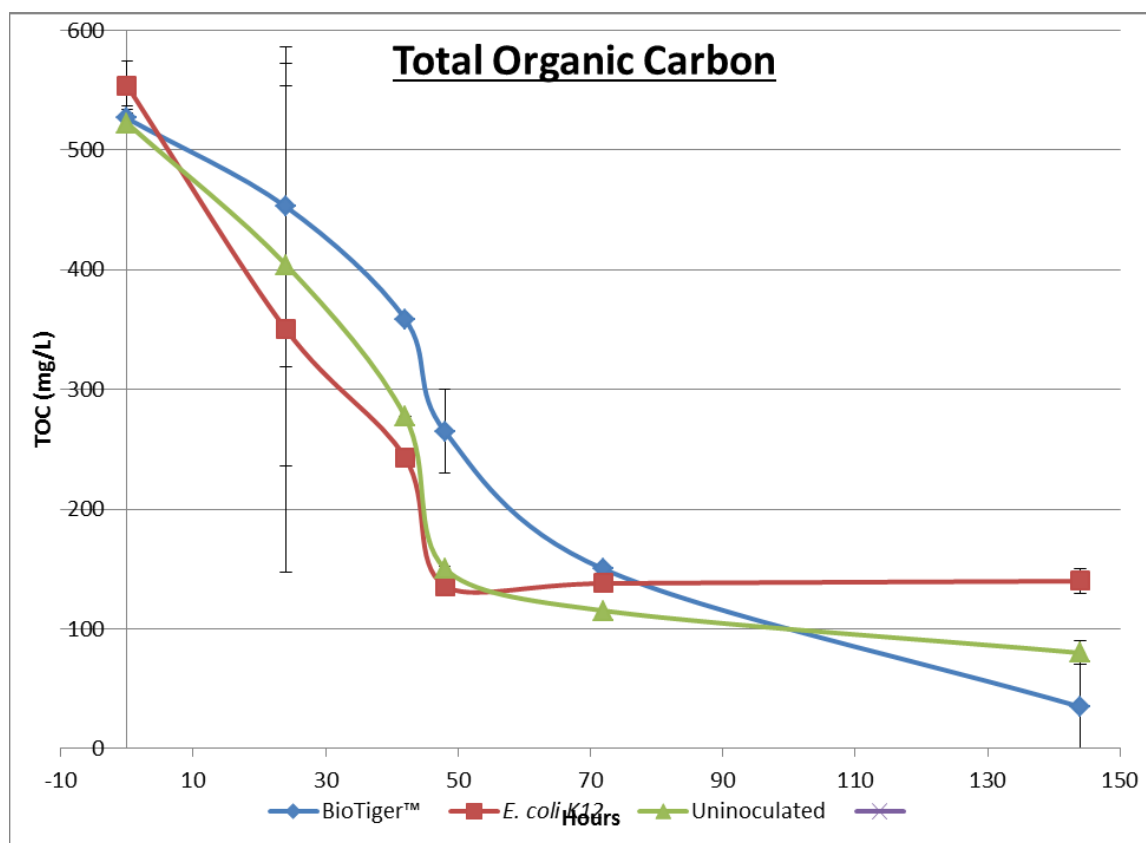
534

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536   **Figure 3. Total Organic Carbon (TOC) concentrations in overlay water of**

537   **sedimentation cylinders over 144 hours. Results represent the mean of two columns**

538   **for each reading. Bars are standard deviation of two measurements.**
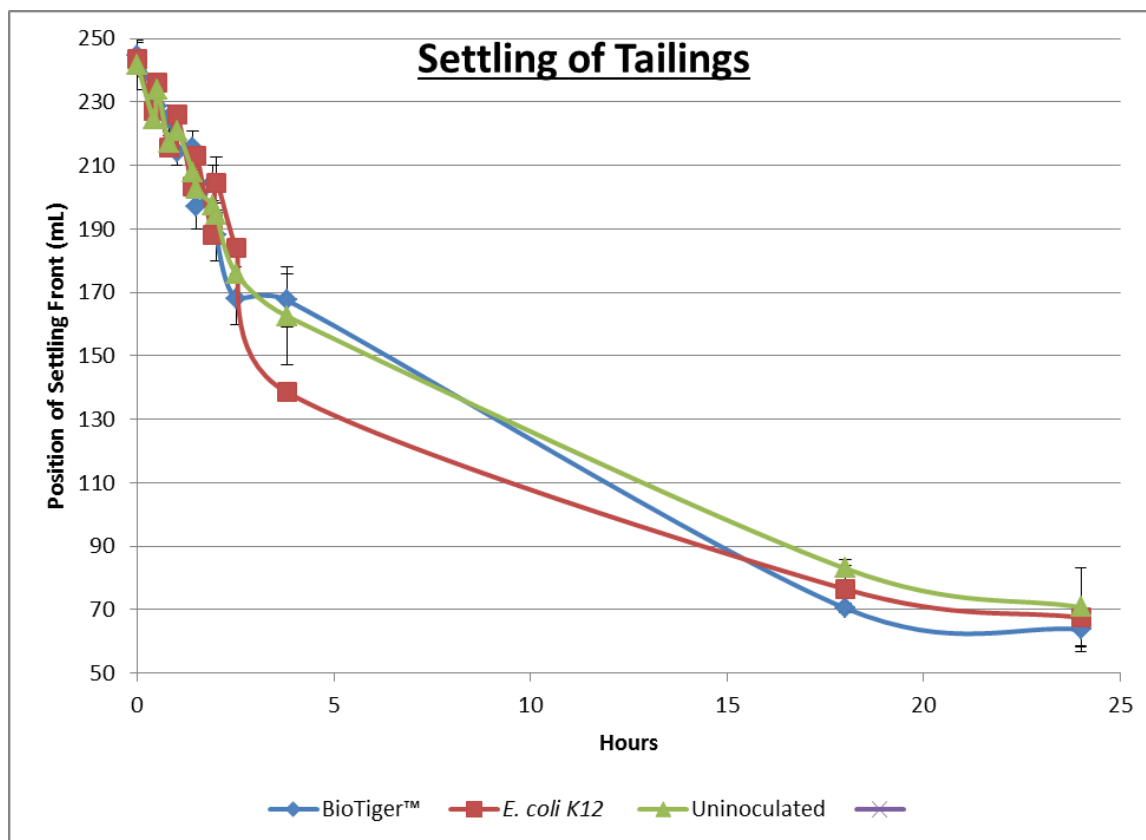
Figure 4.

Figure 4. Oil sands tailings levels of sedimentation (v/v) per ml @ 24 hr. Results represent the mean of two columns for each reading. Bars are standard deviation of two measurements.

546   **Figure 5.**

547
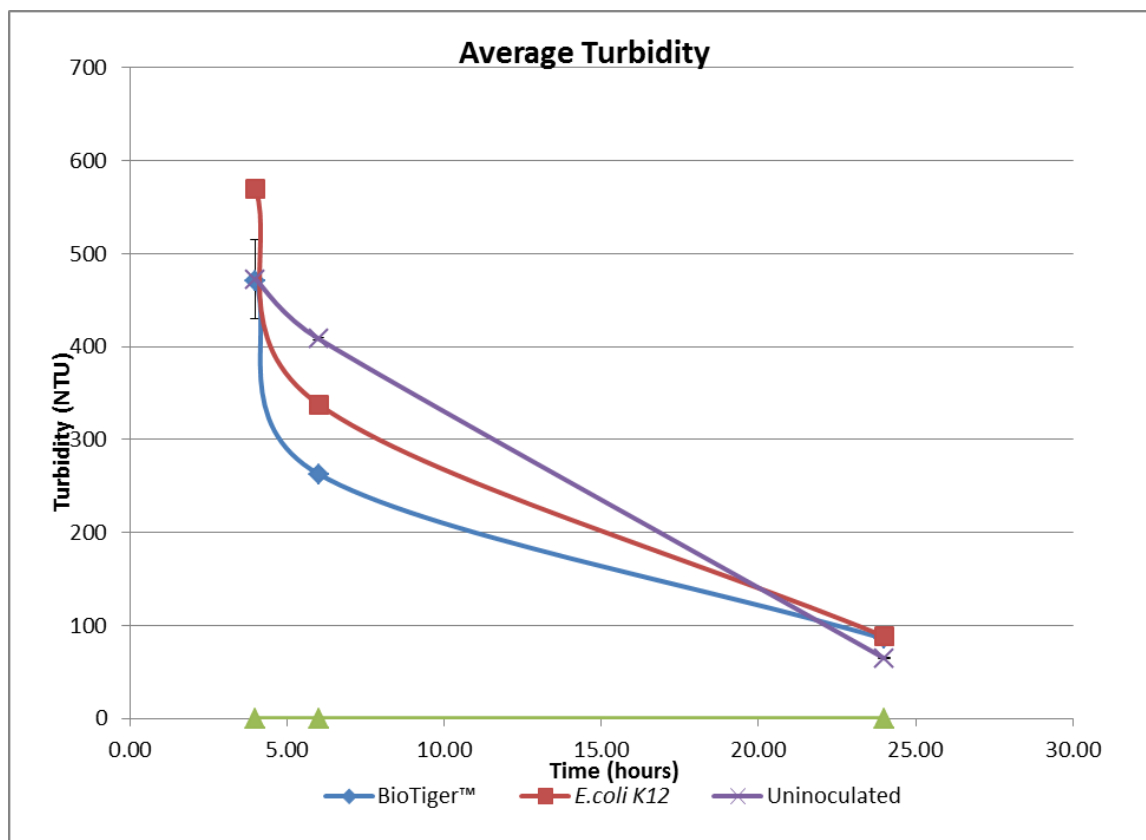
548   **Figure 5. Turdbity (NTU) of oilsands tailings in water overlay measurement for 24**

549   **h. Results represent the mean of two columns for each reading. Bars are standard**

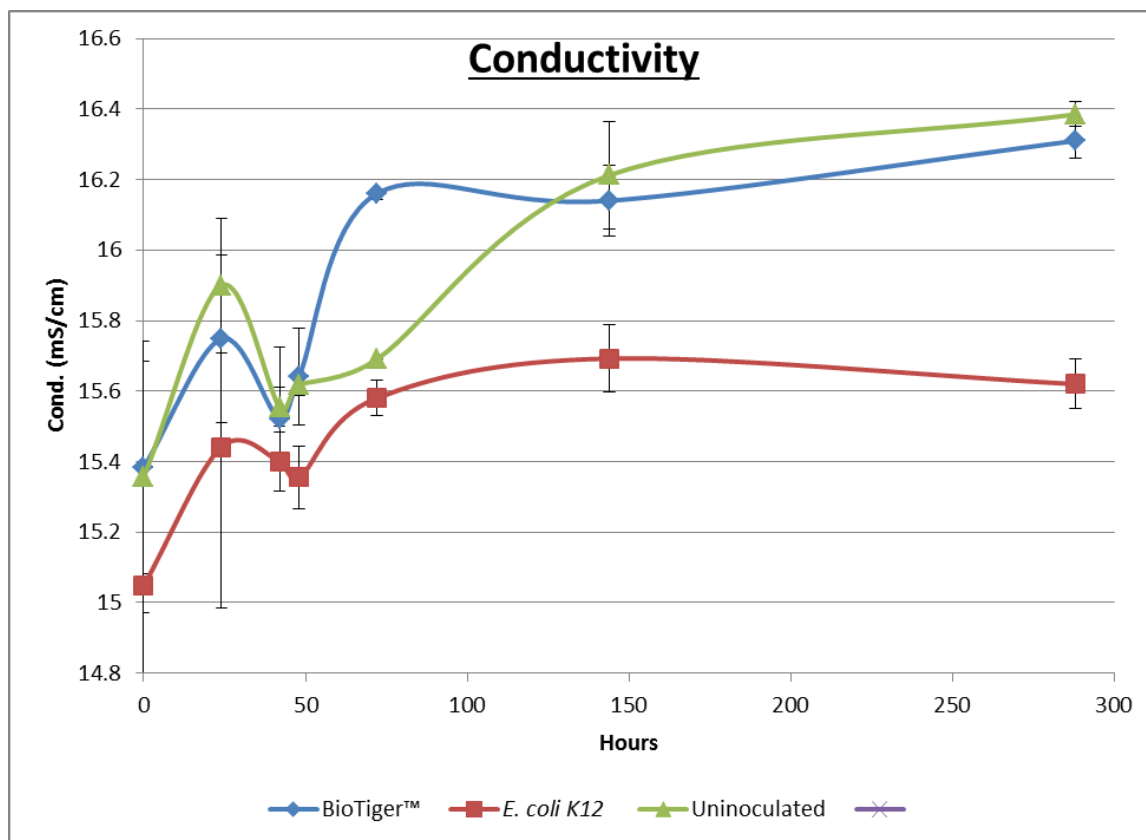550   **deviation of two measurements.**

551

552 **Figure 6.**
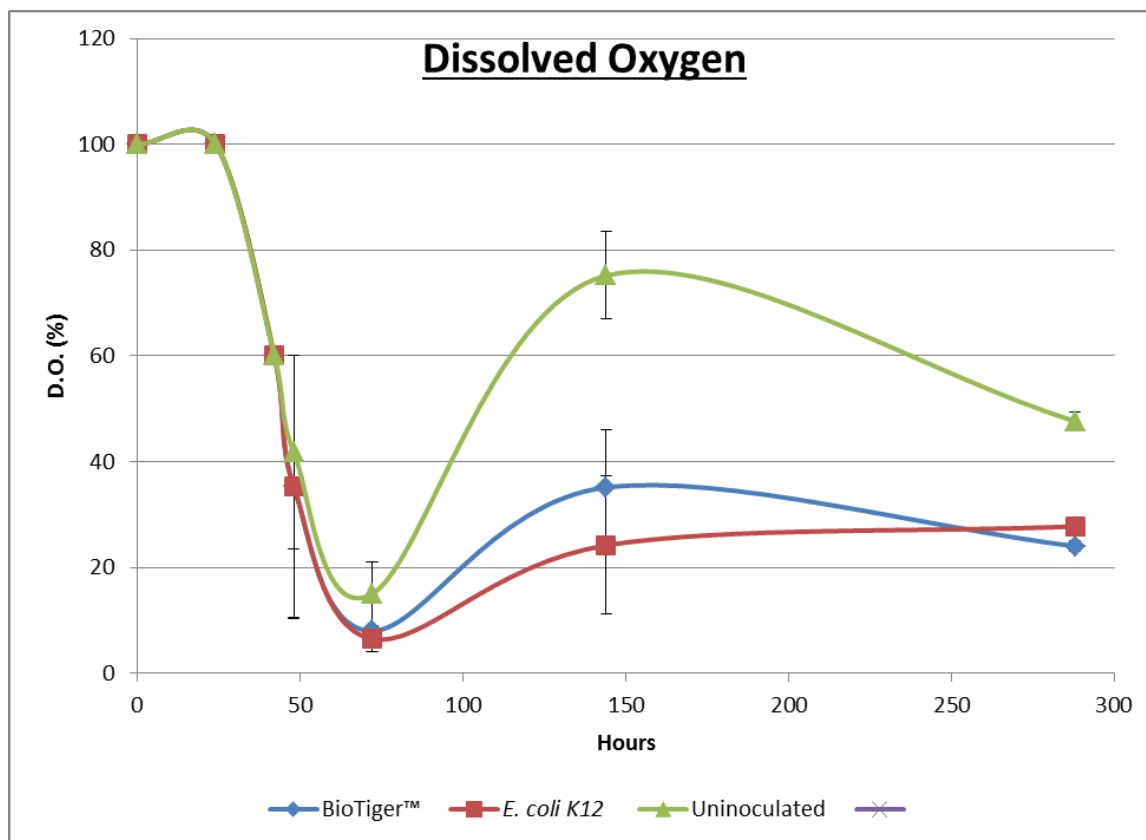
553

554 **Figure 6. Dissolved oxygen (DO) measured out to 288 h in the settling experiment.**

555 **Results represent the mean of two columns for each treatment. Bars are standard**

556 **deviation of two measurements.**
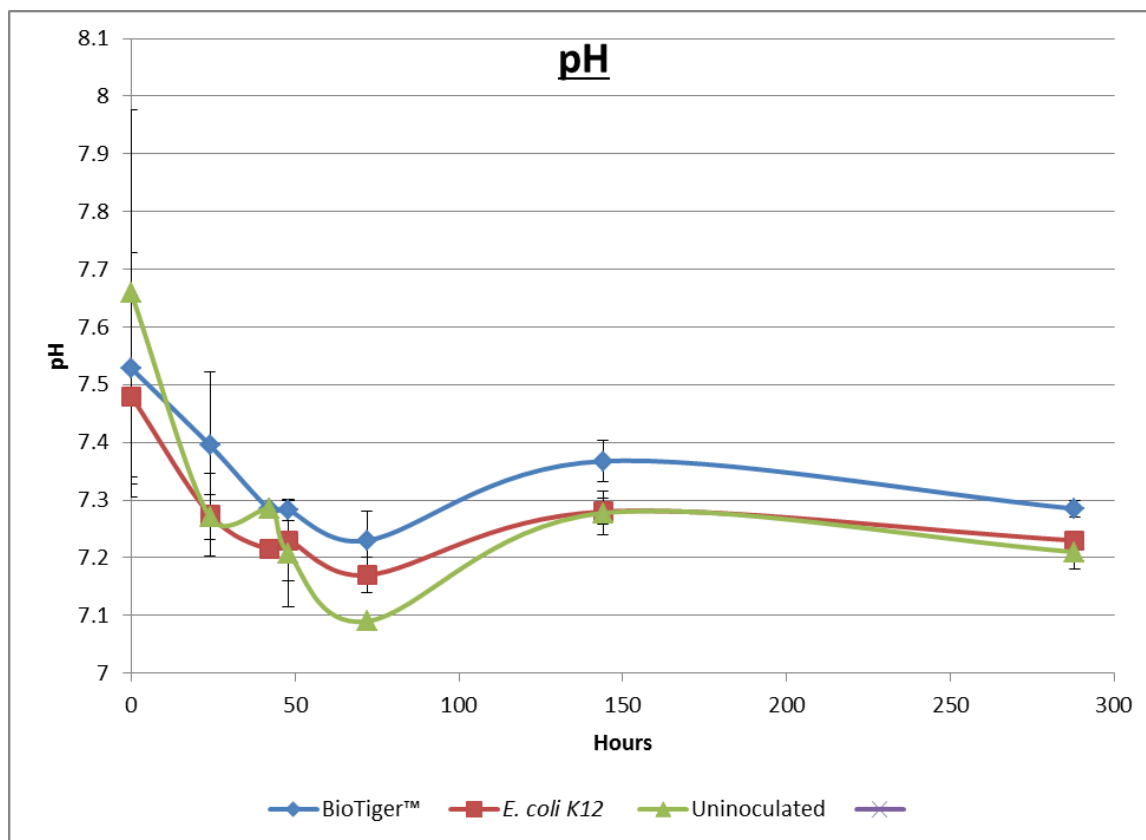
557

558   **Figure 7.**

559

560   **Figure 7. Conductivity (mS/cm) measured out to 288 h in the settling experiment.**

561   **Results represent the mean of two columns for each reading. Bars are standard**

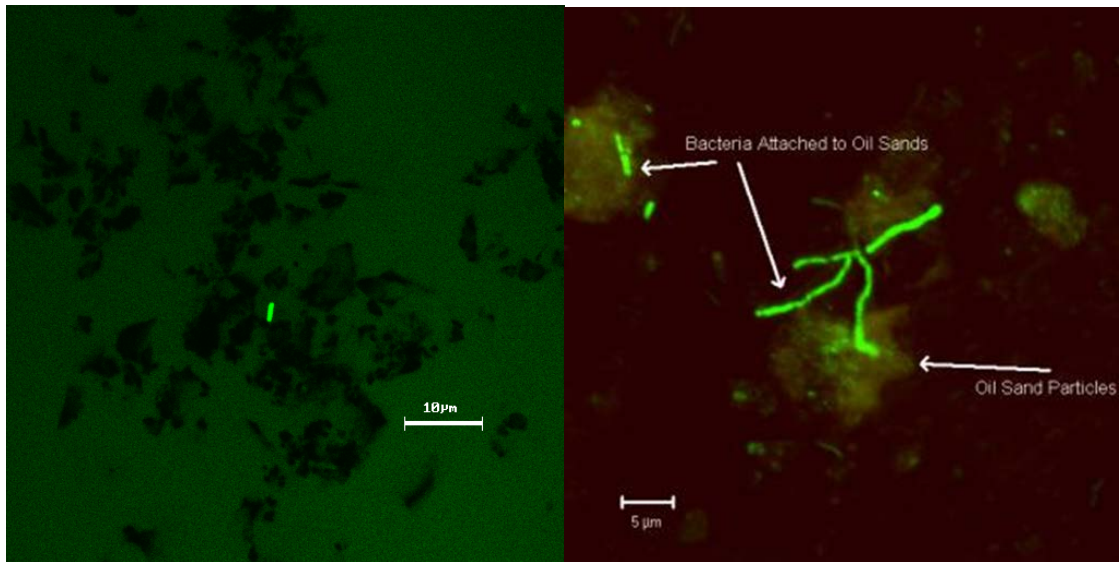562   **deviation of two measurements.**

563

564 **Figure 8.**

565

566 **Figure 8. Over lay water pH measured out to 288 h in the settling experiment.**

567 **Results represent the mean of two columns for each treatment. Bars are standard**

568 **deviation of two measurements.**

569

570   **Figure 9.**

571

572

573   **Figure 9. Bacteria observed in untreated oil sands were as few as 1 per field labeled**

574   **with FITC (L).   After adding BioTiger™ bacteria were observed binding to**

575   **oilsands particles within 30 min (R).**

576