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SAVANNAH RIVER LABORATORY

DPST-84-228

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December 9, 1983

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L-AREA CAVITATION TESTS
FINAL ANALYSIS - LIMITS APPLICATION

INTRODUCTION AND SUMMARY

The L Area cavitation test was designed to better define the onset of cavitation in the reactor system. Preliminary tests began in early 1983 and the L Area tests were completed in October, 1983. The onset of gas evolution in the effluent piping and pump cavitation was measured using state-of-the-art equipment to provide data with a high confidence and low uncertainty level. The limits calculated from the new data will allow an approximate 2% increase in reactor power if the reactor is effluent temperature limited with no compromise in reactor safety.

*Appendix Not Included

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Purpose of L Area Test

The L Area cavitation test was designed to better determine the conditions at onset of pipe and pump cavitation. Cavitation can adversely effect system performance and, over a long period (several months), cause pump impeller erosion. The reactor effluent temperature limit protects the SRP reactors from cavitation. The limits are currently based on a series of tests run in K Area in 1957¹ and tests by the Bingham Pump Company² run in 1956. The data from these earlier tests have a large uncertainty applied to them because of nonidealities, measurement techniques, and undefined differences among the reactor systems to which they are applied.

Review of Preliminary Work

Several preliminary tests were run to study the cavitation phenomena and establish detection techniques. This preliminary work is described in detail in DPST-83-2006.³ The basic conclusions drawn from these tests were:

1. Gas evolution will precede cavitation.
2. Damage to pipe walls would be less severe than previously thought.
3. Cavitation can be easily detected with acoustic monitoring techniques.
4. Cavitation can also be detected by an increase in pressure drop through the effluent piping.

Test Description - Instrumentation

A special instrumentation package was designed for the L Area cavitation test. The Equipment Engineering Department assisted in the procurement, calibration, and installation of the following instruments in 105-L.

- 1 Displacement probe (system #2 ramshorn)
- 6 Bingham Pump DP transducers
- 6 Pump suction pressure transducers
- 6 Temperature transducers (failed due to improper electrical isolation)
- 1 Low pressure header transducer
- 1 Bottom tank centerline pressure transducer
- 1 Effluent line pressure tap (system 1 by biological shield)
- 2 Ultrasonic flowmeters (failed at temperatures above 80°C)
- 2 Fast response pressure transducers (connected to monitor pins)
- 1 Atmospheric pressure transducer (in process room)

The outputs from these transducers were connected to the vibration and acoustic monitoring (VAM) system. The VAM is a newly installed permanent system which uses accelerometers to monitor for vibration related problems in the radiation zone.

Twelve of the accelerometers were used during the test to monitor for cavitation noise.

The location of all of the transducers and the instrumentation layout are shown schematically in Figures 1 and 2.

The VAM took only 35 seconds to scan all of the sensors. Approximately 10 MBYTES of data were collected and stored on disk.

Procedure

Five separate cavitation tests were run with different and varying number of pumps on line. No blanket gas was applied and the septifoil flow was shut off. During each test, pump heat was used to increase the temperature of the flowing fluid and take the system into cavitation. When one of the following limits was reached cooling water flow to the heat exchangers was cut on to cool the fluid and stop the cavitation.

Limits:	10%	drop in pump DP
	5%	drop in flow
	6.5 g's	pump acceleration
	150 mils	ramshorn displacement
	98°C	moderator temperature

It should be noted that the 10% drop in pump DP limited all of the tests because the pump DP becomes very erratic as soon as the pump begins to cavitate.

AC Start Up

The startup of the AC motors was monitored during all of the testing. The accelerations during startup ranged from 8 to 13 gs if the system was cold and only 2 to 3 gs if the system was at 50°C or higher.

Three Pump Test

The three pump test was run with the tank at overflow. Systems 1, 2, and 5 were operating. During the three pump test, system flows were approximately 30 KGPM.

Five Pump Test

The test was run with the tank at overflow. Only system six was not operating. System flows ranged from 26 to 28 KGPM.

Six Pump Tests

Three tests were run with all six systems operating, one test was run at a tank level of 8.2 feet* and the others at a tank level of 9.2 feet*. The tank level was lowered to induce cavitation below the 98°C limit. System flows ranged from 24 to 26.5 KGPM.

Description of the Phenomena

The cavitation tests had three distinct stages - heat-up, gas evolution, and pump cavitation. These stages can be seen on the preliminary data plots of acceleration, pump DP, and temperature verses time shown in Figure 3. The first stage includes the normal operating region. Pump DP and acceleration decrease slowly as the system temperature increases.

Gas Evolution

The second stage is marked by an increasing pump DP and decreasing acceleration caused by the evolution of dissolved gases in the fluid. This phenomenon was seen in the preliminary tests at Georgia Iron Works. As conditions at the muff begin to approach the saturation temperature and pressure of the flowing fluid, dissolved non-condensable gases come out of solution. These gases cause an increase in the pressure drop from the tank to the pump suction - lowering the suction pressure and increasing the pump DP. The evolved gases also allow slight compressibility of the flowing fluid which decreases the flow noise and pipe/pump acceleration.

Pump Cavitation

Because the pump suction pressure is dropping and temperature is still increasing during stage two, the pump soon begins to cavitate. The third and last stage of the phenomena is marked by extremely erratic pump DP and a marked increase in acceleration. This is the pump cutoff point. The pump itself is cavitating, impeller erosion is beginning, and any increase in temperature or reduction in system pressure will cause a significant flow reduction.

*See Appendix E

Technical Limit

The technical limit is set to prevent steady state operation of a reactor in a region where damage may take place.⁴ The technical limit is set at the first indication of gas evolution in the effluent lines. Several measurements were used to determine the onset of gas evolution. Plots of pump DP, pump acceleration, and effluent line (elbow) DP verses temperature were analyzed. The raw data is shown in Table 1; the plots are in Appendix A; and the technical limit as calculated for L reactor with 5 PSIG blanket gas is shown in Figure 4. The raw data was adjusted by the procedure described in Appendix B.

The adjusted L-Area data can be curve fitted using the following equation in a range of 24 to 30 KGPM system flow.

Technical Limit, °C at 5 PSIG blanket gas pressure

$$T = 49.2296 + 5.31218 \times F - 0.12177 \times F^2$$

where F is system flow in KGPM

Pump Cutoff Curves

The pump cutoff curve is used in the transient protection limits analyses to establish temperatures at which pump flow is significantly affected by cavitation.^{4,5} Plots of pump DP and pump acceleration (Appendix A) were analyzed to determine the pump cut off point. Also the data from the Bingham Pump Company tests, contained in Appendix C, was analyzed to assure that this was the pump cutoff point. The raw data is shown in Table 2 and Figure 5 show the pump cutoff curves for L reactor at 5 psig blanket gas pressure.

The adjusted L-Area pump cutoff data can be curve fitted using the following equations in a range of 24 to 30 KGPM system flow.

Pump Cutoff limit, °C at 0 PSIG blanket gas pressure

$$T = 2.34795 + 8.56714 \times F - 0.1883 \times F^2$$

Pump Cutoff limit, °C at 5 PSIG blanket gas pressure

$$T = 41.78315 + 5.91187 \times F - 0.131216 \times F^2$$

where F is system flow in KGPM

Uncertainty Analysis*

The uncertainties of the measured parameters during the L

*Appendix C contains instrument calibration data.

area test are described below. Each uncertainty is converted to a temperature uncertainty by the use of the D₂O saturation curve, the current pump cutoff curve, or the moderator heat up data. As shown, the uncertainties (ω) are combined as independent variables (square root of sum of squares) to yield an overall value.

ω_{TL} Tank Level $\pm 3''$ (0.12 psi x 2.5°C/1 psi @ 90°C)	$\pm 0.3^\circ\text{C}$
ω_{**F} Flow (pump DP) ± 1.8 psid (± 0.4 KGPM x 1.2°C/1 KGPM @ 25 KGPM)	$\pm 0.48^\circ\text{C}$
ω_t Time ± 30 sec. (x 0.3°C/60 sec)	$\pm 0.15^\circ\text{C}$
ω_{RTD} RTD $\pm 0.15^\circ\text{C}$	$\pm 0.15^\circ\text{C}$
ω_{CRE} Curve Reading Error	$\pm 0.15^\circ\text{C}$

$$\omega_{DATA} = (\omega_{TL}^2 + \omega_F^2 + \omega_t^2 + \omega_{RTD}^2 + \omega_{CRE}^2)^{1/2} = 0.62^\circ\text{C}$$

An uncertainty must be applied to account for the differences in the six reactor systems. Figure 6 was used to determine this uncertainty.

$$\omega_{RS} = \pm 1.45^\circ\text{C}$$

An uncertainty must be applied to account for the fact that the six reactor systems do not have the same flow. Even though the limit is applied to the hottest system in a reactor, this could be the lowest flow system.

$$\omega_{SF} = \pm 1.32^\circ\text{C} \quad (\pm 1100 \text{ GPM})$$

Two more uncertainties⁶ unrelated to the test, but related to the limits application must be included. The uncertainty in reactor temperature monitoring and the uncertainty in blanket gas pressure.

$$\omega_M = \pm 0.9^\circ\text{C} \quad \omega_{BGP} = \pm 0.8^\circ\text{C}$$

$$\omega_{Total} = (\omega_{DATA}^2 + \omega_{RS}^2 + \omega_{SF}^2 + \omega_M^2 + \omega_{BGP}^2)^{1/2} = \pm 2.4^\circ\text{C}$$

With this uncertainty applied to the L Area test data the limits can be used in P, K, L reactors with high confidence. Note that by using several different types of analysis techniques, (pump DP, acceleration, and suction line DP) the confidence in the data is greatly increased. Also, the good agreement between the K-Area,

**Flow was calculated from pump DP using equation in DPST-83-282.

Bingham Pump Co., and L-Area data indicates that there is no significant variation in the cavitation temperatures for different reactors.

It should be noted that the effect of temperature on fluid properties was not accounted for in the adjustment of the raw data (see Appendix D). This conservatism amounts to approximately 1.5°C. Further laboratory testing could possibly prove the assumptions made in Reference 3 and allow the reduction of this conservatism.

C-Area Limits^{4,8}

The data from L Area cannot be directly applied to C Area. It is the opinion of the author that no extrapolations or similitude analyses would improve the uncertainty of the C Area limits. However, it is comforting to note that the new L Area data lined up so well with the Bingham Pump Company data that is used in calculating the C-Area limits.

Audit

The calculation procedure and limits presented in this document have been audited by W. M. Massey, Jr. of Reactor Technology Department of SRP and L. L. Hamm of the Nuclear Engineering Division of SRL.

Summary

The onset of gas evolution and pump cavitation has been well defined by the L Area tests. The lower uncertainty associated with the new data will allow a safe increase in reactor power.

DCW:cjl

REFERENCES

1. DPSP-57-1405, "Cavitation Characteristics of Bingham Pumps".
2. Bingham Pump Company Tests 1-64160, K to O.
3. DPST-83-2006, "Preliminary and Intermediate Cavitation Tests".
4. DPSTM-110.
5. DPSP-66-1322, "Limits On Reactor Effluent Temperature".
6. TA-1-2134, "Reduction of Reactor Effluent Uncertainty Analysis".
7. Stepanoff, A. J. Centrifugal and Axial Flow Pumps, 2nd. Edition, John Wiley & Sons.
8. DPST-81-845, "Revised Effluent Technical Limit for C-Reactor".
9. DPST-84-227, "L-Area Cavitation Tests - Raw Data".
10. Laboratory Notebook E35146, DPSTN-4197.
11. Laboratory Notebook E35145, DPSTN-4196.

TABLE 1
TECHNICAL LIMIT - RAW DATA

Test	System	Flow	T (Pump DP)	T (Accel)	T (Elbow DP)
6 - 1	1	25360 GPM	83° C	80° C	81° C
	2	26310	83	83.5	83
	3	26125	82.8	82	82
	4	24980	82.6	83	83
	5	24317	85.5	85	82
	6	-	-	-	-
6 - 2	1	25321	84.5	84	82
	2	26274	84.5	85.2	84.5
	3	26085	84.5	83	84
	4	25091	82	86.4	84.5
	5	24256	84	85	84
	6	-	-	-	-
6 - 3	1	25341	83.7	-	82.7
	2	26455	84.8	-	84.8
	3	26251	85.5	-	83.5
	4	25110	85.2	-	85.5
	5	24311	85.7	-	85
	6	-	-	-	-
5	1	27309	92	93.5	91.5
	2	28073	94.5	92	92.7
	3	27981	90.5	92	92
	4	26753	92	95	94.5
	5	26234	94	94	93.2
3	1	30591	82	85.5	82
	2	31640	84.5	86	85.5
	5	30413	82.5	82.5	82

(-) Indicates Bad Data

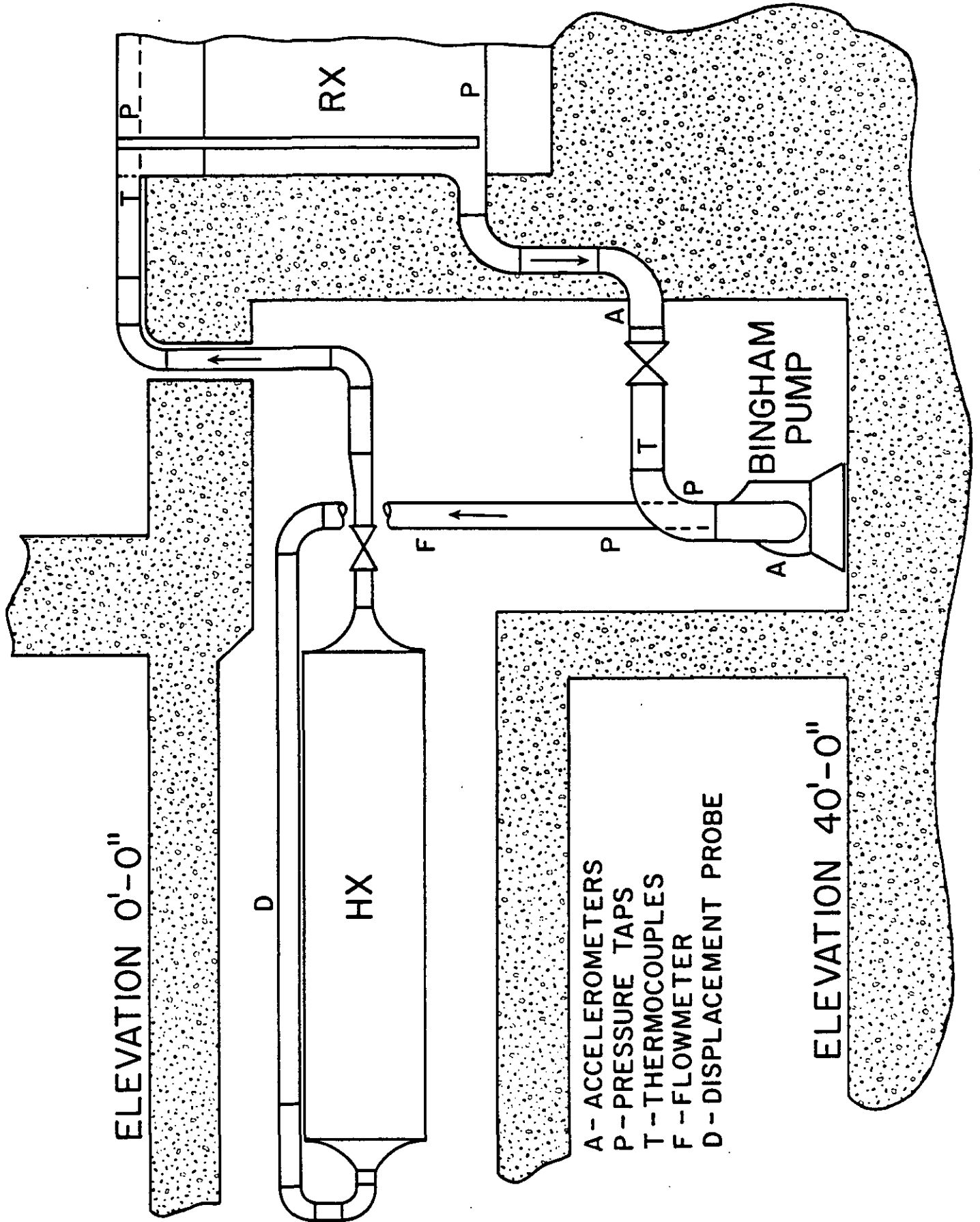
TABLE 2
PUMP CUTOFF LIMIT - RAW DATA

Test	System	Flow	T (Pump DP)	T (Accel)
6 - 1	1	25360 GPM	84.8	87.0
	2	26310	86.0	87.5
	3	26125	85.5	88.0
	4	24980	87.7	88.0
	5	24317	86.8	87.5
	6	-	-	-
6 - 2	1	25321	86.0	86.5
	2	26274	86.5	87.3
	3	26085	87.0	86.9
	4	25091	87.0	89.0
	5	24256	87.0	87.5
	6	-	-	-
6 - 3	1	25341	86.0	-
	2	26455	87.0	-
	3	26251	87.8	-
	4	25110	88.8	-
	5	24311	87.3	-
	6	-	-	-
5	1	27309	93.0	95.5
	2	28073	95.5	95.4
	3	27981	95.0	96.0
	4	26753	95.0	97.0
	5	26234	96.0	95.8
3	1	30591	86.0	87.0
	2	31640	86.5	88.5
	5	30413	86.0	87.0

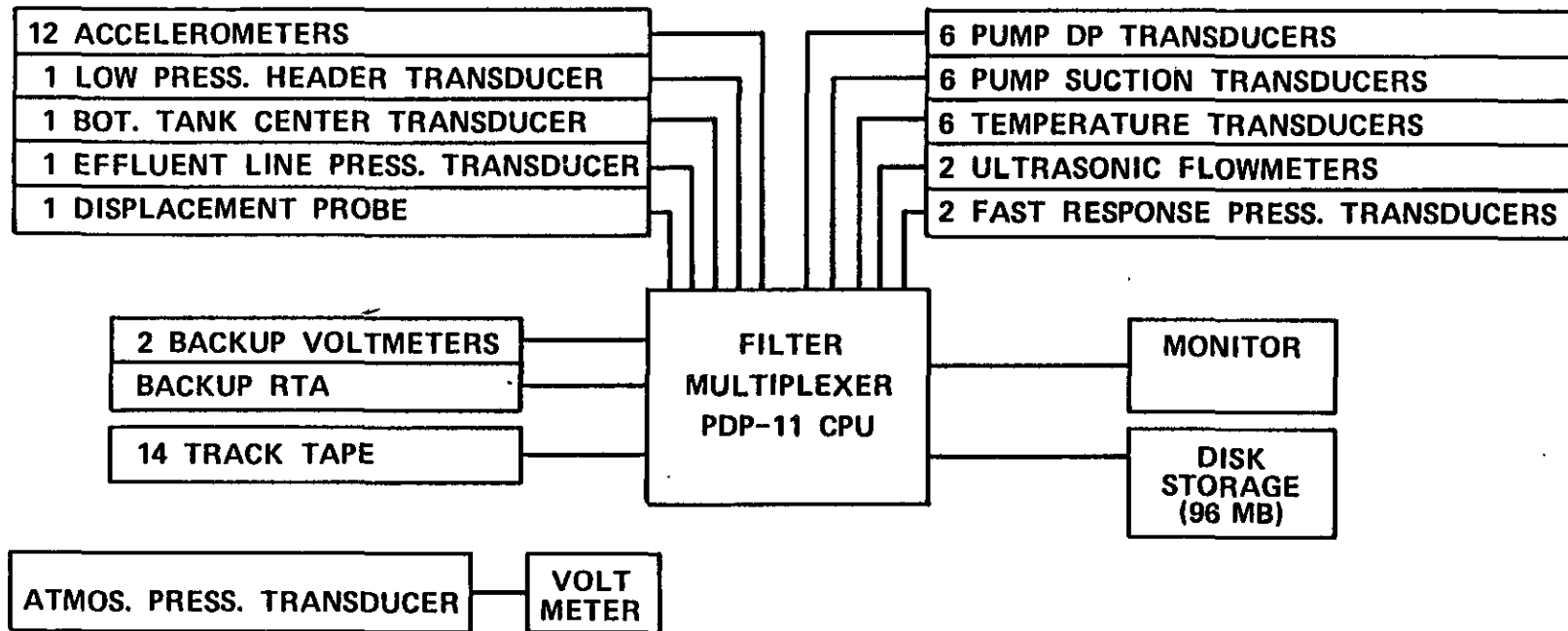
(-) Indicates Bad Data

FIGURE ONE

INSTRUMENTATION LOCATIONS



INSTRUMENTATION LAYOUT SCHEMATIC

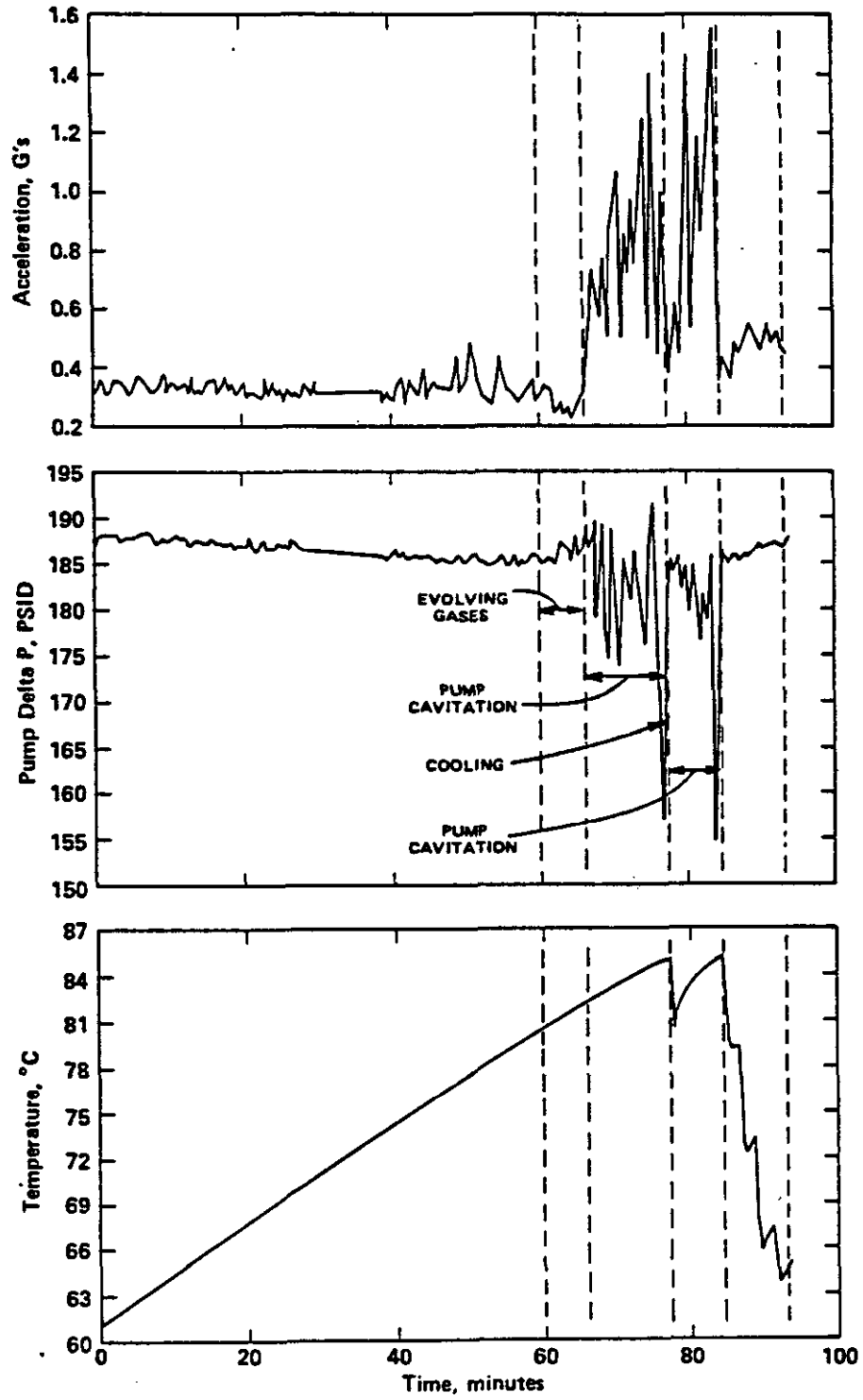


- ⑫ HEISE GAGES → PUMP SUCTION & DISCHARGE
 - ① HEISE GAGE → LOW PRESS. HEADER
 - ① PLENUM PRESSURE
 - ⑥ PUMP SUCTION RTDs
- } → CONTROL COMPUTER

FIGURE TWO

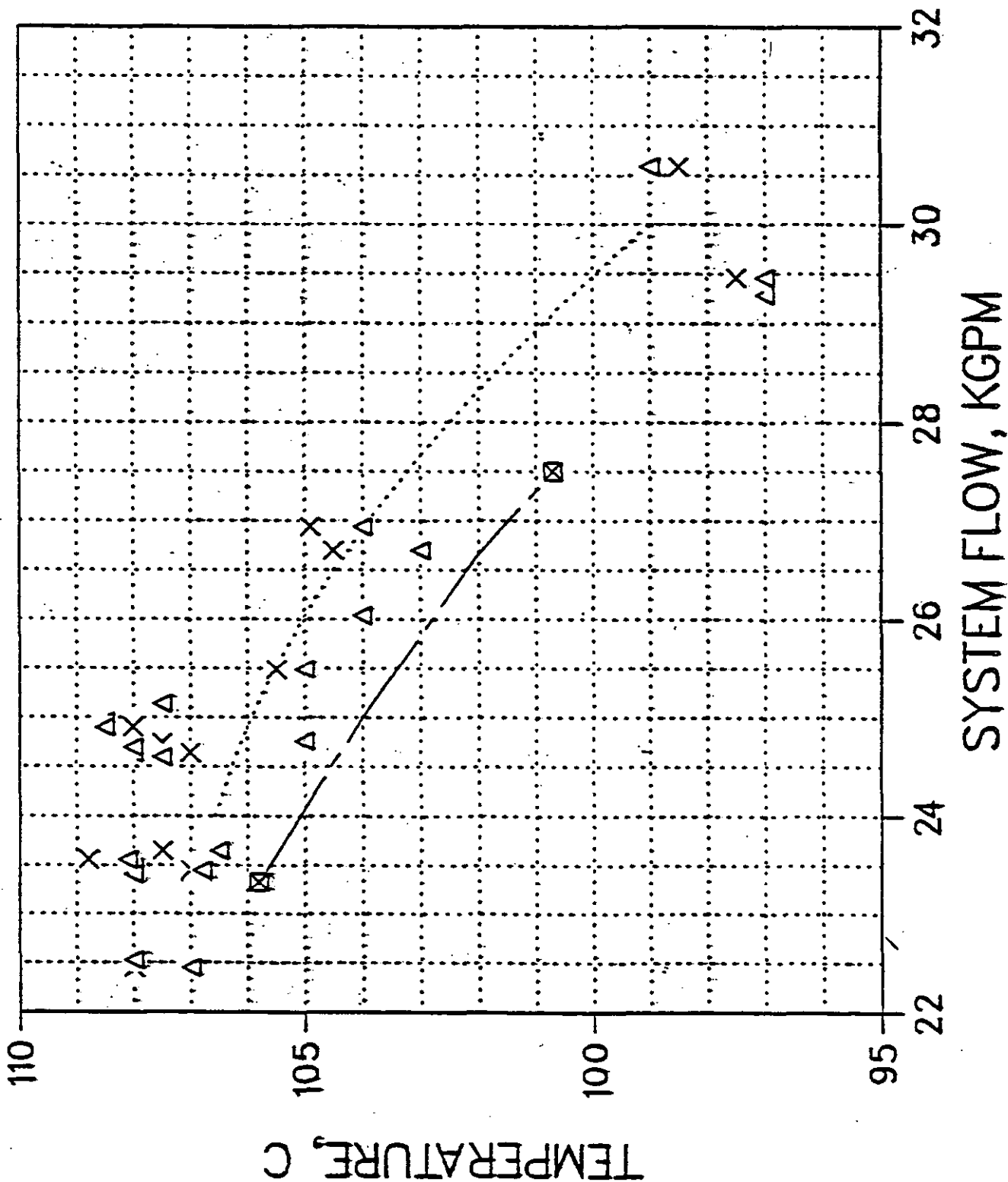
FIGURE THREE

CAVITATION PHENOMENA



RX EFFLUENT TECHNICAL LIMIT 5 PSIG BLANKET GAS

FIGURE FOUR



- Legend
- Δ PRESSURE DATA
 - X ACCEL DATA
 - LSTSOR FIT
 - ⊠ DPSTM-110

PUMP CUTOFF LIMIT - JAN 9, 1984

5 psig BLANKET GAS PRESSURE

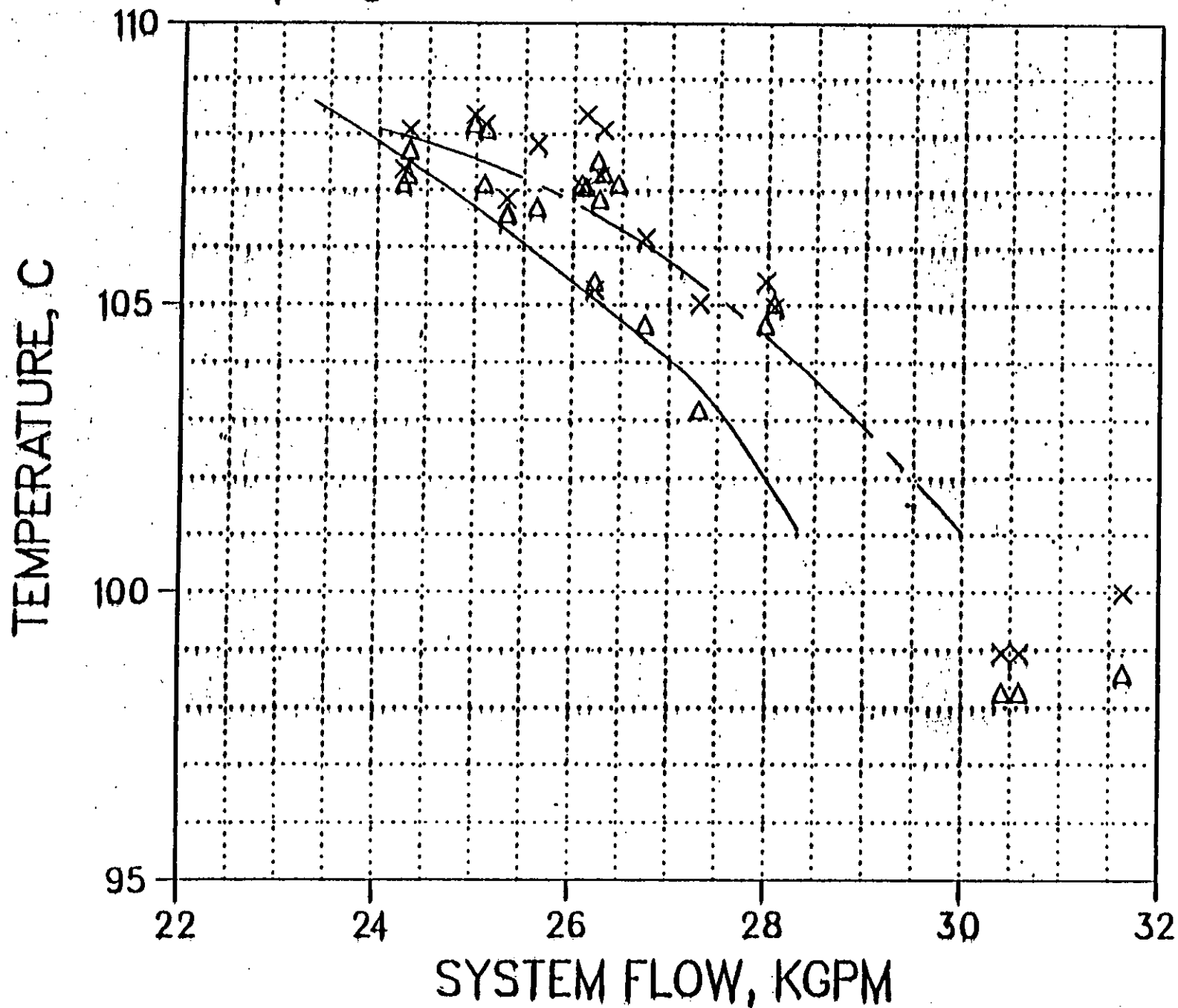


FIGURE FIVE

Legend
A PRESSURE DATA
X ACCEL DATA
LSTSQ FIT
DPSTM-110

PUMP CUTOFF CURVE by SYSTEM

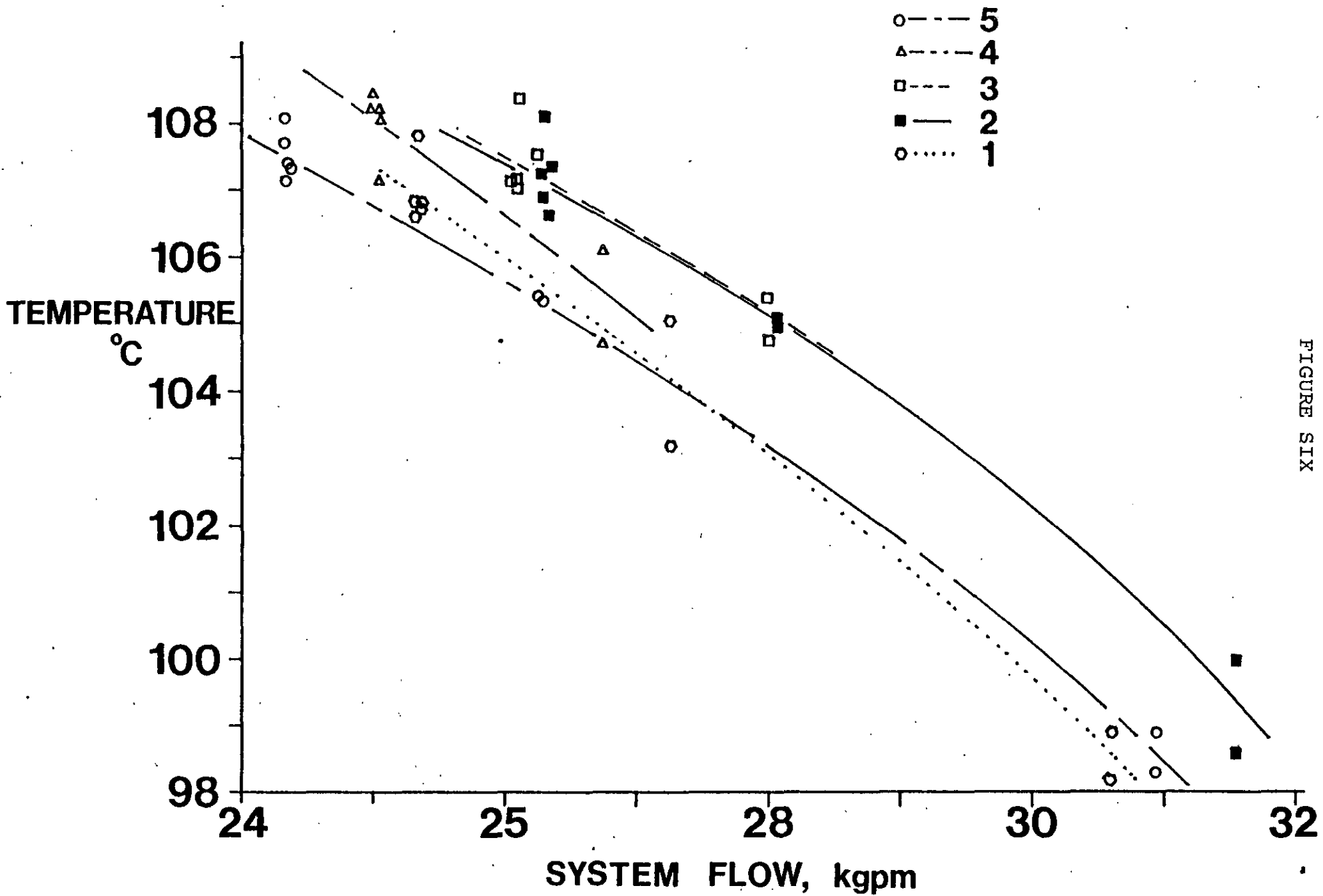


FIGURE SIX

APPENDICES

- A) Data Curves
 - 1) Pump DP vs. Temperature
 - 2) Acceleration vs. Temperature
 - 3) Elbow DP vs. Temperature
- B) Data Adjustment Procedure
- C) Calibration Data
- D) Fluid Property Effects
- E) Low Pressure Header and Tank Level
- F) Dissolved Gases
- G) Bingham Pump Company Data
- H) Uses of the L-Area Test Data and Miscellaneous Calculations

Appendix A - Data Curves

1) Pump DP vs. Temperature

These curves contain the pump delta P measured during each of the cavitation tests plotted against the associated RTD temperature readings. The pump DP becomes very erratic with cavitation. The system 6 pump DP is in error because of a problem in the pump suction pressure tap.

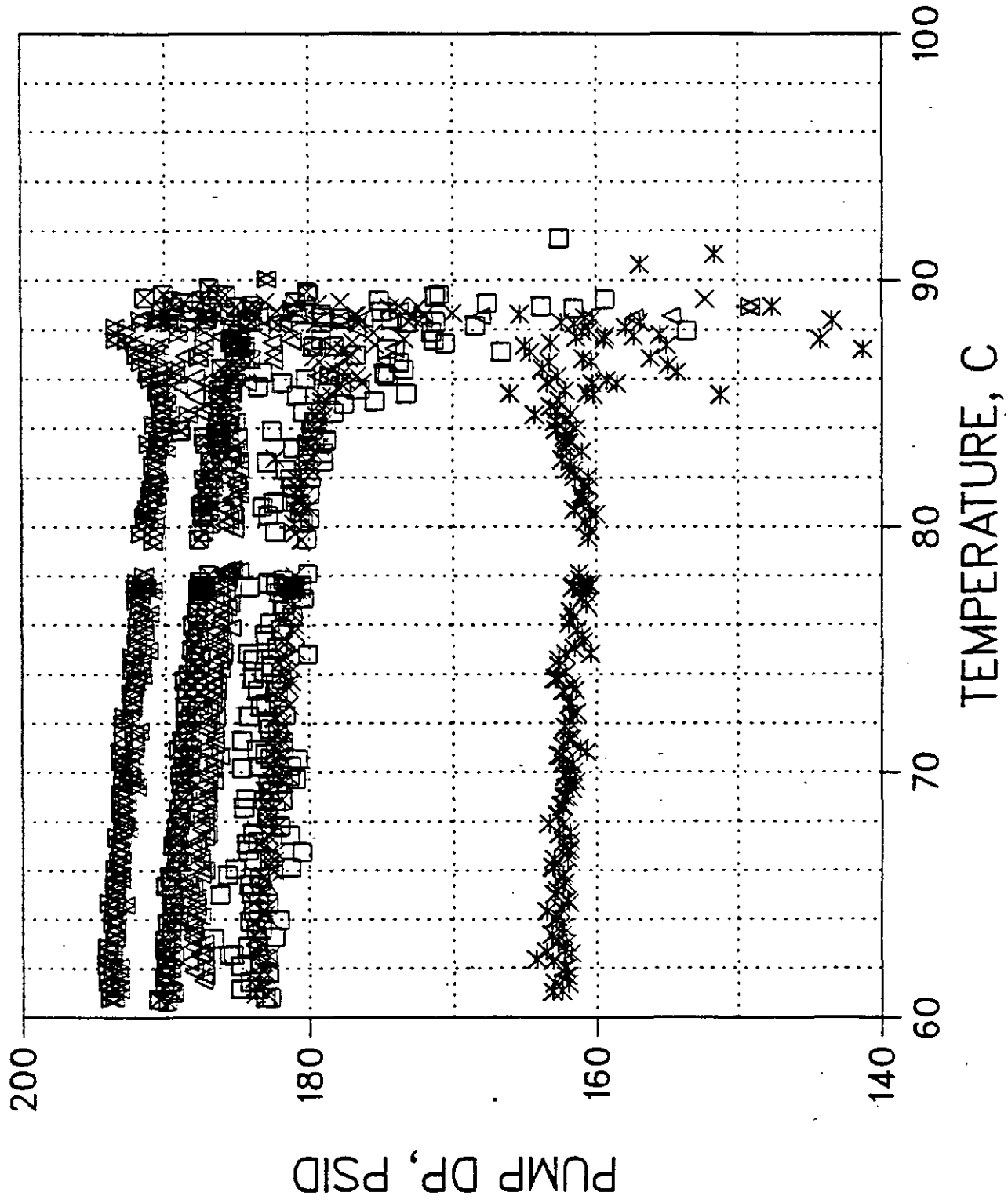
NOTES: The first plot in each set shows all system curves and the individual system curves flow.

Any lines or markings on the curves are not necessarily representative of the limits.

PUMP CAVITATION TESTS

JAN. 06 1984

UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 1

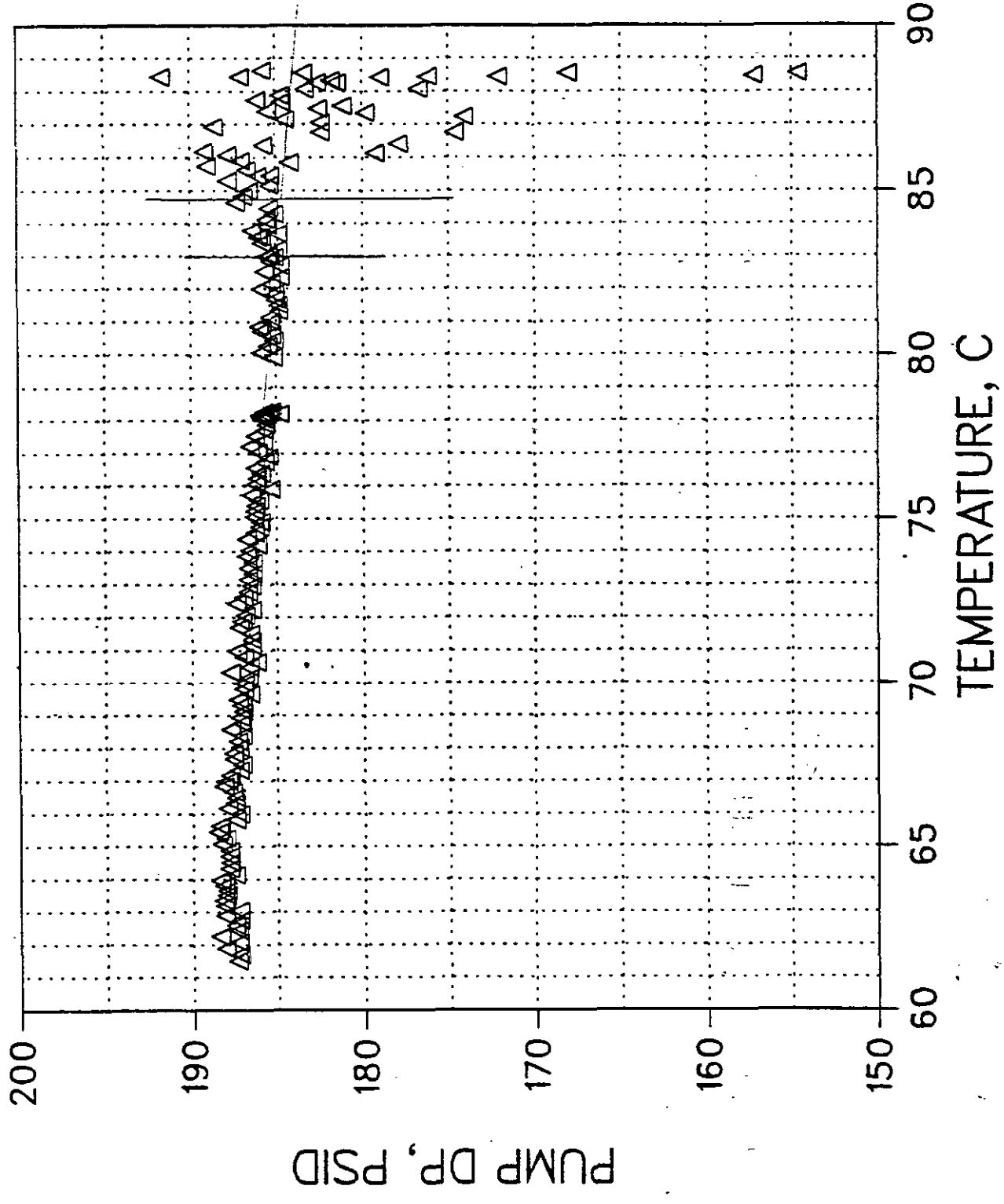


Legend

- △ SYS 1
- × SYS 2
- SYS 3
- ⊠ SYS 4
- ⊞ SYS 5
- * sys 6

JAN. 05 1984

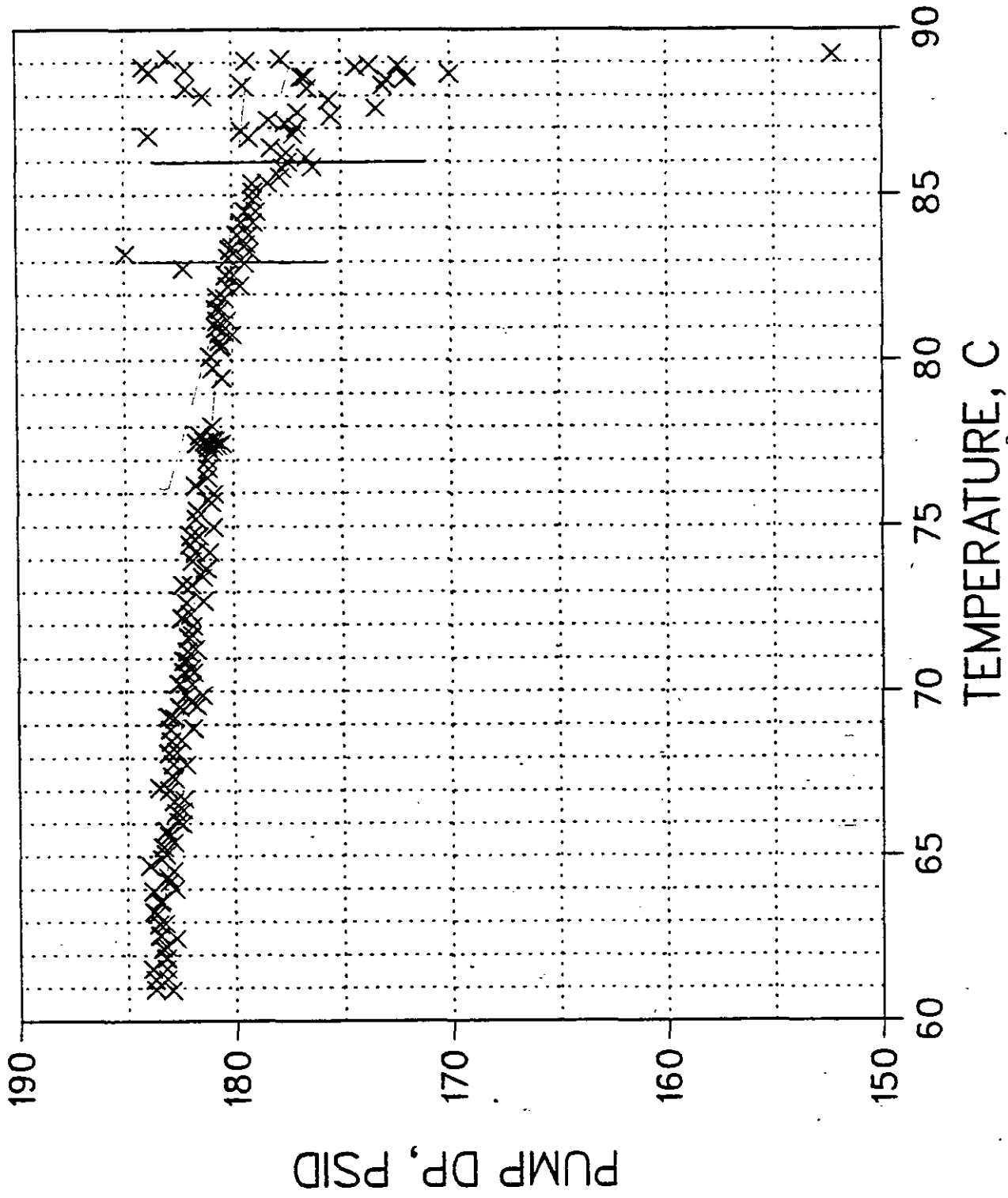
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 1



PUMP CAVITATION TESTS

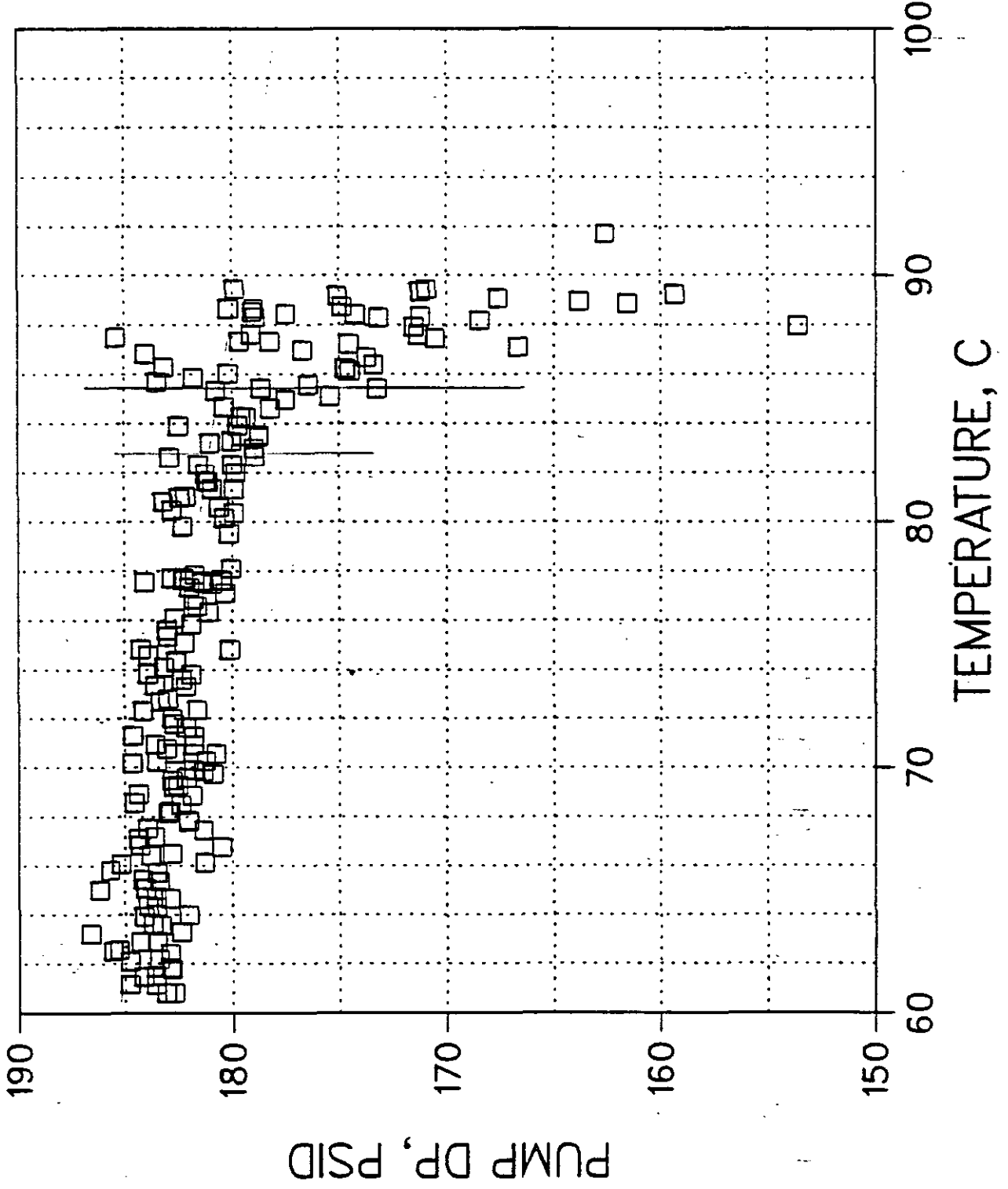
UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 1

JAN. 06 1984



PUMP CAVITATION TESTS

UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 1

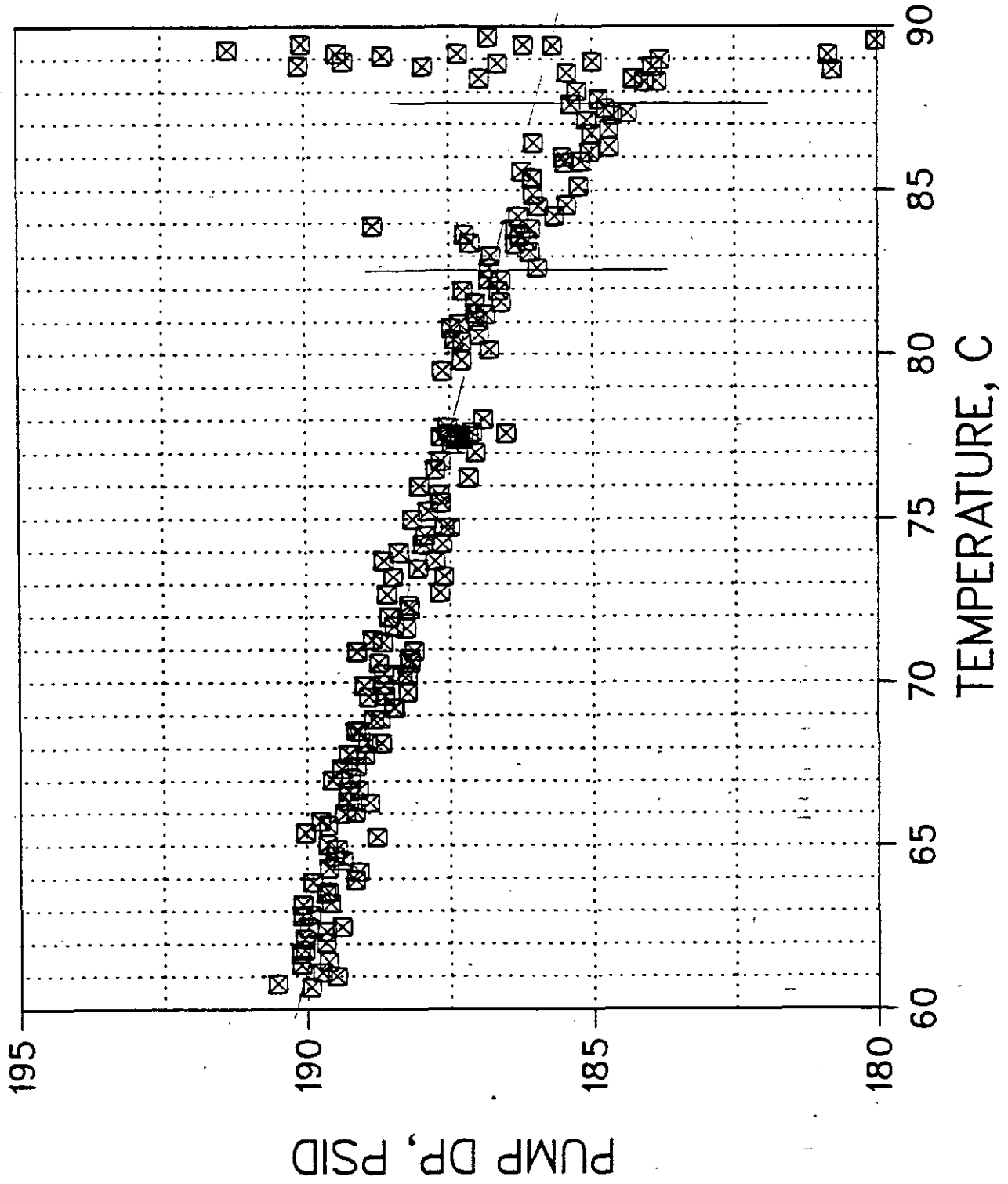


JAN 06 1988

PUMP CAVITATION TESTS

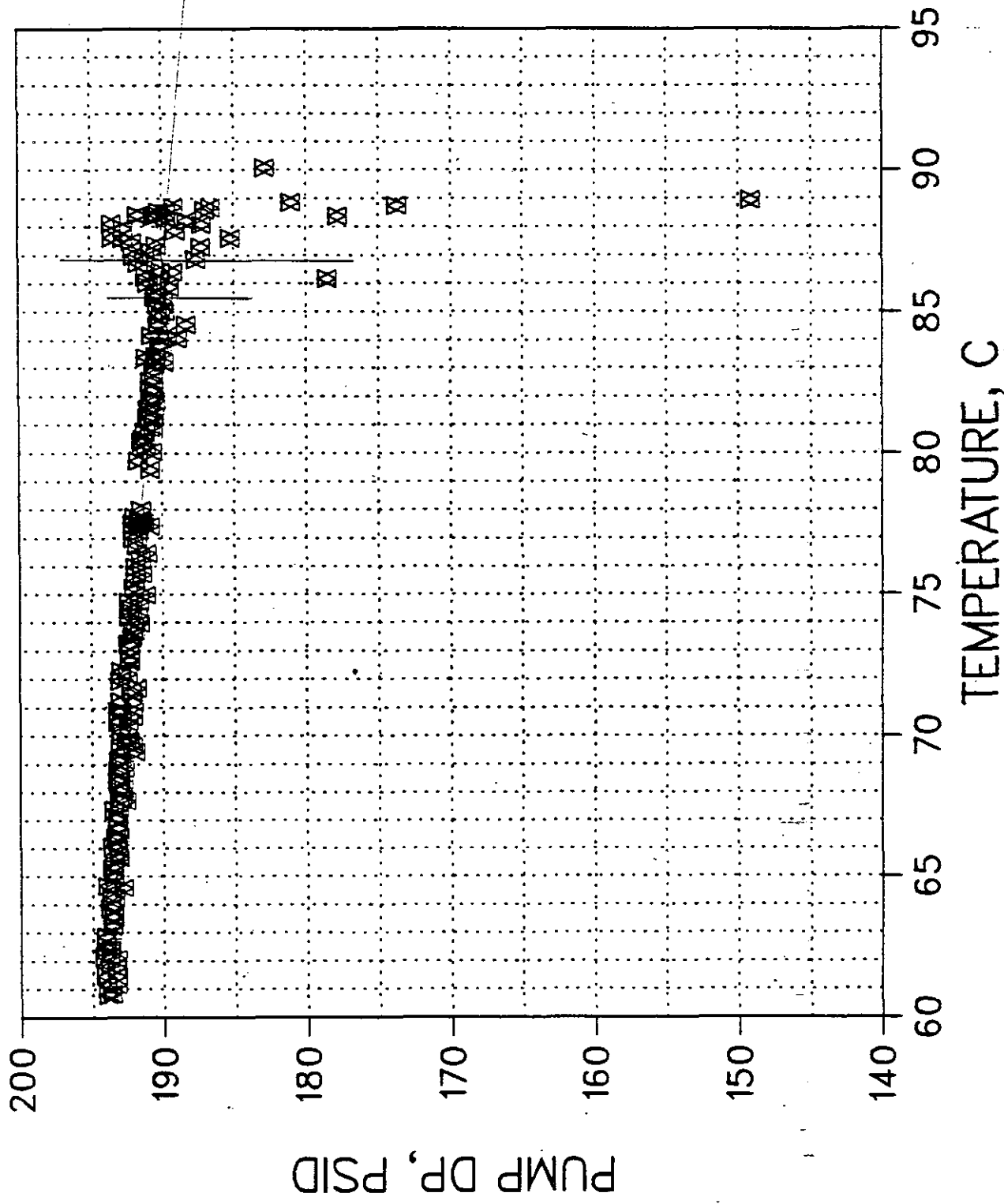
UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 1

JAN. 0 B 1964



JAN 10 1984

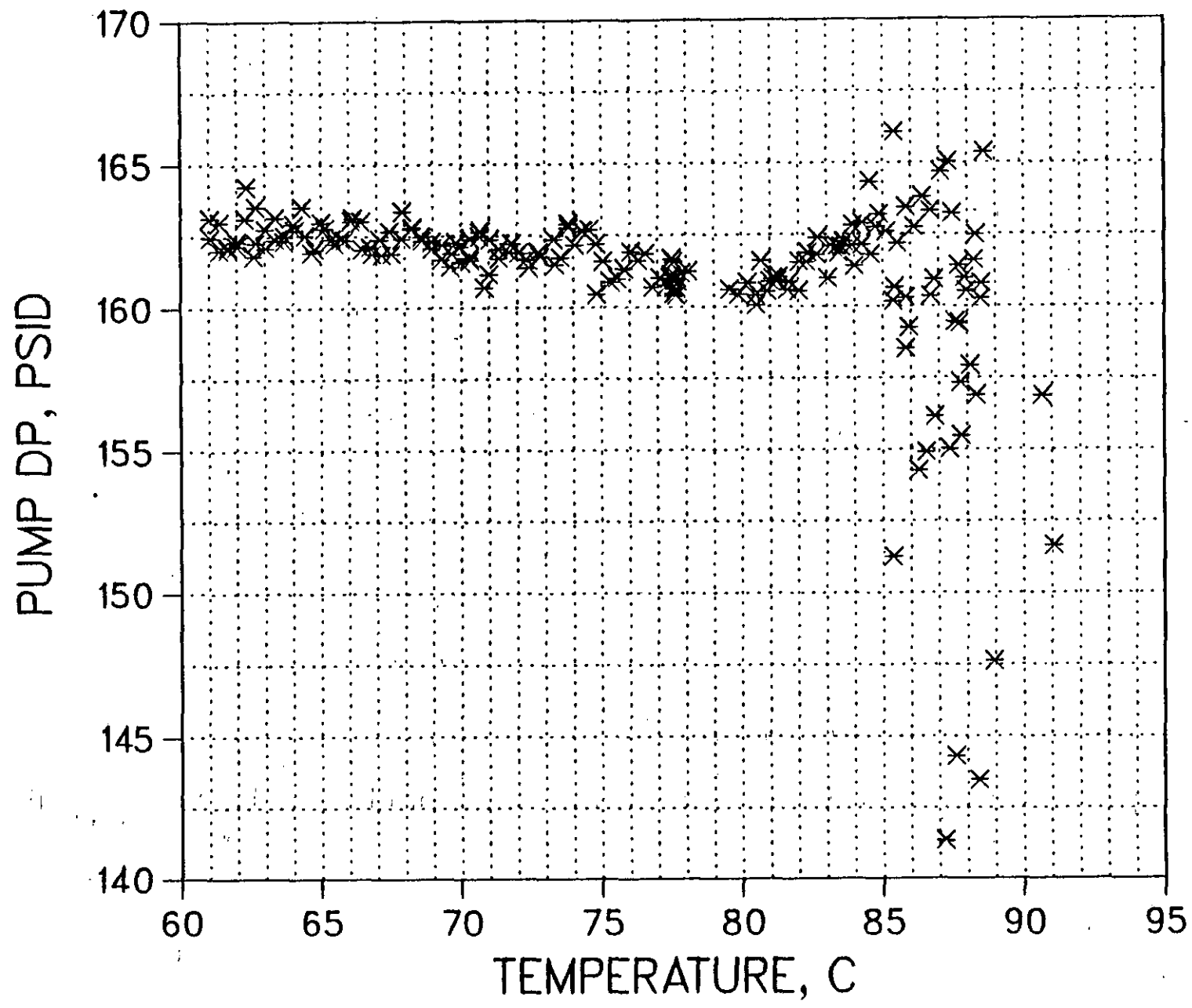
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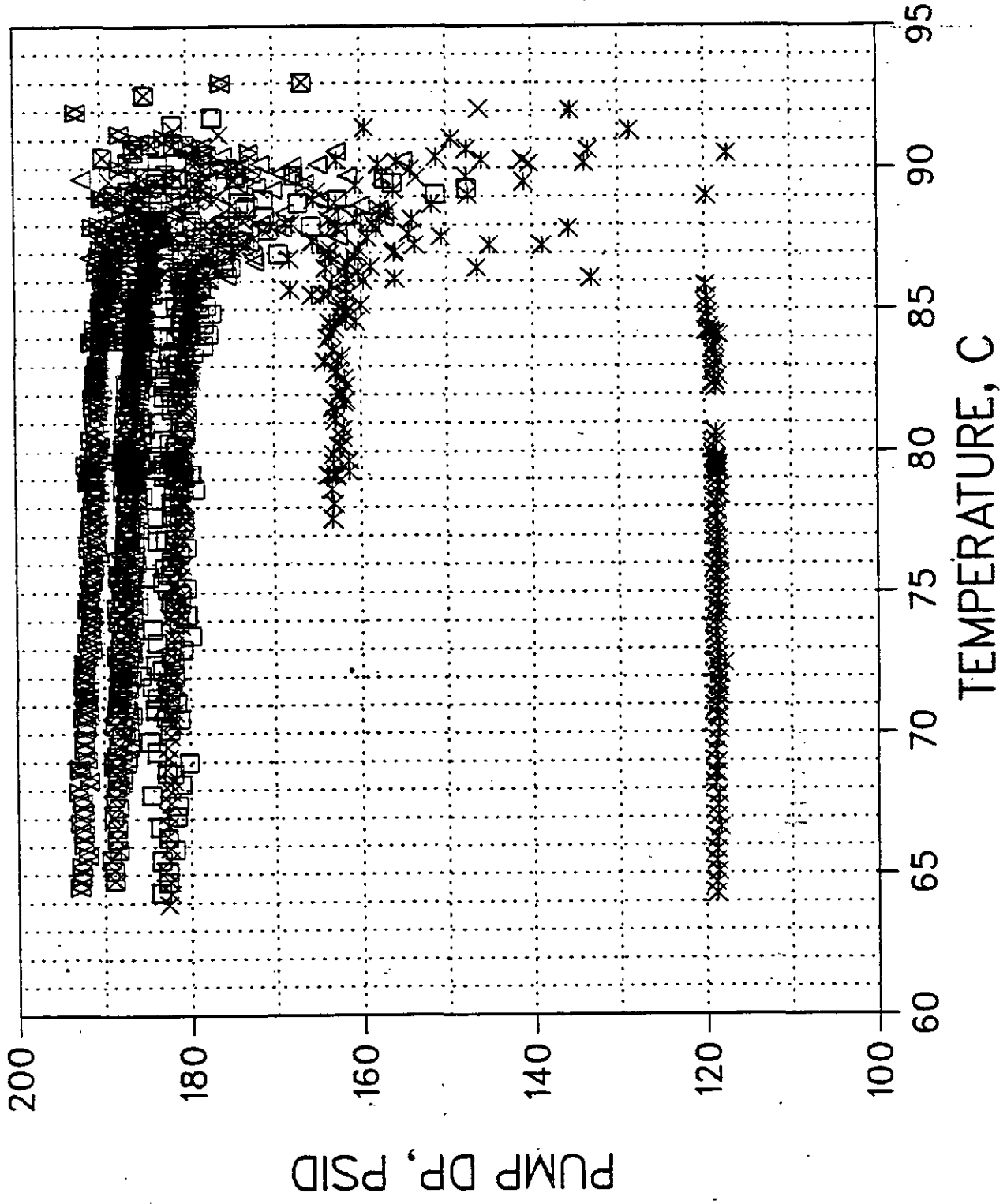
PUMP CAVITATION TESTS

UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 1 JAN. 06 1984

b



PUMP CAVITATION TESTS
UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 2



Legend

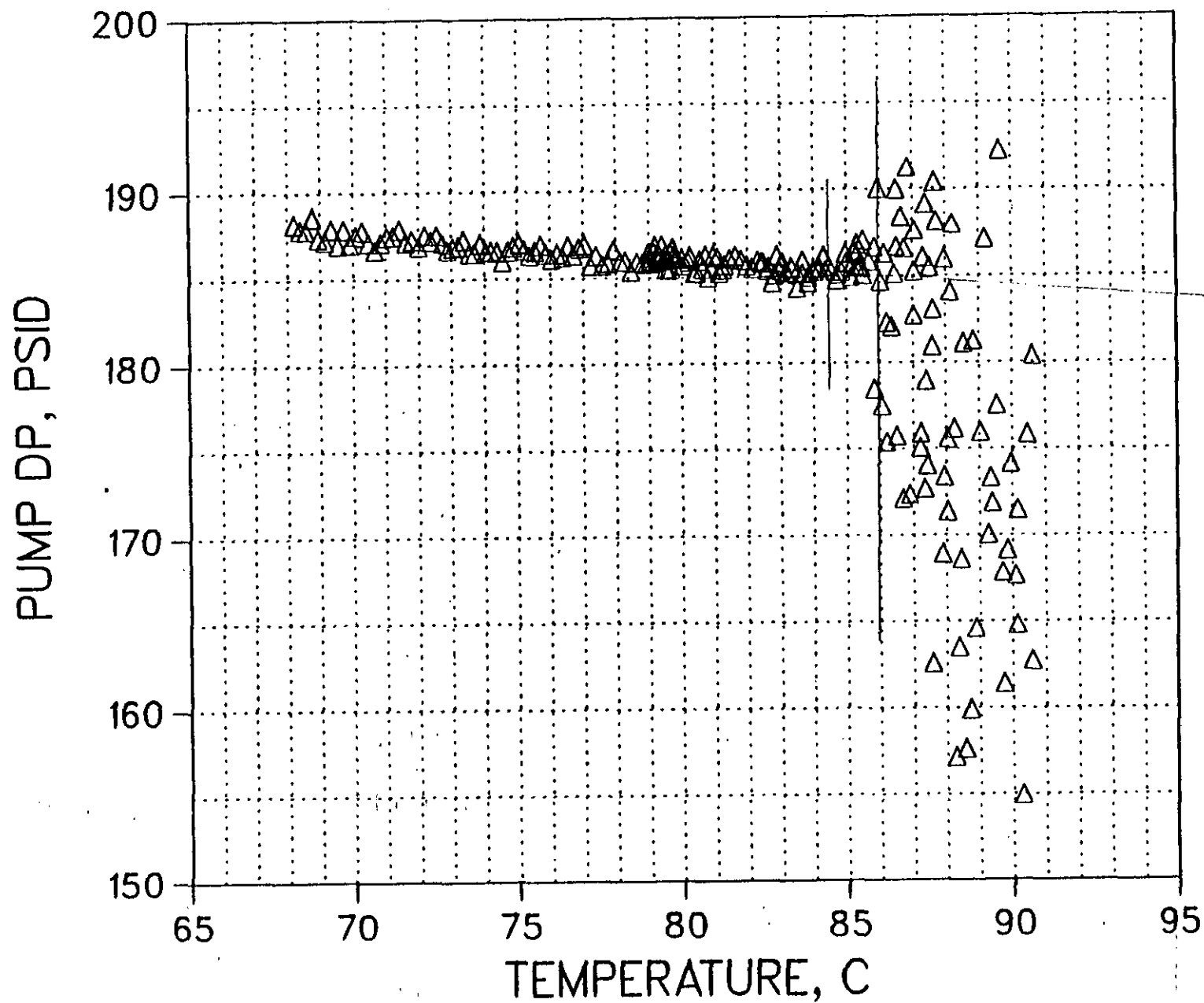
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- × SYS 2
- SYS 3
- ⊠ SYS 4
- ⊡ SYS 5
- * SYS 6

JAN. 06 1981

PUMP CAVITATION TESTS

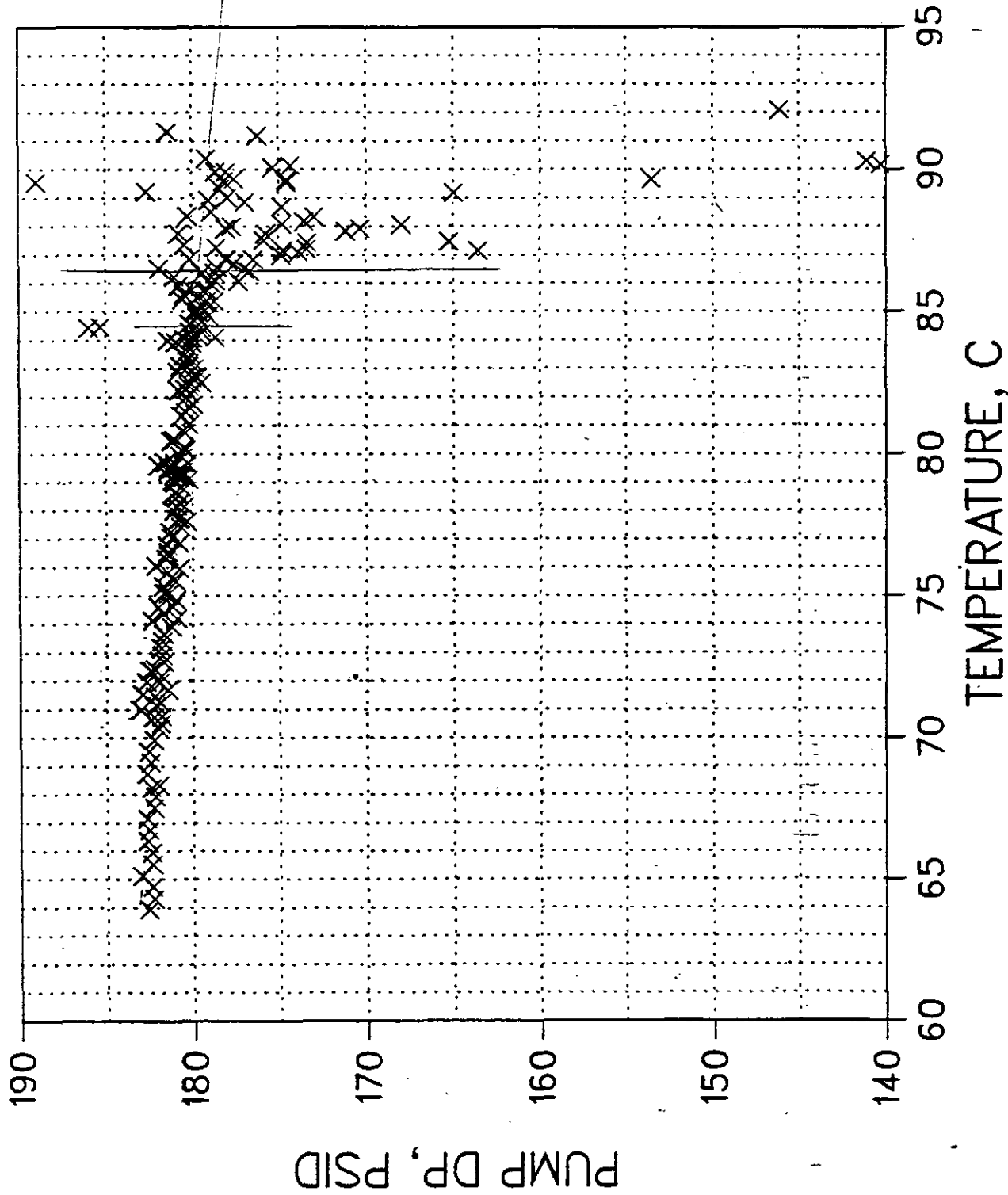
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JAN. 03 1984



PUMP CAVITATION TESTS

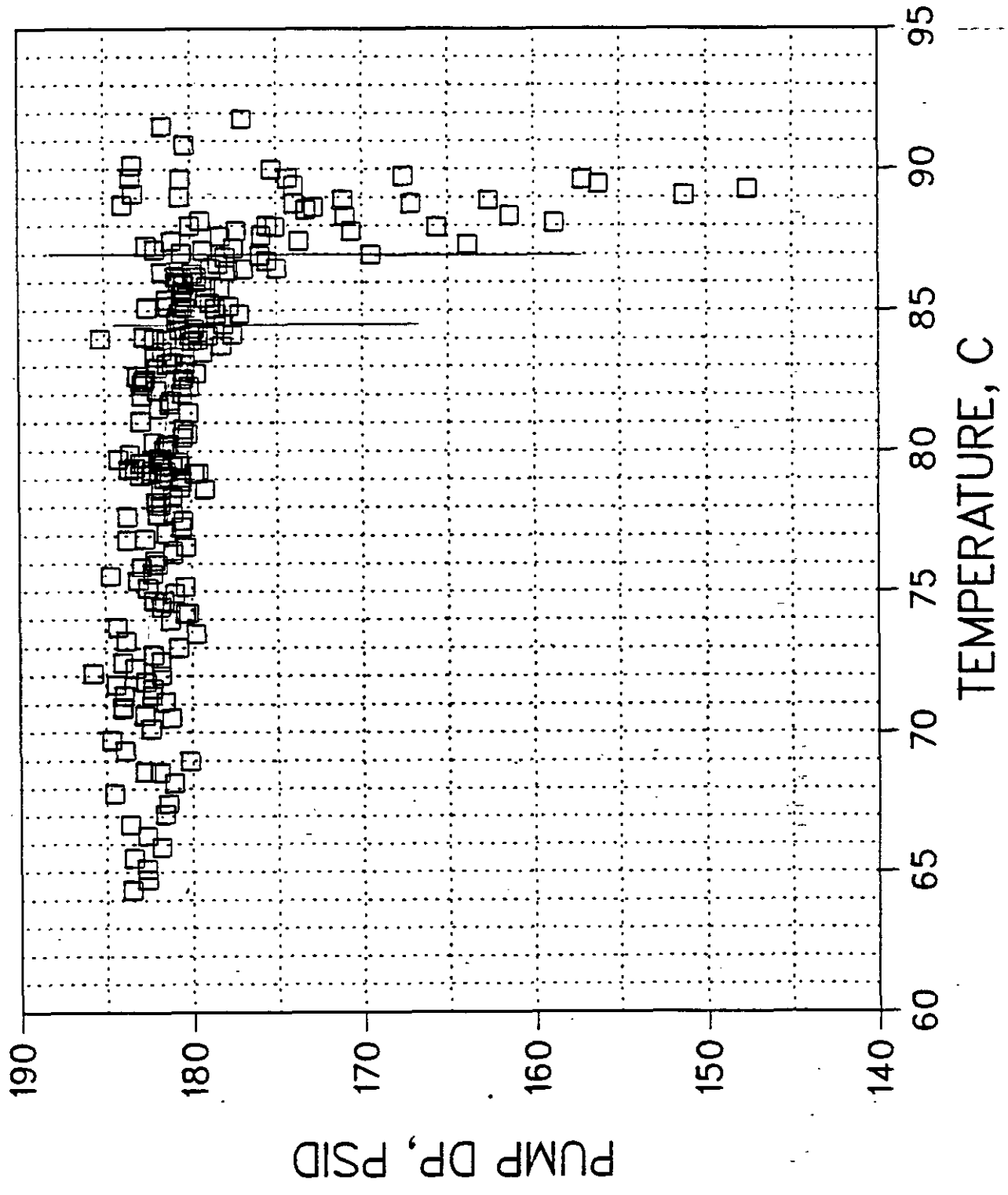
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JAN 06 1981

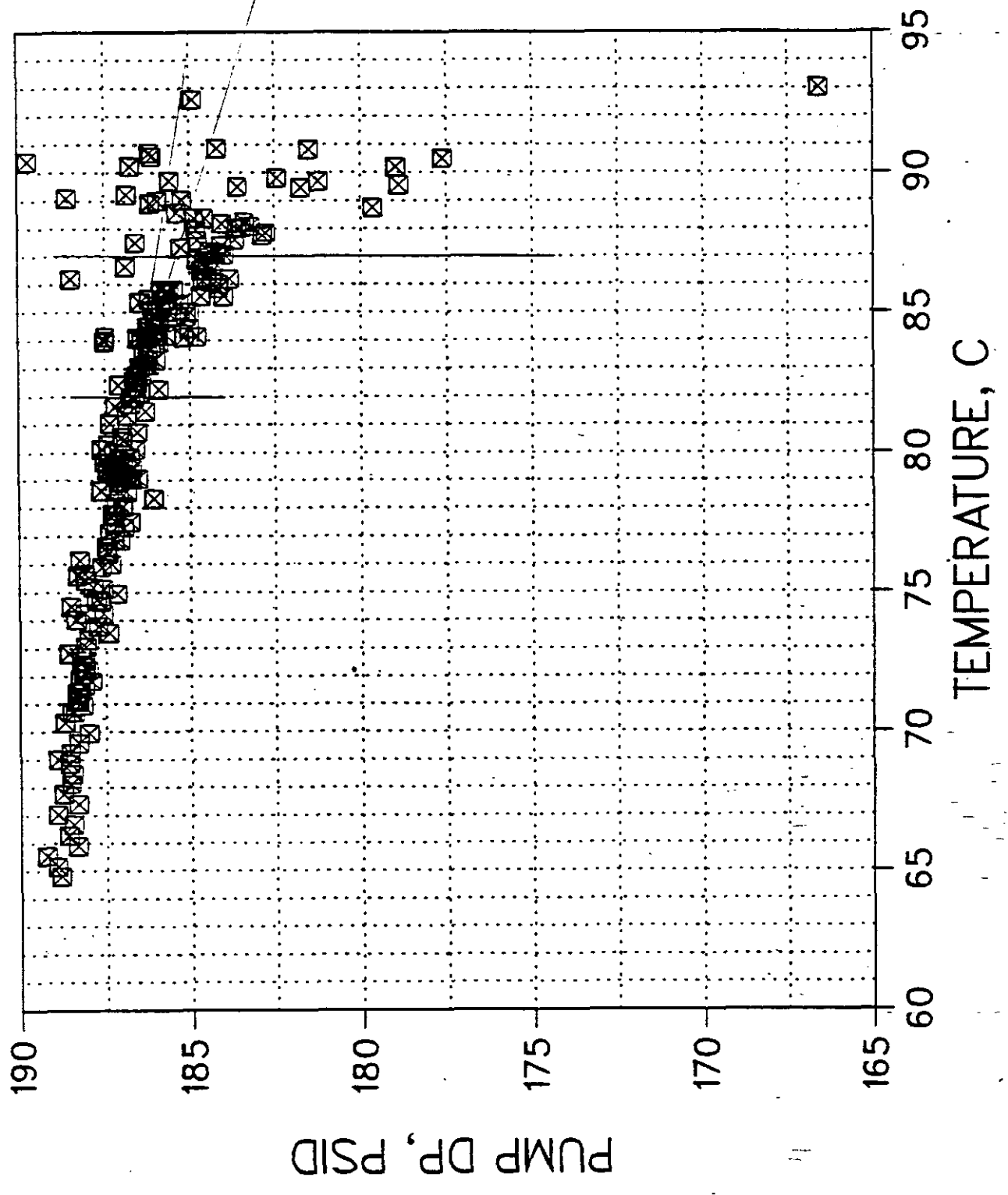
JAN 06 1984

PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 2



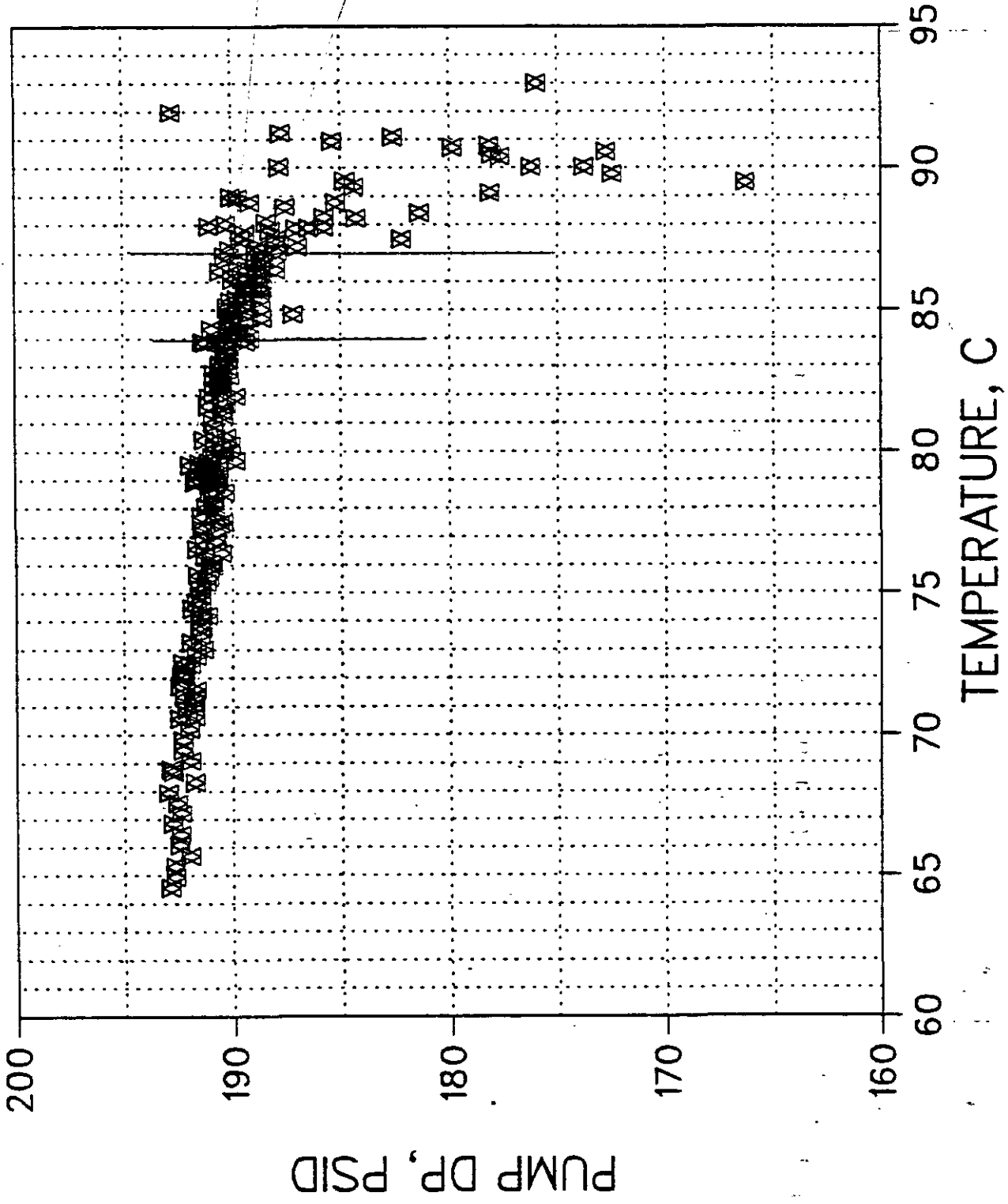
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PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 2



PUMP CAVITATION TESTS

UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 2



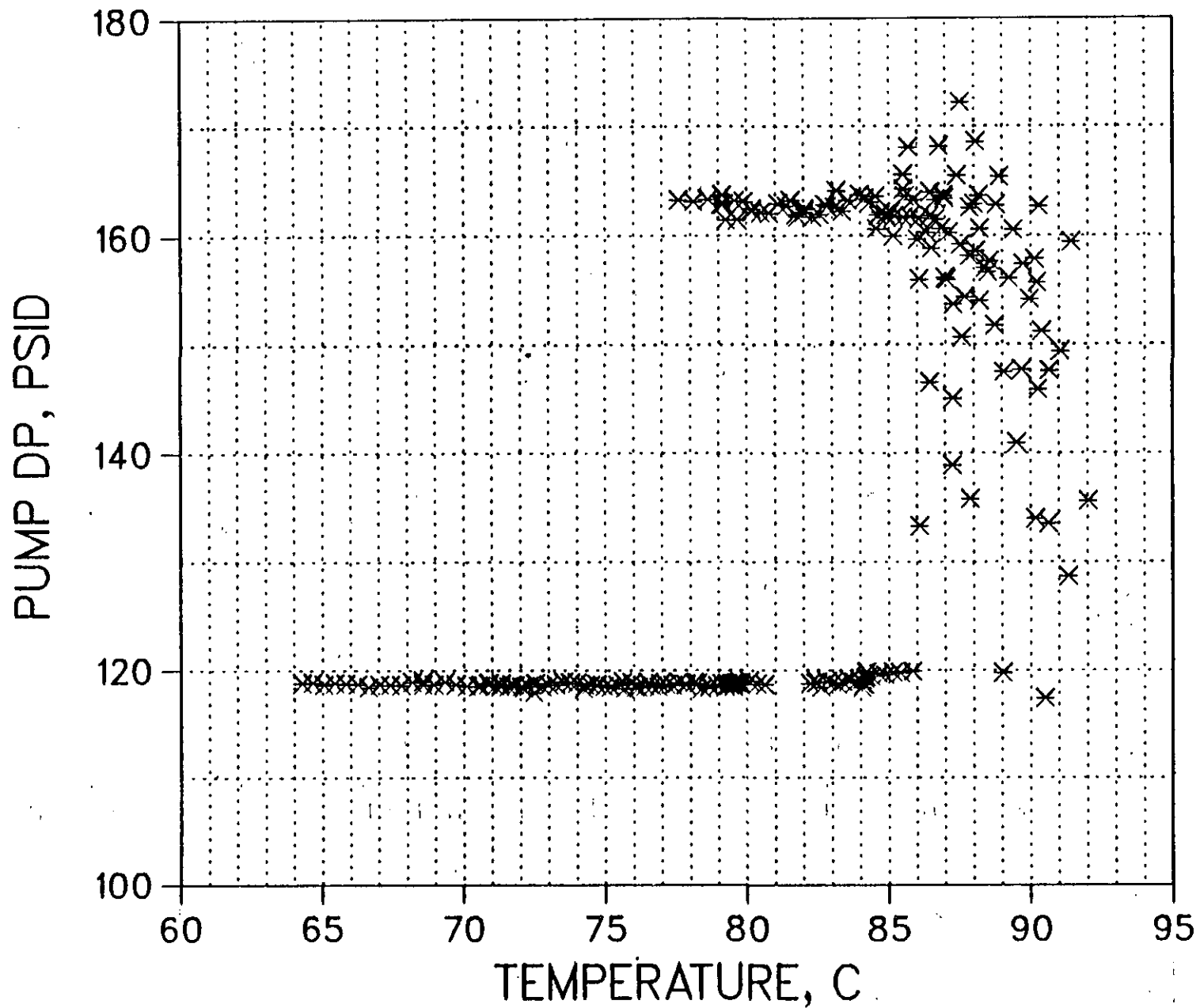
JAN 06 1984

18-04-04 BARBER TERRACE BOX 1000

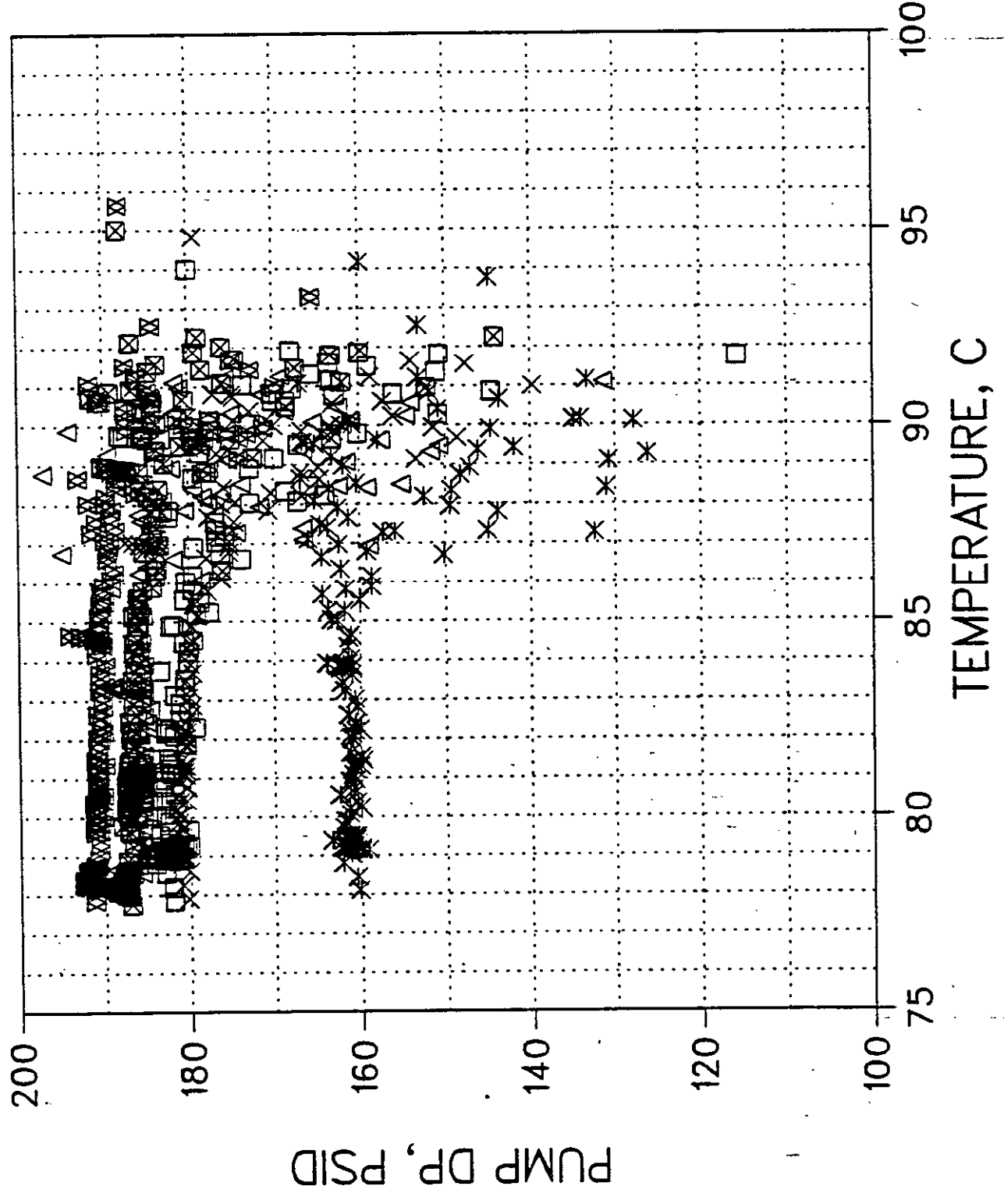
PUMP CAVITATION TESTS

UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 2

JAN. 06 1994

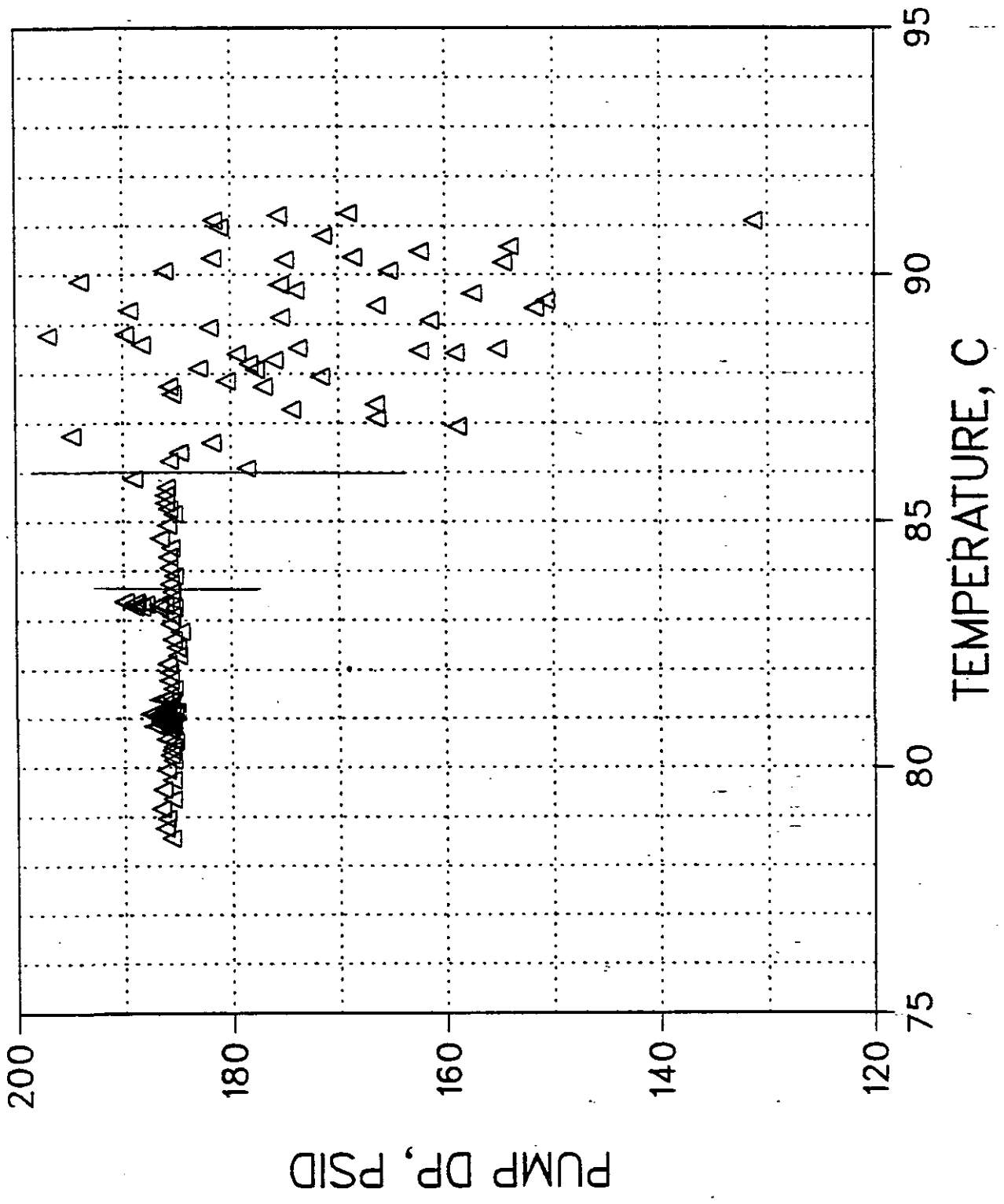


PUMP CAVITATION TESTS
UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 3

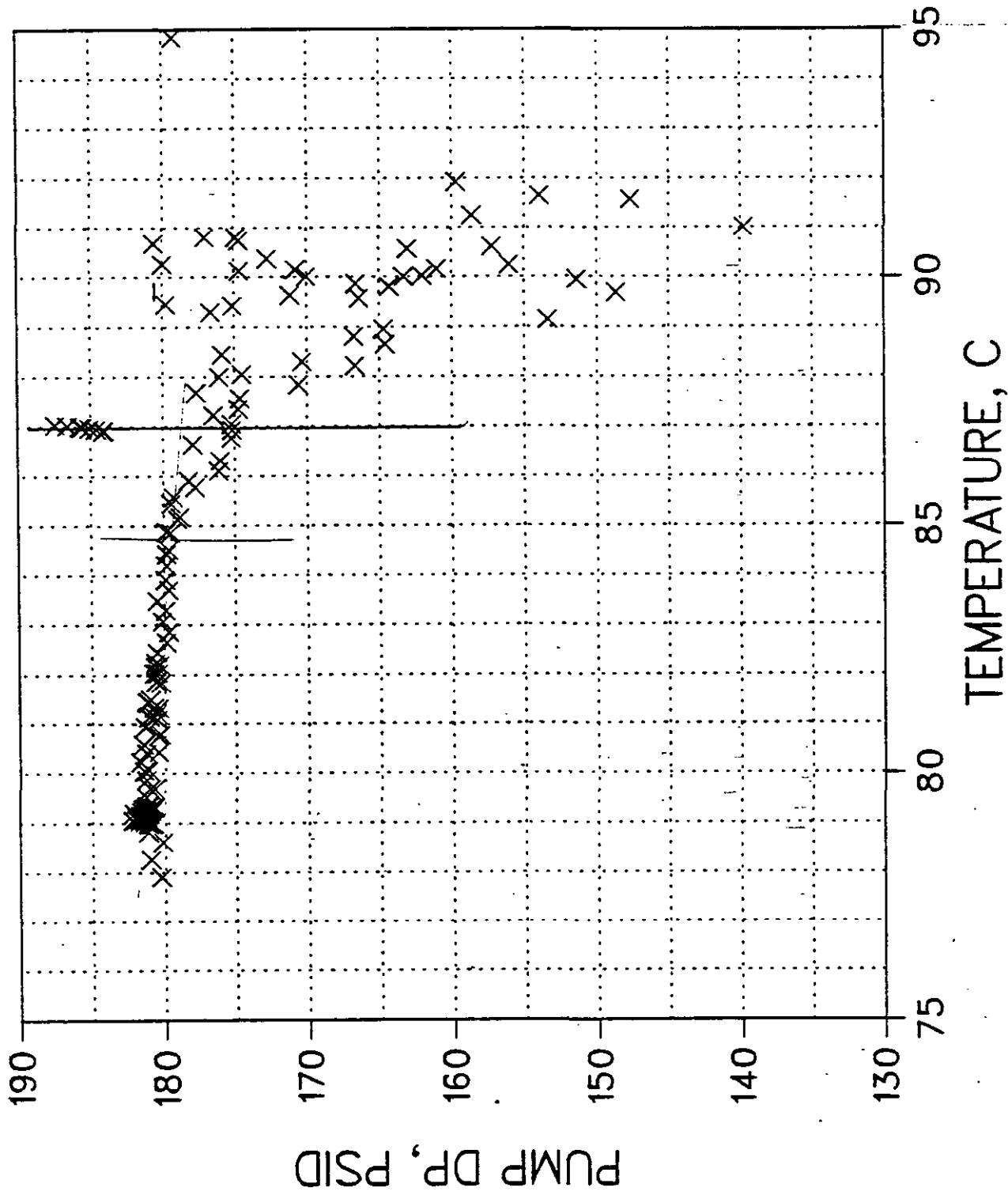


JAN. 06 1984

PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 3



PUMP CAVITATION TESTS
UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 3



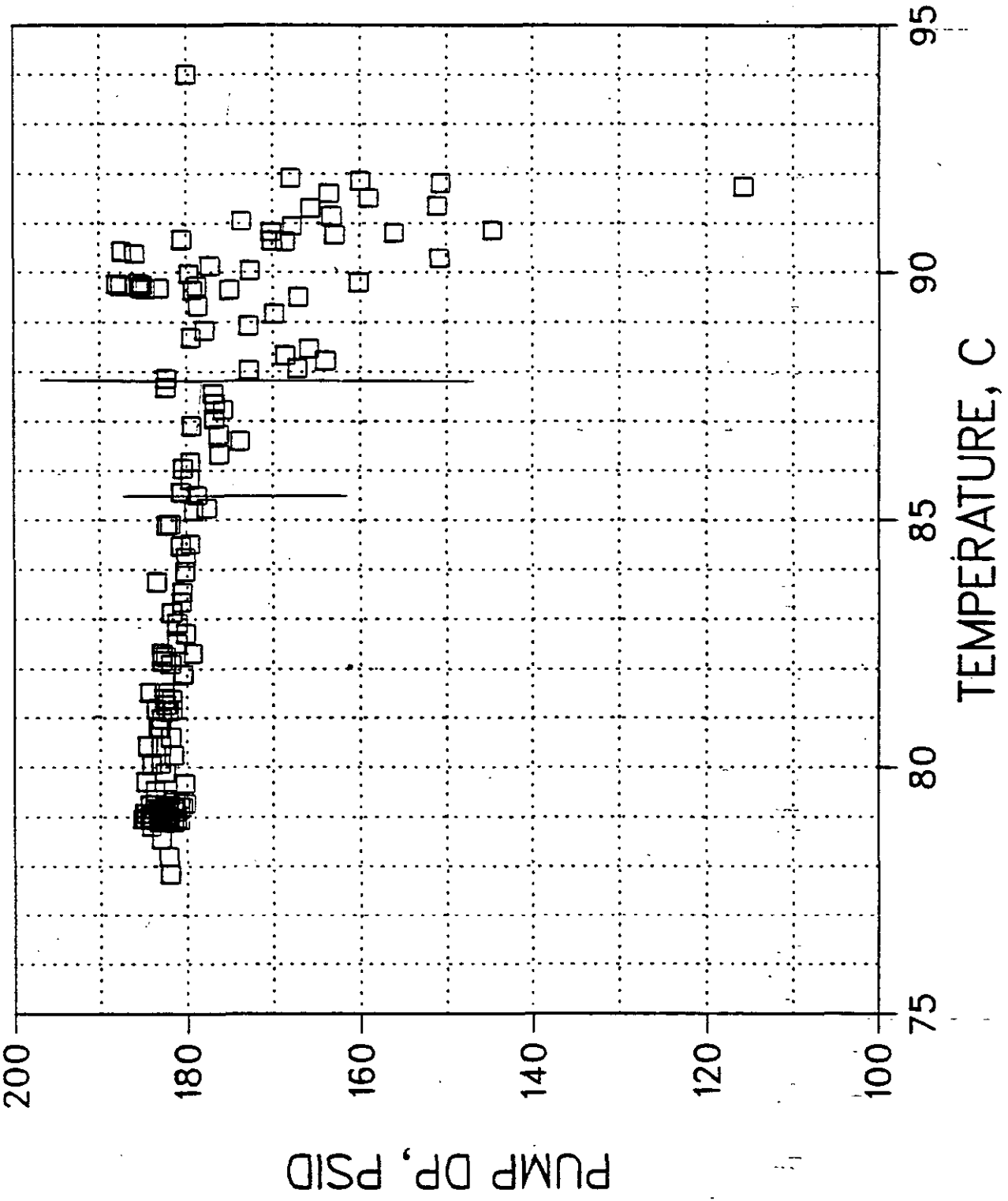
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NOV 05 1934

PUMP CAVITATION TESTS
UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 3

JAN 05 1991

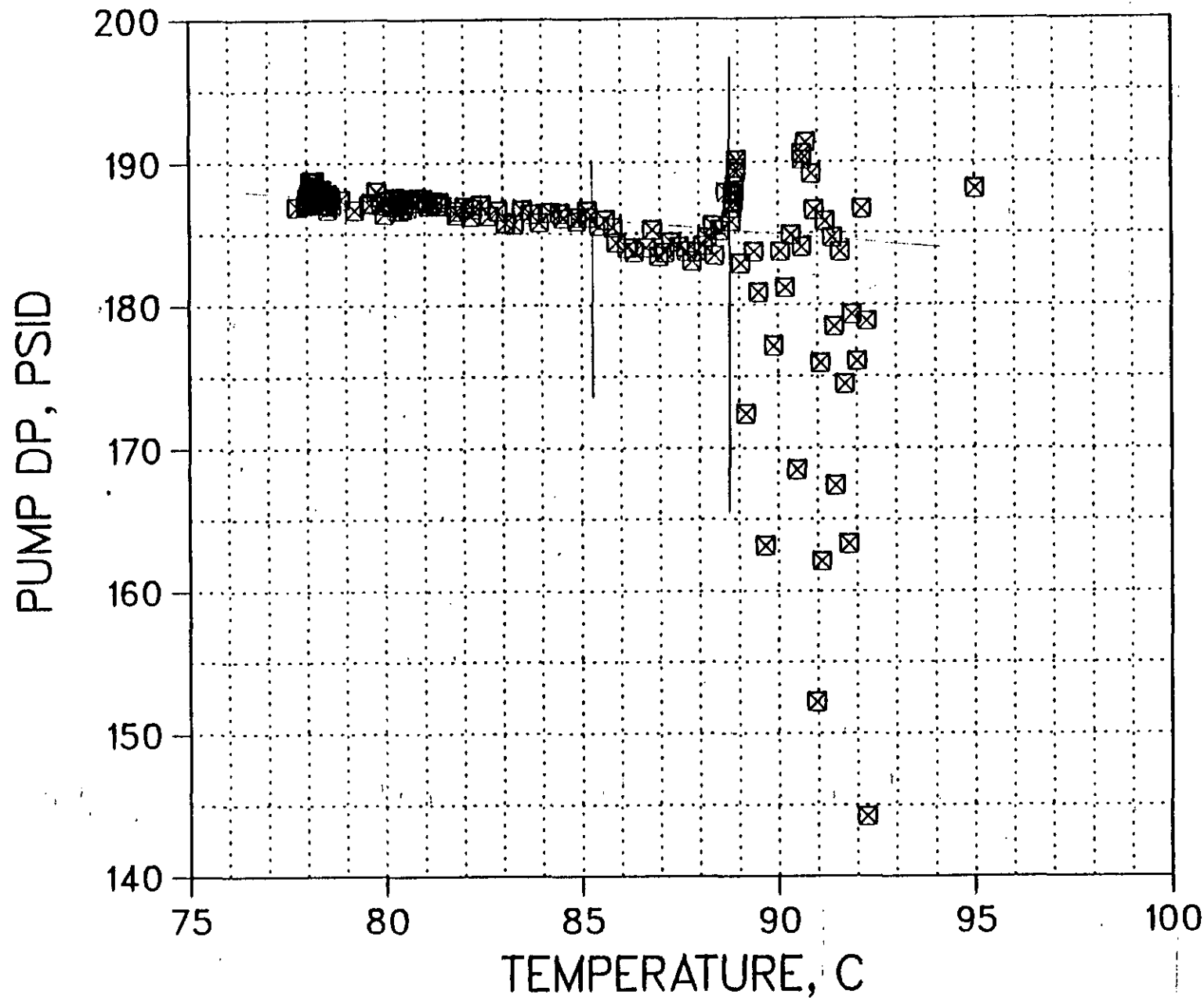
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PUMP CAVITATION TESTS

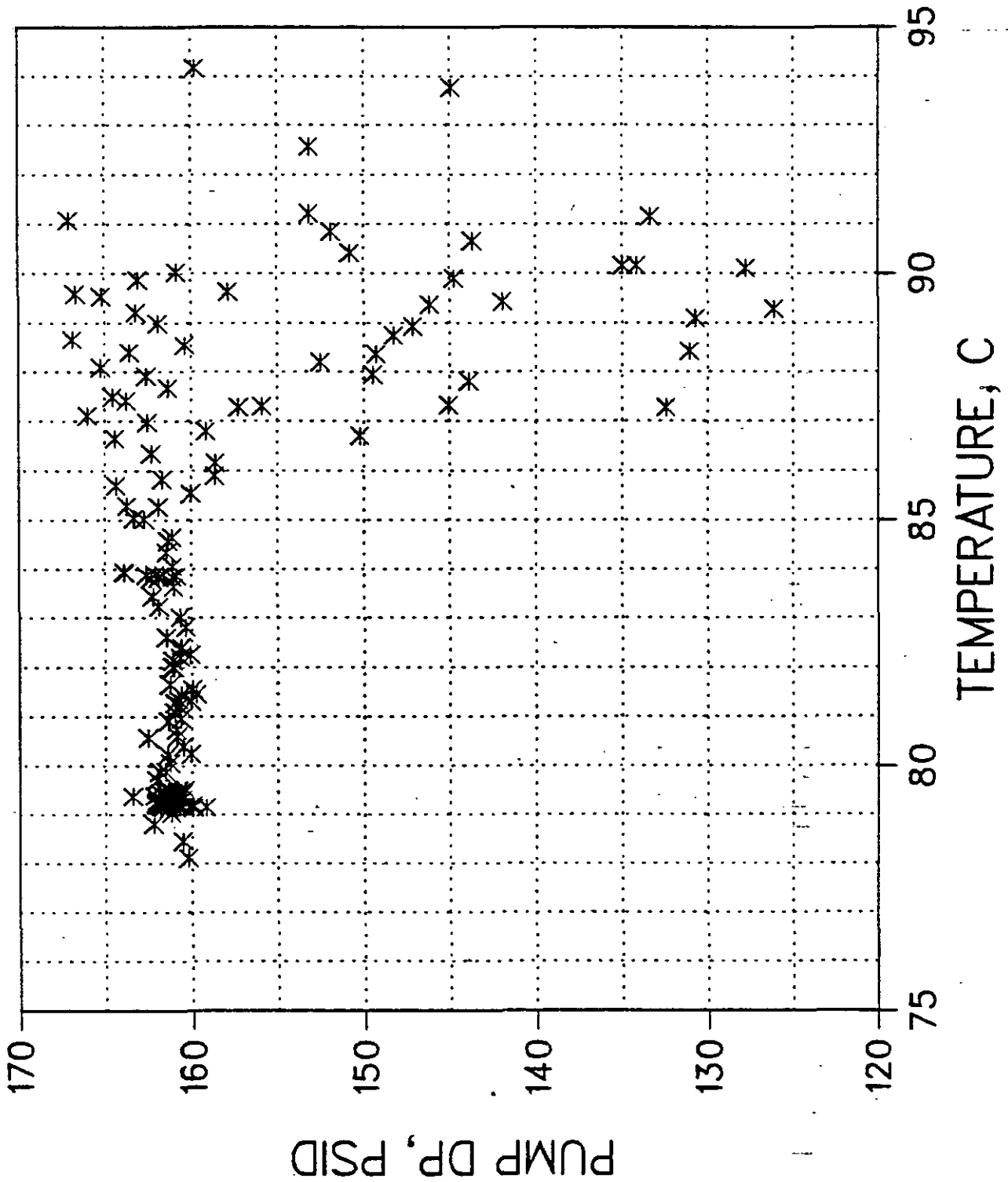
UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 3

JAN. 06 1984



JAN. 06 1961

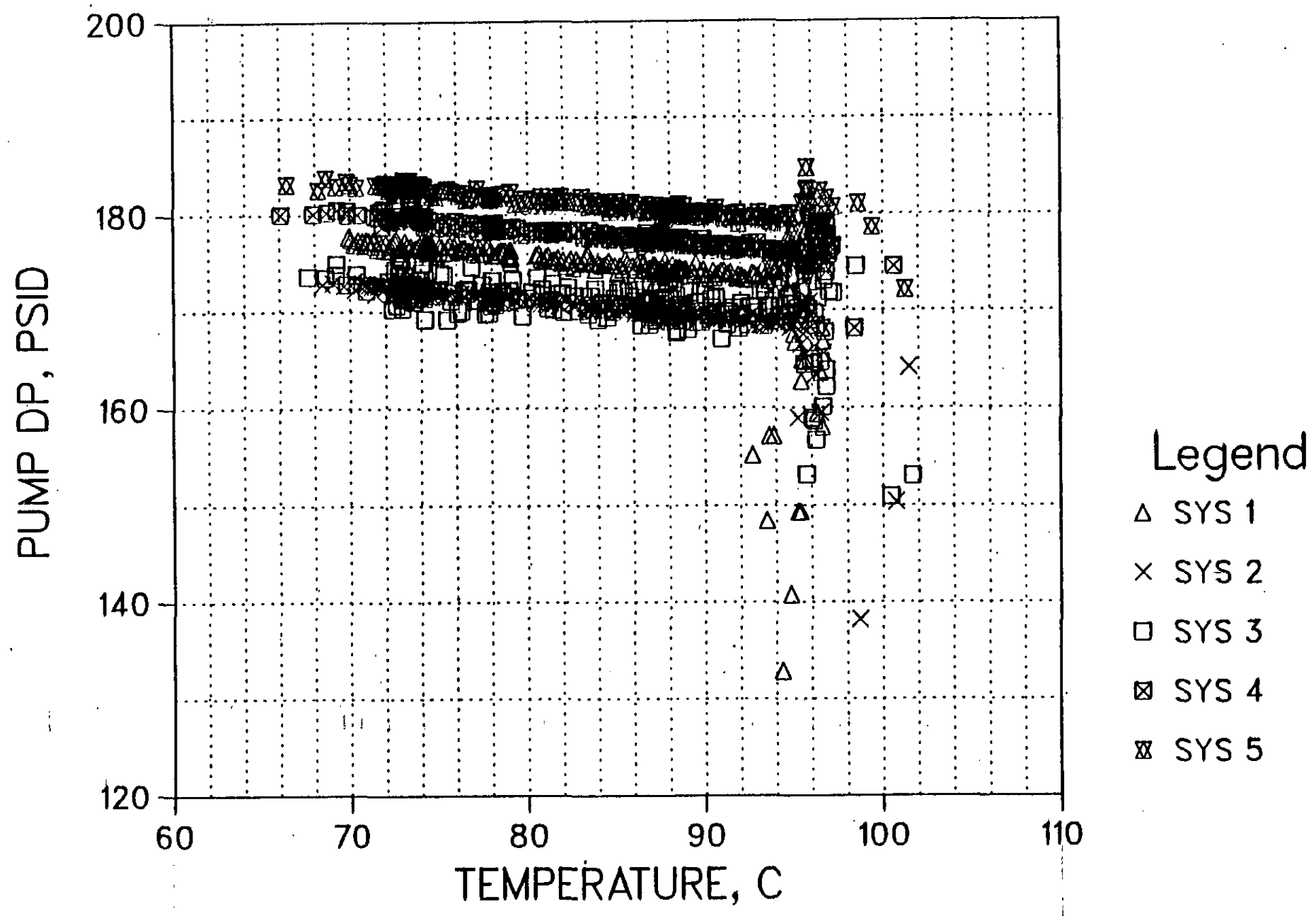
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 6 pumps, 3



JAN. 06 1981

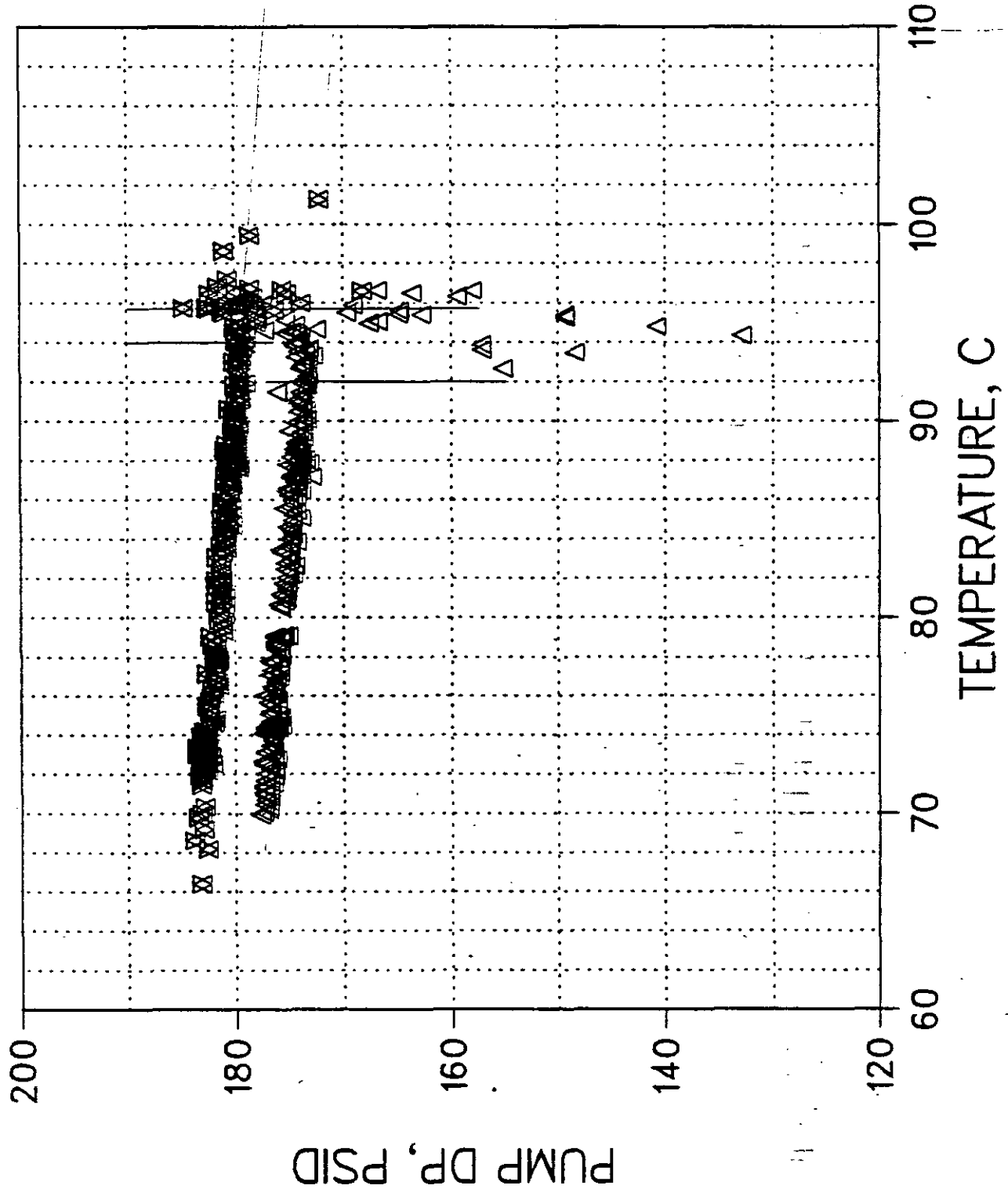
PUMP CAVITATION TESTS

UNADJUSTED TEMPERATURE VS PUMP DP 5 pumps



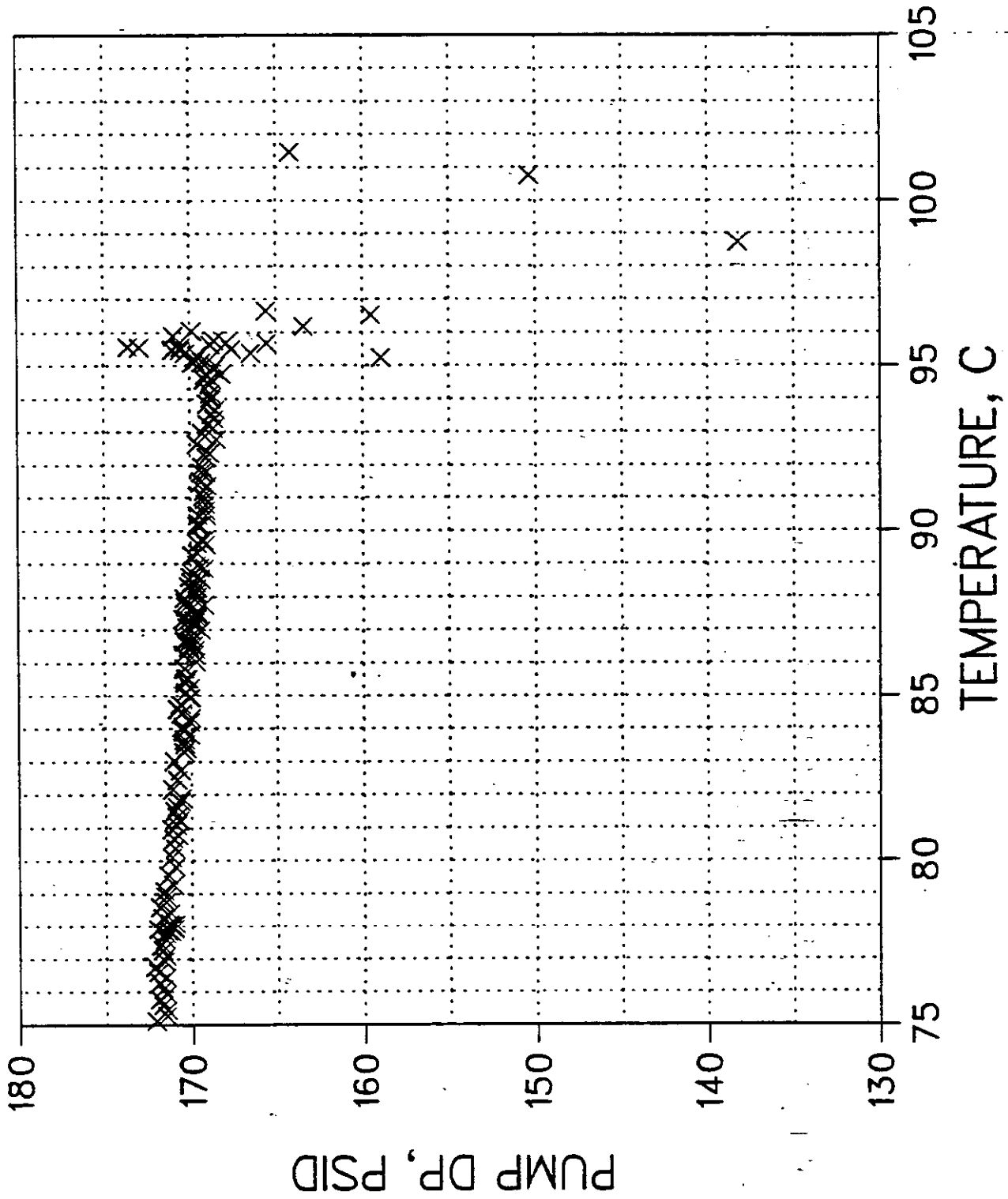
PUMP CAVITATION TESTS
UNADJUSTED TEMPERATURE VS PUMP DP 5 pumps

JAN. 06 1984

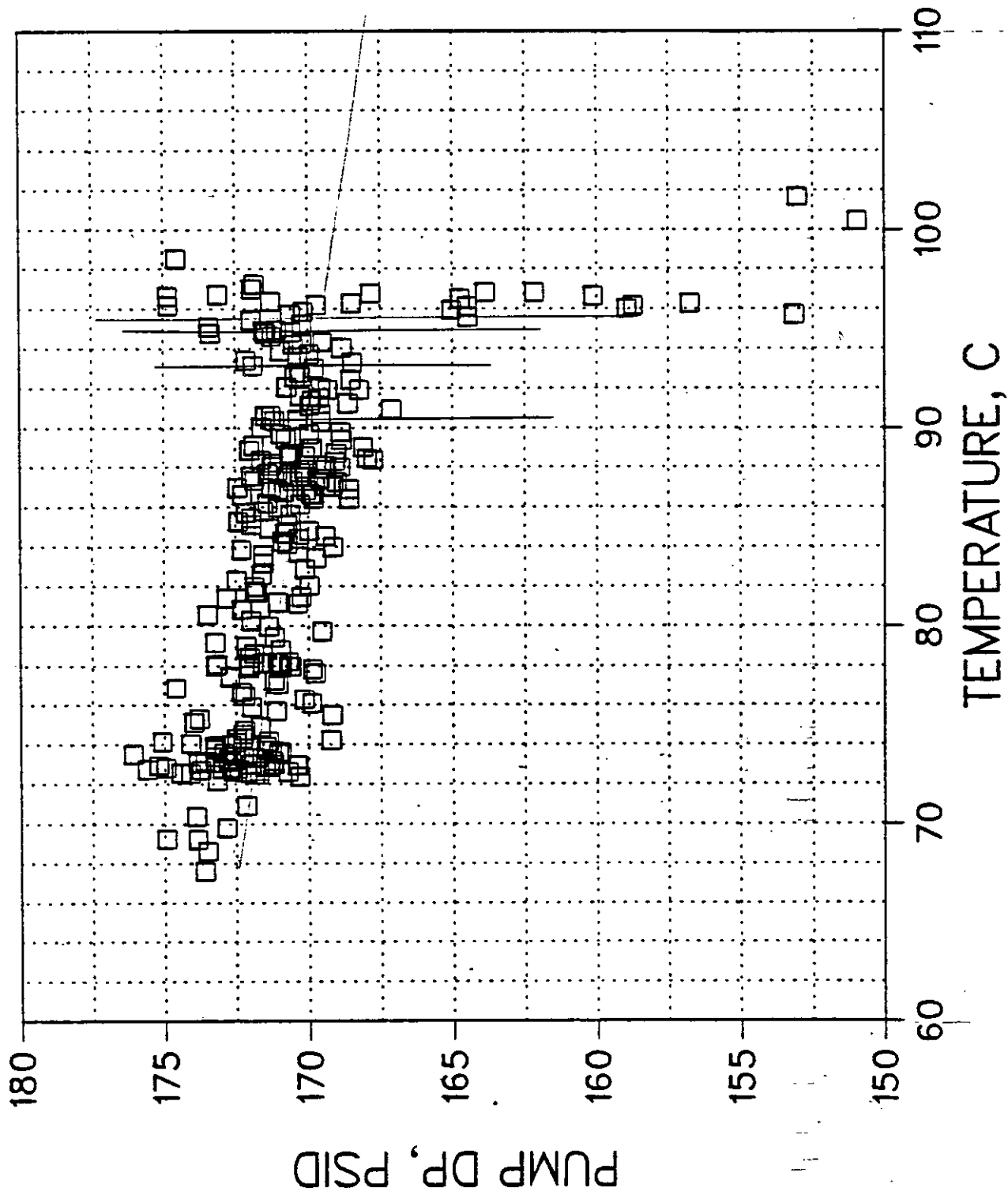


Legend
△ SYS 1
⊗ SYS 5

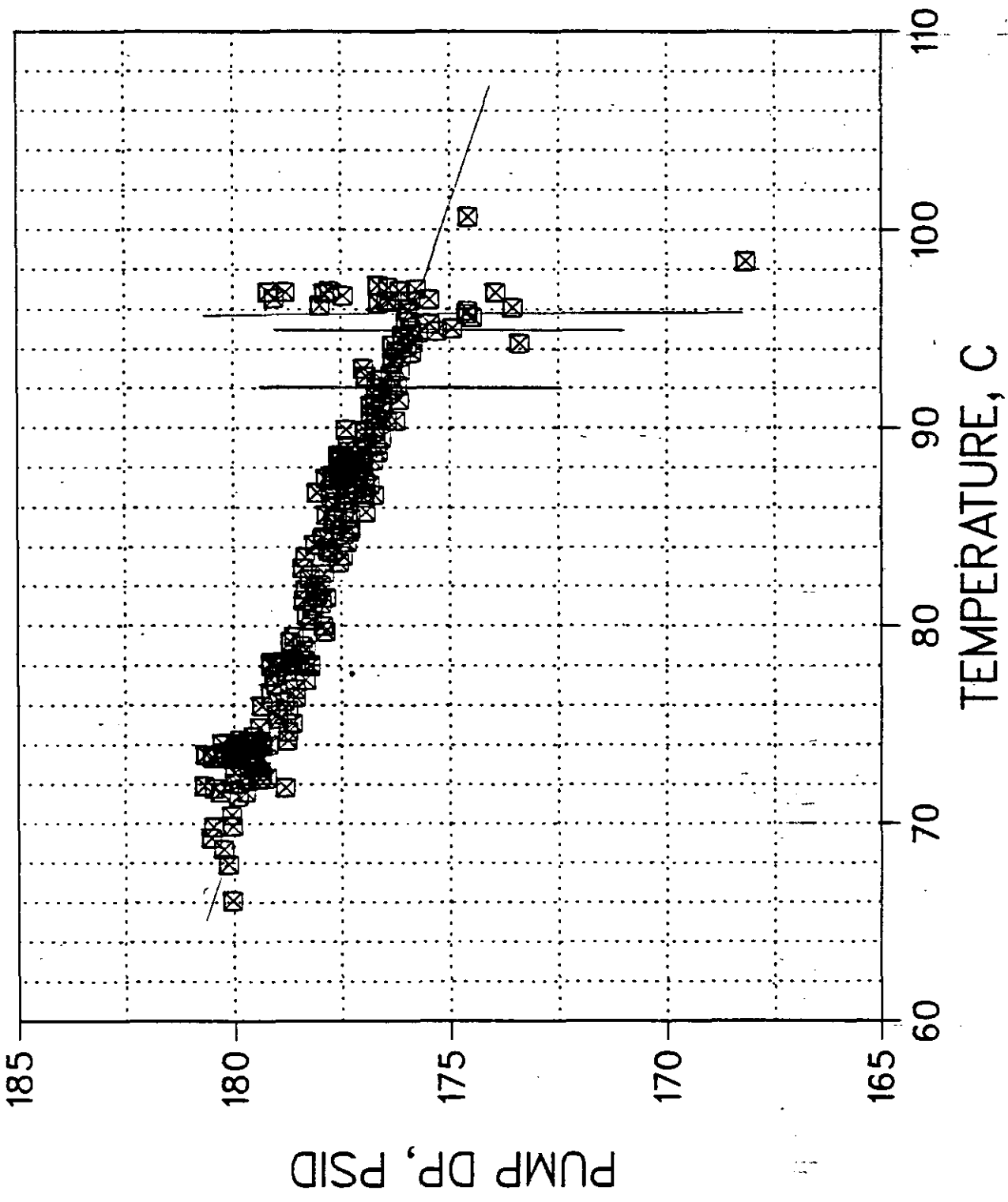
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 5 pumps



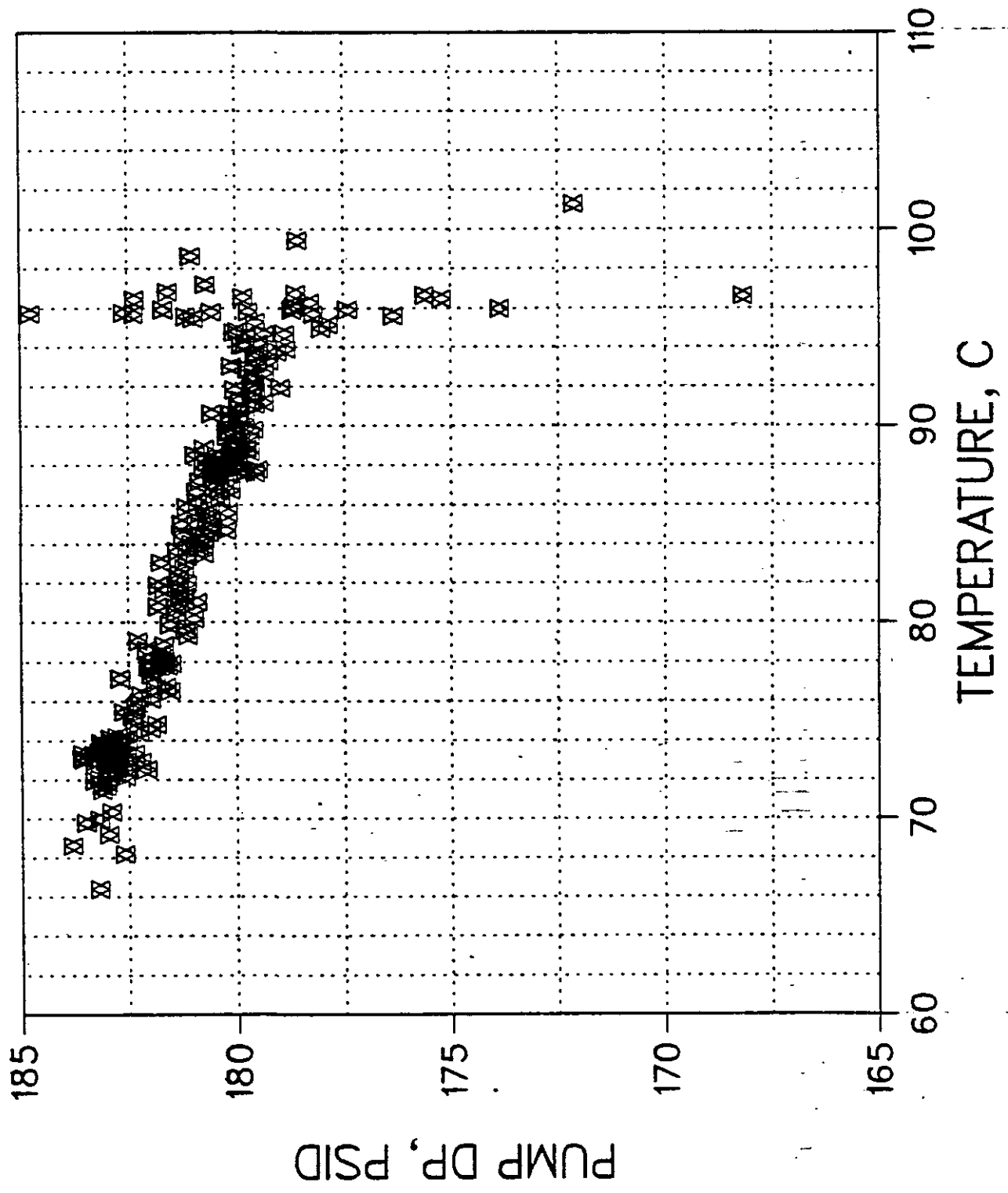
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 5 pumps



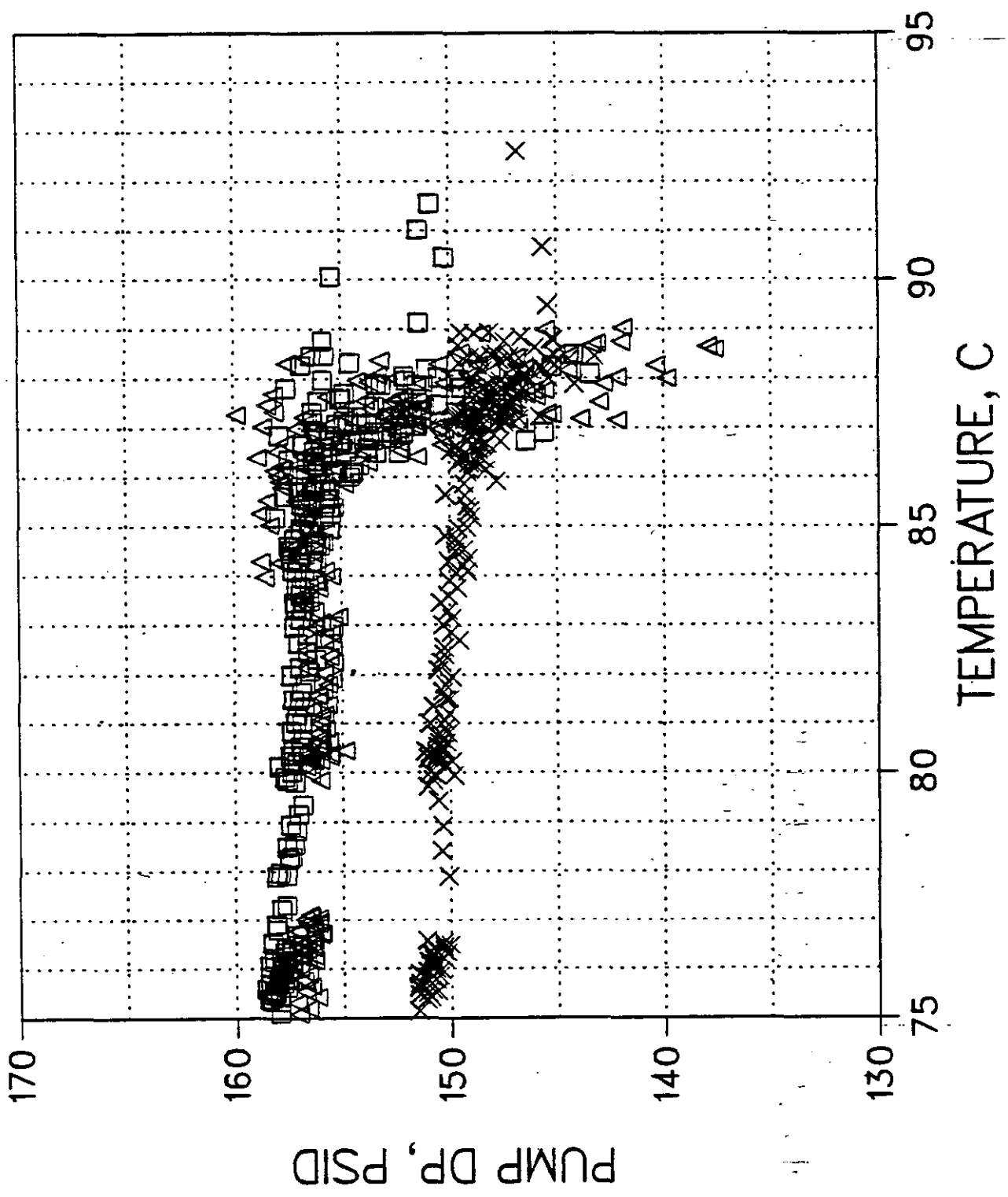
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 5 pumps



PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 5 pumps



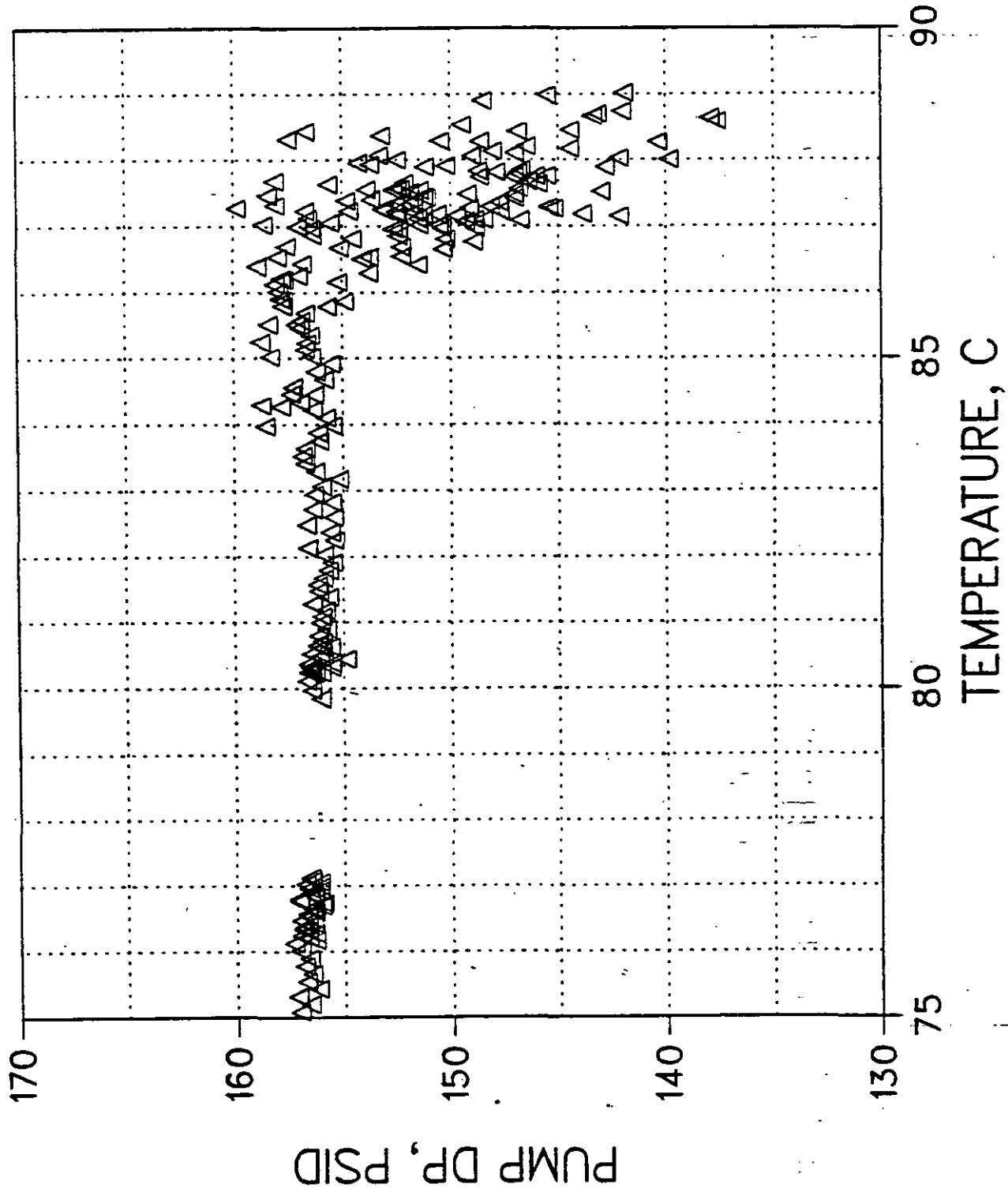
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 3 pumps



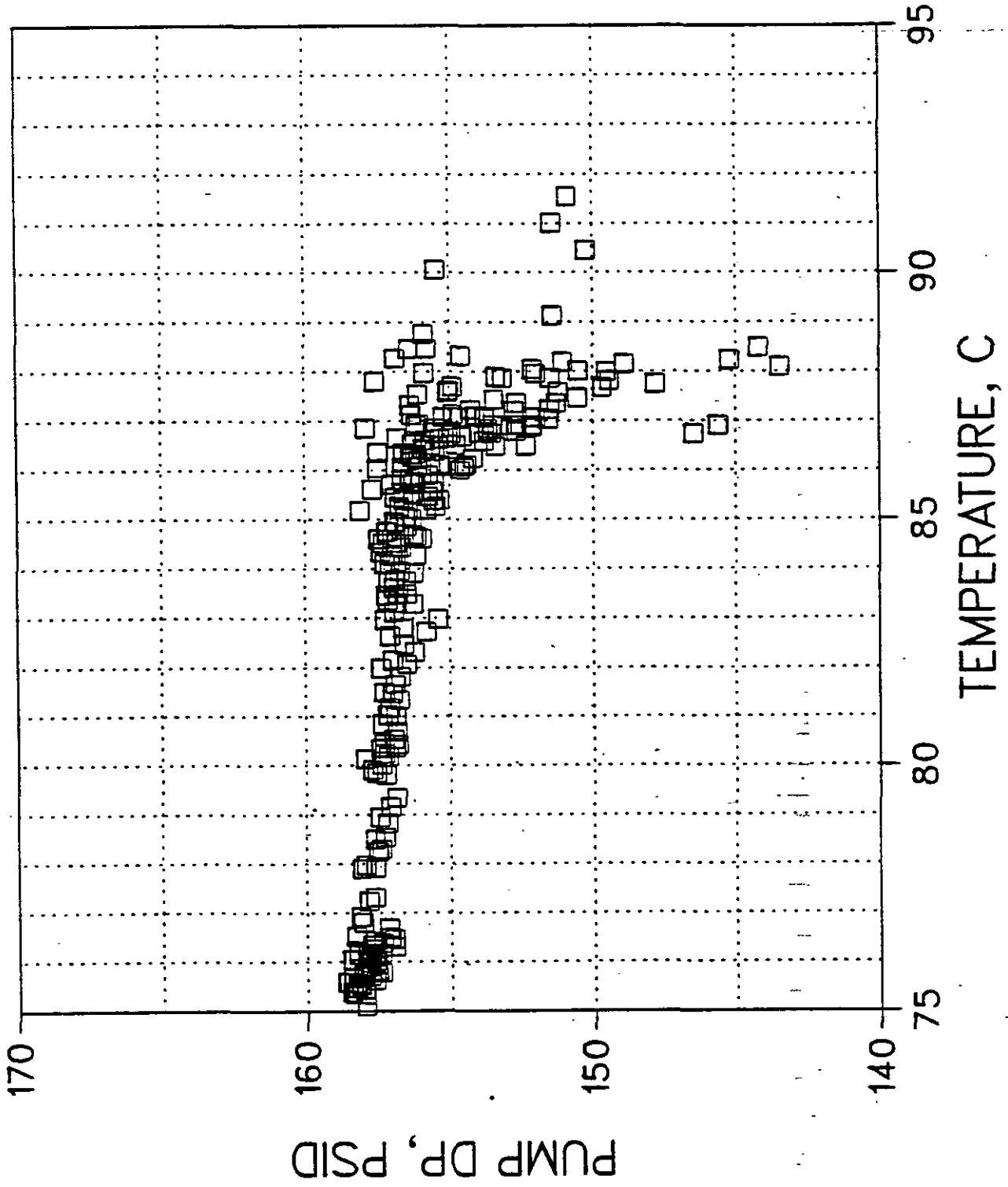
Legend

- △ SYS 1
- × SYS 2
- SYS 5

PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP 3 pumps



PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS PUMP DP. 3 pumps



A) Data Curves

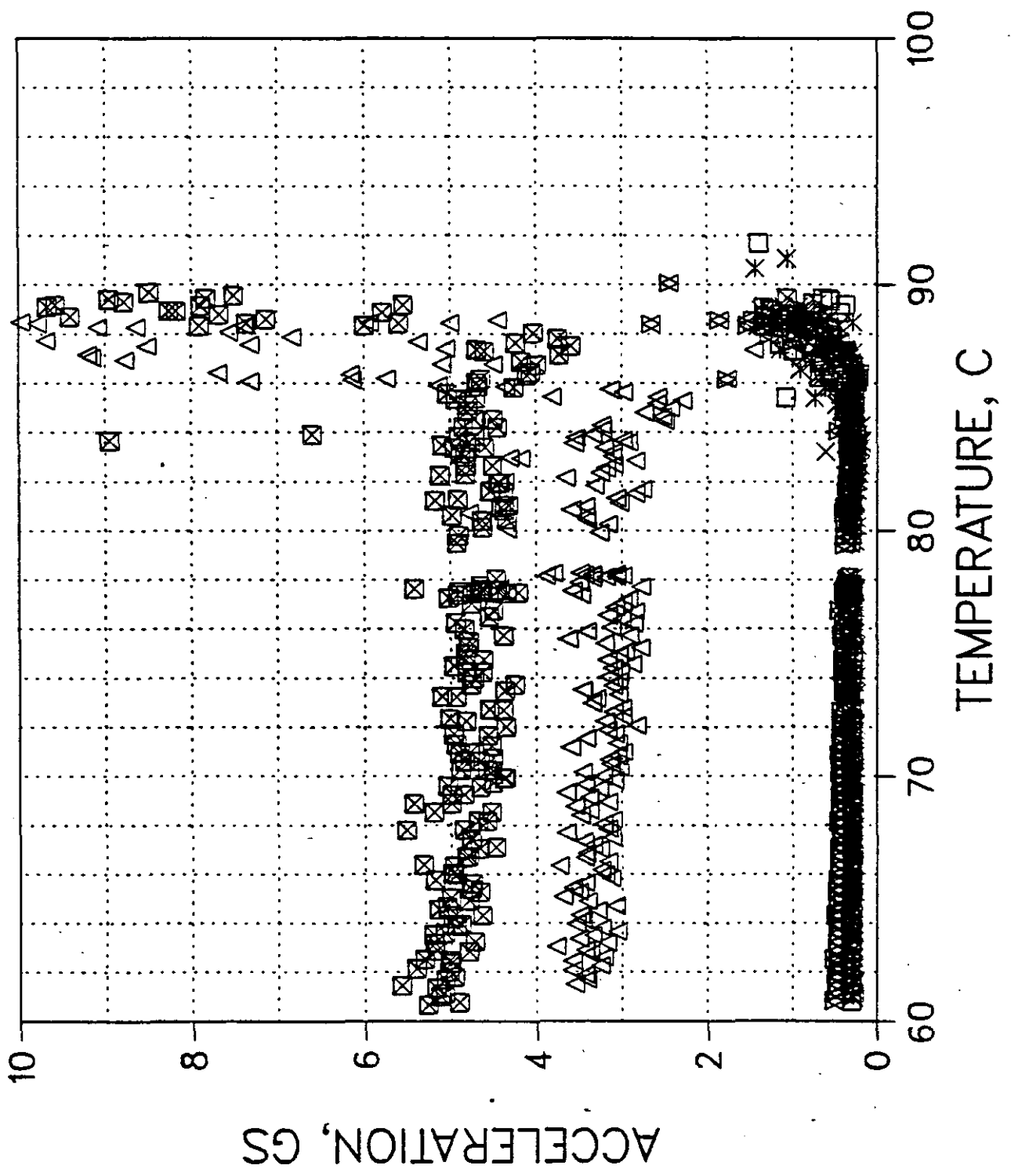
2) Acceleration vs. Temperature

The pump casing acceleration is plotted against the associated RTD temperature. Note that in the middle of the (number 3) 6 pump test these signals were lost due to a filter failure.

See notes at Appendix A-1.

PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 1

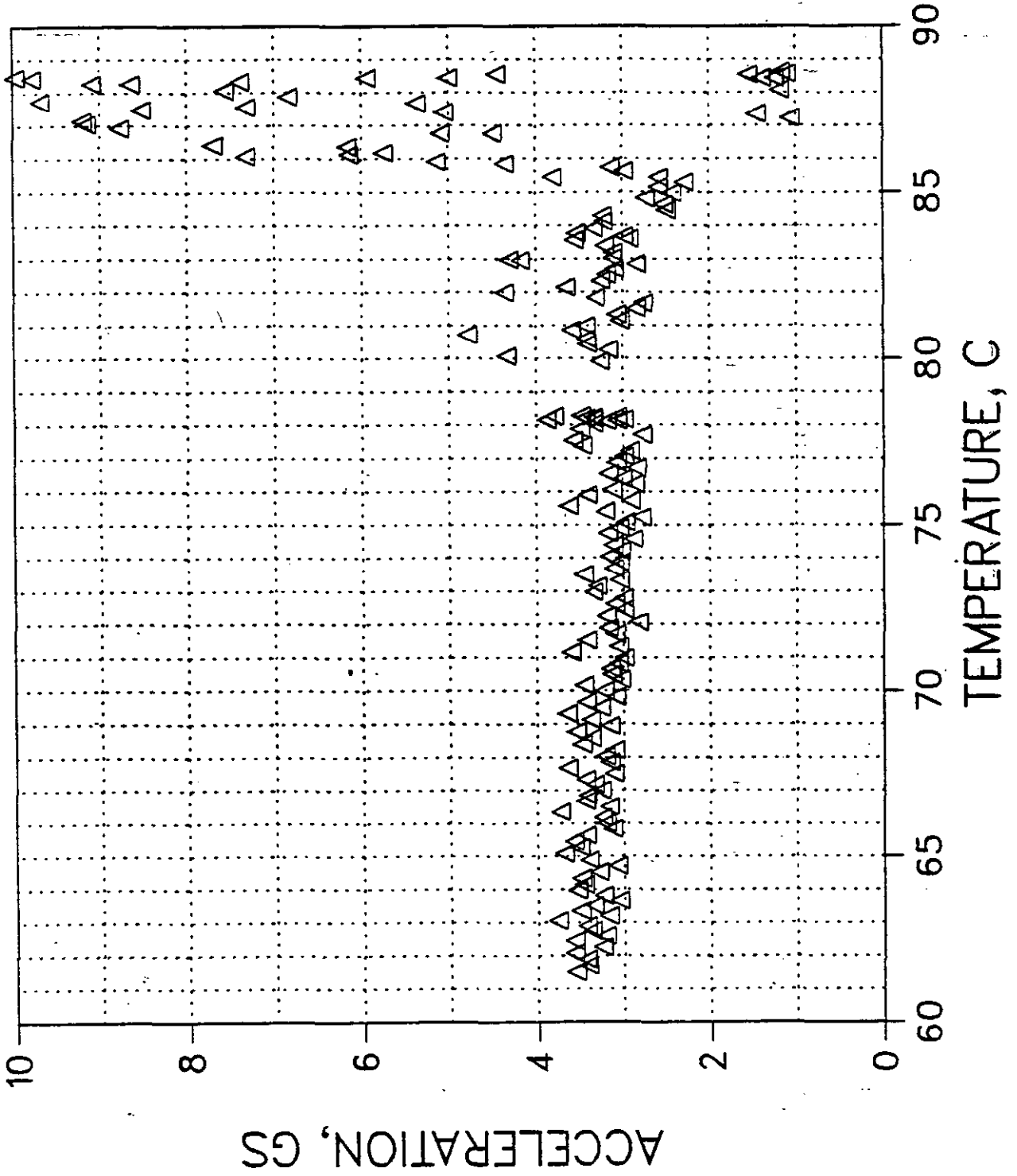


Legend

- △ SYS 1
- × SYS 2
- SYS 3
- ⊠ SYS 4
- ⊞ SYS 5
- * SYS 6

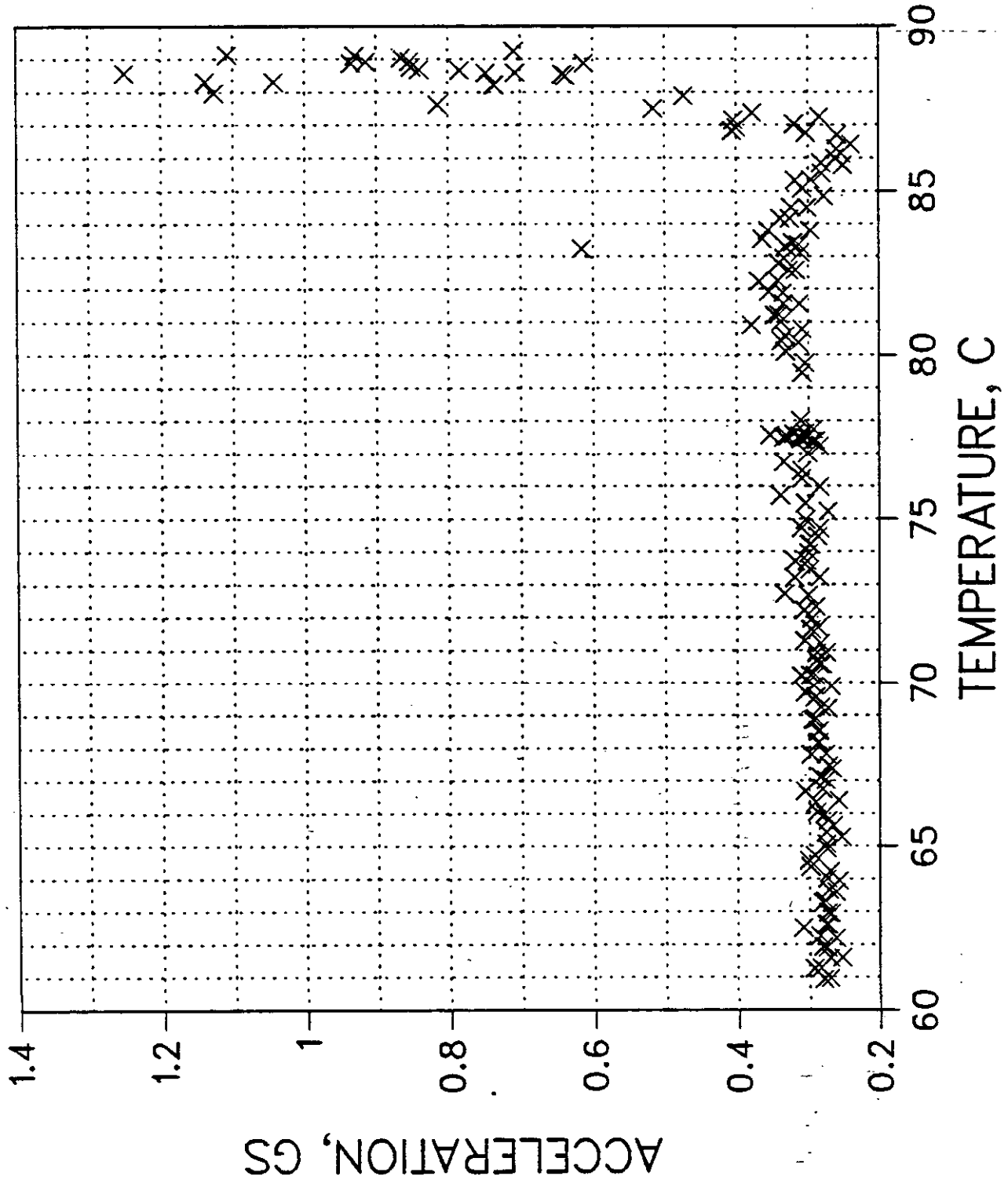
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 1



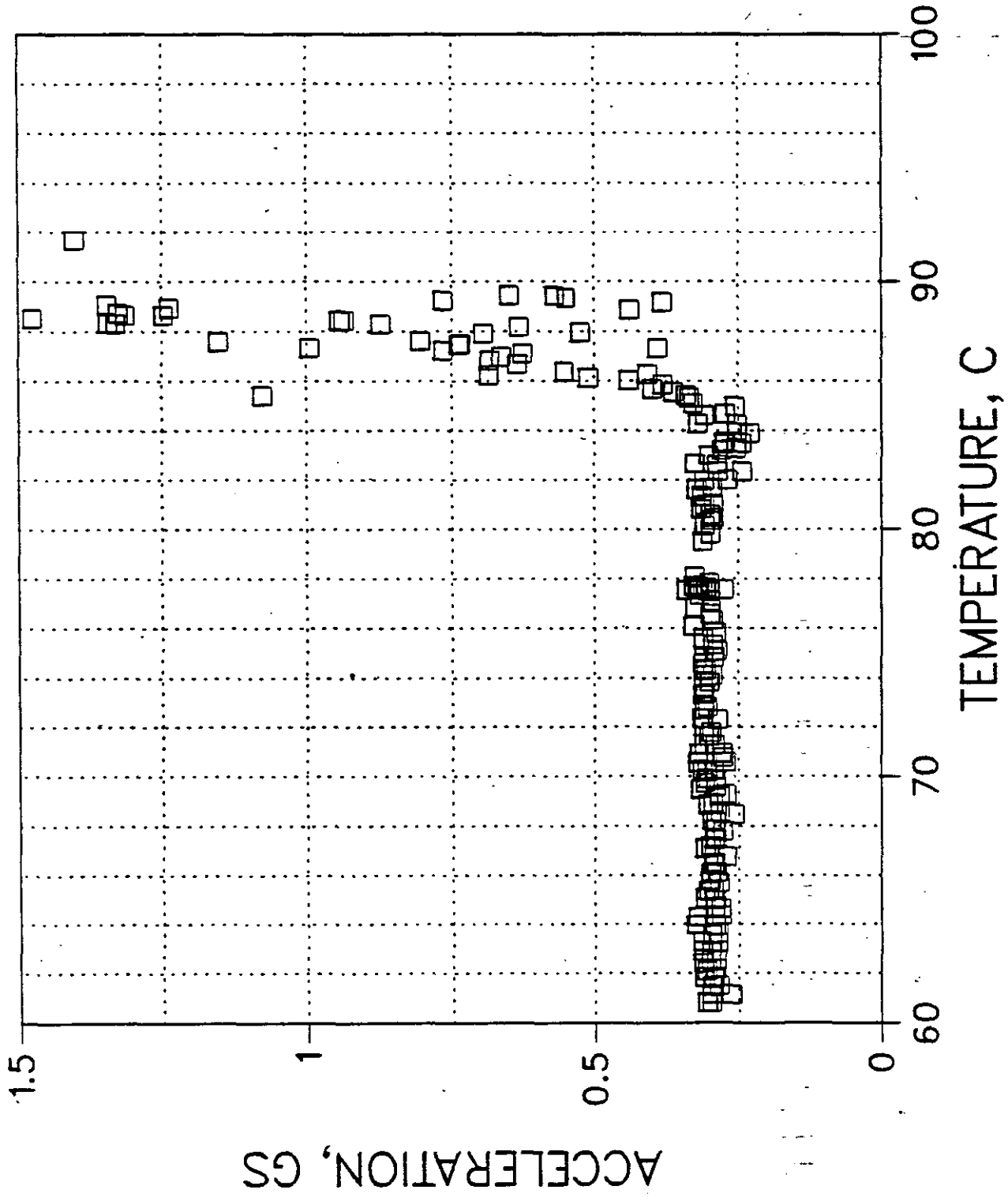
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 1



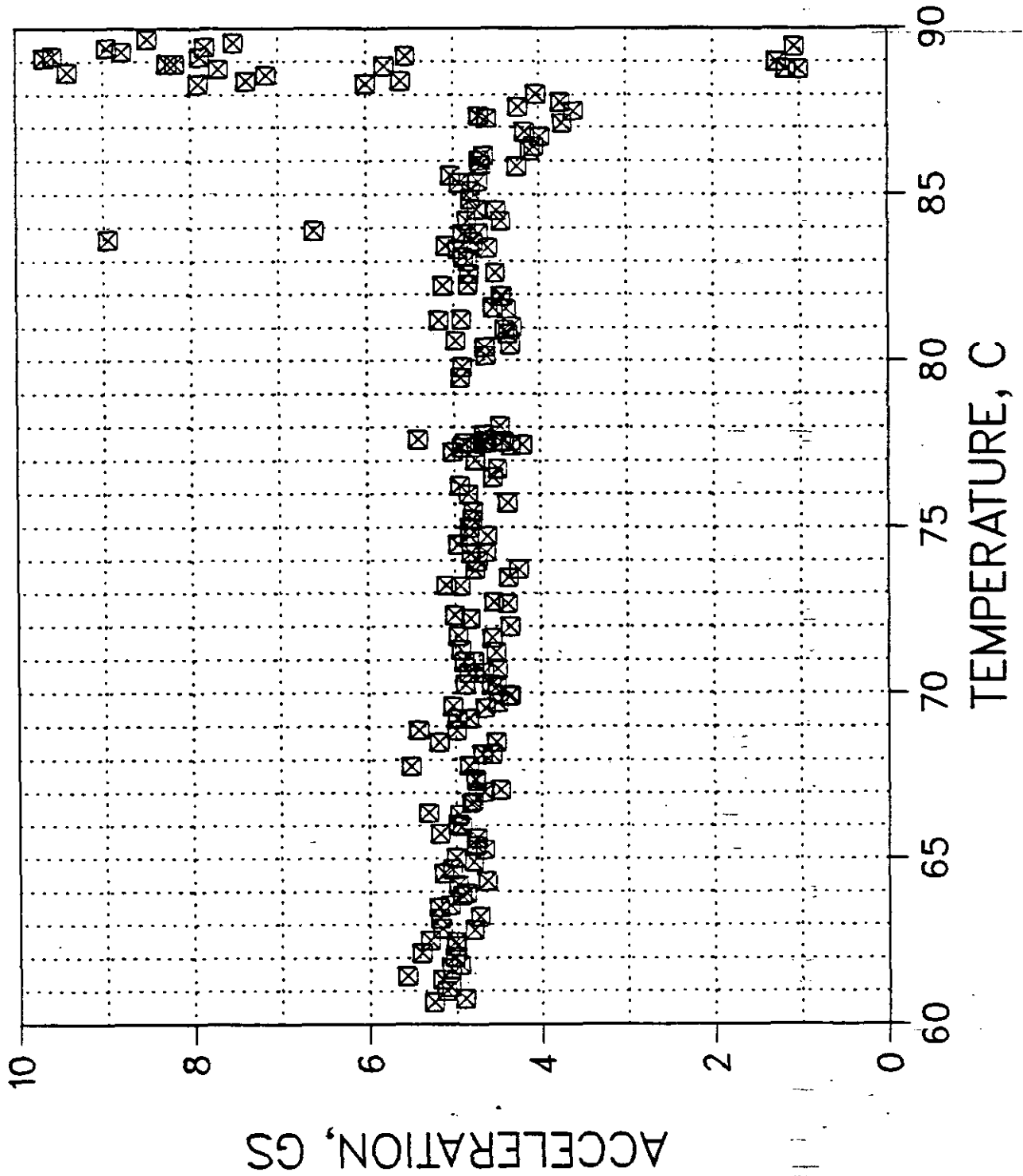
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 1

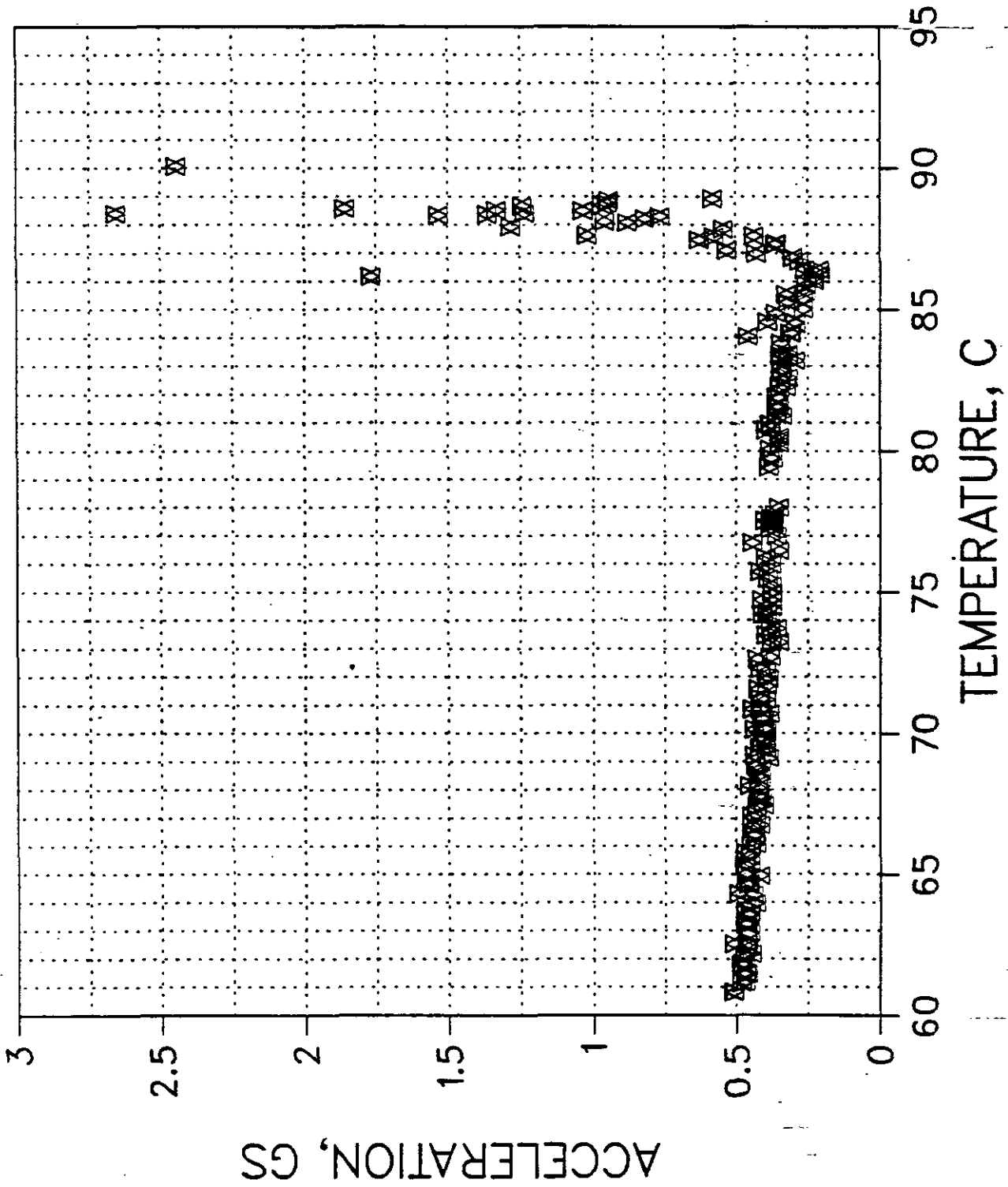


PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 1

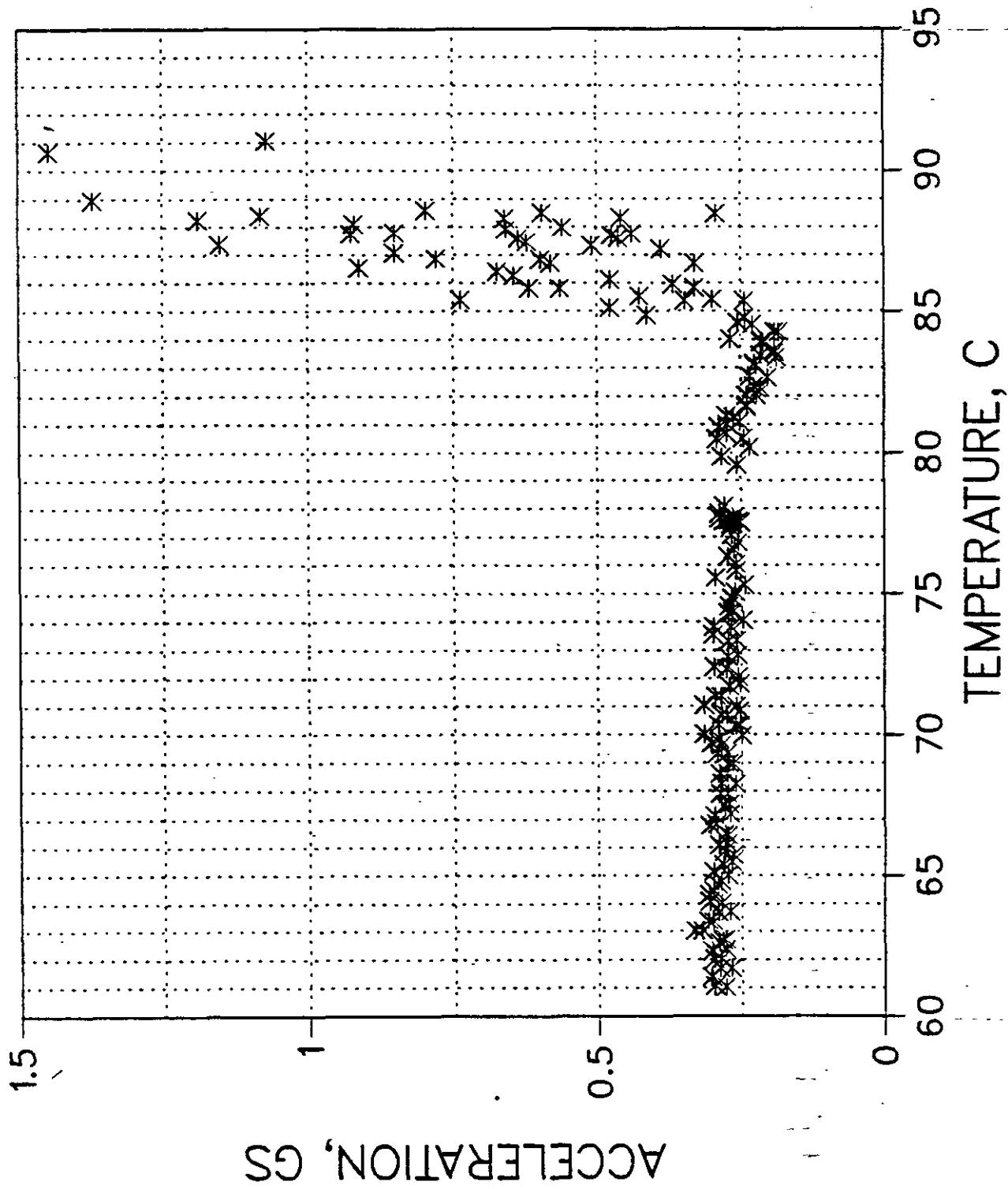


PUMP CAVITATION TESTS
UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 1



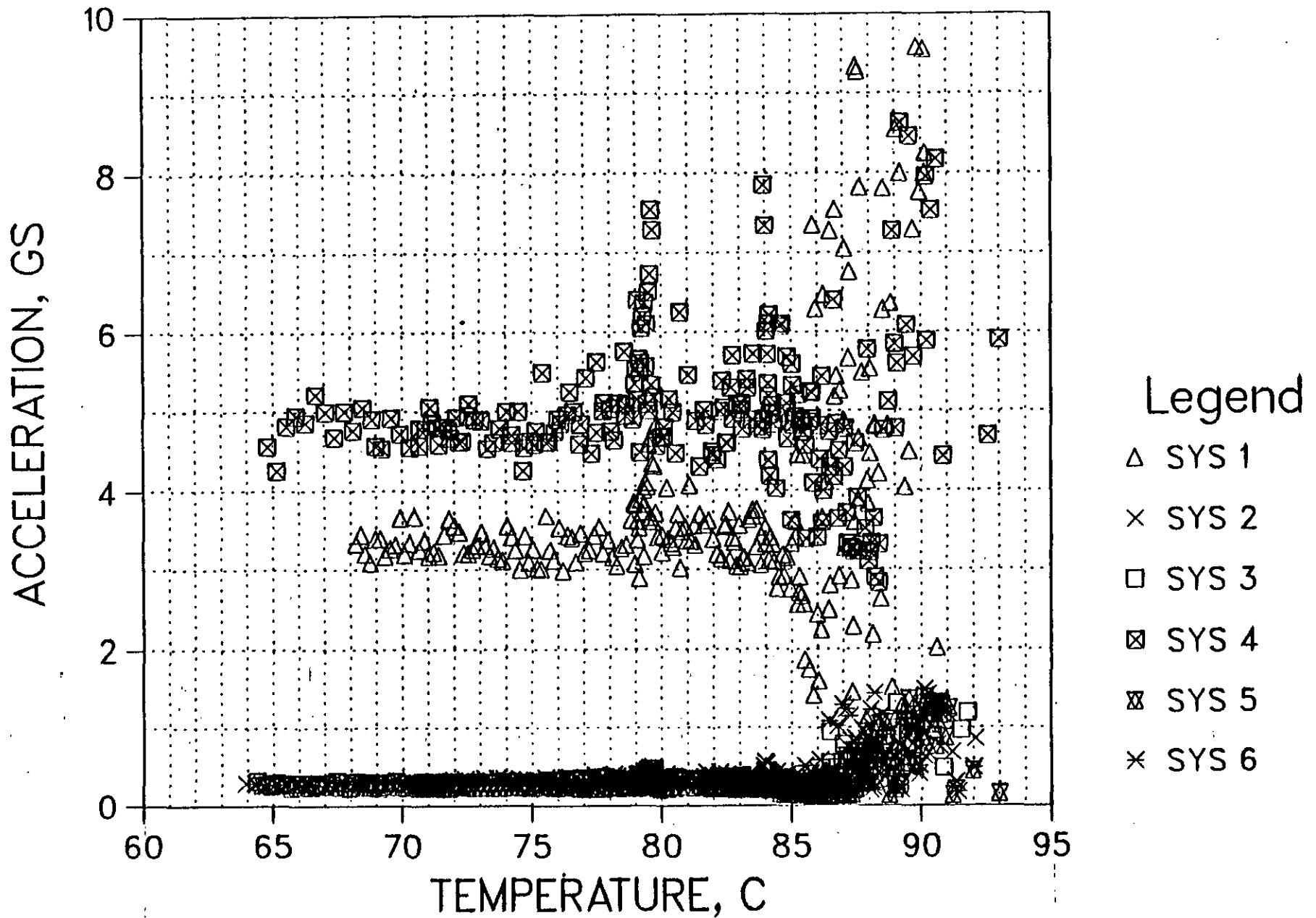
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 1



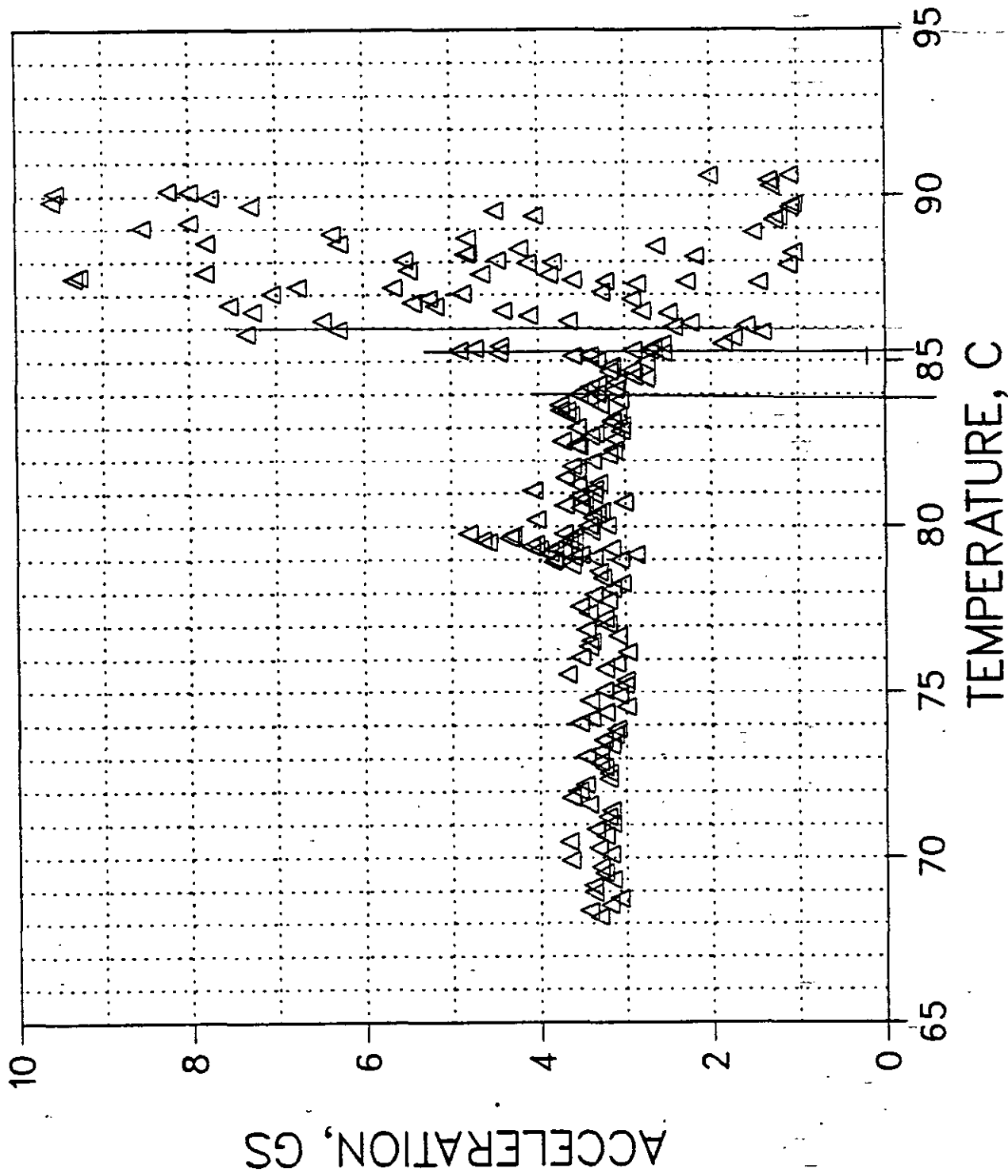
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 2



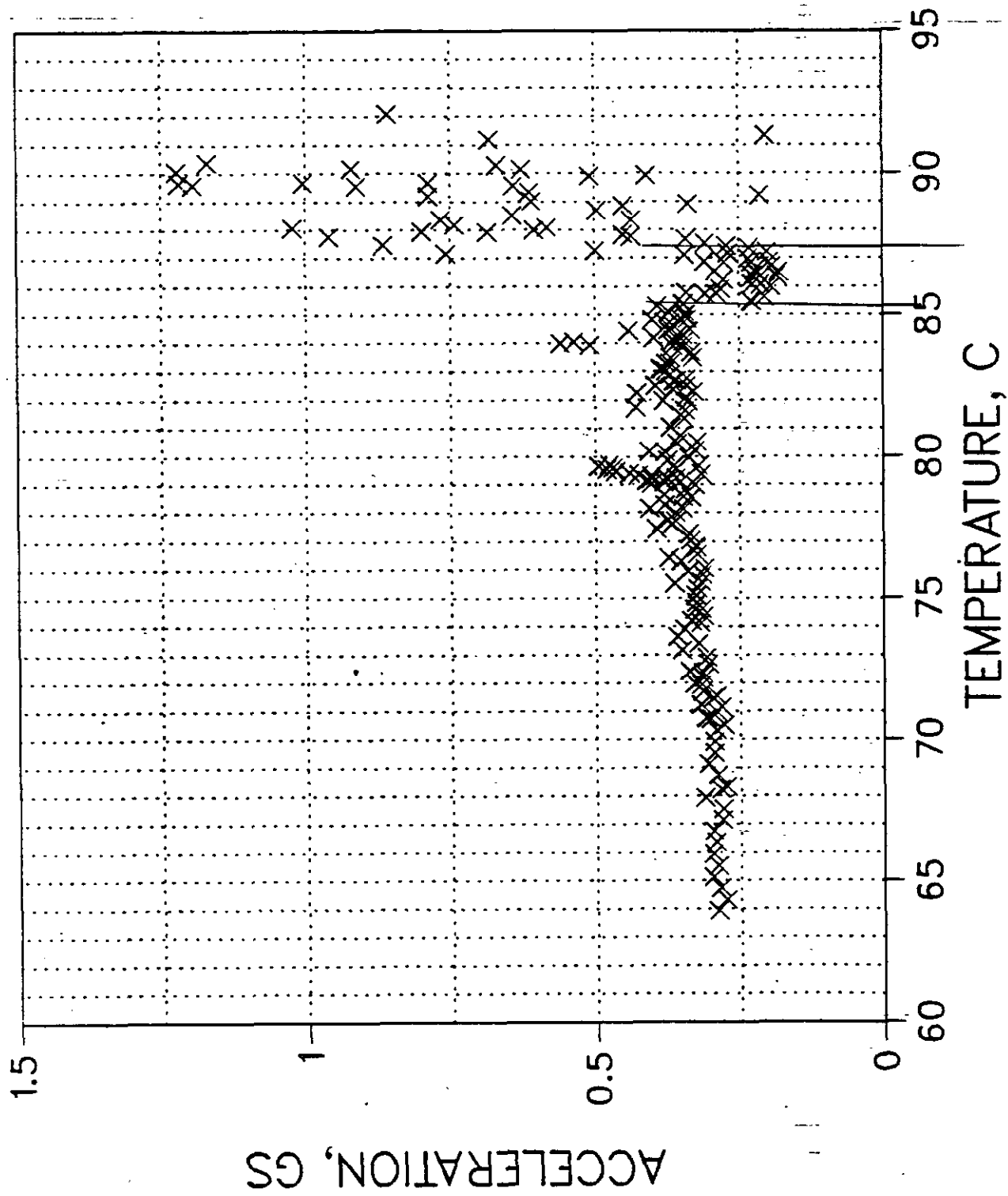
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 2



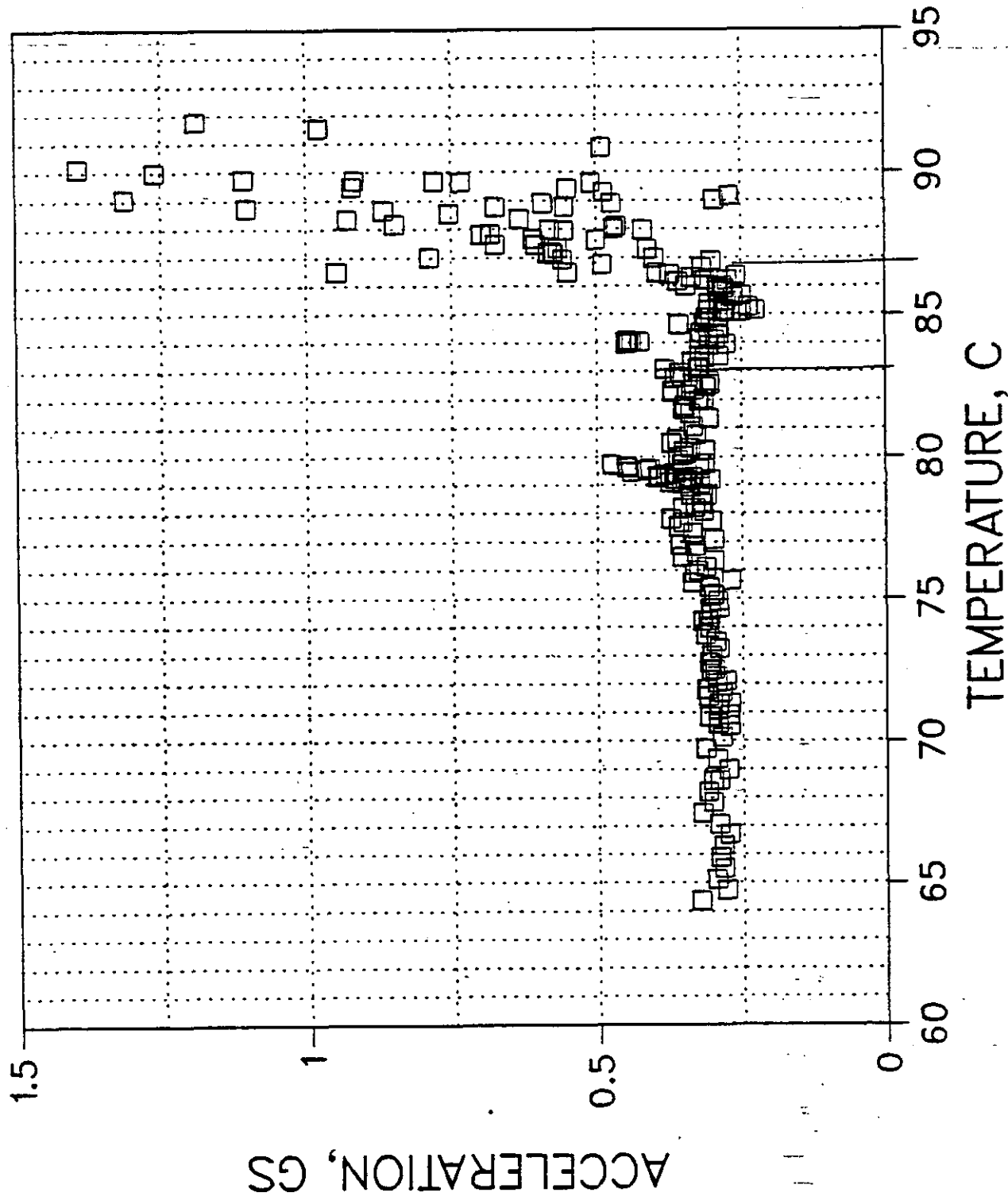
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 2



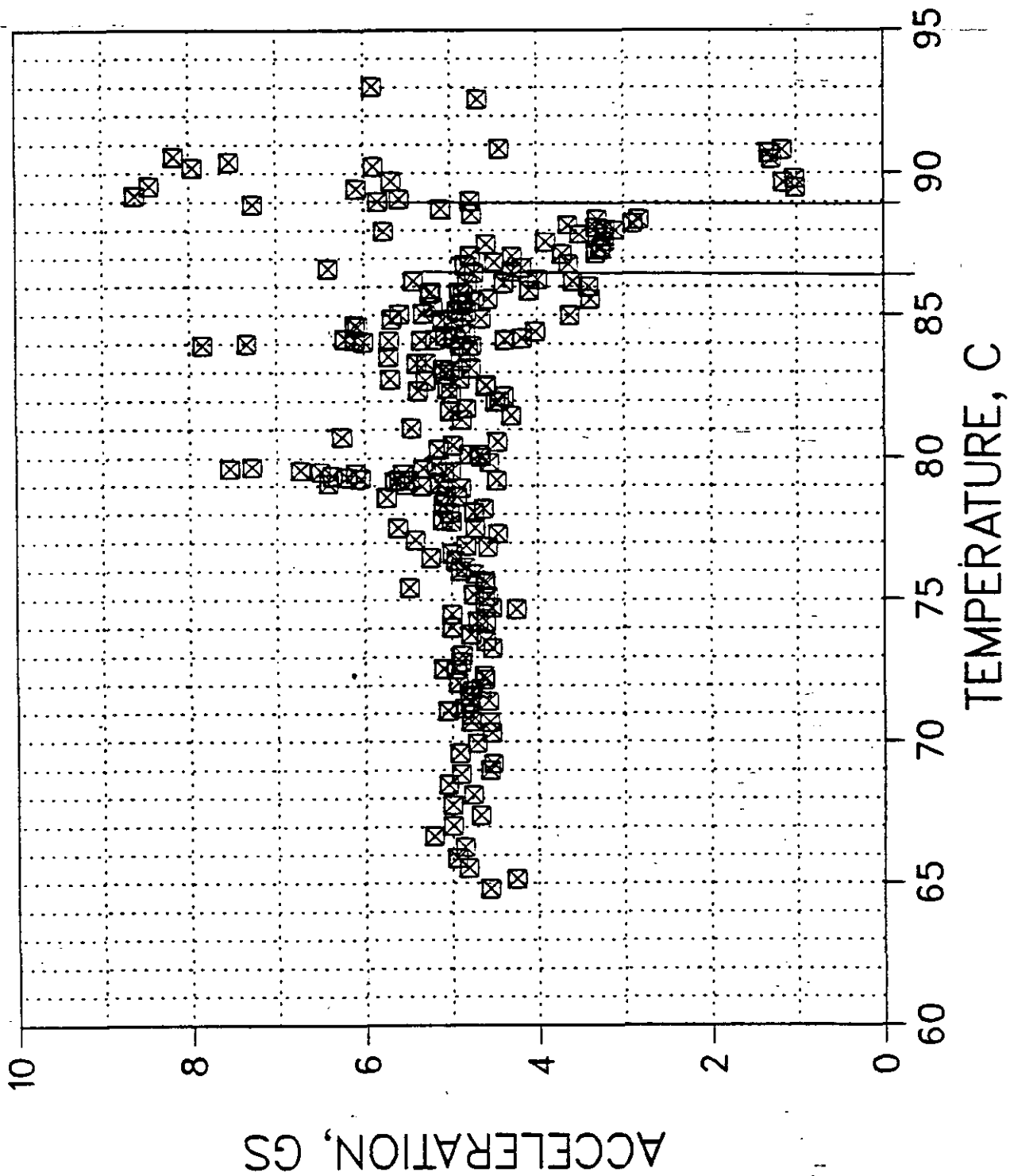
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 2

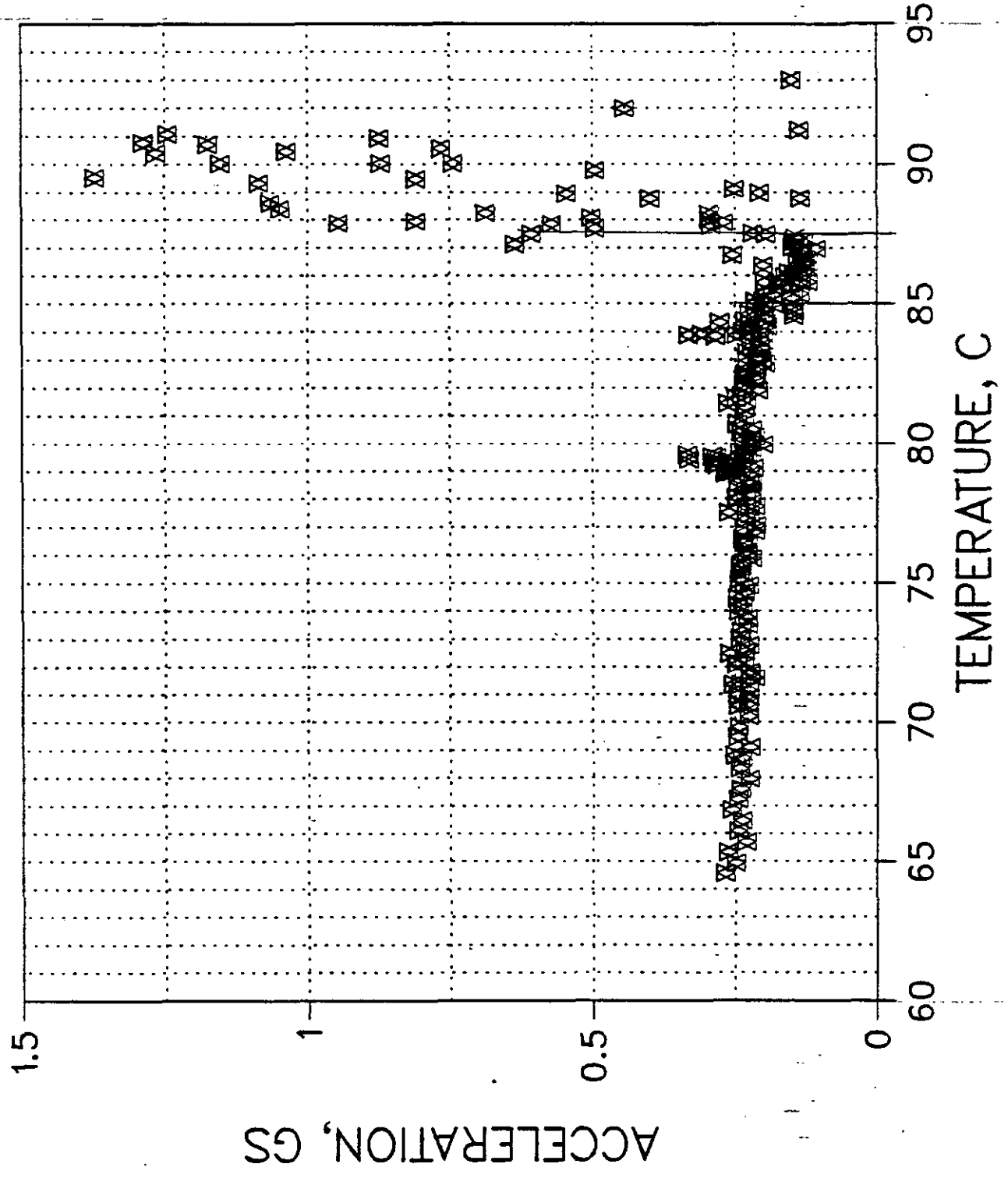


PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 2

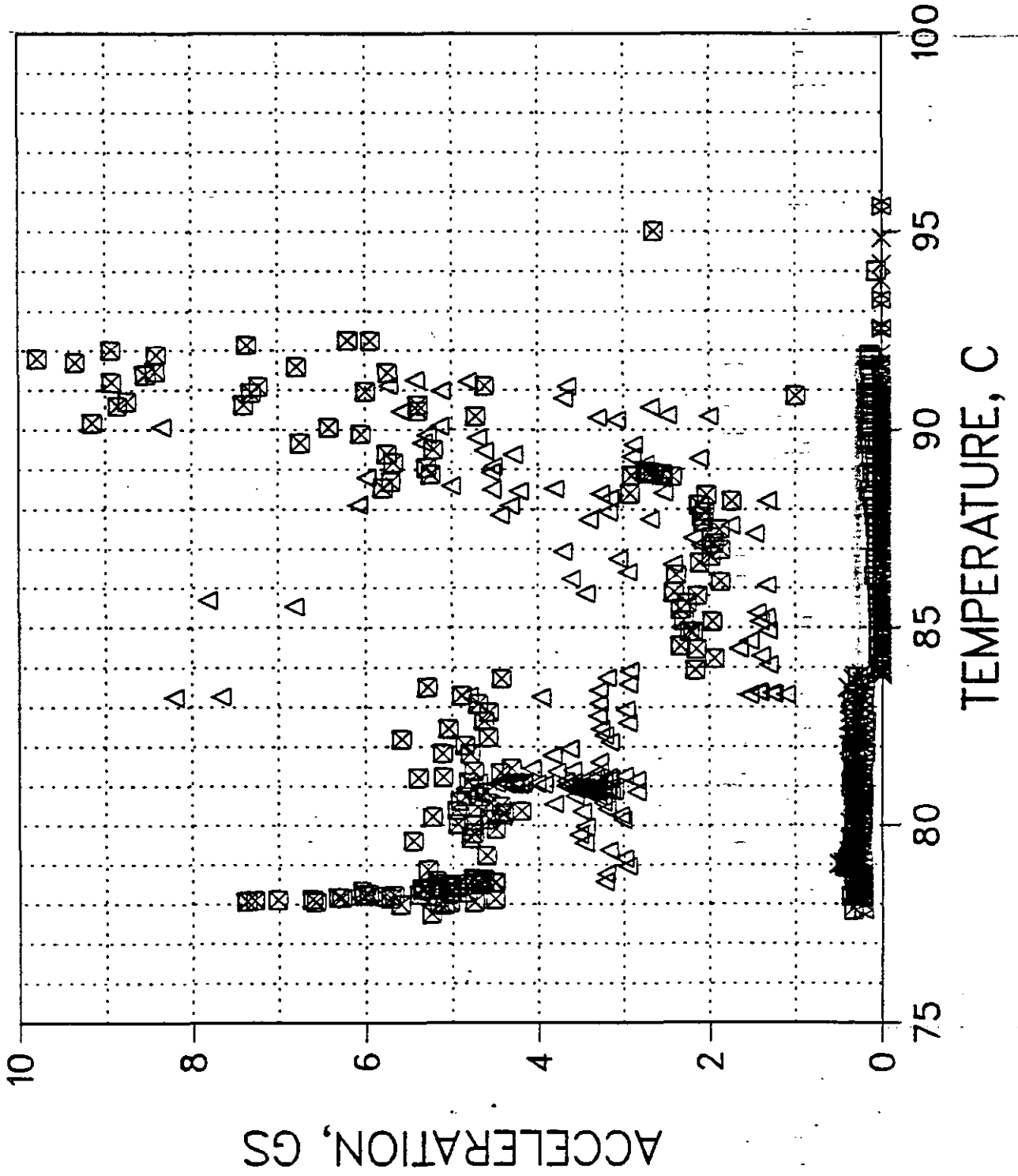


PUMP CAVITATION TESTS
UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 2



PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 3

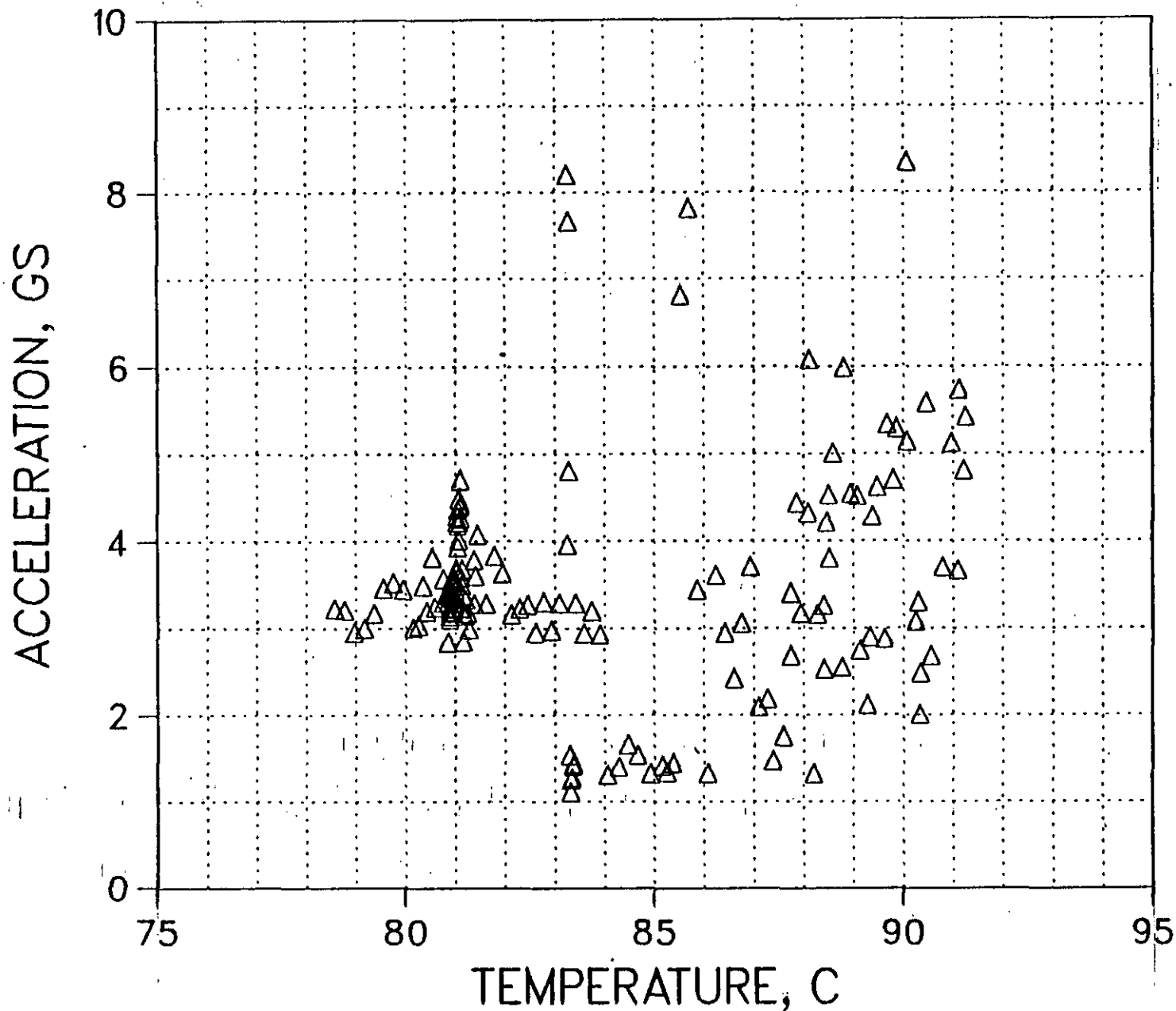


Legend

- △ SYS 1
- × SYS 2
- SYS 3
- ⊠ SYS 4
- ⊞ SYS 5
- * SYS 6

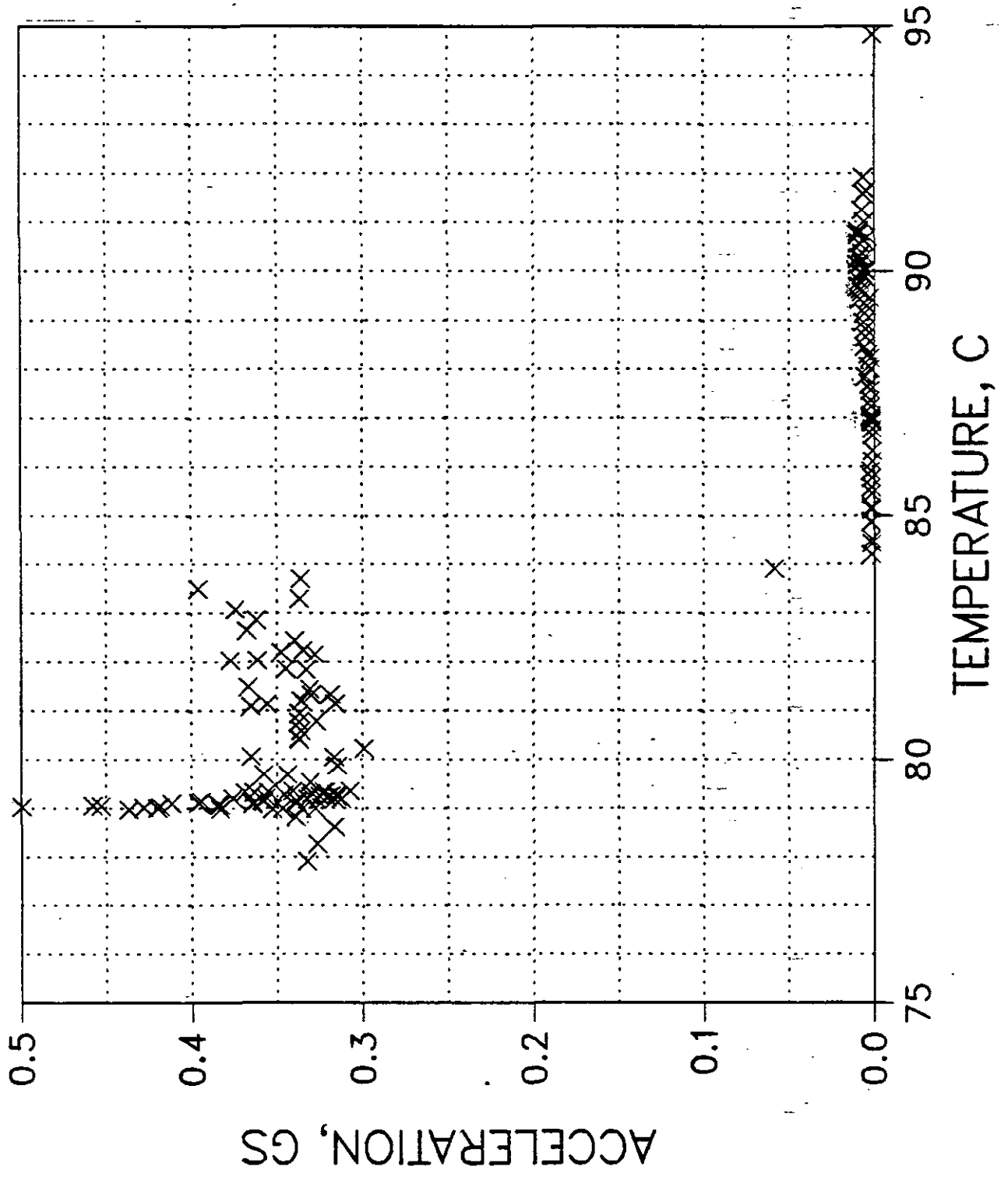
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 3

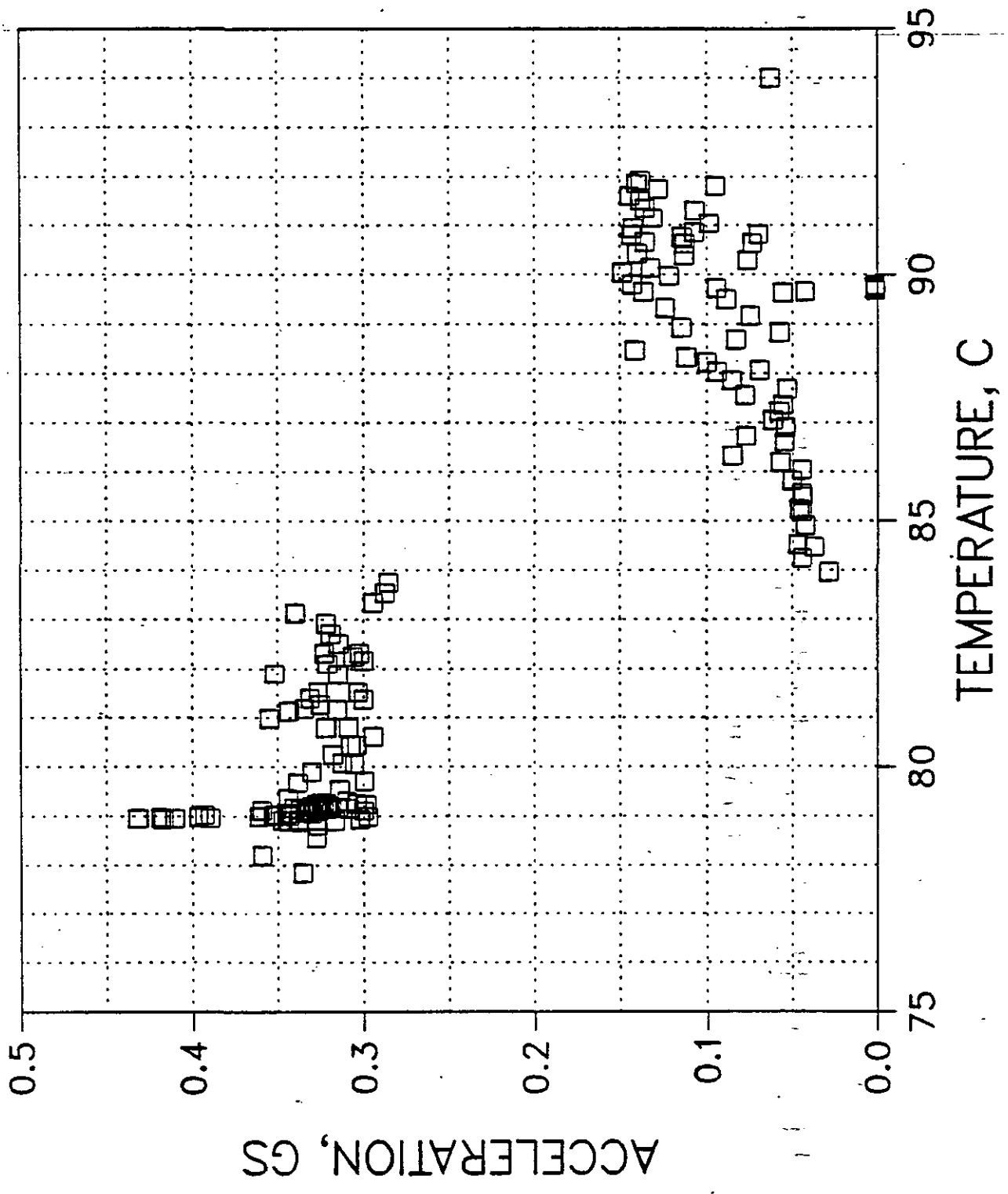


PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 3

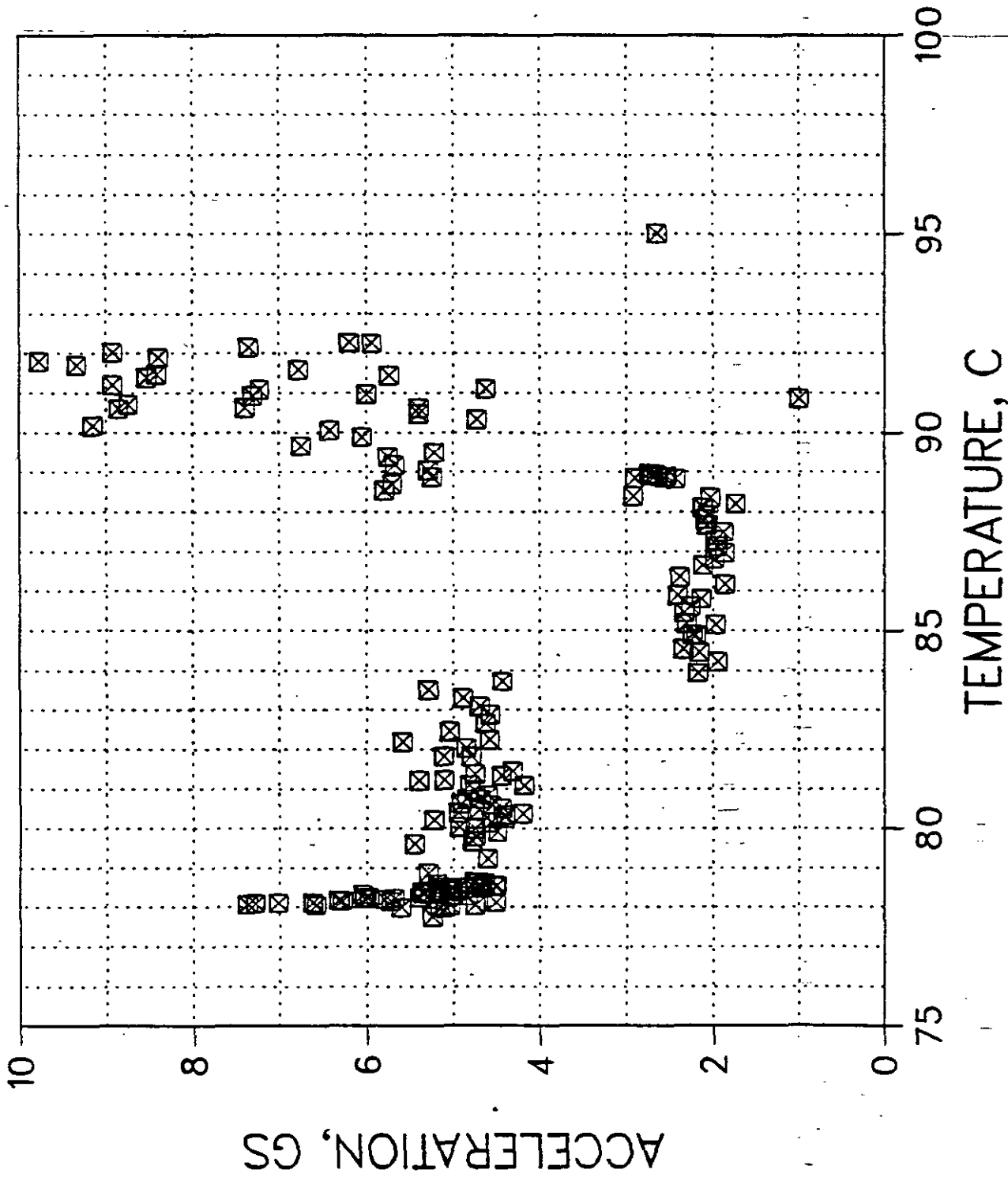


PUMP CAVITATION TESTS UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 3

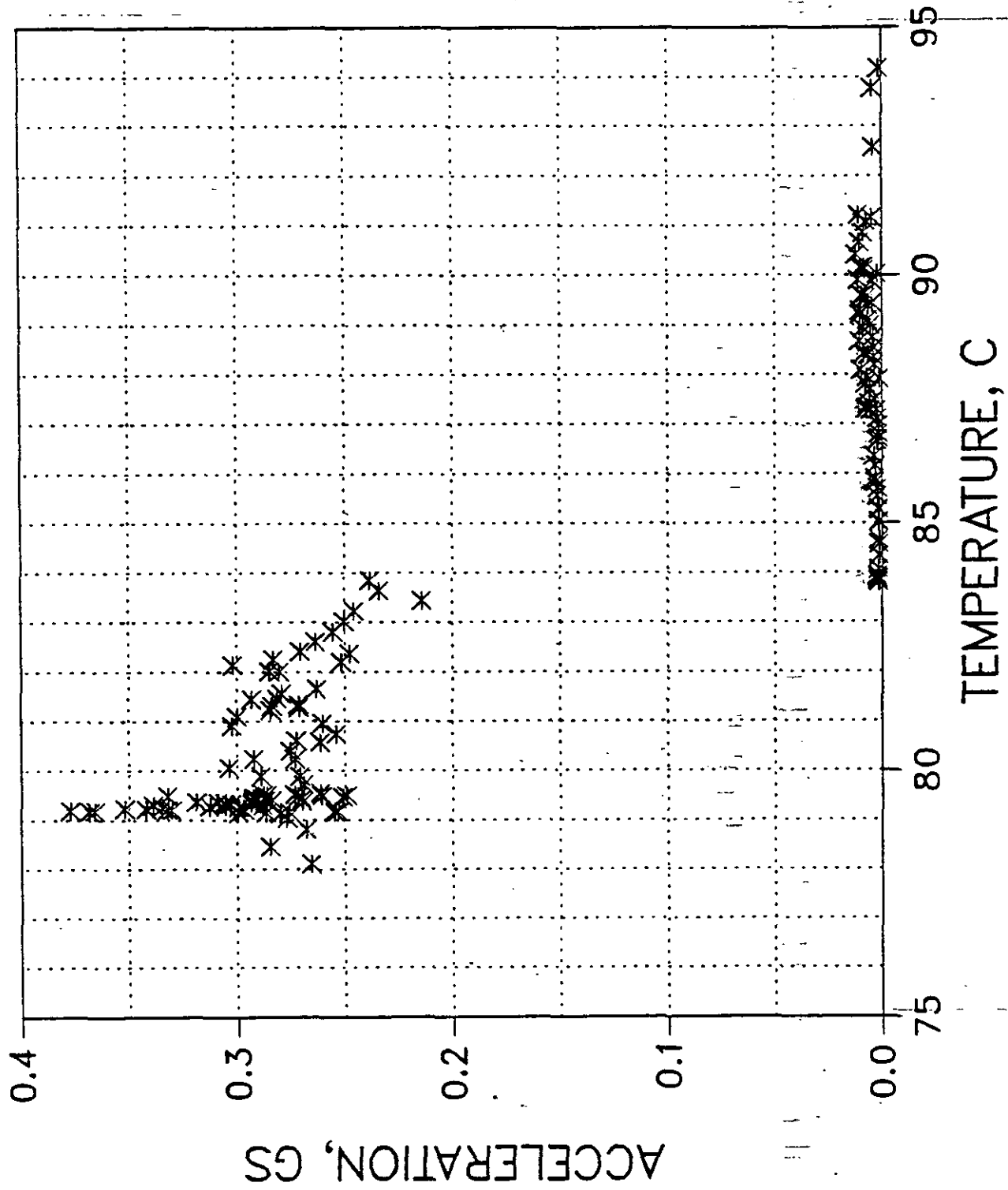


PUMP CAVITATION TESTS

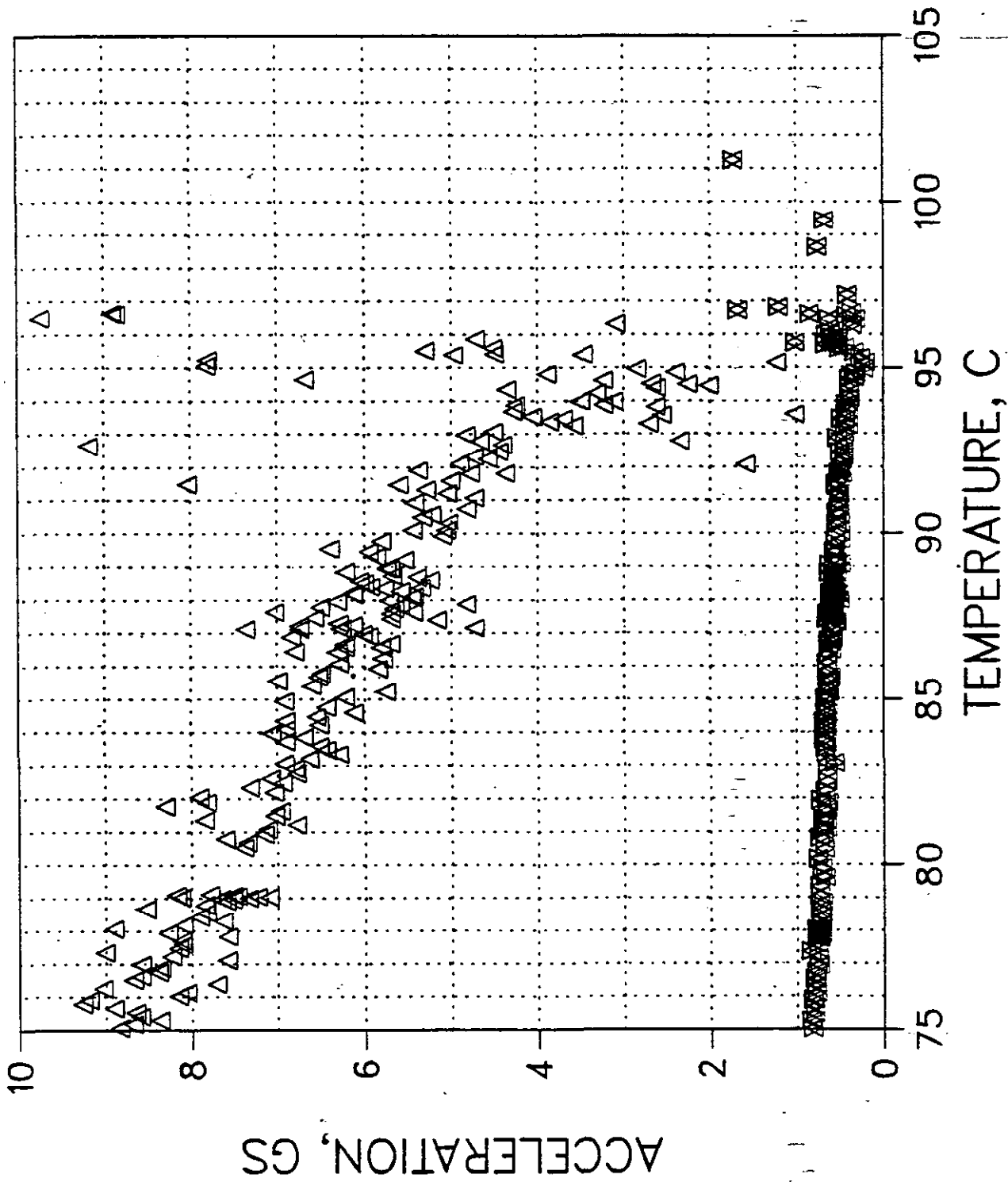
UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 3



PUMP CAVITATION TESTS
UNADJ. TEMP. VS PUMP CASING ACCEL. 6 pumps, 3



PUMP CAVITATION TESTS UNADJ. TEMP. VS PUMP CASING ACCEL. 5 pumps

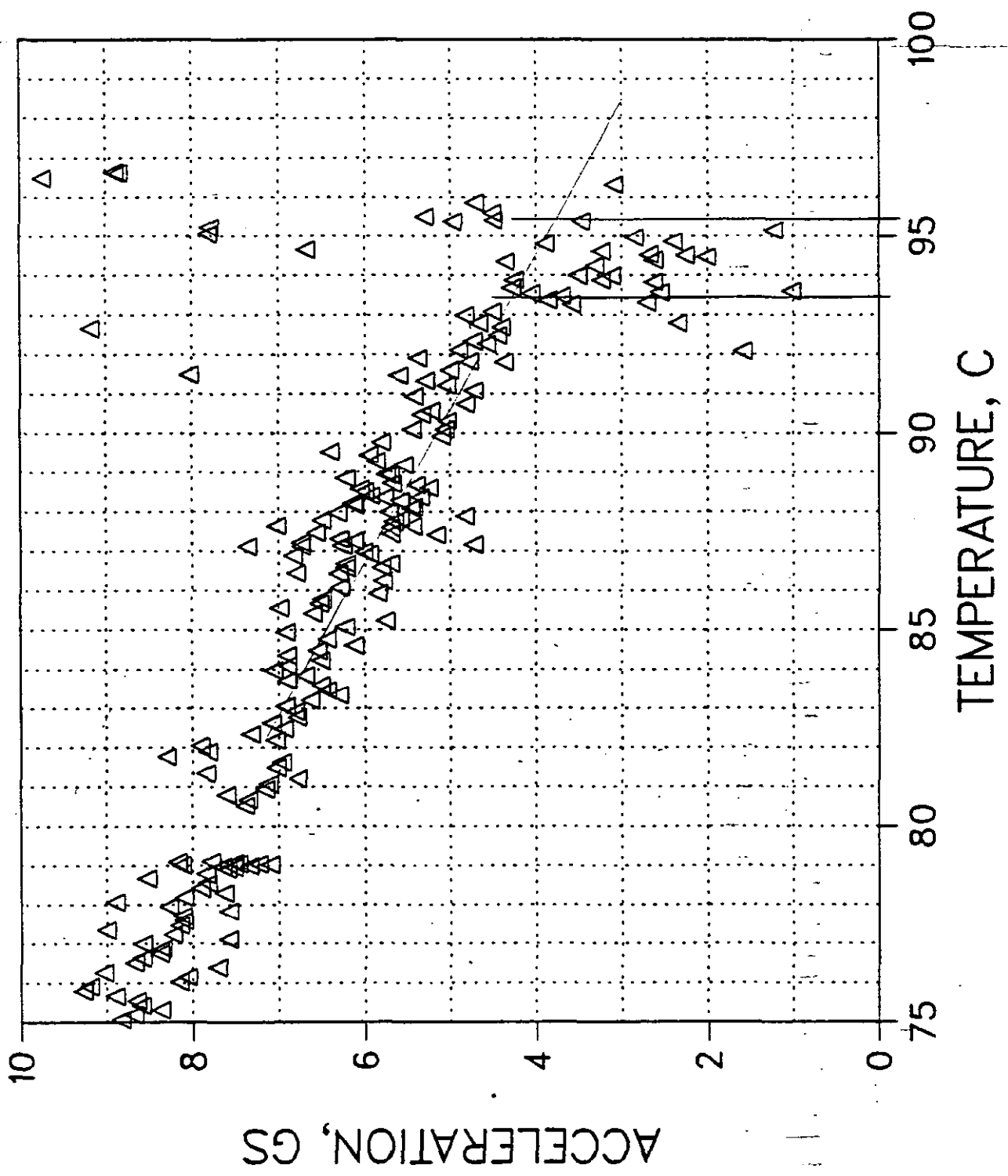


Legend

△ SYS 1

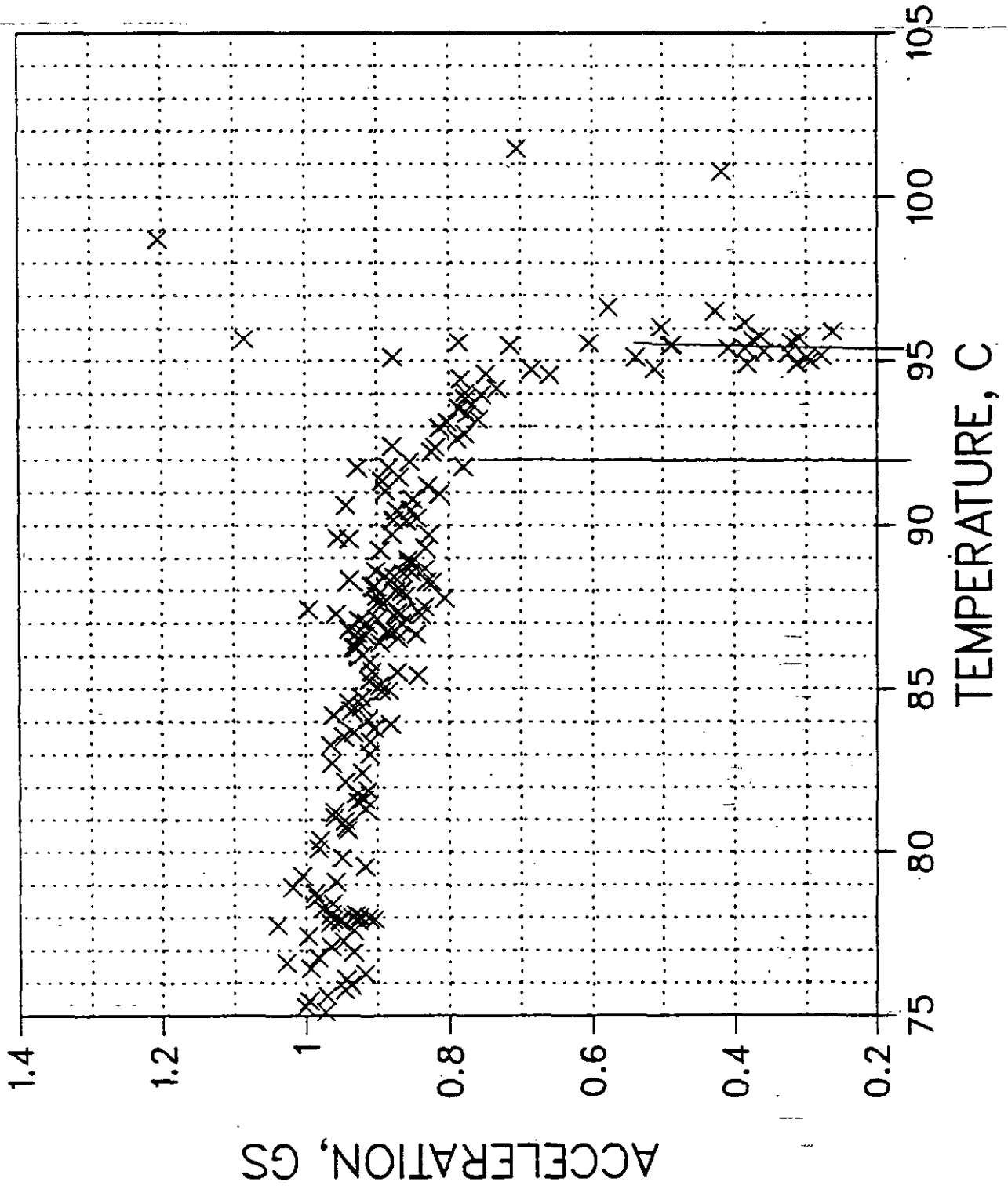
⊗ SYS 5

PUMP CAVITATION TESTS UNADJ. TEMP. VS PUMP CASING ACCEL. 5 pumps

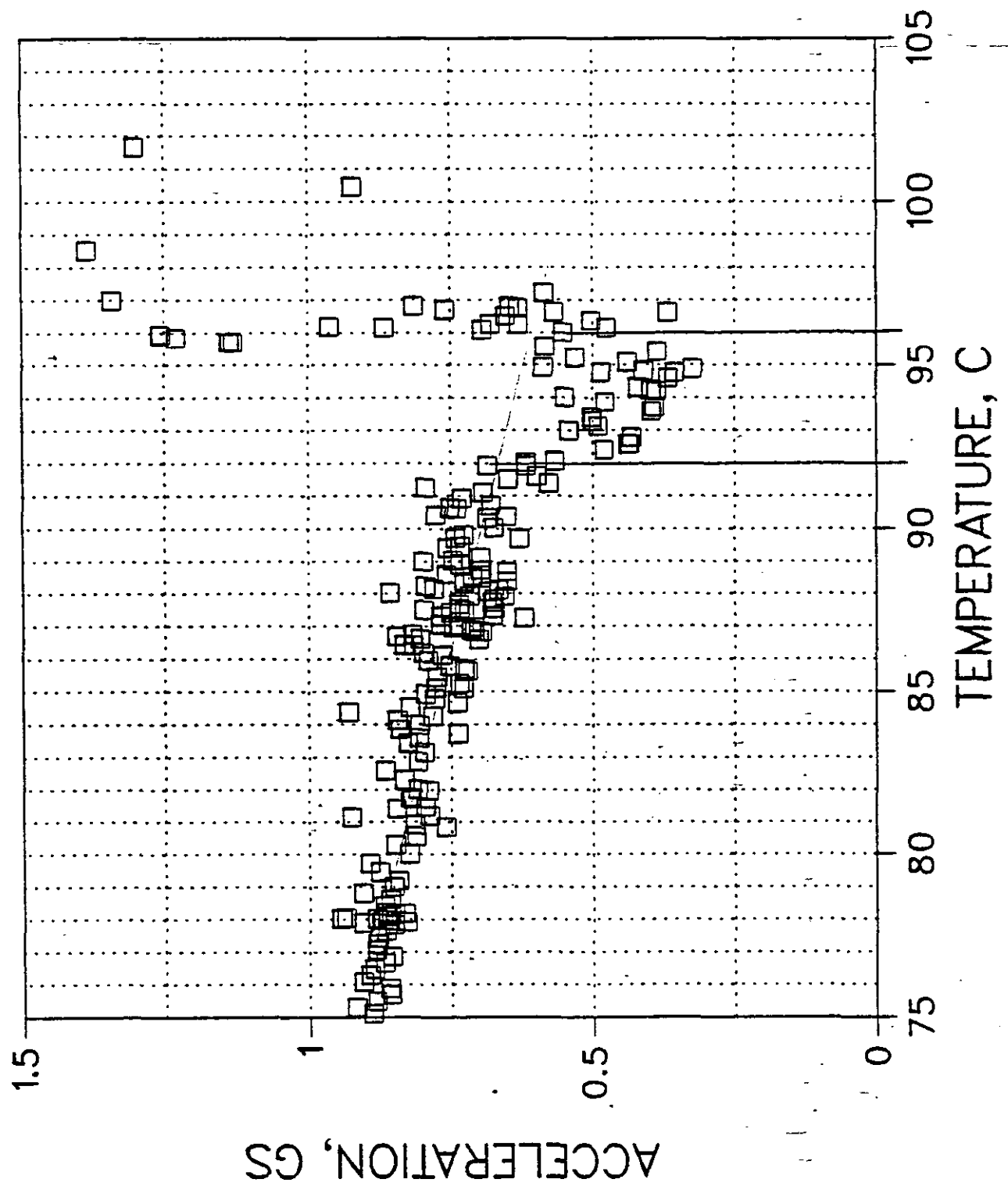


PUMP CAVITATION TESTS

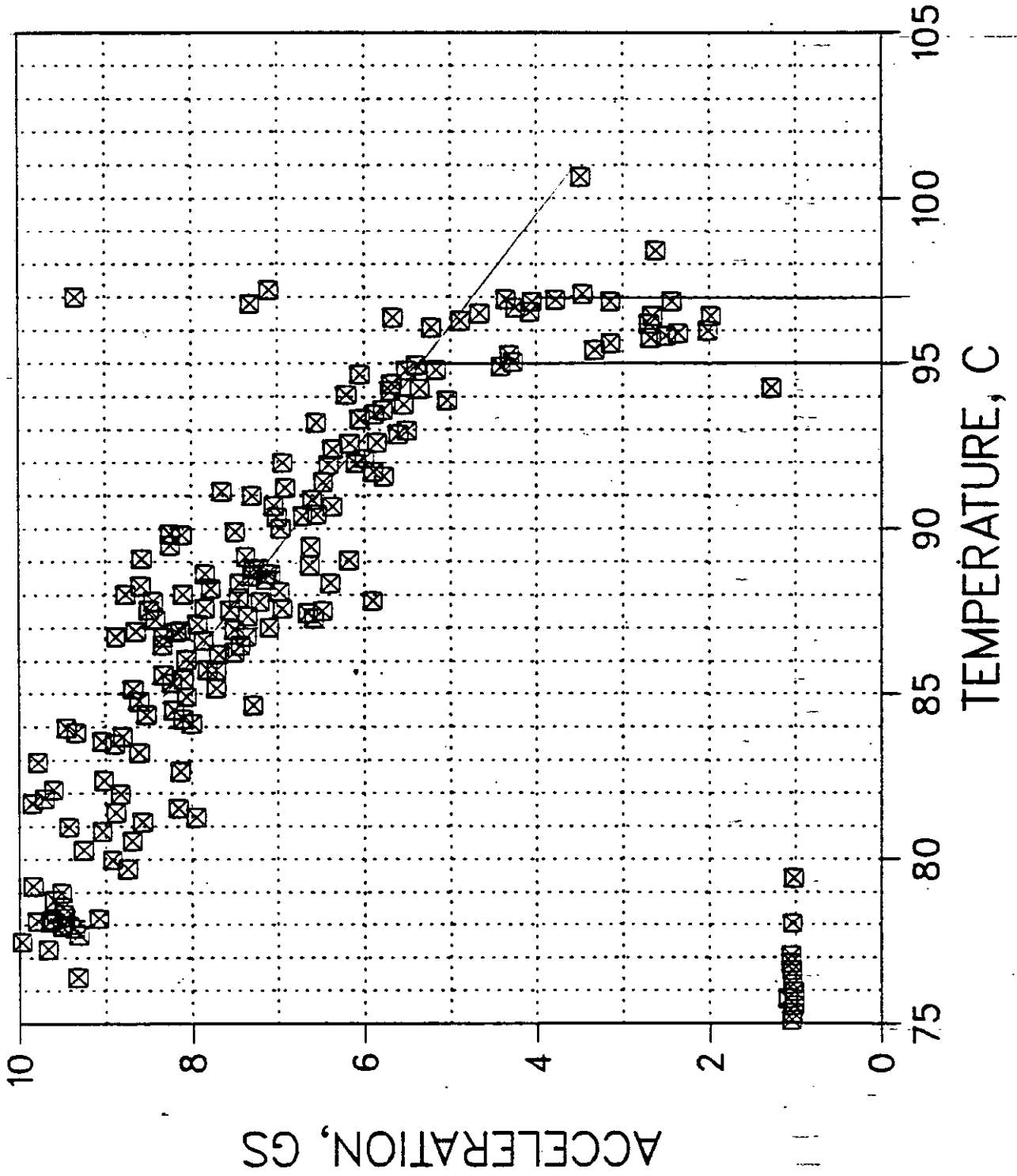
UNADJ. TEMP. VS PUMP CASING ACCEL. 5 pumps



PUMP CAVITATION TESTS
UNADJ. TEMP. VS PUMP CASING ACCEL. 5 pumps

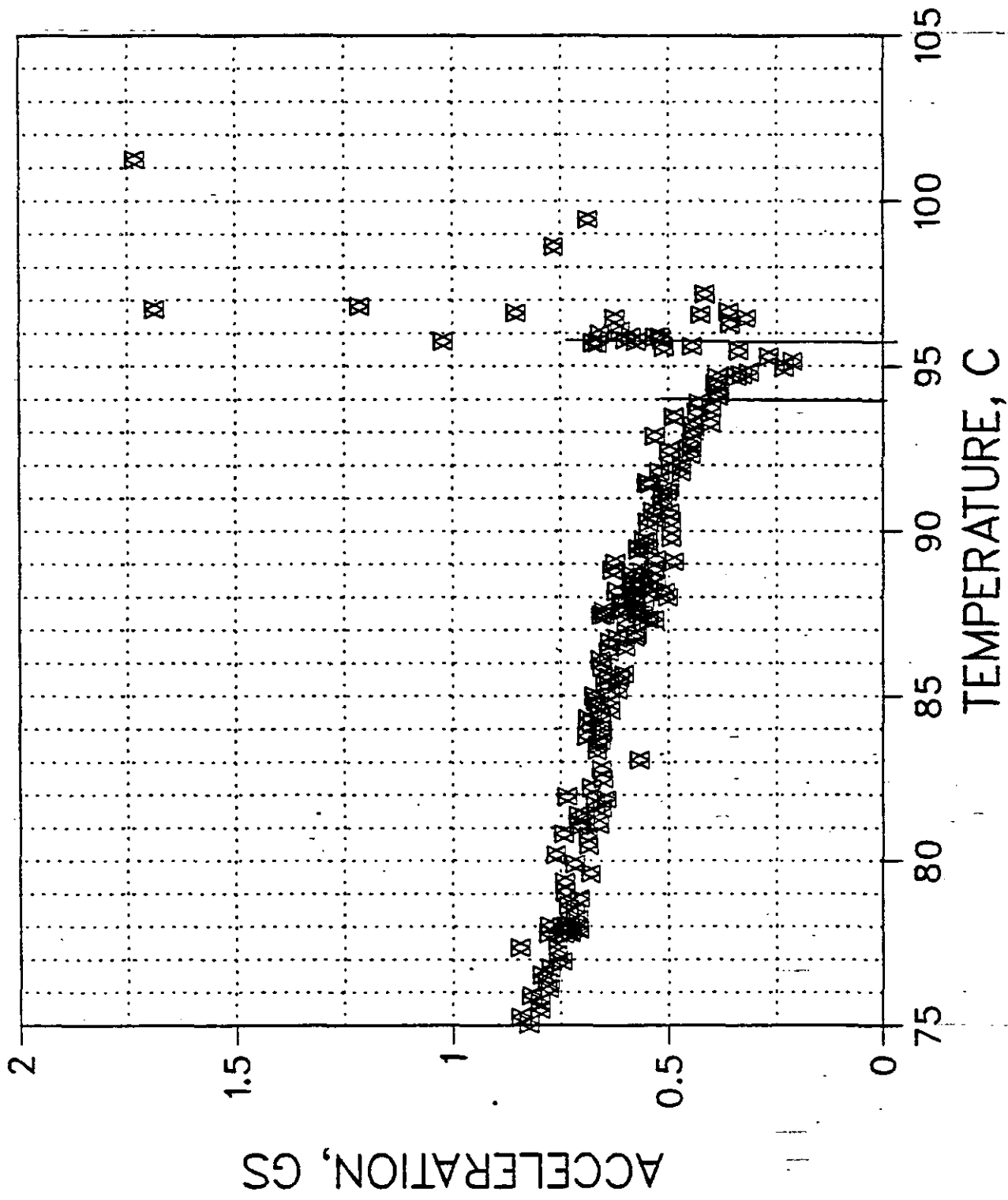


PUMP CAVITATION TESTS UNADJ. TEMP. VS PUMP CASING ACCEL. 5 pumps



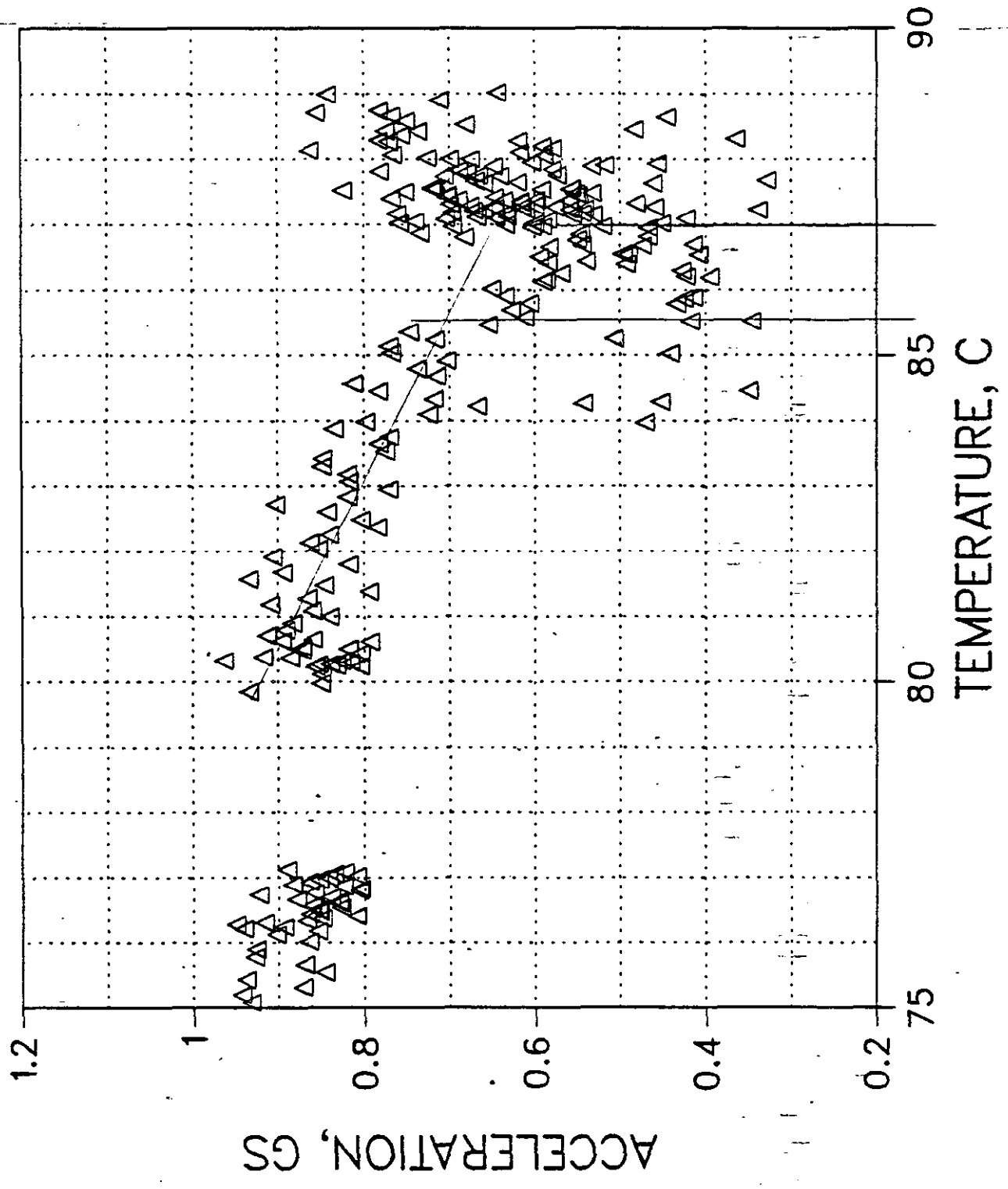
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 5 pumps



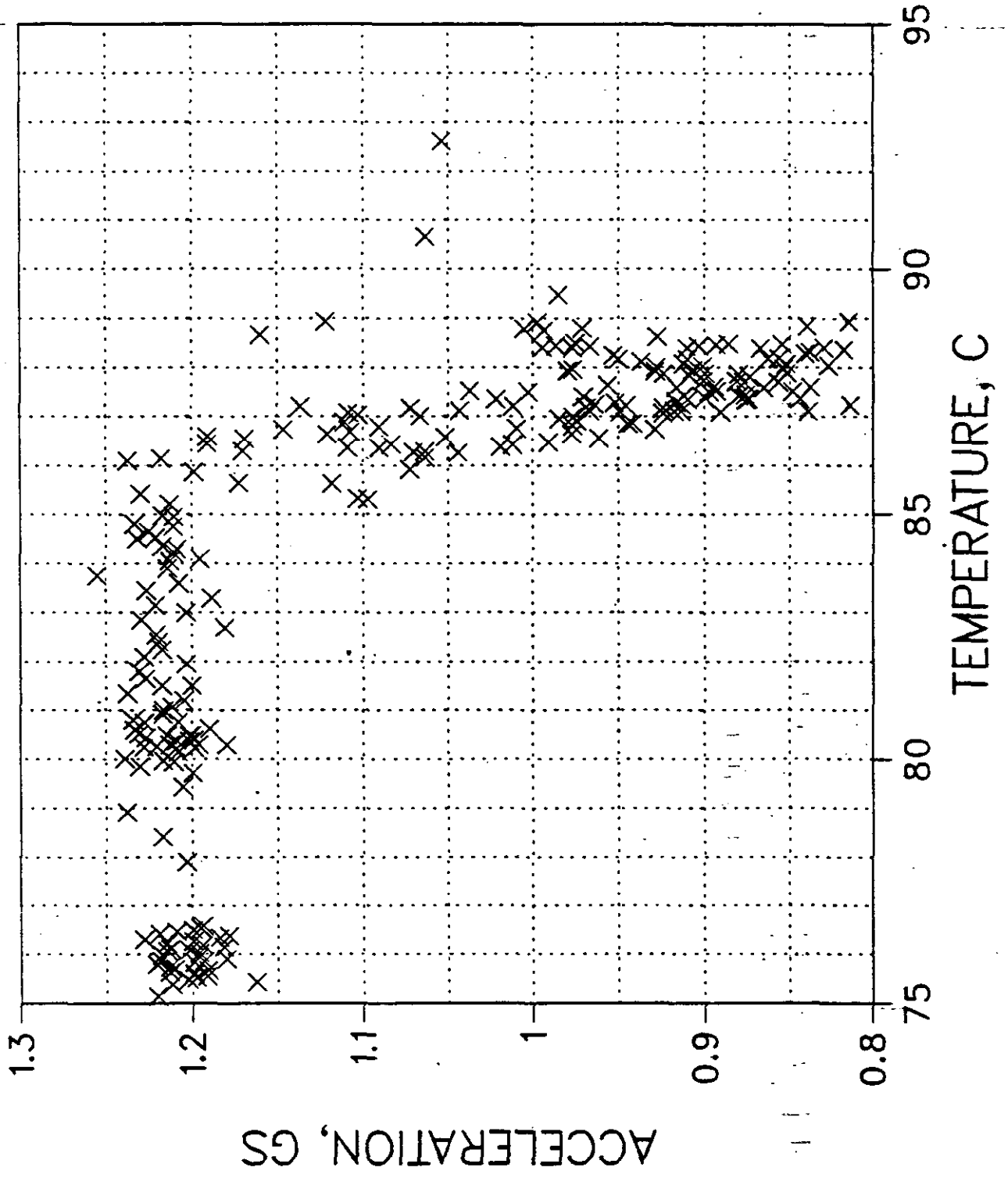
PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 3 pumps



PUMP CAVITATION TESTS

UNADJ. TEMP. VS PUMP CASING ACCEL. 3 pumps



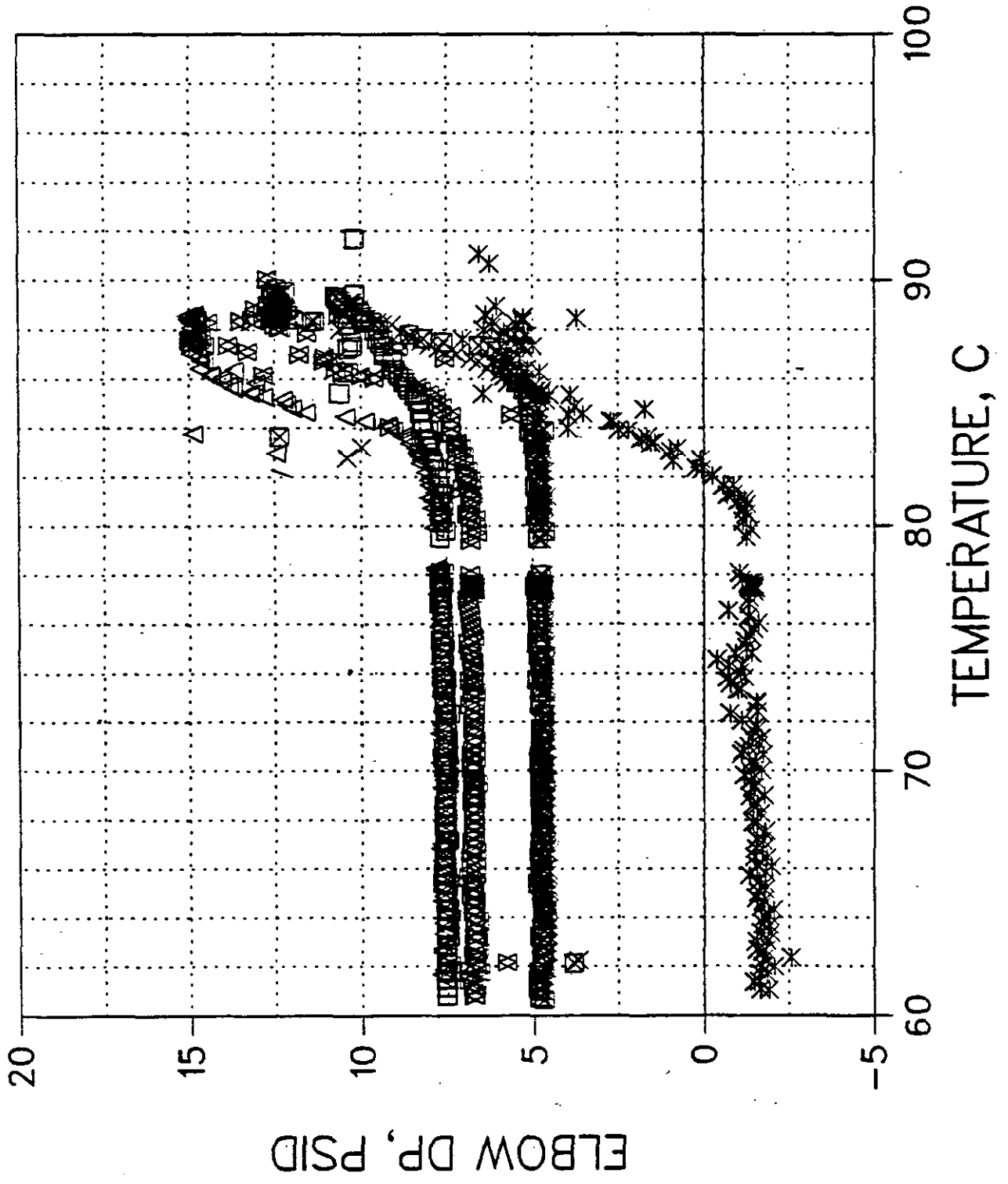
A) Data Curves

3) Elbow (Suction Line) DP vs. Temperature

The low pressure header reading minus the pump suction pressure is plotted against the associated RTD temperature. Appendix E on the low pressure header should be reviewed before these numbers are used for any absolute analysis. System 6 pump suction reading is bad.

See notes at Appendix A-1.

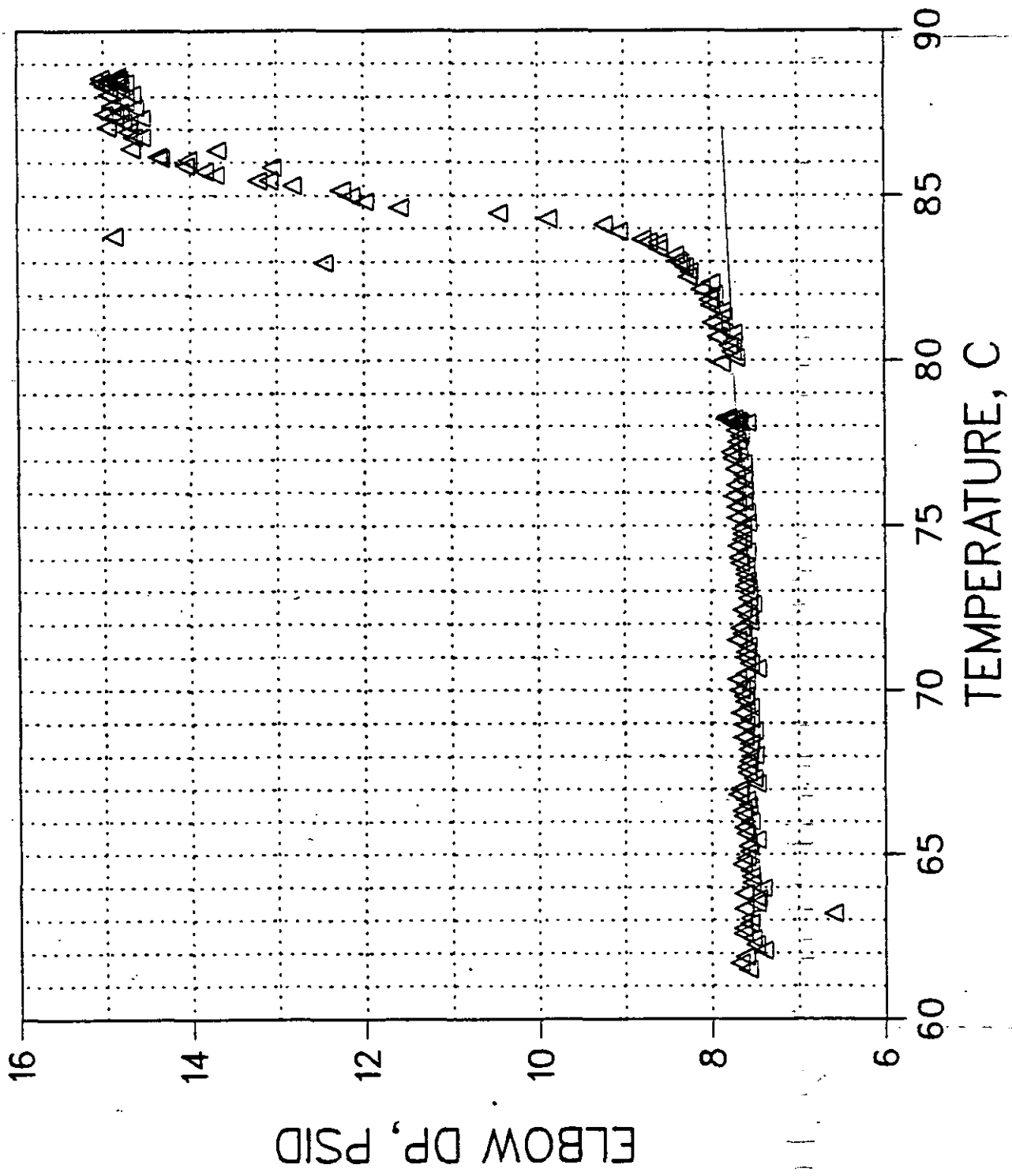
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps,1



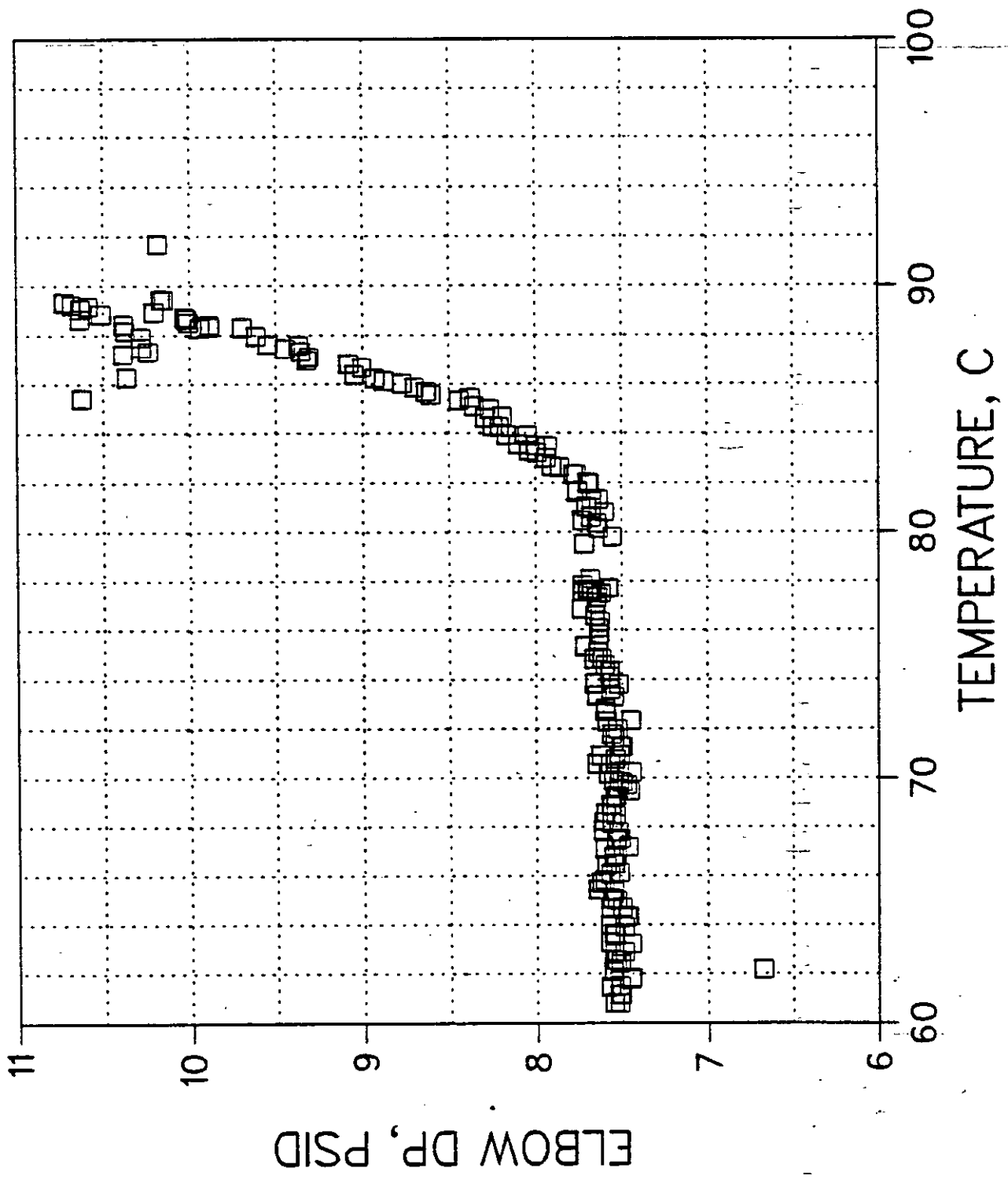
Legend

- △ SYS 1
- × SYS 2
- SYS 3
- ⊠ SYS 4
- ▣ SYS 5
- * sys 6

PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 1

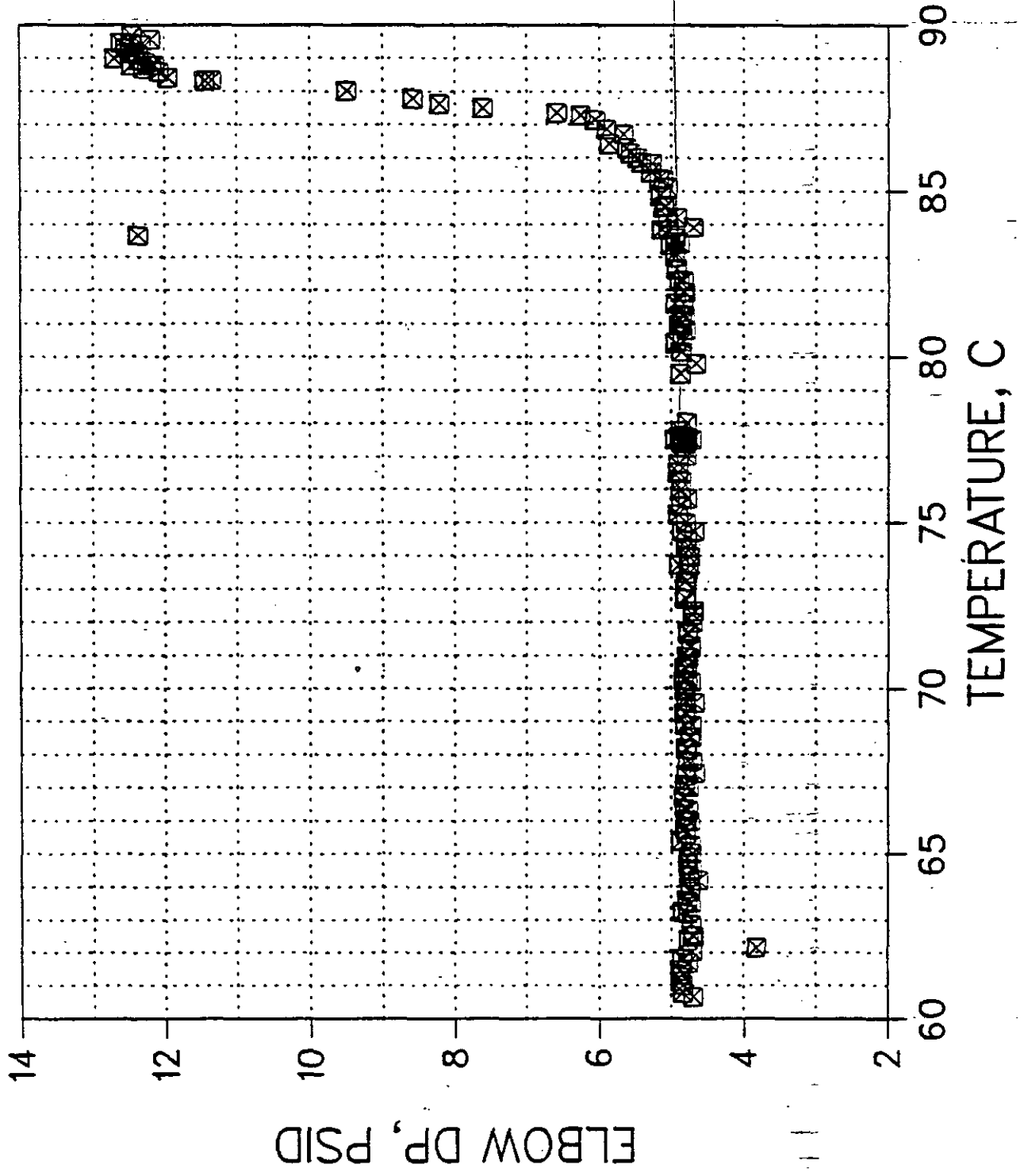


PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 1

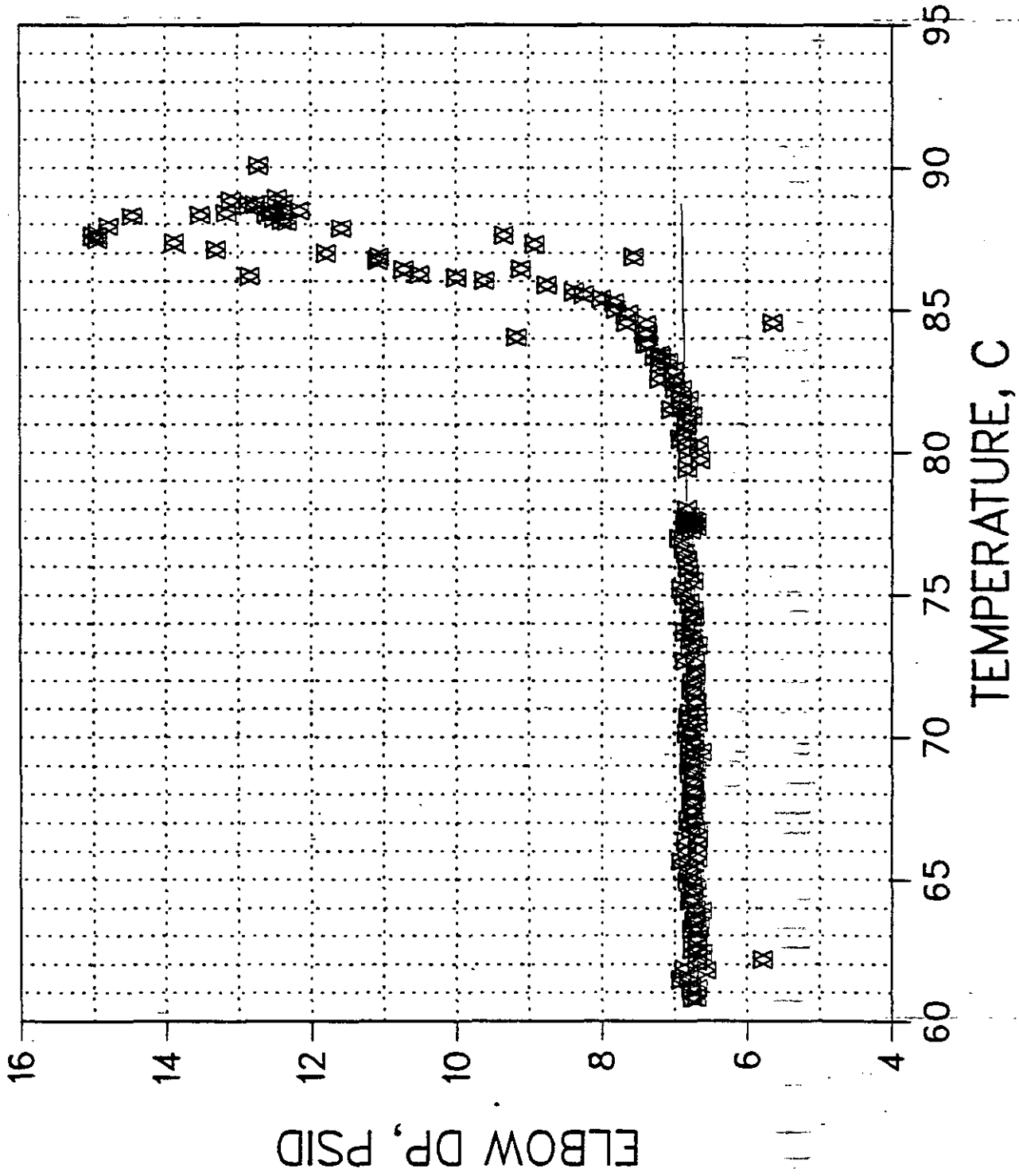


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PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 1

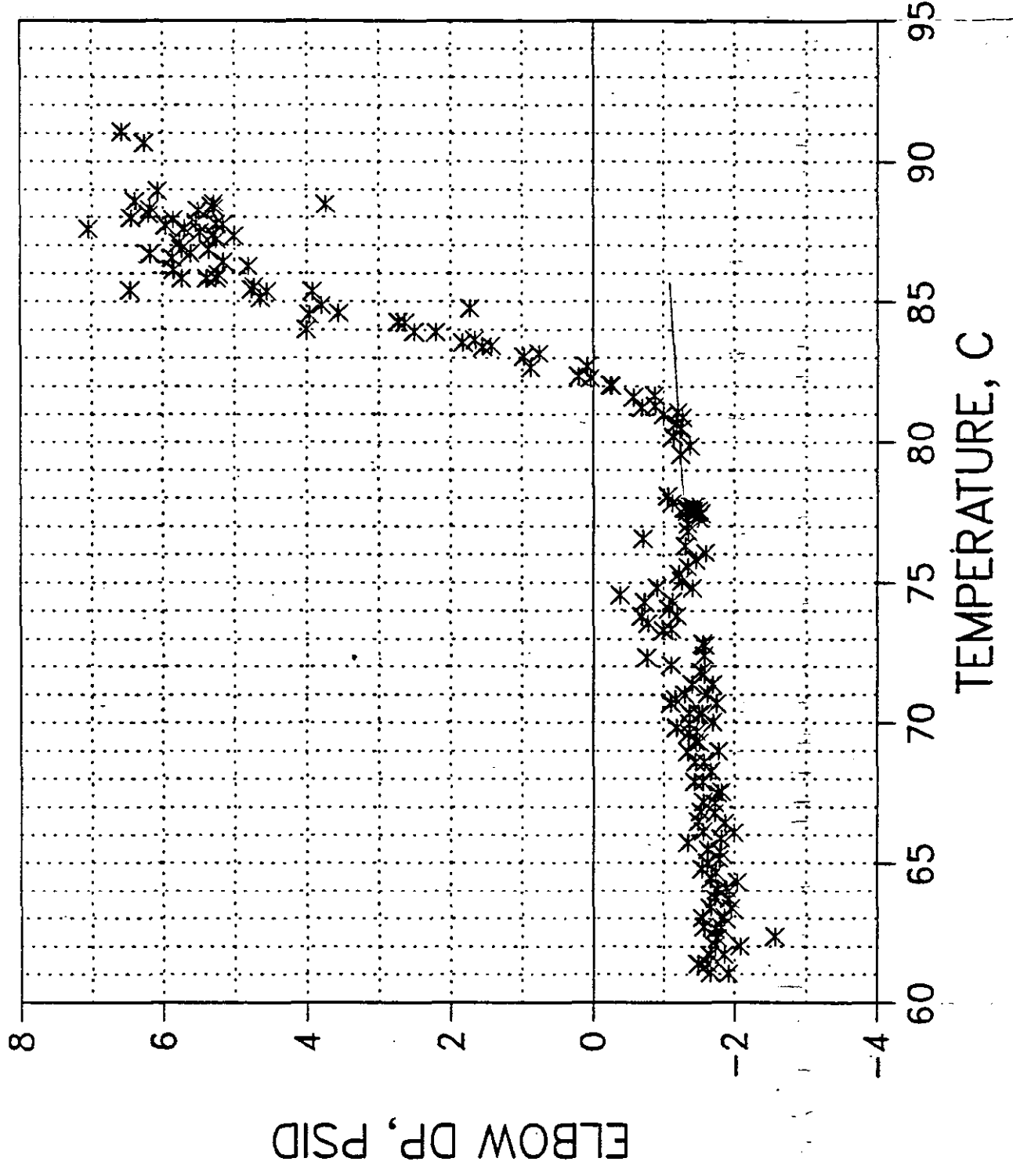


PUMP CAVITATION TESTS
UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 1



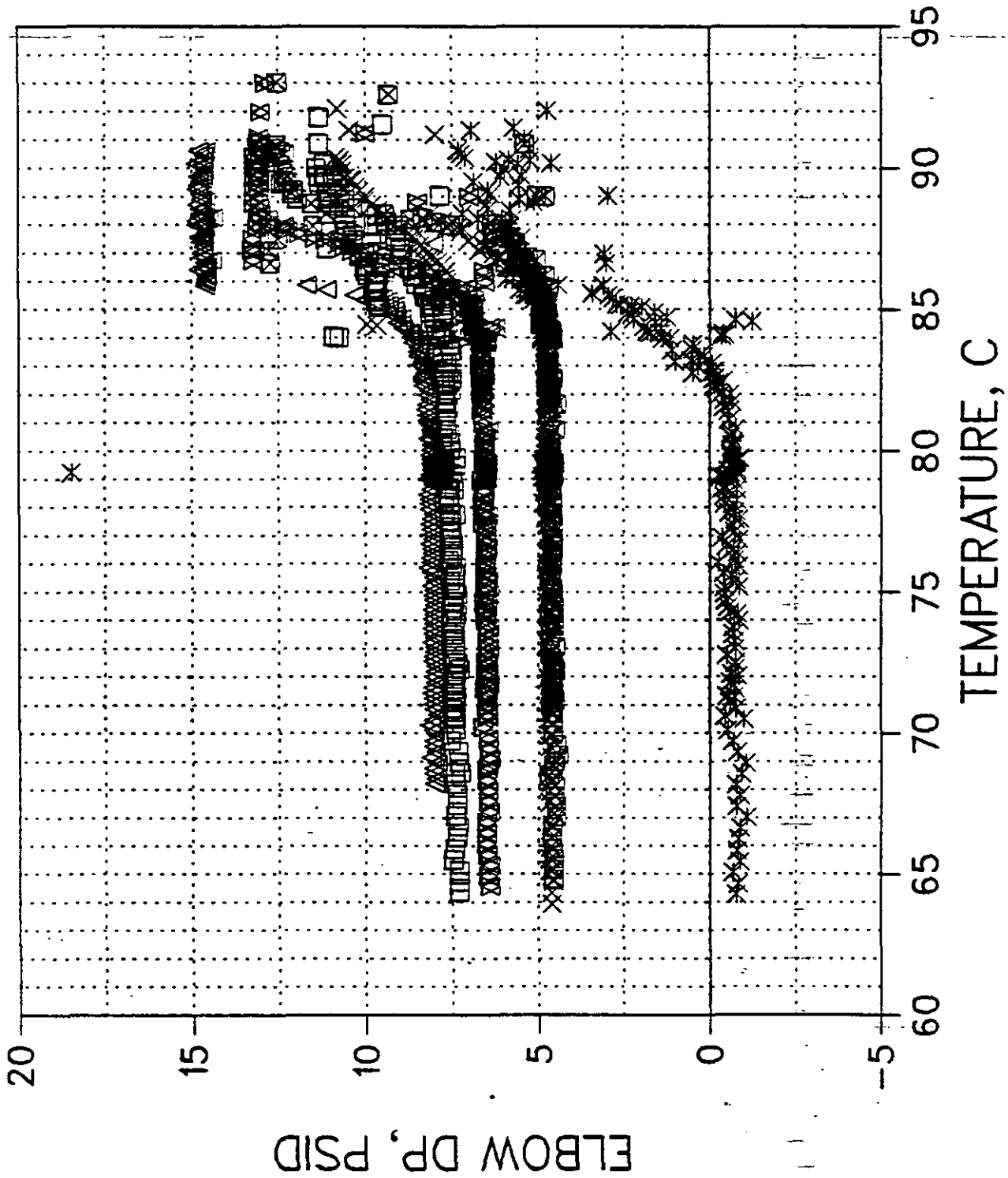
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PUMP CAVITATION TESTS
UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 1



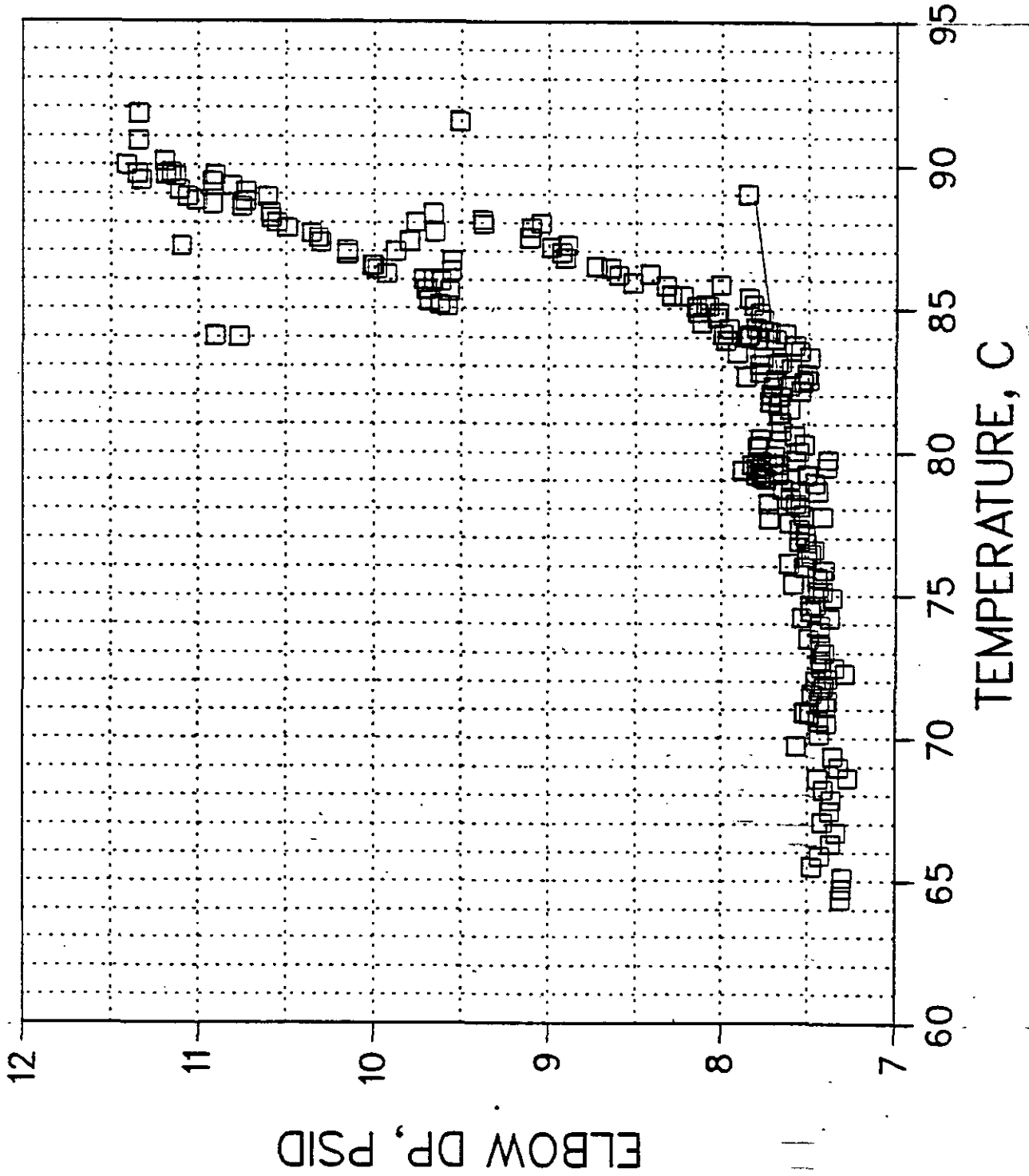
PUMP CAVITATION TESTS

UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps,2

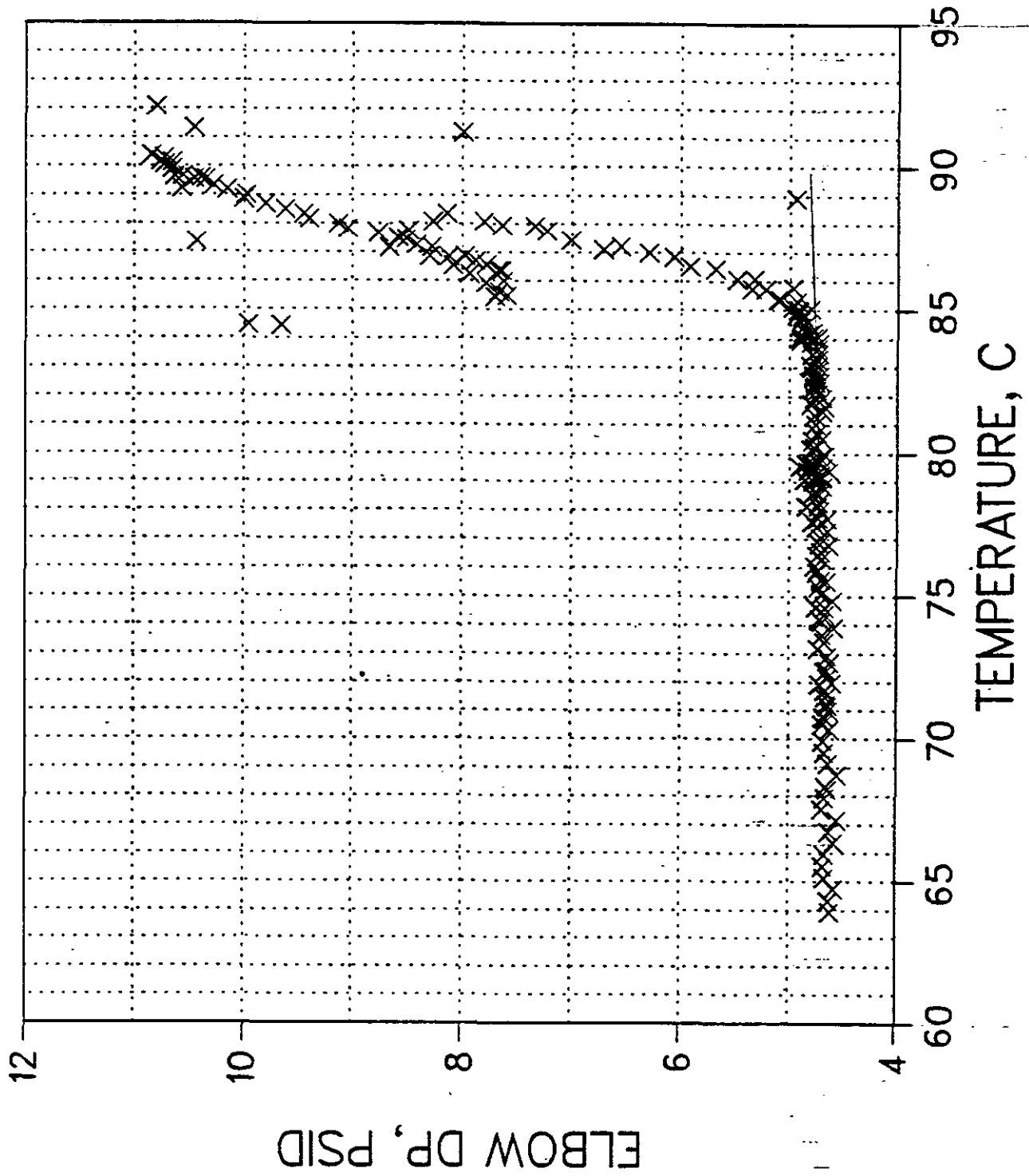


- Legend
- △ SYS 1
 - × SYS 2
 - SYS 3
 - ⊠ SYS 4
 - ⊡ SYS 5
 - * SYS 6

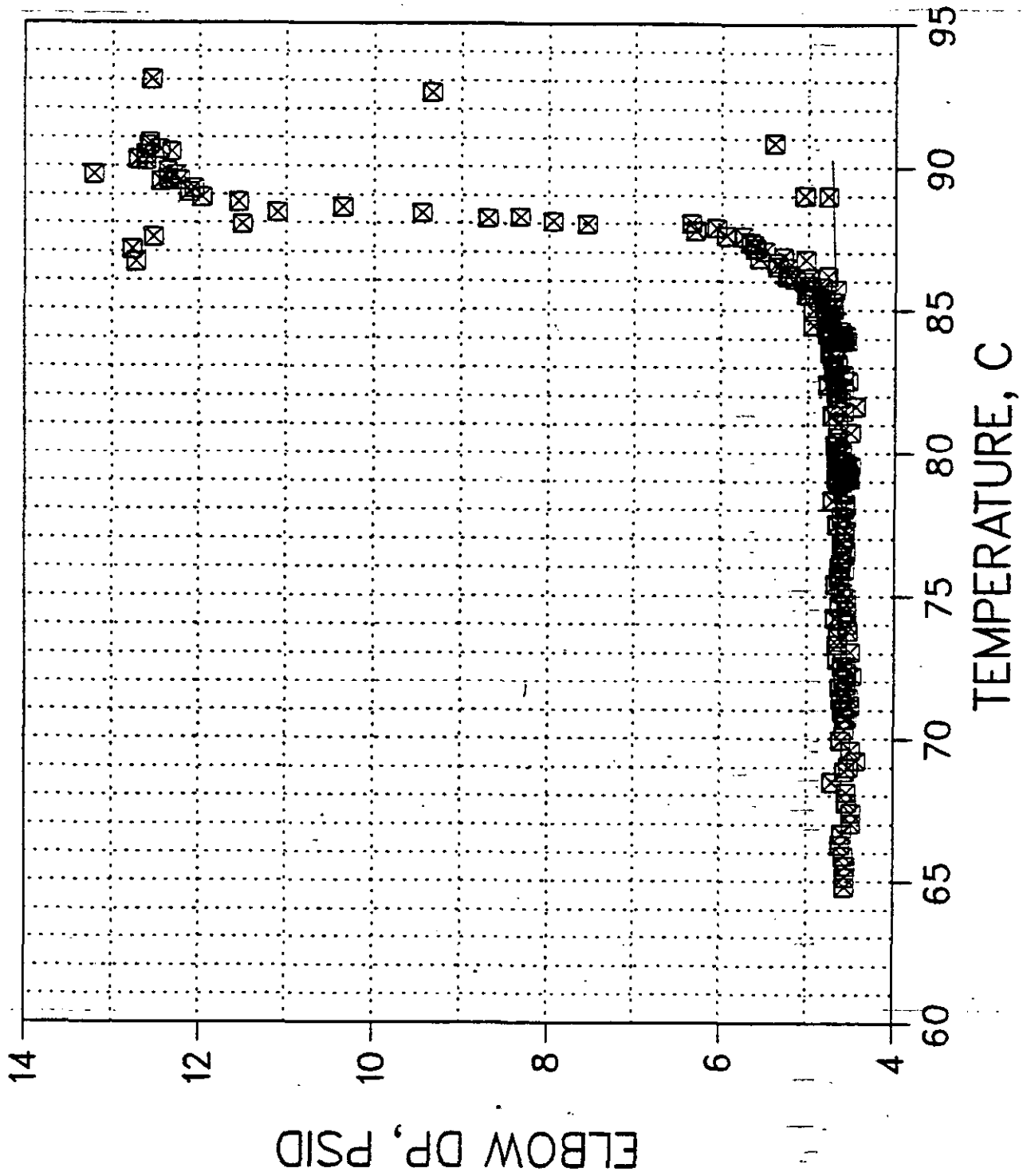
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 2



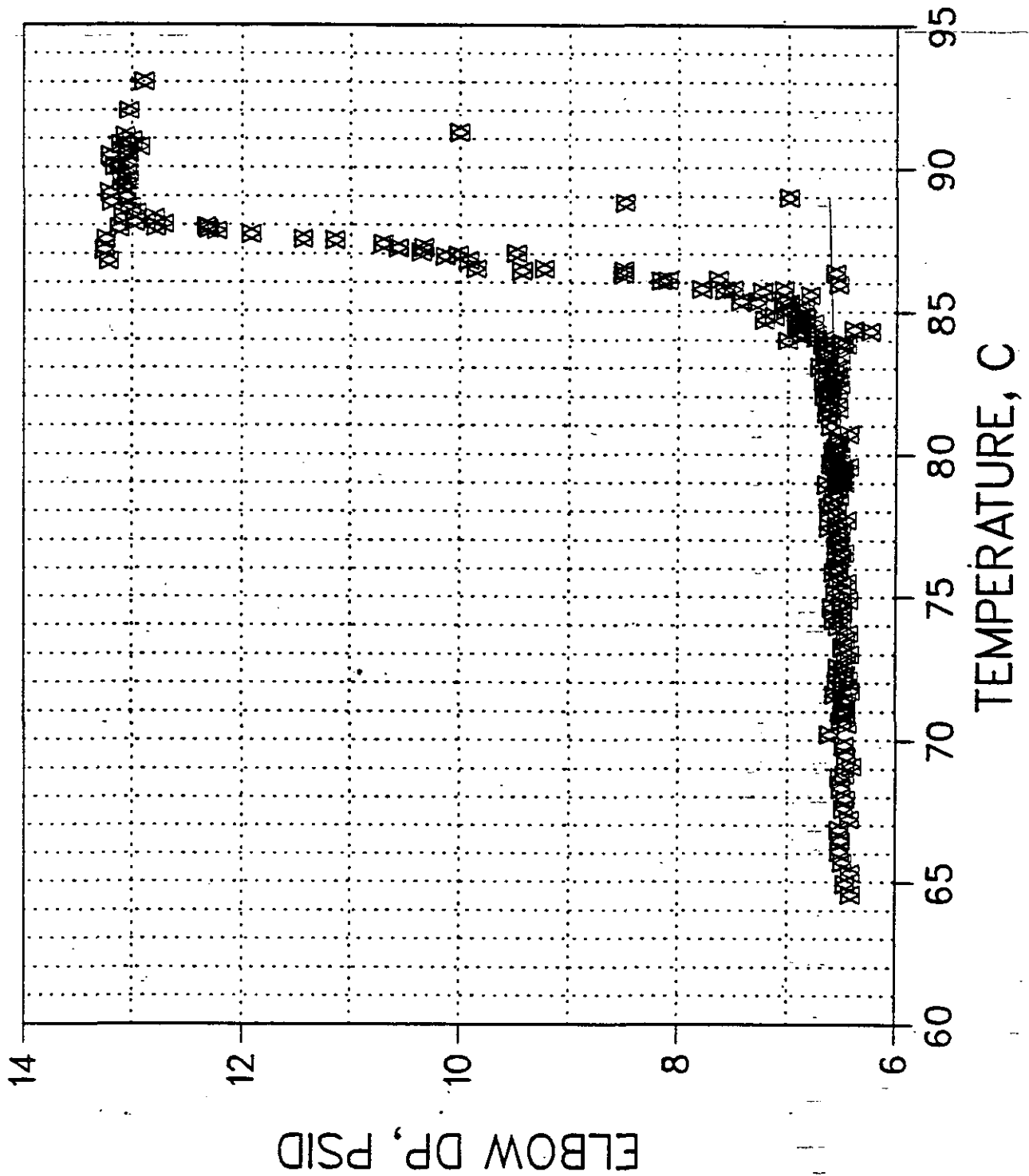
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 2



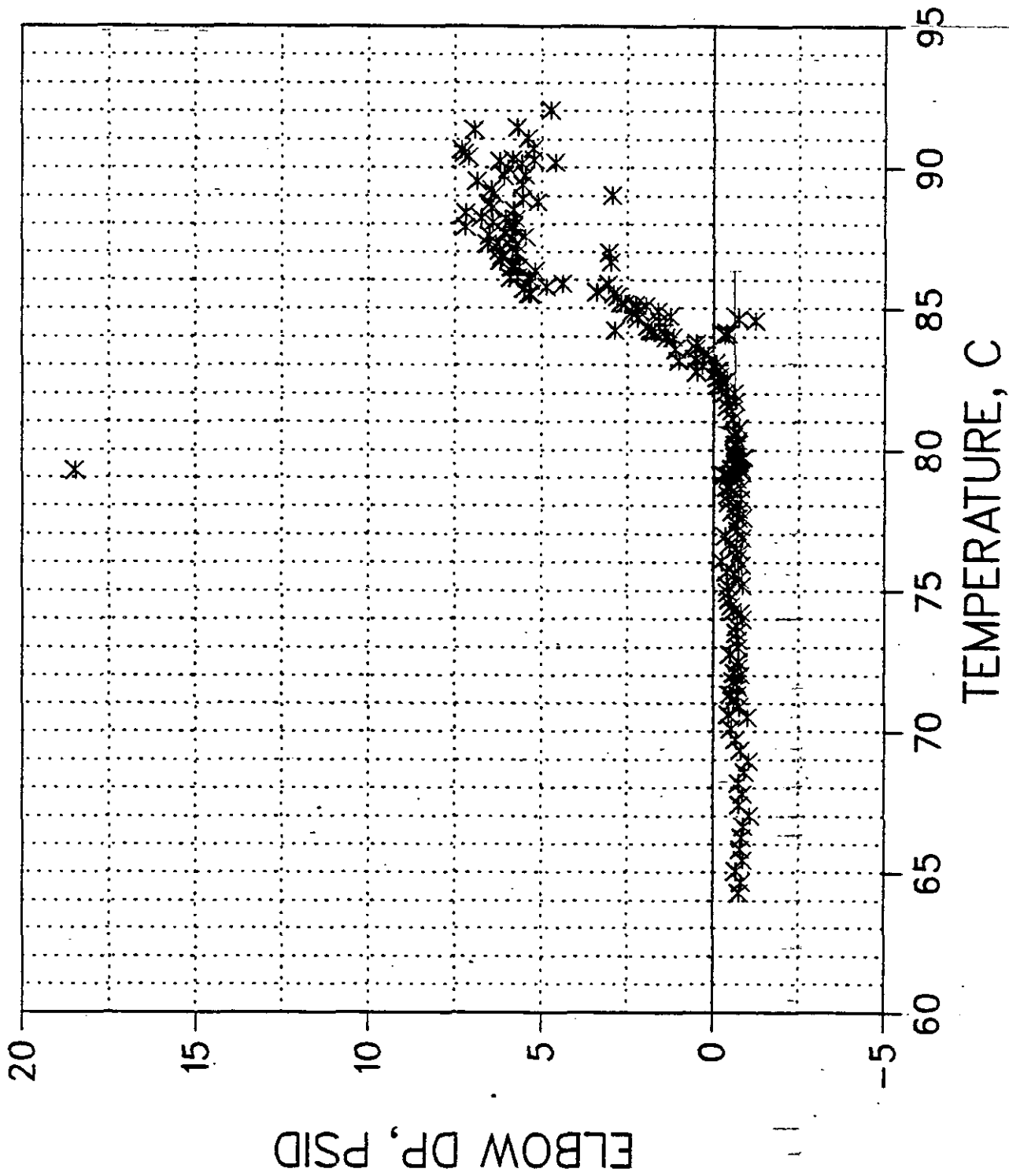
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 2



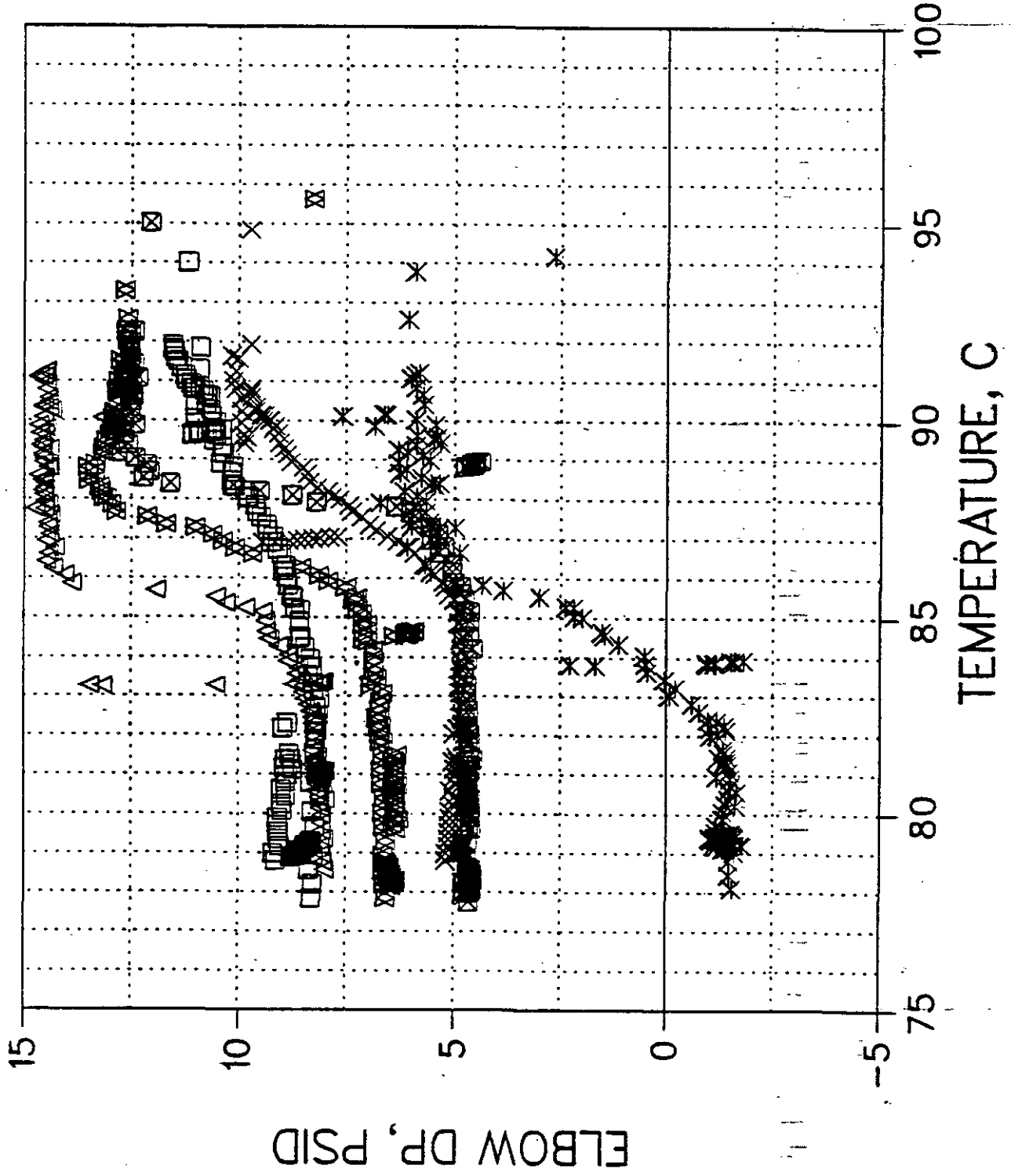
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 2



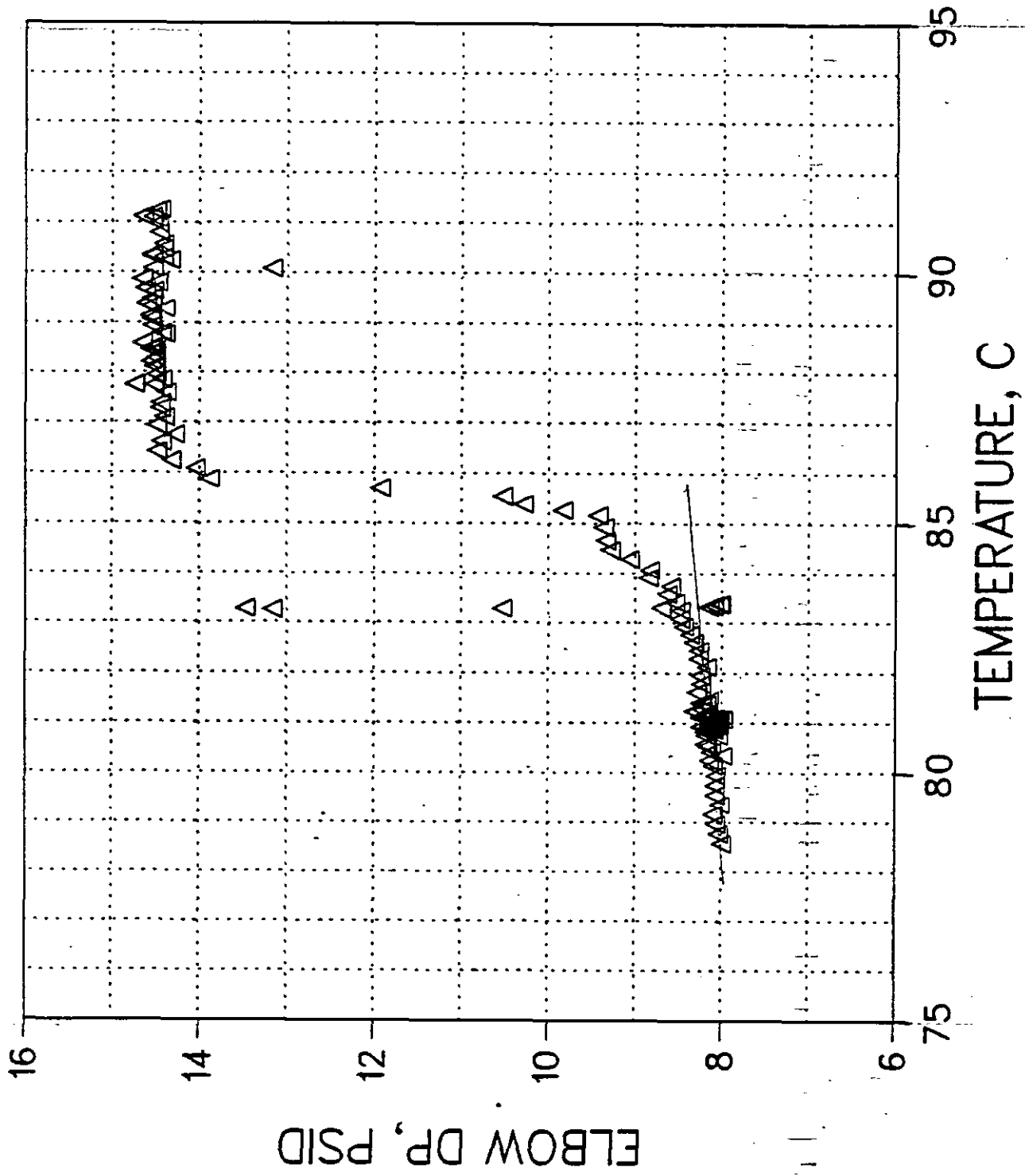
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 2



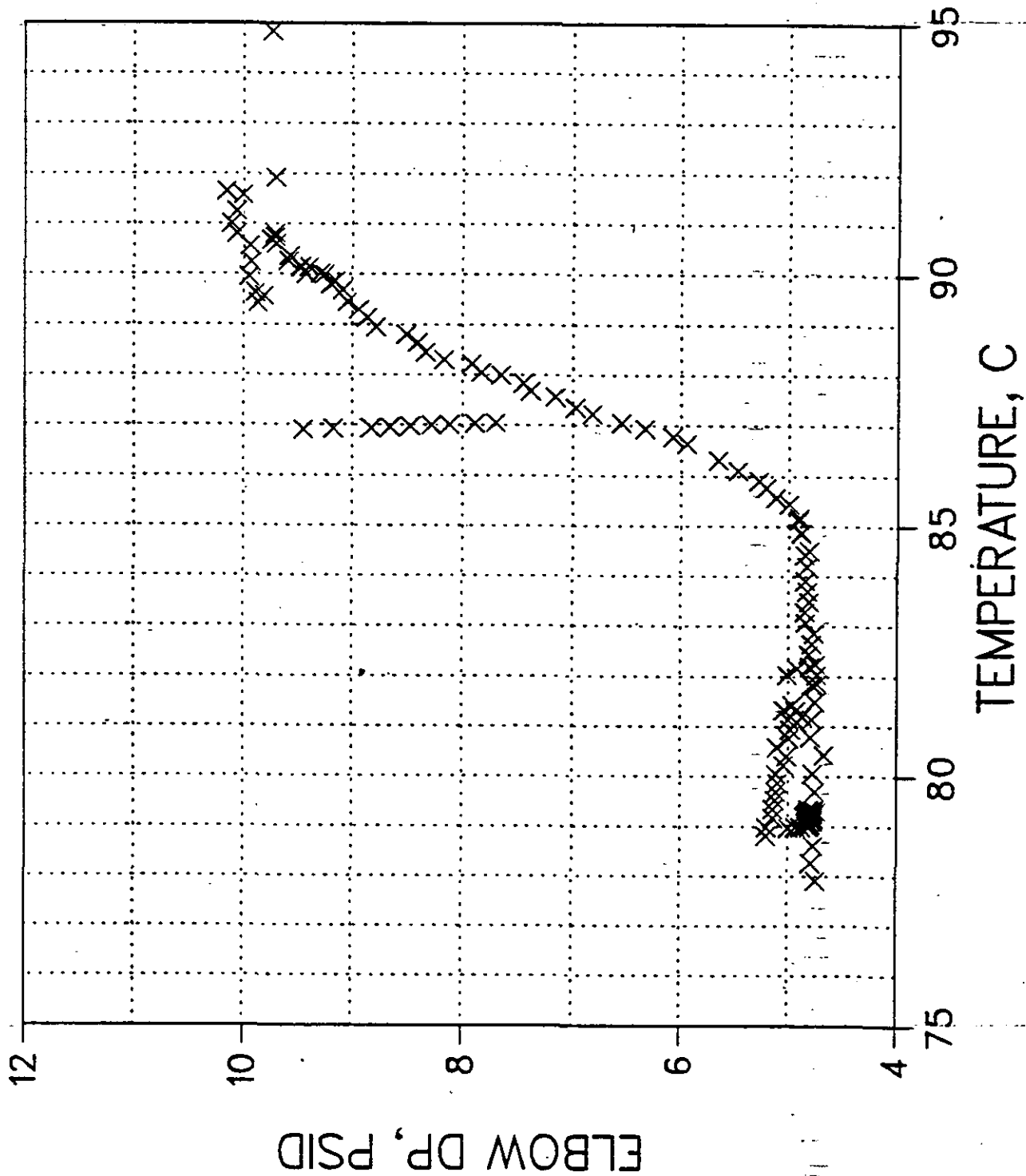
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps,3



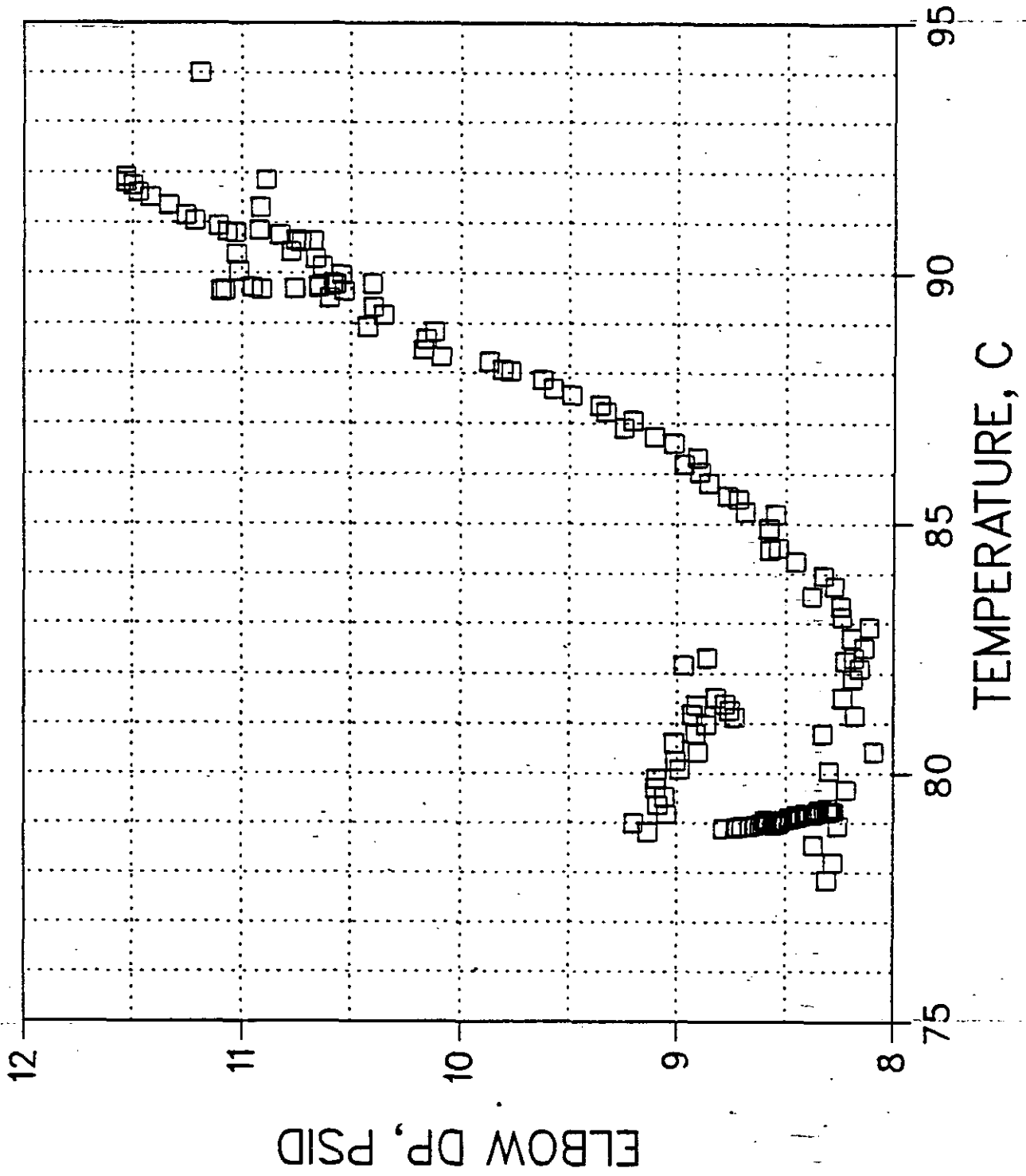
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps,3



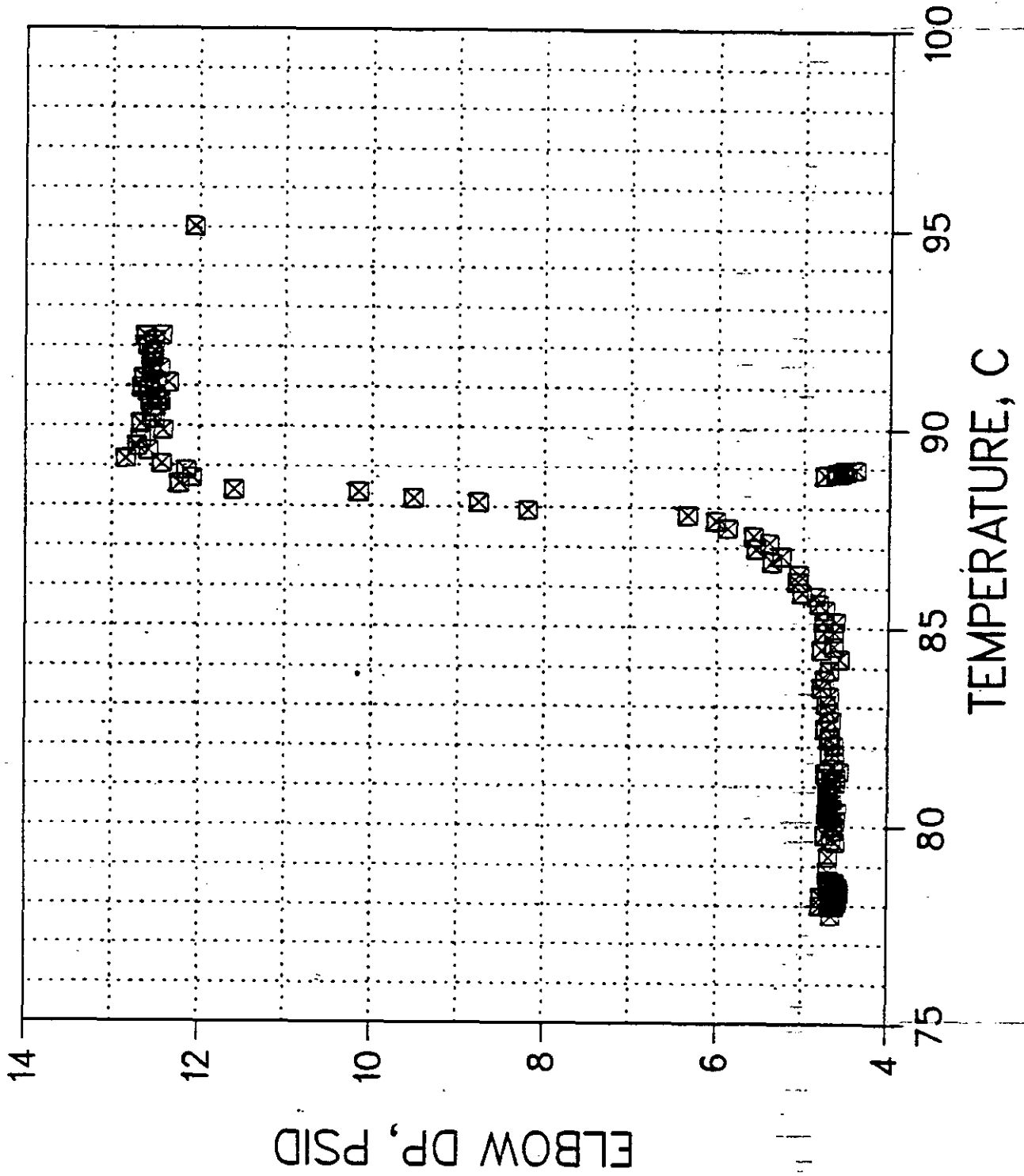
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 3



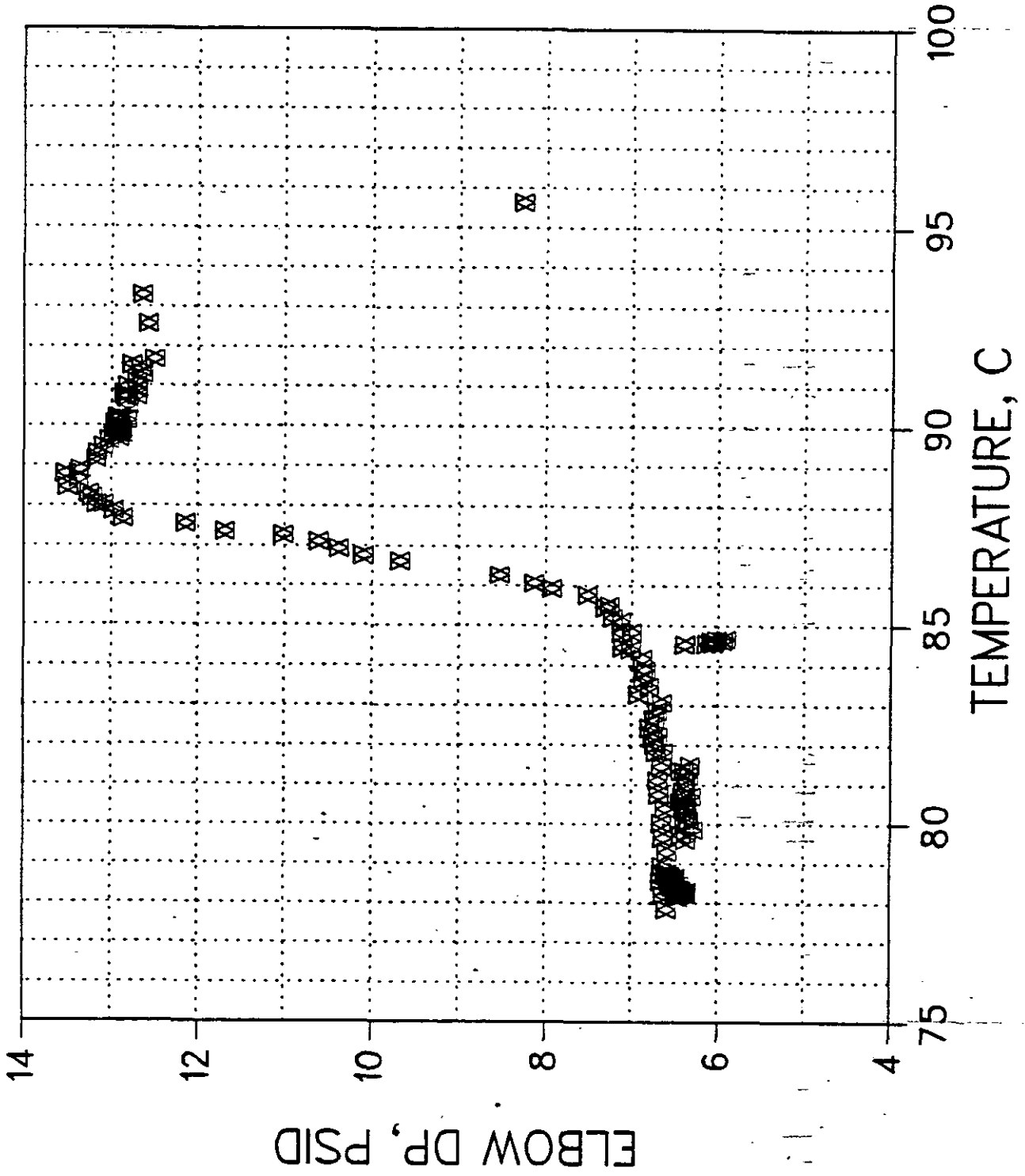
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 3



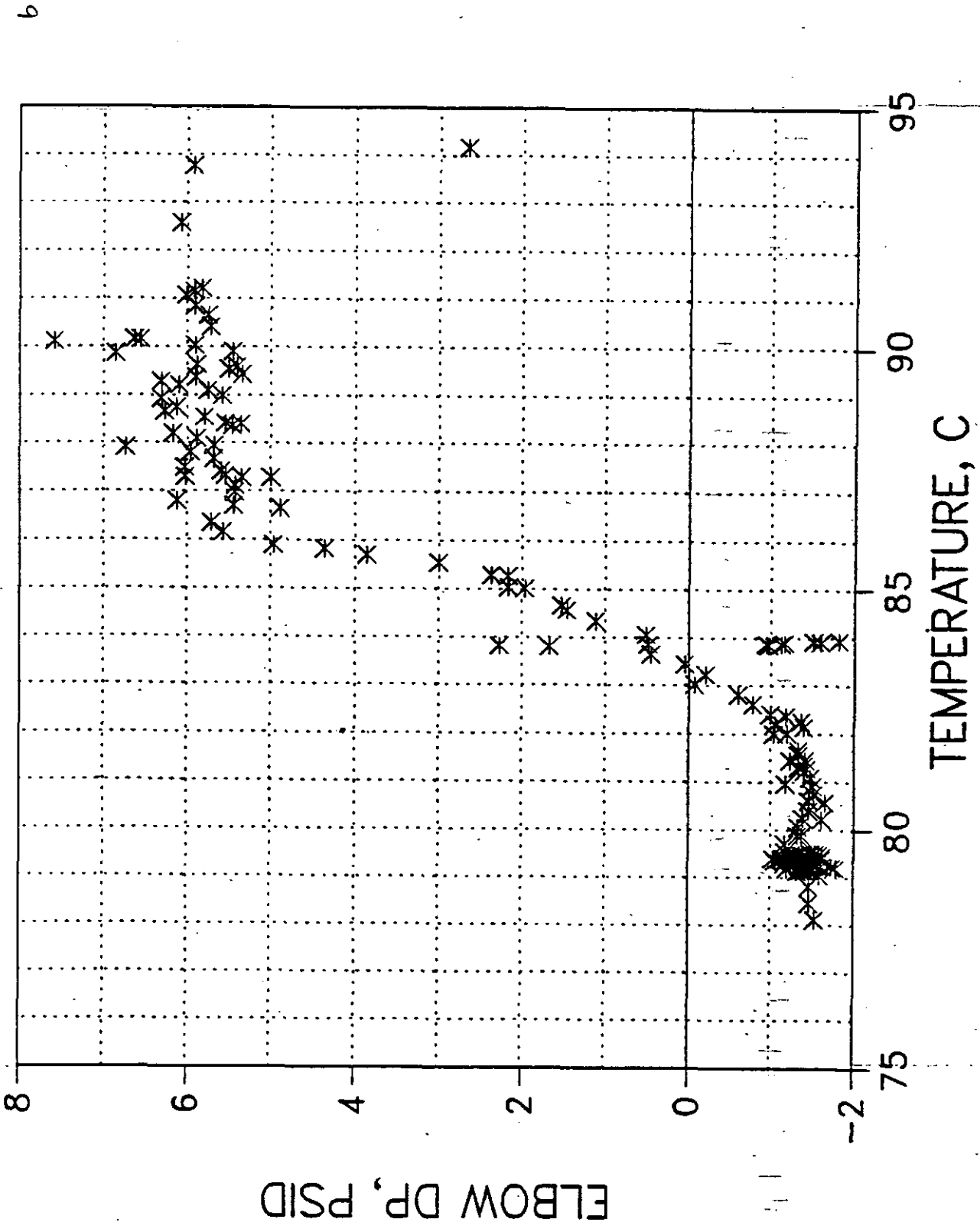
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 3



PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 3

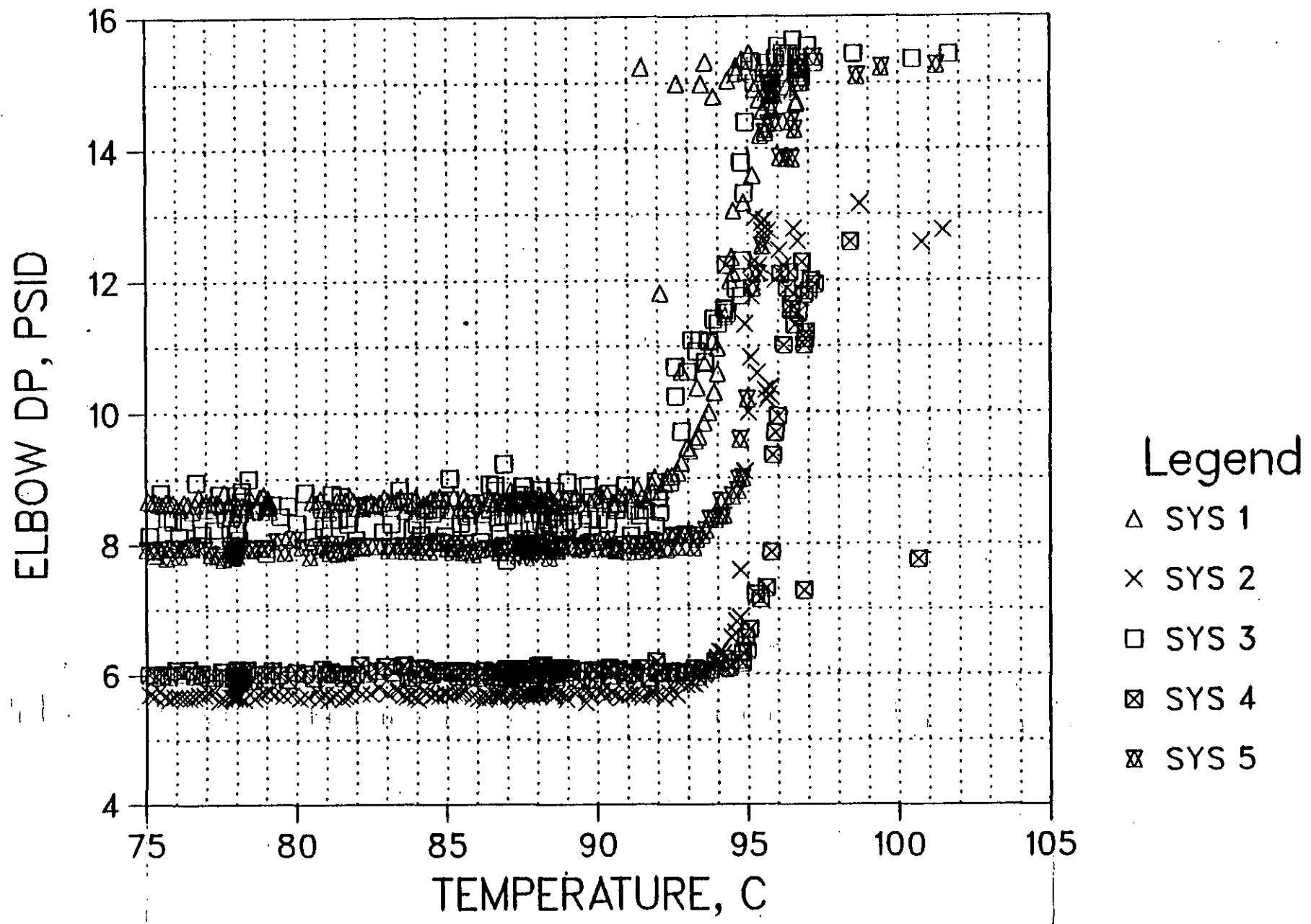


PUMP CAVITATION TESTS
UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 3



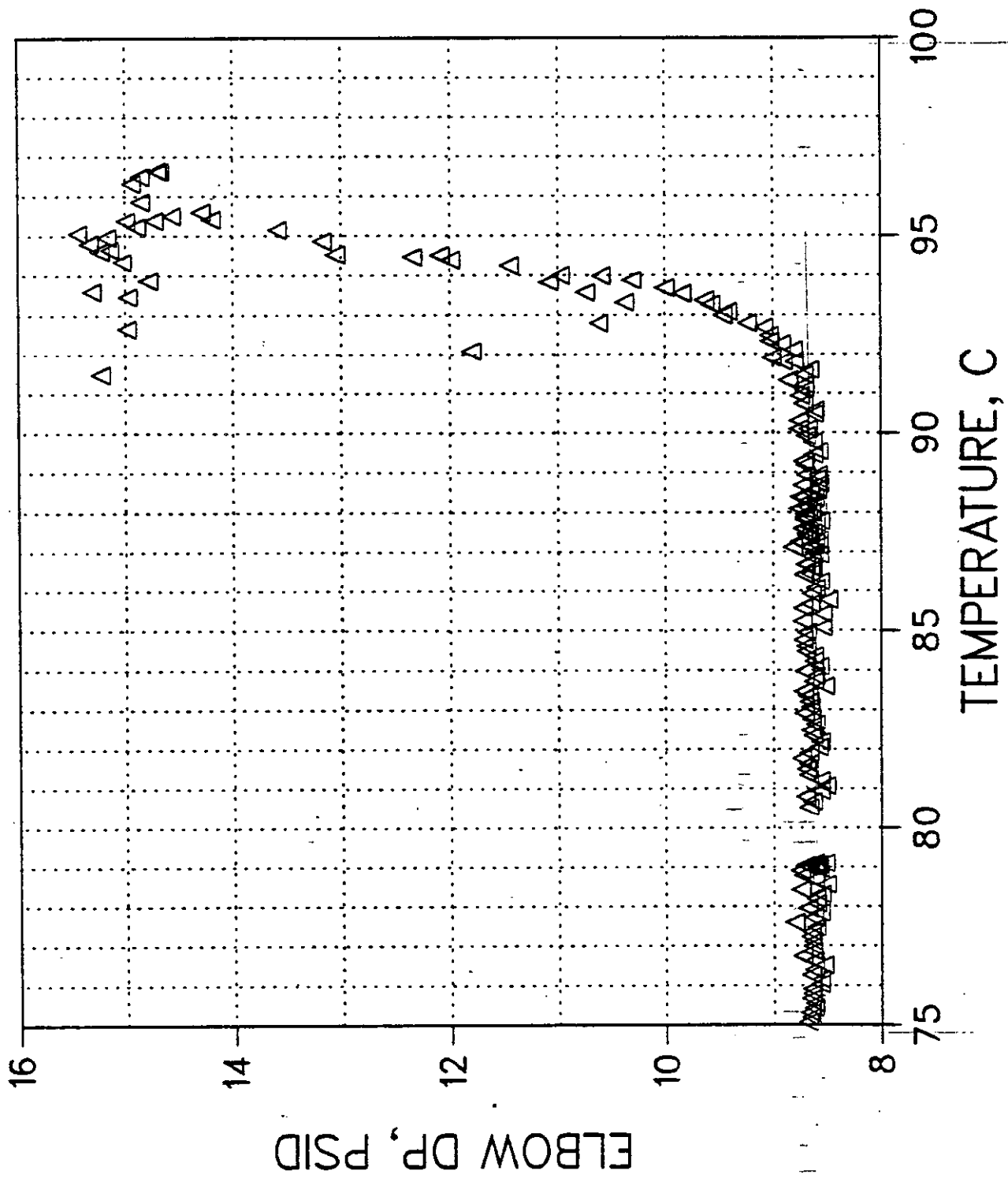
PUMP CAVITATION TESTS

UNADJUSTED TEMPERATURE VS ELBOW DP 5 pumps

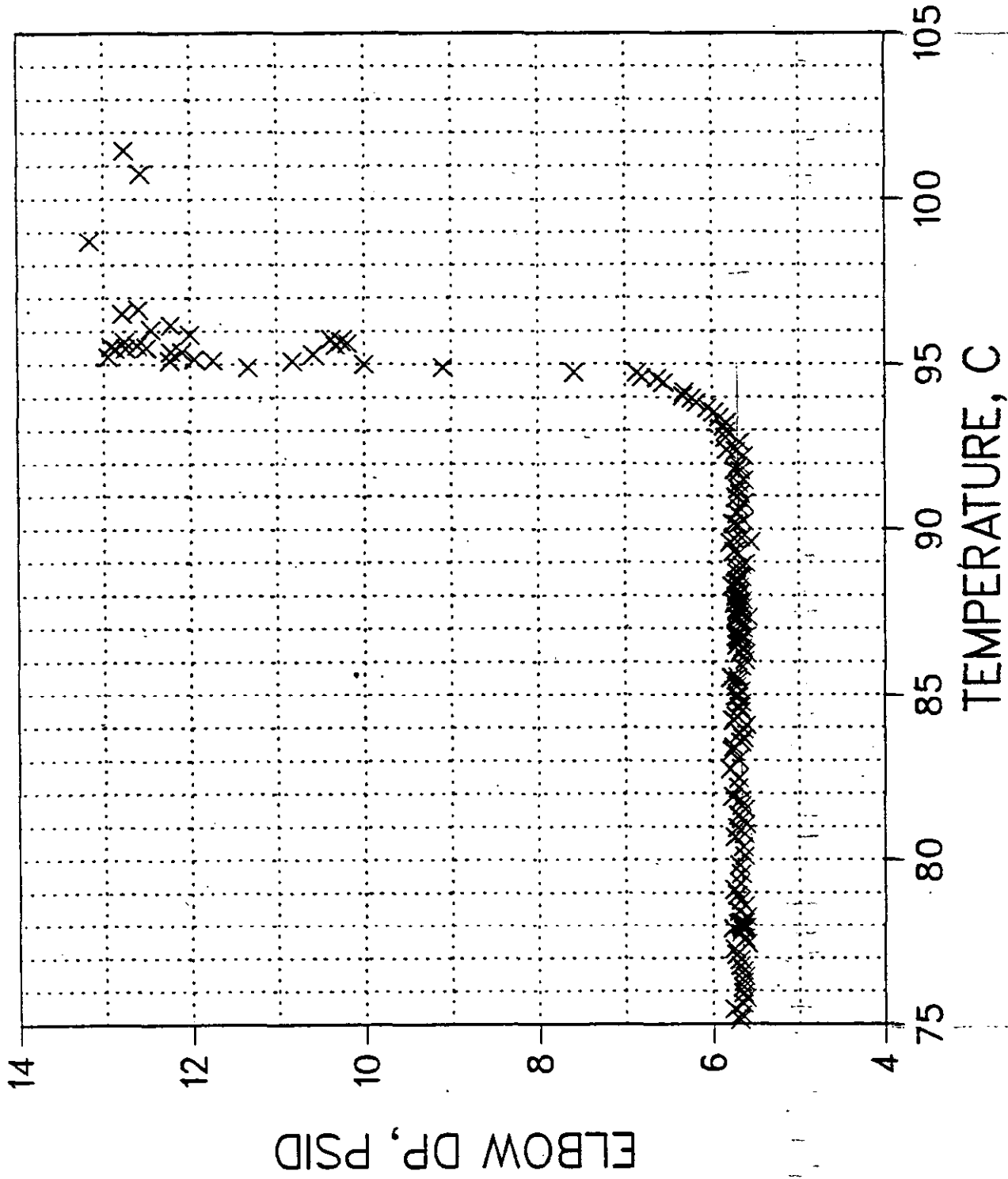


- Legend
- △ SYS 1
 - × SYS 2
 - SYS 3
 - ⊠ SYS 4
 - ⊞ SYS 5

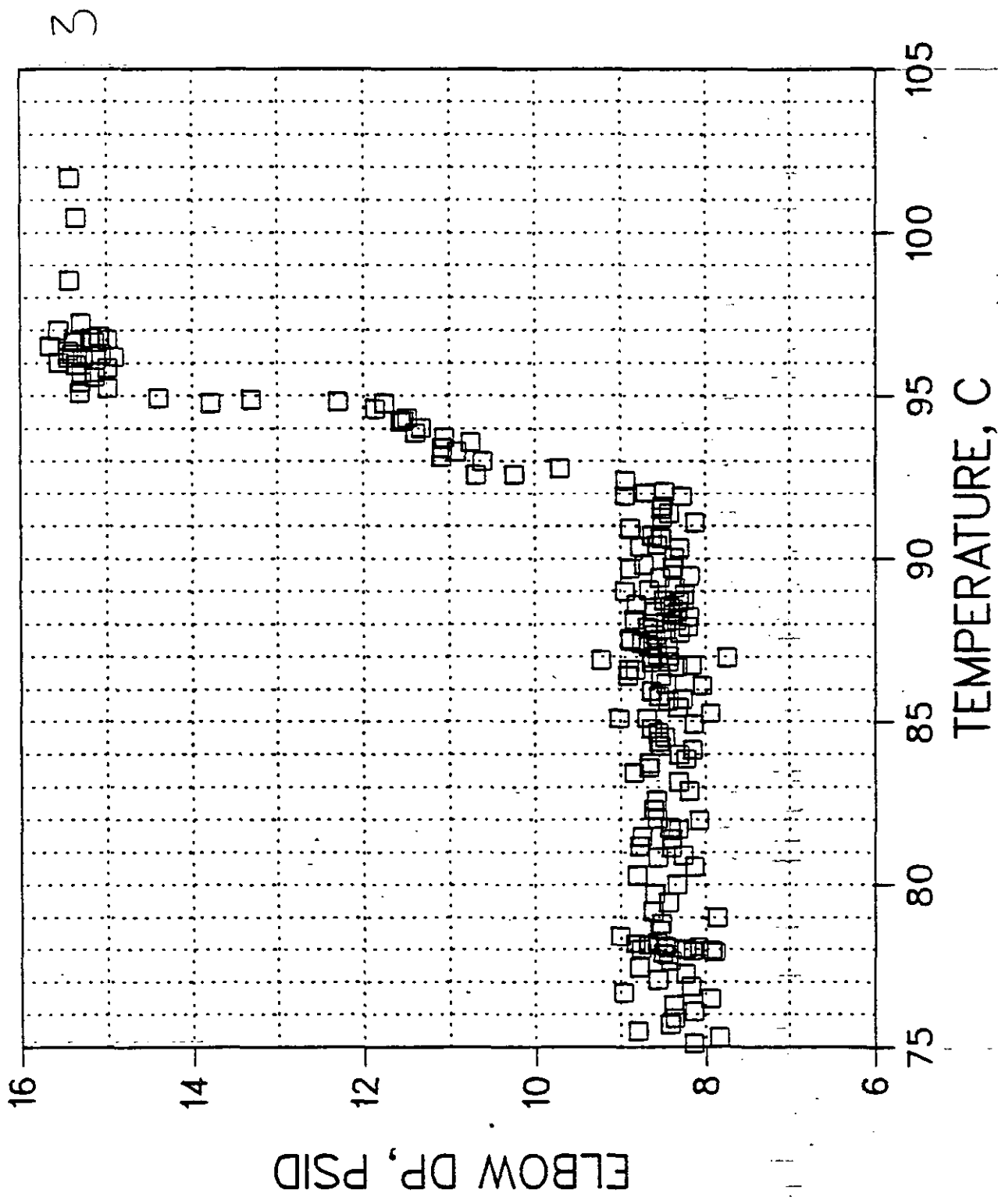
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 5 pumps



PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 5 pumps

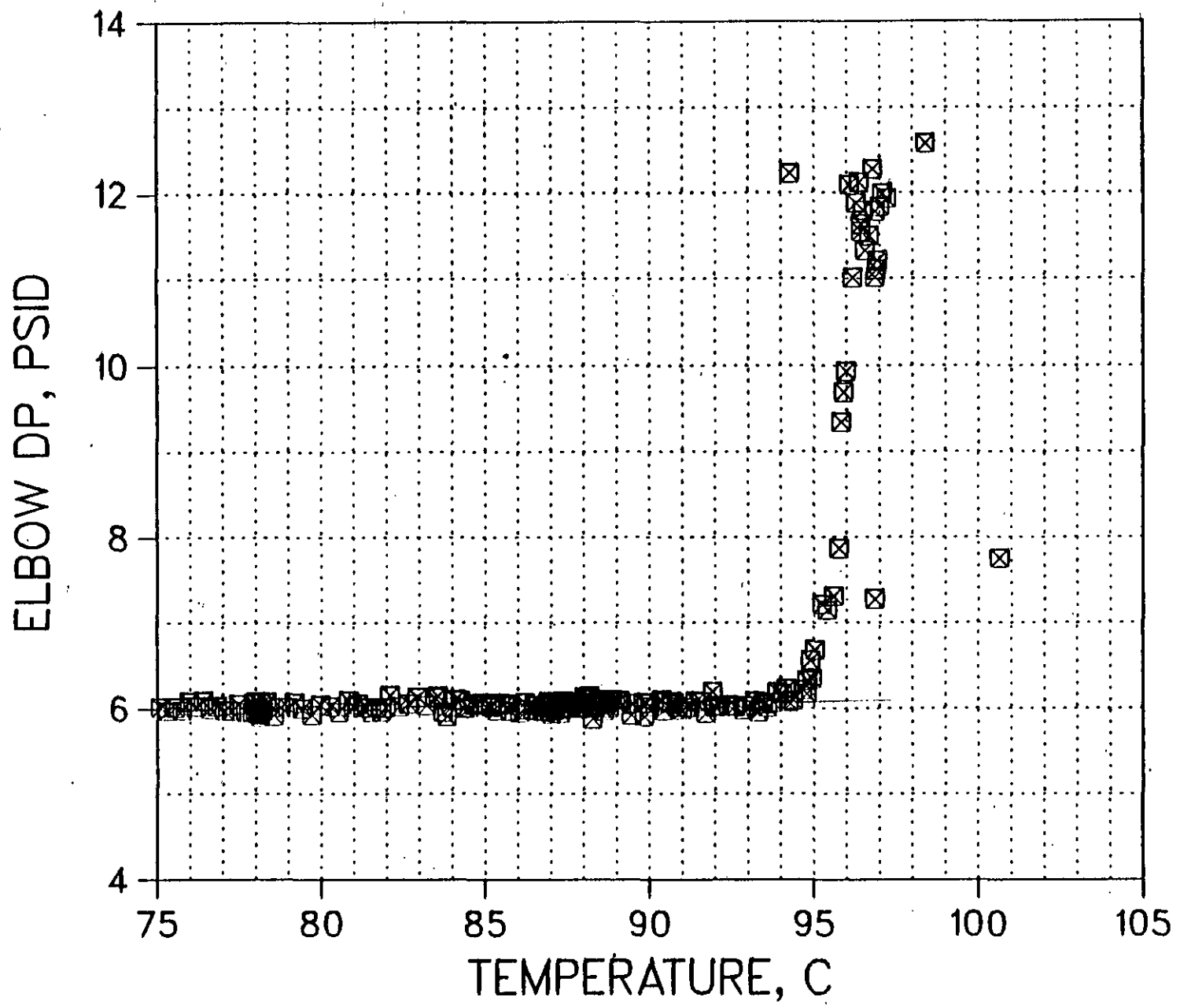


PUMP CAVITATION TESTS
UNADJUSTED TEMPERATURE VS ELBOW DP 5 pumps



PUMP CAVITATION TESTS

UNADJUSTED TEMPERATURE VS ELBOW DP 5 pumps



SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL A-5/3534-01
SERIAL NO. 94504
CAPACITY 0-250 PSID

COMPENSATED TEMPERATURE RANGE FROM 12M °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>% CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>4.9963</u>	Volts
	100	<u>10.0021</u>	Volts
Descending	50	<u>4.9991</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/8-27 NPT female
MATING ELECTRICAL CONNECTOR PT6A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER PINS E AND F PROVIDES AN OUTPUT OF 0.0163 VOLTS DC

ACCEPTED AND CERTIFIED

Michael J. Lucas

DATE

7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL 2/3533-01
SERIAL NO. 97617
CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE FROM 12M °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>% CAPACITY</u>	<u>OUTPUT</u>
	0	<u>0</u> Volts
Ascending	50	<u>4.9946</u> Volts
	100	<u>10.0012</u> Volts
Descending	50	<u>4.9983</u> Volts
	0	<u>0</u> Volts

PRESSURE PORT FITTING 1/4-18 NPT

MATING ELECTRICAL CONNECTOR PT6A-10-68

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
TERMS E AND F PROVIDES AN OUTPUT OF 0.0116 VOLTS DC

ACCEPTED AND CERTIFIED

Michael J. Jucum

DATE

7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL 2/3533-01
SERIAL NO. 97606
CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE FROM RM °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>% CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>5.0000</u>	Volts
	100	<u>10.0034</u>	Volts
Descending	50	<u>5.0016</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/4 - 18 NPT

MATING ELECTRICAL CONNECTOR PT6A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS E AND F PROVIDES AN OUTPUT OF 0.0034 VOLTS DC

ACCEPTED AND CERTIFIED Michael J. Jansen

DATE 7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL Z/3533-01
SERIAL NO. 97605
CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE FROM 12M °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>% CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>4.9936</u>	Volts
	100	<u>10.0001</u>	Volts
Descending	50	<u>4.9970</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/4-18 NPT

MATING ELECTRICAL CONNECTOR PT6A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS E AND F PROVIDES AN OUTPUT OF 0.0193 VOLTS DC.

ACQUITS AND CERTIFIES

Michael J. Jansen

DATE

7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL 2/3533-01
SERIAL NO. 97607
CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE FROM 12M °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>% CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>4.9958</u>	Volts
	100	<u>10.0002</u>	Volts
Descending	50	<u>4.9968</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/4 - 18 NPT

MATING ELECTRICAL CONNECTOR PT6A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS E AND F PROVIDES AN OUTPUT OF 7.9936 VOLTS DC

ROUTED AND CERTIFIED Michael J. Jenson

DATE 7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL Z/3533-01
SERIAL NO. 97616
CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE FROM 12M °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>% CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>4.9979</u>	Volts
	100	<u>10.0047</u>	Volts
Descending	50	<u>4.9973</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/4-18 NPT Male
MATING ELECTRICAL CONNECTOR Pt6A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS C AND D PROVIDES AN OUTPUT OF 7.9980 VOLTS DC

ACCEPTED AND CERTIFIED Michael J. Jansen
DATE 7/8/83

*Cavitation Test
for 105-L*

*J. Cooney
Rec'd 15 July 83
PX 612078*

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-250 PSI, 0-10V Date 8-1-83
 Equipment Under Test Sensotec A5 No. 704-77
 Standard Used S/N 10568 No. S/N 1169
 Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK
 Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F
 Equipment From: Foreman J. CATHY Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .003		21	199.940	8.002	
2	25.000	.999		22	175.020	7.004	
3	50.030	2.001		23	150.000	6.001	
4	75.000	3.006		24	124.940	4.997	
5	100.075	4.006		25	100.015	3.998	
6	125.050	5.005		26	74.985	2.995	
7	149.975	6.003		27	50.040	1.996	
8	174.955	7.003		28	25.050	.999	
9	200.030	8.006		29	00.000	.005	
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-250 PSI, 0-10V Date 8-1-83
 Equipment Under Test SENSOTEC A5 No. 94511
 Standard Used S/N 10568 r No. S/N 1169
 Range 0-250 PSI Calibration Expires 8-5-83 By E. KIRK
 Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F
 Equipment From: Foreman S. CAThey Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .012		21	199.945	7.965	
2	25.030	.986		22	175.040	6.974	
3	50.040	1.983		23	150.050	5.978	
4	75.065	2.982		24	125.000	4.978	
5	100.025	3.978		25	99.970	3.979	
6	125.080	4.978		26	75.020	2.983	
7	150.030	5.974		27	50.010	1.983	
8	175.070	6.973		28	25.040	.985	
9	200.050	7.968		29	00.000	.015	
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

122-A E 61 SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-250 PSI, 0-10V Date 8-1-83

Equipment Under Test SENSOTEC A5 No. 94509

Standard Used S/N 10568 No. S/N 1169

Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK

Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F

Equipment From: Foreman J. CATNEY Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	.009		21	199.915	8.001	
2	25.020	1.009		22	174.960	7.006	
3	50.050	2.008		23	150.025	6.010	
4	75.005	3.006		24	124.995	5.009	
5	100.015	4.007		25	99.960	4.008	
6	125.050	5.008		26	75.015	3.011	
7	150.070	6.009		27	49.910	2.007	
8	174.980	7.005		28	24.990	1.010	
9	199.980	8.003		29	00.000	.014	
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

122-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-250 PSI, 0-10 V Date 8-1-83

Equipment Under Test SENSOTEC A 5 No. 94508

Standard Used S/N 10568 r No. S/N 1169

Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK

Barometric Pressure 30" Hg Humidity _____ % Temperature 80° F

Equipment From: Foreman J. C. Atney Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .008		21	199.930	7.977	
2	25.020	.990		22	175.010	6.983	
3	50.065	1.989		23	149.990	5.982	
4	74.990	2.985		24	124.955	4.982	
5	99.980	3.983		25	99.990	3.984	
6	125.040	4.985		26	75.090	2.989	
7	150.090	5.986		27	49.985	1.986	
8	175.050	6.984		28	25.050	.992	
9	200.060	7.982		29	00.000	- .006	
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

722-A EG 1 SHOT
 CALIBRATION DATA SHEET

Unit of Measure 0-250 PSI, 0-10V Date 8-1-83

Equipment Under Test Sensotec AS No. 94510

Standard Used S/N 10568 r No. S/N 1169

Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK

Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F

Equipment From: Foreman J. EAThey Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	0.038		21	200.075	8.026	
2	24.925	1.033		22	175.005	7.027	
3	50.060	2.037		23	149.920	6.025	
4	75.020	3.036		24	125.030	5.030	
5	99.930	4.032		25	100.075	4.032	
6	124.970	5.034		26	74.965	3.027	
7	150.030	6.035		27	50.025	2.030	
8	175.030	7.032		28	24.970	1.027	
9	199.983	8.028		29	00.000	0.031	
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-250 PSI, 0-10V Date 8-1-83
 Equipment Under Test Sensotec AS No. 73827
 Standard Used S/N 10568 No. S/N 1169
 Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK
 Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F
 Equipment From: Foreman J. EAThey Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	.009		21	199.990	8.001	
2	25.000	1.008		22	175.020	7.003	
3	50.050	2.009		23	150.015	6.003	
4	74.990	3.005		24	125.015	5.002	
5	100.055	4.008		25	100.035	4.003	
6	124.960	5.003		26	75.070	3.004	
7	150.055	6.007		27	50.075	2.004	
8	174.980	8.002		28	20.085	1.004	
9	200.040	7.001		29	00.000	.007	
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

Unit of Measure 0-250 PSI, 0-10 V Date 8-1-83
 Equipment Under Test SENSOTEC A5 No. 94504
 Standard Used S/N 10568 No. S/N 1169
 Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK
 Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F
 Equipment From: Foreman S. CAThey Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	.009		21	200.040	8.007	
2	25.080	1.009		22	174.960	7.004	
3	50.030	2.005		23	150.080	6.009	
4	75.070	3.007		24	124.890	5.000	
5	100.070	4.007		25	100.060	4.007	
6	125.000	5.003		26	75.060	3.007	
7	150.010	6.004		27	50.040	2.007	
8	174.990	7.004		28	25.040	1.008	
9	200.055	8.007		29	00.006	.011	
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

CALIBRATION DATA SHEET

Unit of Measure 0-50 PSIA, 0-10Y

Date 8-2-83

Equipment Under Test SENSOTEC Z

No. 97607

Standard Used S/N 10568

r No. S/N 1169

Range 0-200 PSI Calibration Expires 8-5-83

By E. KIRK

Barometric Pressure 29.96" Hg Humidity _____

% Temperature 75°F

Equipment From: Foreman P. A. Mey

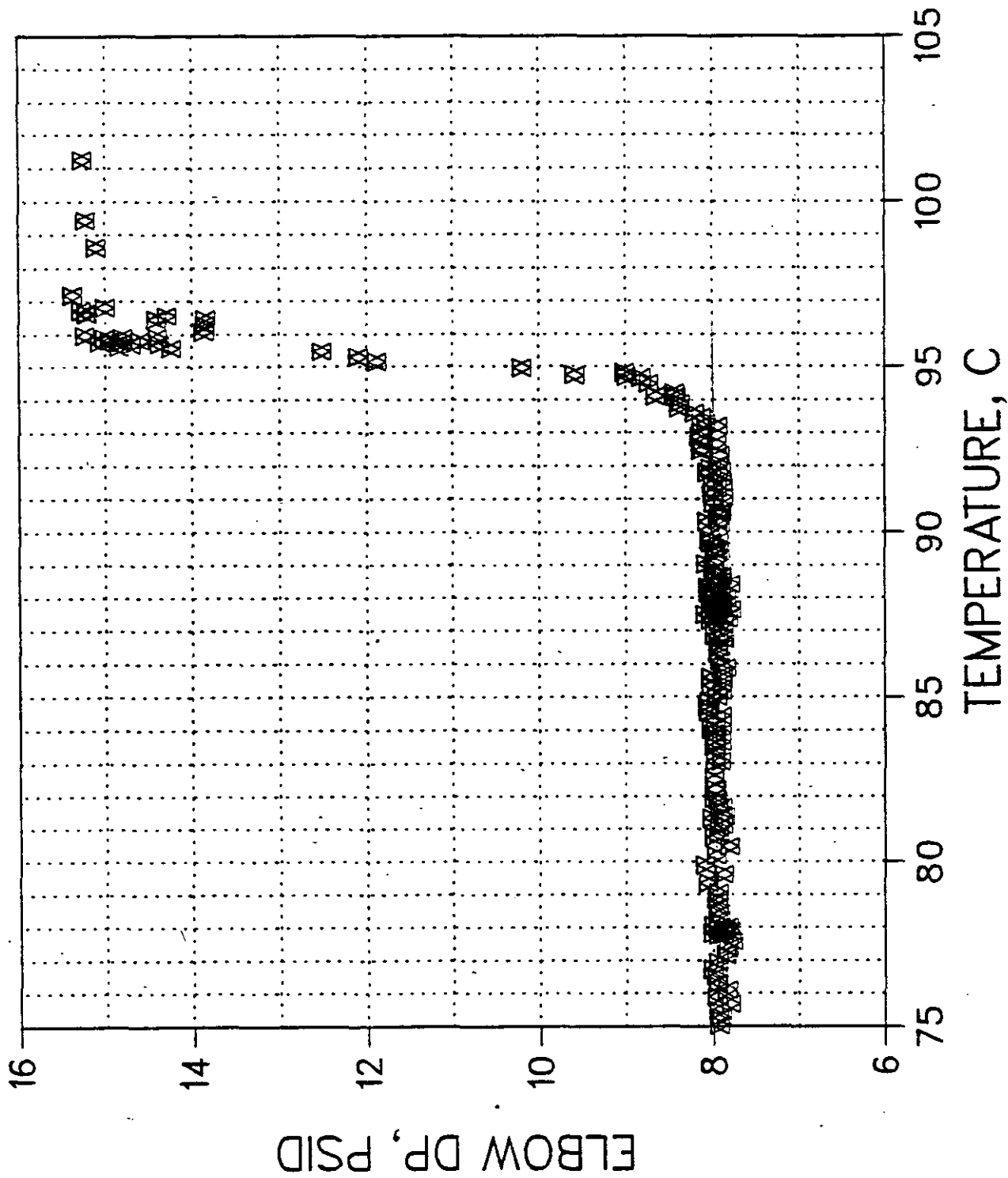
Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.006	- .014		21	49.930	10.012	
2	14.710	2.877		22	39.946	8.011	
3	14.975	3.996		23	30.040	6.023	
4	30.030	6.013		24	14.940	3.998	
5	40.030	8.022		25	14.710	2.910	
6	50.040	10.031		26	00.000	- .005	
7				27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

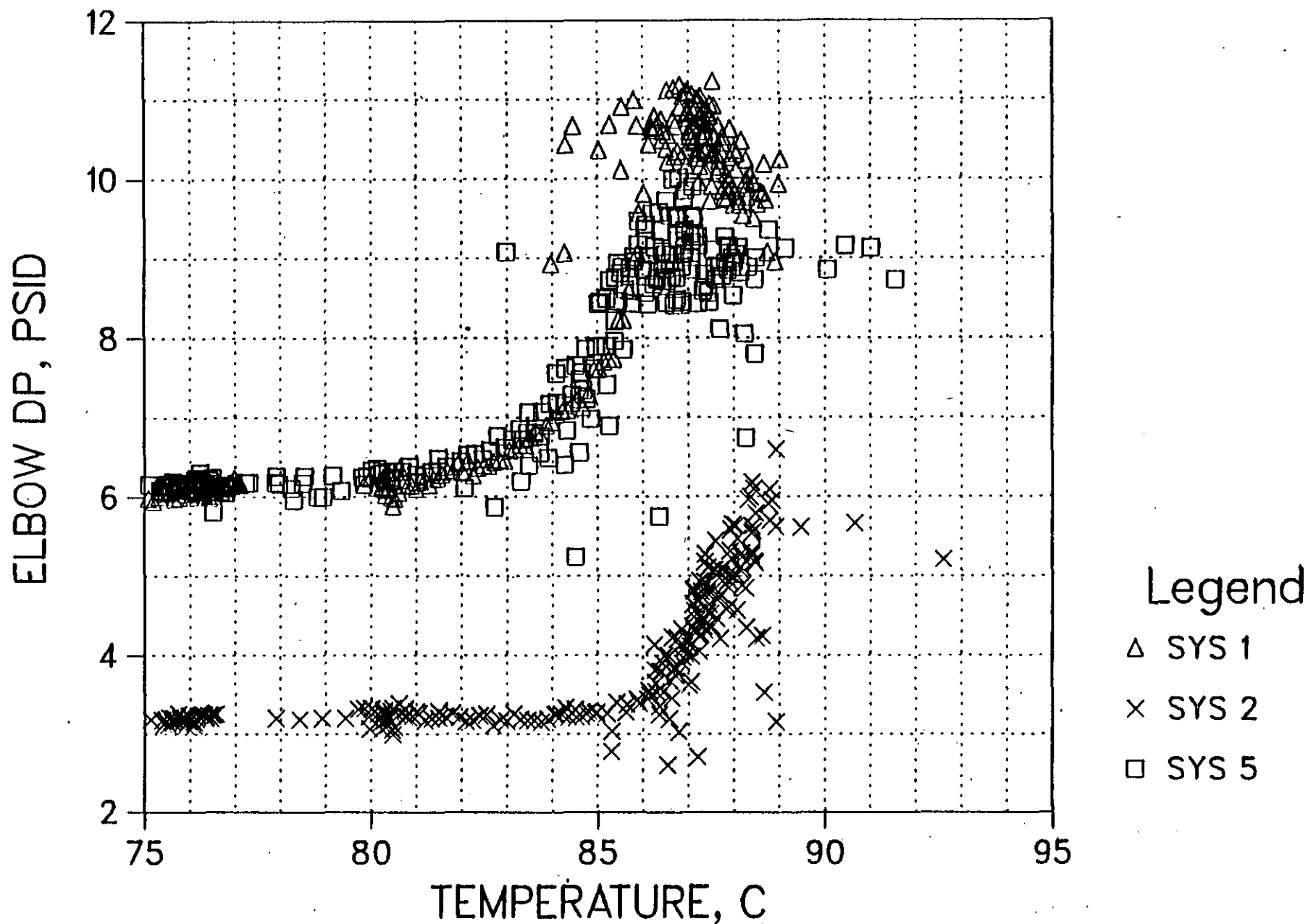
This not set no other data sheets
 Emory Kirk sent over a day later

PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 5 pumps

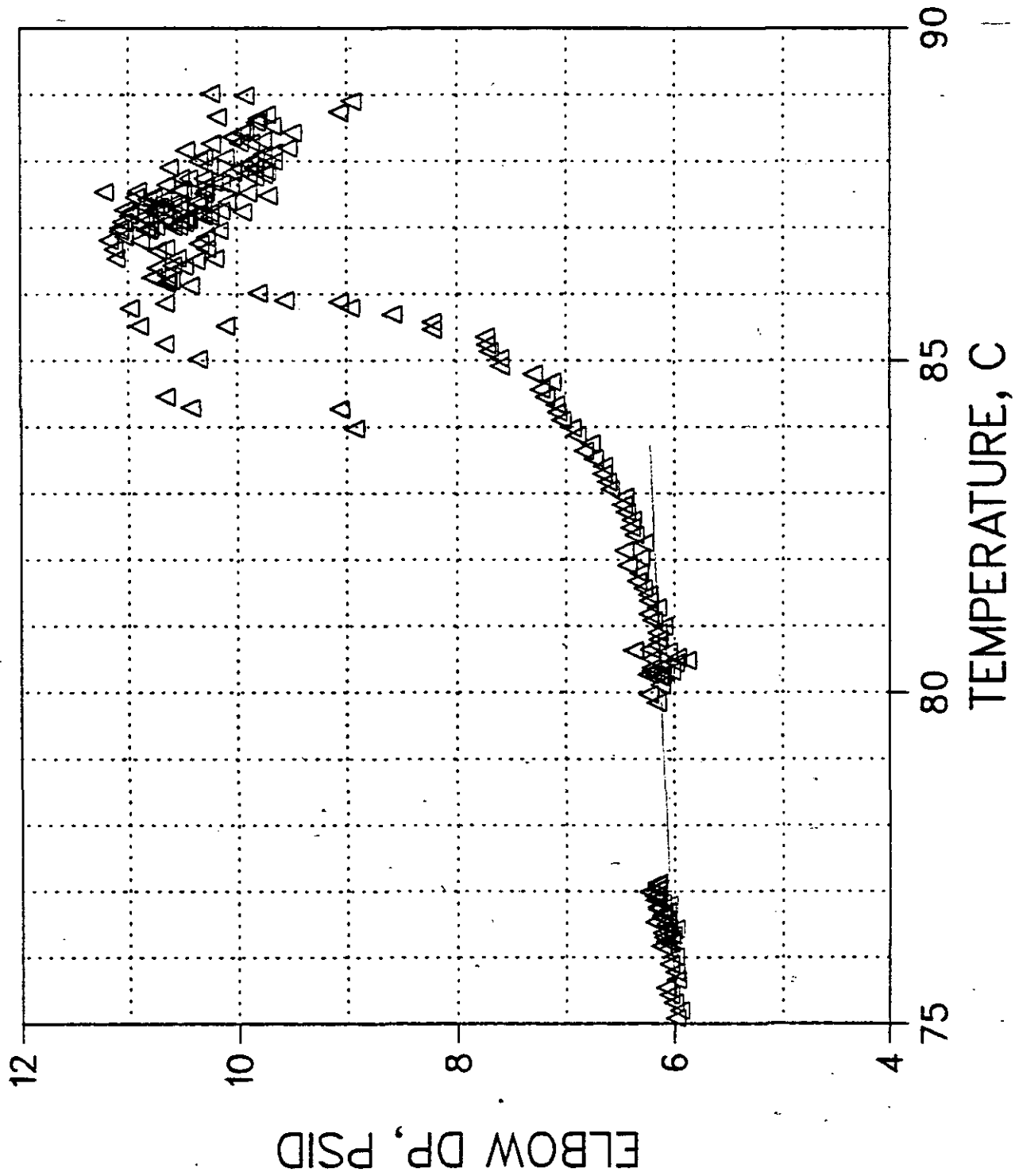


PUMP CAVITATION TESTS

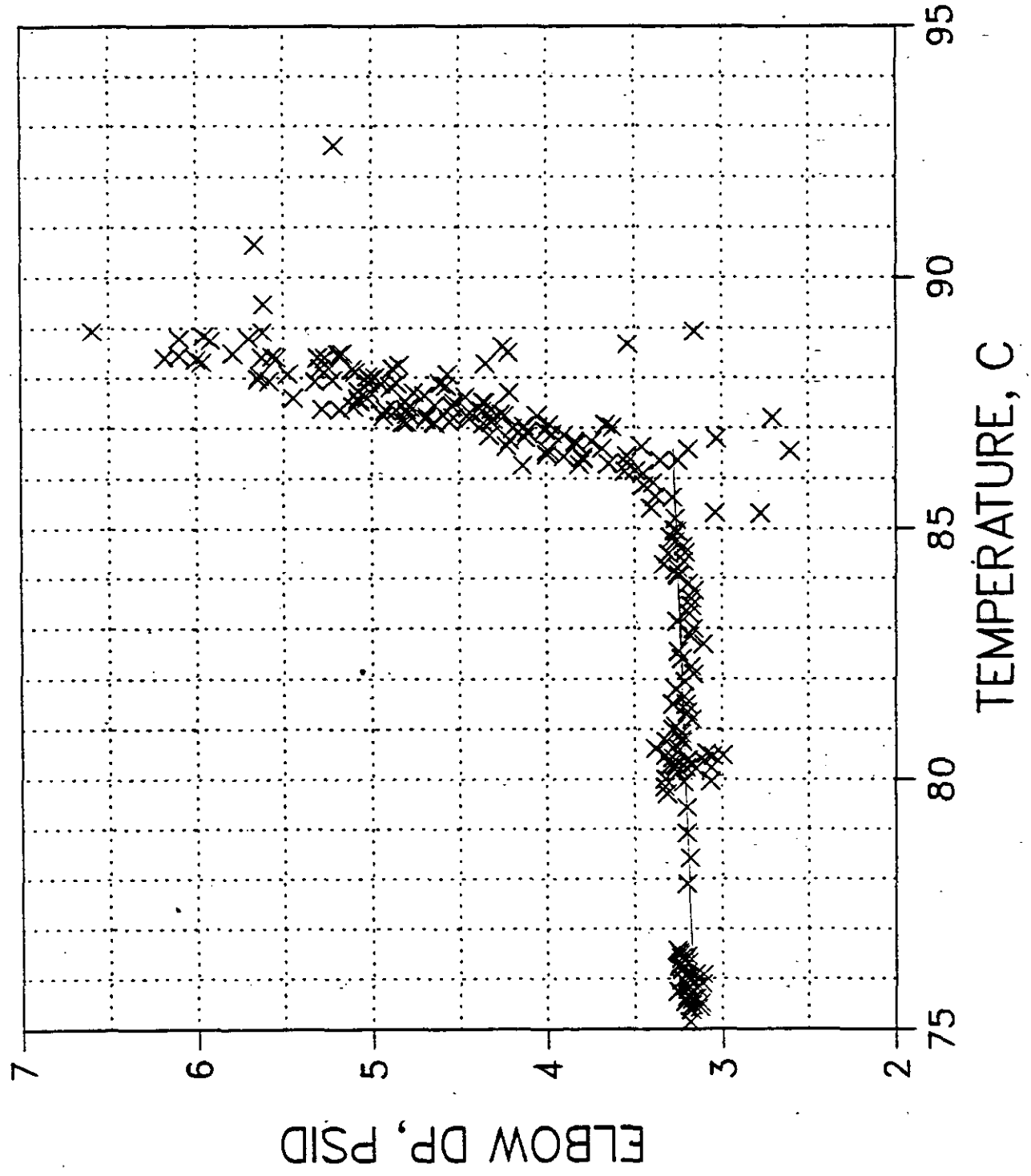
UNADJUSTED TEMPERATURE VS ELBOW DP 3 pumps



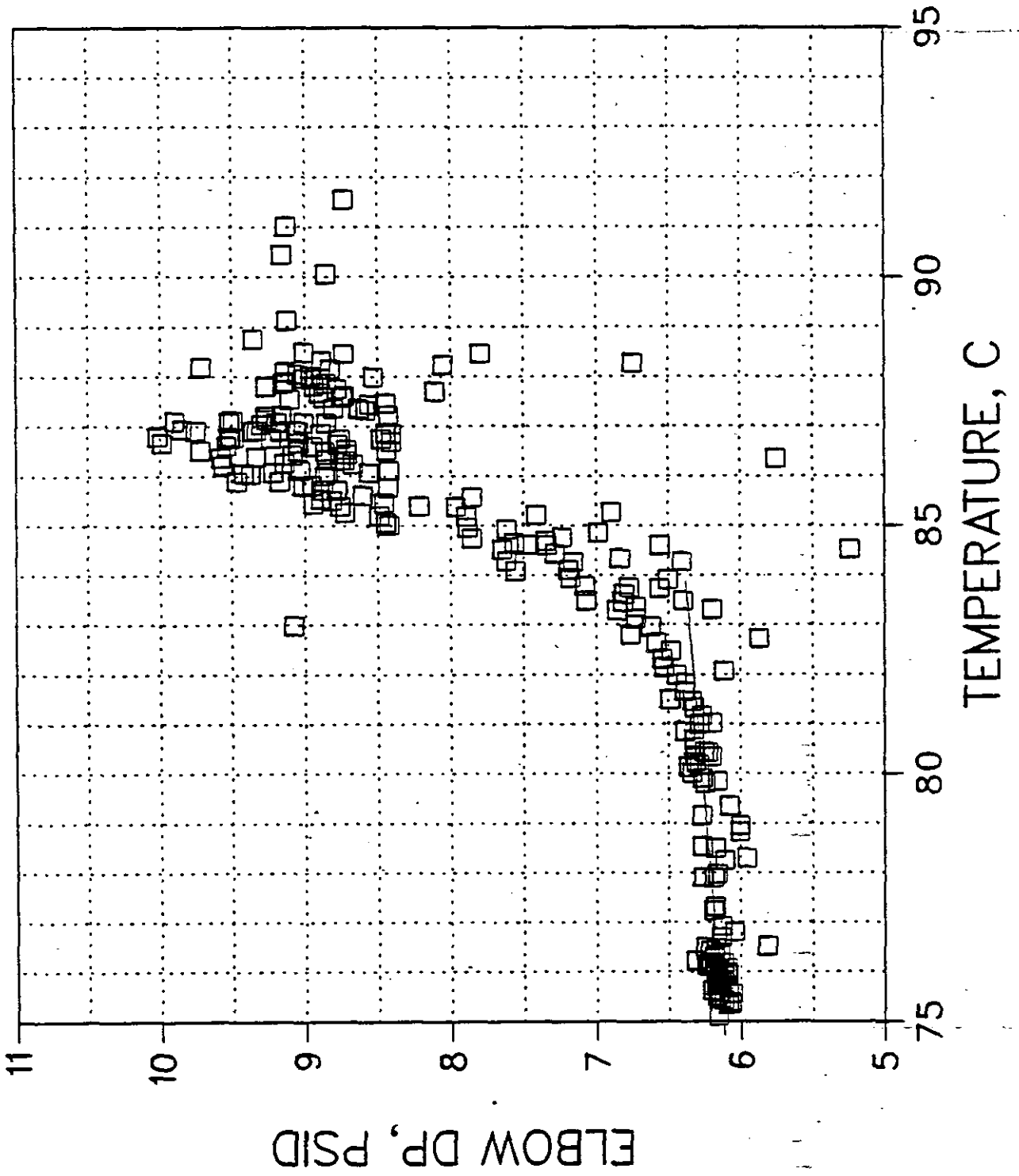
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 3 pumps



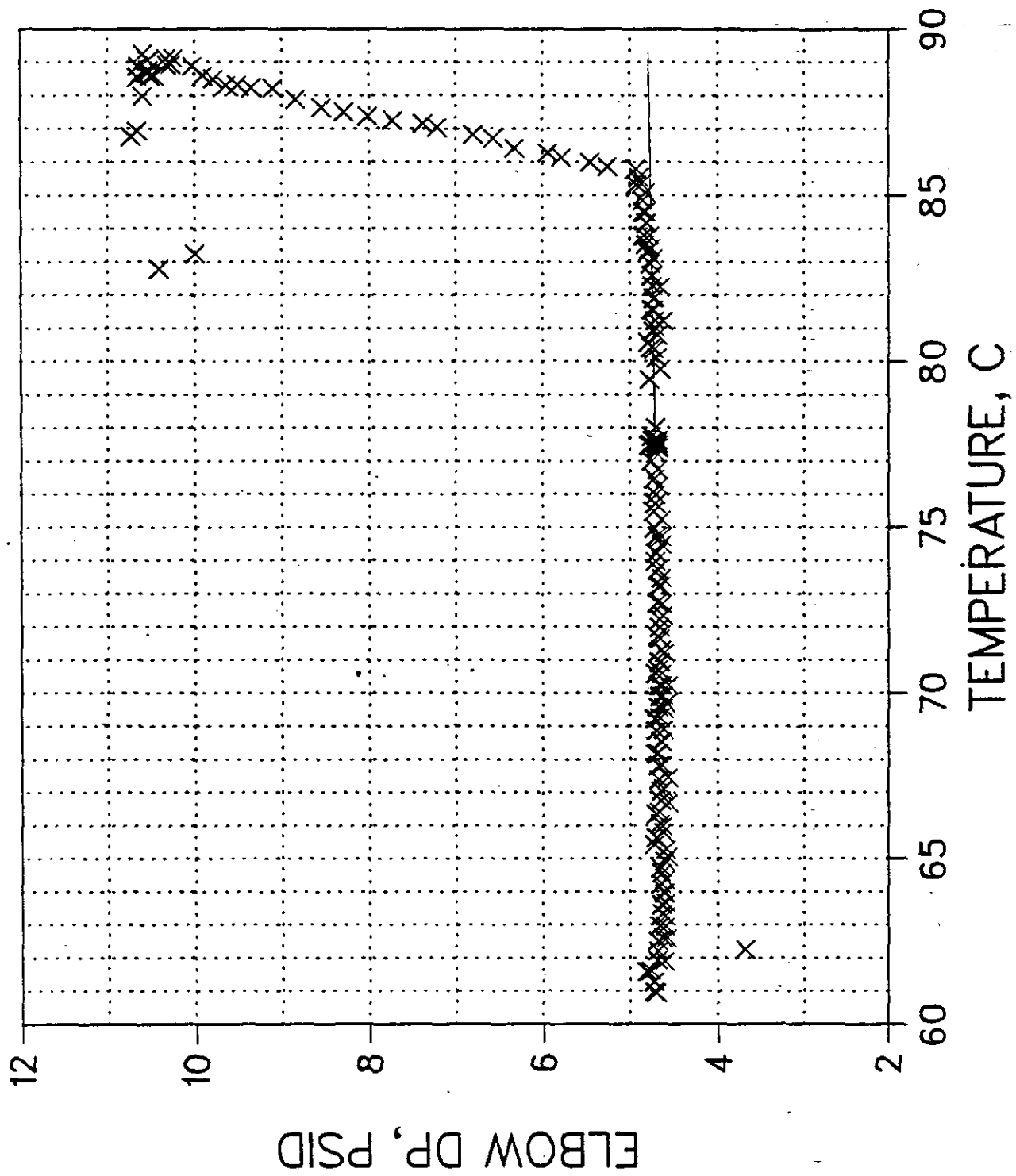
PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 3 pumps



PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 3 pumps



PUMP CAVITATION TESTS UNADJUSTED TEMPERATURE VS ELBOW DP 6 pumps, 1



Appendix B - Data Adjustment Procedure

To calculate the operating limits the L-Area test data had to be corrected to normal condition of a full tank and 5.0 psig of blanket gas pressure. The following procedure was automated in the program listed in this appendix.

- 1) $P_{\text{saturation in test}} = [(6.4537 - 0.3977(228.3315 - T_{\text{Test}})^{1/2})^4]$
- 2) $P_{\text{adjustment}} = \text{blanket gas pressure} + (19.2 - \text{Tank Level})$
- 3) $P_{\text{operating}} = P_{\text{saturation in test}} + P_{\text{adjustment}}$
- 4) $T_{\text{operating}} = -34.9645 + 81.9577 (P_{\text{operating}})^{1/4} - 6.3218 (P_{\text{operating}})^{1/2}$

All pressures are in psi, temperatures in °C, and the tank level is in feet. Equations (1) and (4) are univalued fits of the D₂O saturation curve obtained from J. P. Morin, SRL.

C) Calibration Data

This appendix contains the following calibration data for QA purposes.

1. Calibration for effluent line RTDs.
2. Calibration of atmospheric pressure transducer.
3. Calibration and identification of 0-25 psig, 0-250 psid, 0-50 psia transducers.

cc: J. W. Joseph, 703-A
R. R. Butterworth, 723-A
M. M. Widener, 105-L
M. T. Cox, 704-L
T. C. Sealy, 704-L
~~_____~~
J. L. Jones, 706-C
J. L. Cathey, 723-A
C. M. Schaumann, 706-C
V. D. Vandervelde, 706-C

October 12, 1983

TO: D. R. MUHLBAIER, 704-L

FROM: A. W. GARTNER, 723-A *awg*

PUMP SUCTION RTD CALIBRATION

References: 1) "L-Area RTD Calibration", DSIWI to J. L. Cathey from D. R. Muhlbaier, 9/30/83.
2) L-Area Pump Suction RTD Calibration Test Results (attached).

Introduction

Accurate pump suction temperature is important to efficient reactor operation. It was desirable to verify the calibration of the pump suction RTDs.

Summary

Calibration was accomplished during the week of October 3rd using an NBS traceable RTD and a temperature bath. Data points were taken at approximately 30, 70, and 90°C. It was desired to obtain differences of less than 0.3°C. With the exception of pump #4 and the low temperature readings, results were within a few hundredths of a degree.

Discussion

The low measurement error was higher than the error for the mid and the high measurements. This did not cause any concern

because, they were still within the desired accuracy, all pumps were similiar, and the reactor would not normally be operating in this range.

The measurements for pump #4, though within the desired accuracy range, deviated greatly from the other pumps. Reactor Tech adjusted the offset by 0.18°C in the control computer and the test was run again. The results are now accurate and comparable with the other pumps.

L-AREA PUMP SUCTION RTD CALIBRATION TEST RESULTS

<u>Pump #</u>	<u>Control Computer (°C)</u>	<u>Known RTD (°C+/-0.01°C)</u>	<u>Difference (°C)</u>
5	30.68	30.60	0.08
	70.40	70.39	0.01
	93.97	93.97	0.00
6	30.65	30.58	0.07
	72.16	72.17	-0.01
	92.85	92.85	0.00
1	25.24	25.18	0.06
	71.11	71.14	-0.03
	93.59	93.61	-0.02
2	26.17	26.05	0.12
	51.90	51.86	0.04
	72.29	72.26	0.03
	95.76	95.78	-0.02
4* (1st run)	26.14	26.25	-0.11*
	70.80	70.97	-0.17*
	90.58	90.76	-0.18*
3	23.32	23.23	0.09
	71.14	71.13	0.01
	90.77	90.78	-0.01
4 (2nd run)	24.55	24.47	0.08
	71.62	71.60	0.02
	90.14	90.13	0.01

* Original measurements yielding results inconsistent with the other pumps.

AWG

RMS

STANDARDS LAB CALIBRATION SHEET

STD. NO TR-420 . CALIBRATION DATE 10/83 . CALIBRATOR GCL

EXPIRATION DATE 10/84 CALIBRATION FREQUENCY 12 MO.

SL EQUIPMENT USED SL-138A

NBS TEST NO. N/A

CALIBRATION UNCERTAINTY IS .1% UNCERTAINTY OF CALIB. GAGE IS .25%

PROCEDURE USED IS DPSTOM - 72 - 311 TYPE GAGE CALIBRATED TRANSDUCER

135

SL-138A	READING PSI	IN/HG	WESTON READING
	0	29.76	3854
	.2	30.17	4082
	.4	30.58	4308
	.6	30.99	4483
	.8	31.40	4658
	1.0	31.80	4828
	1.2	32.21	5118

BAROMETER PRESSURE 29.76

POWER SUPPLY READING 28.08V

CERTIFIED BY *George W. Cooney*



INC. TECHNICAL SALES REPRESENTATIVES

PRICE QUOTATION

DMS 10647

J. K. Kelly

TO: Mr. Tommy Sessions
E. I. Dupont
Savannah River Plant
Building 723A
Aiken, SC 29808

DATE	5/10/83
YOUR INQUIRY NO.	Verbal
PROPOSED SHIPPING DATE	4-6 weeks ARO
TERMS	Net 30 days
F.O.B.	Columbus, OH
TO BE SHIPPED VIA	Best Way
THIS QUOTATION VALID FOR 30 DAYS.	

GENTLEMEN:

WE APPRECIATE THE OPPORTUNITY OF MAKING THE FOLLOWING PROPOSAL AND QUOTATION.

ITEM	QUAN.	DESCRIPTION	UNIT PRICE	TOTAL
A.	9	<u>Sensotec Type Z Pressure Transducer with Amplifier Output and Mating Connector</u> Range: 0-50 psia Output: 0-10 VDC Accuracy: ±0.25% of full scale	\$550.00	\$ 4,950.00
B.	6	<u>Sensotec A-5 Differential Pressure Transducer with Amplifier Output and Mating Connector</u> Range: 0-250 psid Output: 0-10 VDC Accuracy: ±0.5% of full scale	\$740.00	\$ 4,440.00
C.	2	<u>Sensotec Z Type Pressure Transducer with Amplifier Output and Mating Connector</u> Range: 0-25 psig Output: 0-10 VDC Accuracy: ±0.25% of full scale All other specifications on these transducers as per Pages 4, 5, 6, & 7 of the enclosed catalog. A photograph showing the 0-50 and the 0-25 transducers is on the lower left corner of <u>Page 4</u> . On the lower left corner of <u>Page 7</u> , there is a photograph of the differential transducer and its amplifier. The amplifiers that are shown are actually a part of transducer in that it slips inside of that extended "can". These transducers will be temperature compensated to operate at 95°C. The mating connector that I am talking about would mate directly to the Bendix connection which is clearly shown in the drawings on the bottom half of Page 5. That is the transducer connection and we are offering the mate that goes with that. In your	\$565.00	\$ 1,130.00

Connector Number P106A-10-65

SESCO, INC.

PAGE 1 OF 2 PAGES

Prices shown are applicable ONLY to the quantities quoted herein. Any change in quantity or deletion of one or more items may require quotation revision. All prices are subject to the approval of the manufacturer.

Daryl Swiss
Daryl Swiss
* Daryl 7/1 95° temp comp → no significant error until that temp is reached
20 May 83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL Z/3533-01

SERIAL NO. 97609

CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE FROM 12M °F TO 203 °F

WIRING CODE

- A.) +15 VOLTS IN
- B.) COMMON
- C.) -15 VOLTS IN
- D.) OUTPUT
- E.) SHUNT
- F.) SHUNT

<u> CAPACITY</u>		<u>OUTPUT</u>	
	0	<u> 0 </u>	Volts
Ascending	50	<u> 4.9939 </u>	Volts
	100	<u> 10.0000 </u>	Volts
Descending	50	<u> 4.9943 </u>	Volts
	0	<u> 0 </u>	Volts

PRESSURE PORT FITTING 1/4-18 NPT MALE

MATING ELECTRICAL CONNECTOR 7 to 6pt -10-65

INTERNAL SWITCH CAL RESISTANCE INSTALLED. SHORTING TOGETHER
THIS SWITCH PROVIDES AN OUTPUT OF 1.9923 VOLTS DC

ACCEPTED AND CERTIFIED

Michael J. Jones

DATE

7/6/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL 2/3533-01

SERIAL NO. 97604

CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE FROM RM °F TO 203 °F

WIRING CODE

- A.) +15 VOLTS IN
- B.) COMMON
- C.) -15 VOLTS IN
- D.) OUTPUT
- E.) SHUNT
- F.) SHUNT

	<u>% CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>7.9953</u>	Volts
	100	<u>10.0006</u>	Volts
Descending	50	<u>7.9454</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/4-18 NPT MALE

MATING ELECTRICAL CONNECTOR RT06A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS E AND F PROVIDES AN OUTPUT OF 7.9675 VOLTS DC

ACCEPTED AND CERTIFIED

Michael L. Johnson

DATE

7/6/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL 2/3533-01

SERIAL NO. 97612

CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE FROM 12M °F TO 203 °F

WIRING CODE

- A.) +15 VOLTS IN
- B.) COMMON
- C.) -15 VOLTS IN
- D.) OUTPUT
- E.) SHUNT
- F.) SHUNT

	<u>3</u> CAPACITY	OUTPUT	
	0	<u>0</u>	Volts
Ascending	50	<u>2.9904</u>	Volts
	100	<u>10.0004</u>	Volts
Descending	50	<u>4.9901</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/4" 18 NPT N/A/E

MATING ELECTRICAL CONNECTOR K-604-10-6E

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS E AND F PROVIDES AN OUTPUT OF 7.9980 VOLTS DC

ACCEPTED AND CERTIFIED Michael J. Spurr

DATE 7/6/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL Z/3533-01
SERIAL NO. 97603
CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE FROM RM °F TO 203 °F

WIRING CODE

- A.) +15 VOLTS IN
- B.) COMMON
- C.) -15 VOLTS IN
- D.) OUTPUT
- E.) SHUNT
- F.) SHUNT

	<u>3 CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>4.4906</u>	Volts
	100	<u>10.0006</u>	Volts
Descending	50	<u>4.9918</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/4-18 NPT MALE

MATING ELECTRICAL CONNECTOR K TO 6A-10-6E

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS E AND F PROVIDES AN OUTPUT OF 7.9910 VOLTS DC

ACCEPTED AND CERTIFIED Michael J. Fusco

DATE 7/6/83

*Corrosion Test
for 105-L*

*J. C. Catty
Recd 15 July 83
AX612078*

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL Z/3533-01

SERIAL NO. 97611

CAPACITY 0-50 PSIA

COMPENSATED TEMPERATURE RANGE 12M °F TO 203 °F

WIRING CODE

- A.) +15 VOLTS IN
- B.) COMMON
- C.) -15 VOLTS IN
- D.) OUTPUT
- E.) SHUNT
- F.) SHUNT

	<u>3 CAPACITY</u>		<u>OUTPUT</u>	
	0		<u>0</u>	Volts
Ascending	50		<u>4.9919</u>	Volts
	100		<u>9.9993</u>	Volts
Descending	50		<u>4.9937</u>	Volts
	0		<u>0</u>	Volts

PRESSURE PORT FITTING 1/4-18 NPT MALE

MATING ELECTRICAL CONNECTOR HUGA-10-6S

INTERNAL INPUT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS 1 AND 2 PROVIDES AN OUTPUT OF 8.0751 VOLTS DC

ACCEPTED AND CERTIFIED Michael J. Jensen

DATE 7/6/83

*Calibration Test
for Bldg 105-L*
*J. J. Cooney
Rec'd 19 July 83
AX612078*

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL A-5/3534-01
SERIAL NO. 73827
CAPACITY 0-250 PSID

COMPENSATED TEMPERATURE RANGE FROM 12M °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal.

	<u>3 CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>4.9960</u>	Volts
	100	<u>10.0013</u>	Volts
Descending	50	<u>4.9944</u>	Volts
	0		Volts

PRESSURE PORT FITTING 1/8-27 NPT

MATING ELECTRICAL CONNECTOR PT66A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS E AND F PROVIDES AN OUTPUT OF 7.9184 VOLTS DC

ACCEPTED AND CERTIFIED

Michael L. Jansen

DATE

7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL A-5/3534-01
SERIAL NO. 94511
CAPACITY 0-250 PSID

COMPENSATED TEMPERATURE RANGE FROM 12M °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>% CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>4.9981</u>	Volts
	100	<u>10.0003</u>	Volts
Descending	50	<u>4.9984</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/8-27 NPT

MATING ELECTRICAL CONNECTOR PT6A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS 2 AND 3 PROVIDES AN OUTPUT OF 7.9739 VOLTS DC

ACCEPTED AND CERTIFIED Michael J. Jansen

DATE 7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL A-5/3534-01
SERIAL NO. 94508
CAPACITY 0-250 PSID

COMPENSATED TEMPERATURE RANGE FROM RM °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>% CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>4.9986</u>	Volts
	100	<u>9.9995</u>	Volts
Descending	50	<u>4.9958</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/8-27 NPT

MATING ELECTRICAL CONNECTOR PT6A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
PINS E & F PROVIDES AN OUTPUT OF 8.0046 VOLTS DC

ACCEPTED AND CERTIFIED Michael J. Jansen

DATE 7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL A-5/3534-01

SERIAL NO. 94510

CAPACITY 0-250 PSID

COMPENSATION TEMPERATURE RANGE FROM EM °F TO 203 °F

A + 15 VDC
B COMMS
C - 15 VDC
D output +
E & F shunt rail

	% CAPACITY	OUTPUT
Ascending	0	<u>0</u> Volts
	50	<u>5.0002</u> Volts
	100	<u>10.0009</u> Volts
Descending	50	<u>4.9991</u> Volts
	0	<u>0</u> Volts

PRESSURE PORT FITTING 1/8" 27 NPT

MATING ELECTRICAL CONNECTOR Ph6A-10-6S

INTERNAL FROM CAL. AND/OR REVISIONS INCORPORATED. SUCCEEDING TOGETHER
FORMS A COMPLETE RECORD OF CALIBRATION OF 80296 VOLTAGE DO

APPROVED AND CERTIFIED Michael J. Johnson

DATE 7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL A-5/3534-01

SERIAL NO. 94509

CAPACITY 0-250PSID

COMPENSATED TEMPERATURE RANGE FROM RM °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>% CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>5.0009</u>	Volts
	100	<u>9.9996</u>	Volts
Descending	50	<u>5.0007</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/8-27

MATING ELECTRICAL CONNECTOR PT6A-10-6S

INTERNAL SHUNT CAL PRECISION INSTALLED. SHORTING TOGETHER
PINS E AND F PROVIDES AN OUTPUT OF 7.9756 VOLTS DC

ACQUIRED AND CERTIFIED Michael J. Jansen

DATE 7/8/83

SENSOTEC

CALIBRATION RECORD FOR TRANSDUCERS WITH INTERNAL ELECTRONICS

MODEL A-5/3534-01
SERIAL NO. 70477
CAPACITY 0 - 250 PSID

COMPENSATED TEMPERATURE RANGE FROM 121 °F TO 203 °F

A + 15 VDC
B COMMON
C - 15 VDC
D output
E & F shunt cal

	<u>3 CAPACITY</u>	<u>OUTPUT</u>	
	0	<u>0</u>	Volts
Ascending	50	<u>4.9978</u>	Volts
	100	<u>10.0021</u>	Volts
Descending	50	<u>4.9960</u>	Volts
	0	<u>0</u>	Volts

PRESSURE PORT FITTING 1/8-27

MATING ELECTRICAL CONNECTOR Pt66A-10-6S

INTERNAL SHUNT CAL RESISTANCE INSTALLED. SHORTING TOGETHER
TERMS E AND F PROVIDES AN OUTPUT OF 7.9978 VOLTS DC

ASSEMBLED AND CERTIFIED

Michael J. Jansen

DATE

7/8/83

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-50 PSIA 0-10V Date 8-1-83

Equipment Under Test SENSOTEC Z No. 97609

Standard Used S/N 10568 r No. S/N 1169

Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK

Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F

Equipment From: Foreman J CAThey Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	-0.24		21	50.046	10.030	
2	14.730	2.909		22	39.930	8.006	
3	20.030	4.006		23	30.020	6.019	
4	30.070	6.023		24	20.050	4.022	
5	40.030	8.022		25	14.730	2.924	
6	49.980	10.019		26	00.000	0.10	
7				27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

CALIBRATION DATA SHEET

Unit of Measure 0-50 PSIA, 0-10V Date 8-2-83
 Equipment Under Test SENSOTEC Z No. 97616
 Standard Used S/N 10568 r No. S/N 1169
 Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK
 Barometric Pressure 29.96" Hg Humidity _____ % Temperature 75°F
 Equipment From: Foreman C. ATNEY Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .016		21	50.020	10.035	
2	14.710	2.884		22	39.970	8.017	
3	20.030	4.001		23	30.040	6.024	
4	30.060	6.020		24	19.940	3.997	
5	40.060	8.031		25	14.710	2.909	
6	50.065	10.042		26	00.000	- .007	
7				27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-50 PSIA, 0-10Y Date 8-2-83
 Equipment Under Test SENSOTEC Z No. 97611
 Standard Used S/N 10568 r No. S/N 1169
 Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK
 Barometric Pressure 29.96" Hg Humidity _____ % Temperature 75°F
 Equipment From: Foreman P. ATHEY Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.006	- .015		21	44.936	9.947	
2	14.710	2.902		22	40.045	8.018	
3	20.065	4.004		23	30.050	6.013	
4	30.036	5.999		24	19.966	3.990	
5	40.025	8.007		25	14.710	2.908	
6	50.040	10.016		26	00.000	- .012	
7				27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-50 PSIA, 0-10Y Date 8-2-83
 Equipment Under Test SENSOTEC Z No. 97617
 Standard Used S/N 10568 r No. S/N 1169
 Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK
 Barometric Pressure 29.96" Hg Humidity _____ % Temperature 75°F
 Equipment From: Foreman PATHEy Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .034		21	50.050	10.020	
2	14.710	2.884		22	39.980	8.001	
3	20.080	3.999		23	30.035	6.004	
4	30.030	5.998		24	20.030	3.998	
5	40.050	8.011		25	14.710	2.902	
6	50.050	10.019		26	00.000	- .005	
7				27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-50 PSIA, 0-10y Date 8-2-83
 Equipment Under Test SENSOTEC Z No. 97606
 Standard Used S/N 10568 r No. S/N 1169
 Range 0-200 PSI Calibration Expires 8-5-83 By E. KIRK
 Barometric Pressure 29.96" Hg Humidity _____ % Temperature 75°F
 Equipment From: Foreman PATNEY Bldg. 723 Area A

Heading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .427		21	50.000	10.027	
2	00.000	- .010	RE ZERO	22	40.070	8.035	
3	14.710	2.907		23	29.970	1.006	
4	20.040	4.012		24	20.008	4.005	
5	29.980	6.006		25	14.710	2.904	
6	40.080	8.037		26	00.000	- .014	
7	50.040	10.036		27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

722-A F & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-50 PSIA, 0-10 V Date 8-1-83
 Equipment Under Test SENSOTEC Z No. 97612
 Standard Used S/N 10568 r No. S/N 1169
 Range 200 PSI Calibration Expires _____ By E. KIRK
 Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F
 Equipment From: Foreman J. CATHEY Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .039		21	49.990	9.985	
2	14.730	2.881		22	40.040	7.989	
3	20.040	3.979		23	29.990	5.971	
4	30.025	5.977		24	20.030	3.975	
5	39.990	7.978		25	14.730	2.886	
6	50.070	10.001		26	00.000	- .037	
7				27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-50 PSIA, 0-10Y
 Equipment Under Test SENSOTEC Z
 Standard Used S/N 10568
 Range 0-200 PSI Calibration Expires 8-5-83

Date 8-2-83
 No. 97605
 r No. S/N 1169
 By E. KIRK

Barometric Pressure 29.96" Hg Humidity _____ % Temperature 75°F
 Equipment From: Foreman P. ATNEY Bldg. 723 Area A

Heading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .007		21	50.000	10.028	
2	14.710	2.899		22	40.070	8.040	
3	20.000	4.008		23	30.040	6.026	
4	30.055	6.025		24	20.020	4.015	
5	40.010	8.023		25	14.710	2.917	
6	50.060	10.040		26	00.000	00.000	
7				27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-50 PSIA, 0-10V Date 8-1-83
 Equipment Under Test SENSOTEC Z No. 97604
 Standard Used S/N 10568 r No. S/N 1169
 Range 0-200 PSI Calibration Expires 8-5-83 By E KIRK
 Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F
 Equipment From: Foreman J. Cathey Bldg. 723 Area A

Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .011		21	49.920	9.998	
2	14.730	2.907		22	40.080	8.027	
3	14.960	3.986		23	30.000	6.005	
4	29.955	5.989		24	20.025	4.006	
5	40.050	8.016		25	14.730	2.915	
6	50.090	10.030		26	00.000	- .011	
7				27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

722-A E & I SHOP
CALIBRATION DATA SHEET

Unit of Measure 0-50PSIA 0-10V Date 8-1-83
 Equipment Under Test SENSOTEC Z No. 97603
 Standard Used S/N 10568 r No. S/N 1169
 Range 200-PSI Calibration Expires 8-5-83 By E KIRK
 Barometric Pressure 30" Hg Humidity _____ % Temperature 80°F
 Equipment From: Foreman J. CATHEY Bldg. 723 Area A


Reading Number	Standard Reading ↑	Test Reading	Deviation	Reading Number	Standard Reading ↓	Test Reading	Deviation
1	00.000	- .036		21	49.960	10.001	
2	14.730	2.888		22	40.090	8.020	
3	20.060	3.988		23	29.900	5.974	
4	30.010	5.986		24	20.090	4.007	
5	39.980	7.993		25	14.736	2.902	
6	49.960	9.998		26	00.000	- 017	
7				27			
8				28			
9				29			
10				30			
11				31			
12				32			
13				33			
14				34			
15				35			
16				36			
17				37			
18				38			
19				39			
20				40			

Remarks _____

Figure 1

D) Fluid Property Effects

In the adjustment of the L Area test data to operating conditions, the fluid property changes were not taken into account. It is common for a centrifugal pump to require less NPSH at a higher operating temperature due to viscosity, specific heat, and other fluid property changes. This conservative measure was taken because in the SRP reactors gas evolution takes place before cavitation. Without further extensive testing, the effects of evolved gases and two phase flows on the pump characteristics is unknown. In Reference 1 a procedure for accounting for these changes is outlined. The procedure is based around the discussion in Reference 7 and uses the Bingham Pump Company data that was experimentally collected with degassed H₂O (See Appendix G).



Appendix E - Low Pressure Header and Tank Level

The determination of the actual tank level proved to be difficult. This appendix contains the calculations and data used to resolve the discrepancies in the test data. Special attention should be given to the effects of the number of pumps running on the low pressure header readings. Also note that the bottom tank centerline transducer was plugged during most of the testing.

The data listed was collated from references 9, 10, and 11.

Methodology

1. Determine all gauge elevations
2. Determine reading at overflow
3. Adjust for number of pumps running and obtained overflow reference point
4. Calculate tank level from absolute and gage readings (unsuccessful)
5. Calculate levels by subtracting (i.e. using delta) from reference valve
6. Compare different gage readings

Full analysis of all tank level data indicates that at the cavitation test levels approximately 10' and approximately 8' and at the S.L.O.C. test levels 3' to 0' the DMA calculated level is corrected.

Estimated Error \pm 3" (these ranges only)

TITLE OF PROJ. _____ PROJ. NO. _____

SUBJECT _____ WORKS _____

COMPUTER _____ DATE _____ 19__

● CHECK CORRELATIONS

DMA TO LPH (VAMA)

$$\text{ERROR AVG.} = 0.73'$$

$$\text{DMA} = 0.983 \left(\frac{\text{LPH}_{\text{VAMA}}}{\text{FT}} \right) + 0.777$$

$$\text{CORR} = 0.9932$$

DMA TO LPH (HEISE)

$$\text{ERROR AVG.} = -0.01'$$

$$\text{DMA} = 1.172 \left(\frac{\text{LPH}_{\text{HEISE}}}{\text{FT}} \right) + -0.323$$

$$\text{CORR} = 0.9929$$

DRM DATA & ANALYSIS

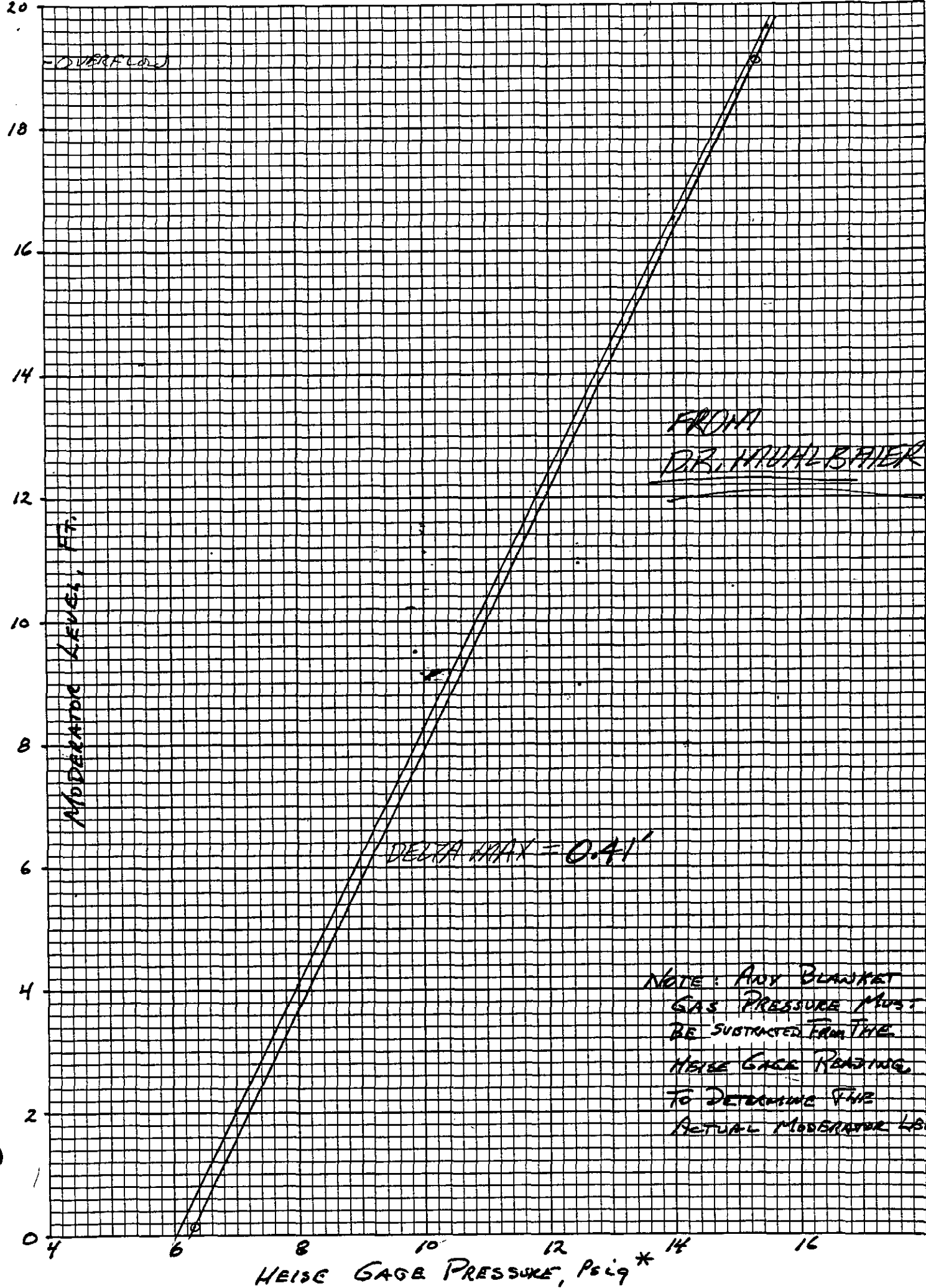
SEE CURVE

$$\text{ABSOLUTE TANK LEVEL, FT} = 2.10 (\text{LPH}_{\text{HEISE}}) + -13.16$$

MY DATA 16 POINTS

$$\text{CORR.} = 0.9976$$

$$\text{ABSOLUTE TANK LEVEL} = 2.071 (\text{LPH}_{\text{HEISE}}) - 12.457$$



OVERFLOW

FROM
DR. WALTER BAUER

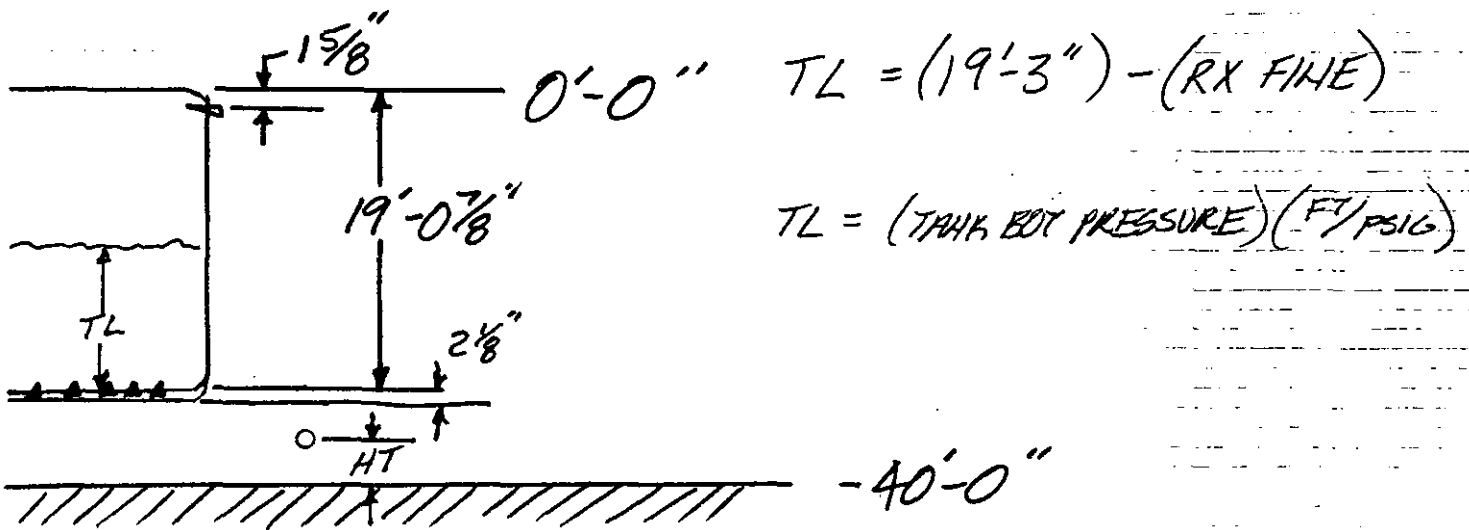
DELTA MAX = 0.41'

NOTE: ANY BLANKET
GAS PRESSURE MUST
BE SUBTRACTED FROM THE
HEISE GAGE READING
TO DETERMINE THE
ACTUAL MODERATOR LEVEL.

CAVITATION TANK LEVEL DATA

11-22 83

- RX FINE LEVEL MEASURES FROM
0'-0" ELEVATION
- BOTTOM OF TANK IS AT -19'-3"
- MONITOR PIN TAP IS AT -19'-0⁷/₈"
- BOTTOM OF OVERFLOW WEIR IS AT -0'-1⁵/₈"
SEE W231138
- ELEVATION OF VAN LPH XDUCCER IS
5'6¹/₂" ABOVE -40' FLOOR
- ELEVATION OF HIESE LPH GAGE IS
6' ABOVE -40' FLOOR



CAVITATION TANK LEVEL DATA

11-22 83

REFERENCE DATA WITH TANK FULL

6 AC -1.2" RX FINE TL = 19' - 1.8"
 8.8 BOT TKP TL = 18.33'
 ~ 29.9 LPH (VAM) TL = 16.87'

ASSUME RX FINE CORRECT - IF TANK IS AT OVERFLOW LEVEL WOULD BE 19' 1 3/8" ± 2/8"

OBTAIN AVERAGE LPH (VAM) READING WITH TANK AT OVERFLOW 6 ACs

T	RX FINE	LPH (VAM)	
23°	-1.2"	29.88	} 10-13
	-1.1"	29.96	
	-1.2"	29.92	
	-1.1"	29.96	
	-	29.97	
	-	29.92	
28°	-0.1"	32.23	} 10-22
65°	-0.1"	32.19	
85°	-0.15"	32.12	
94°	-0.3"	31.85	
			<u>~2 PSI BGP</u>
39°	-1.4"	30.19	} 10-29
50°	-1.5"	30.14	
66°	-1.7"	30.14	
80°	-1.9"	30.05	
			3 AC
67°	-1.8"	30.12	} 10-30
71°	-1.8"	30.14	
73°	-1.9"	30.03	
76°	-1.9"	30.11	
			5 AC

CAVITATION TANK LEVEL DATA

50W

10-2-1983

- USE DATA FROM 10-13, 10-29, 10-30 TO SET BASELINE FOR LPH(VAM)
- EFFECT OF TEMPERATURE COMPENSATE FOR IN DENSITY
- TO GO FROM 3 GAL TO 6 GAL SUBTRACT 0.3
- TO GO FROM 5 GAL TO 6 GAL SUBTRACT 0.1

10-13 CORRECTED TO ELEVATION 0'-0"

29.93, 29.97, 30.01, 30.01

10-29 CORRECTED TO ELEV. 0'-0" AND 6 GAL

29.95, 29.90, 29.91, 29.82*

10-30 CORRECTED TO ELEV. 0'-0" AND 6 GAL

30.09, 30.11, 30.00, 30.08

$$\bar{M}EAN = 29.98 \quad \sigma = 0.0861$$

*USE OF CHAUVENET'S CRITERION ELIMINATES BAD DATA POINT(S)

$$\bar{M}EAN = 30.00 \quad \sigma = 0.0728$$

$$\sigma_{MEAN} = 0.02 \quad \sim \pm 0.5''$$

CAVITATION TANK LEVEL DATA

50W

ANALYSIS SHOWS THAT A TANK LEVEL
OF 19'3" CORRESPONDS TO A
LPH (VAM) READING OF 30.00 PSIA

CALCULATE ABSOLUTE LEVEL

⇒ ASSUME ATM PRESS = 14.5 PSIA

$$\begin{aligned} \text{TANK LEVEL} &= (30 - 14.5) \left(\frac{2.31 \text{ FT}}{\text{PSI}} \right) + (5.54') - (19.25') \\ &= 18.87' \end{aligned}$$

WITHIN 5 INCHES OF ESTIMATE ~.2 PSI

CHECK ATM PRESS ASSUMPTION

OK	10-30	ATM PRESS	≈ 14.8 PSIA	(FROM PROCESS ROOM XDUCE)
"	10-29	" "	≈ 14.7 PSIA	
"	10-13	?		

SRL BAROGRAPH DATA

10-13	1007 mBARs	⇒	14.60
10-22	1016 mB	⇒	14.73
10-29	1008 mB	⇒	14.62
10-30	1021 mB	⇒	14.81
			<hr/>
			AVG. 14.69

(TO GO FROM SRL
TO L-AREA ELEVATION
ADD 0.03
NEGLECTIBLE)

TANK LEVEL w/ TRUE ATM PRESS. ≈ 18.2' ?

CAVITATIONS
TANK LEVEL

DATA

DW

USE "DELTA'S"

FOR REFERENCE

19'3" = 30.00 on LPH (VAM)
"FULL" = 9.0 PSIG ON DMA

DMA PRESSURE	DMA LEVEL	VAM LPH	HIESE LPH	TEMP
① "FULL"	19.0'	30.09	16.1	~25°C
② 3.3	6.8'	24.40		57°C
③ 3.9	8.2'	25.12	10.9	78°C
④ 4.3	9.2'	25.47		84°C
⑤ 4.8	10.2'	26.03		89°C
⑥ -	11.0'	26.35	12.2	~25°C
⑦ "EMPTY"	0'	21.7		~25°C

CAVITATION TANK LEVEL DATA

DW

"FULL" REFERENCE CONDITIONS

DMA PRESS. = 9.0 , LPH (VAM) = 30.00 6AC
 LPH (HIESE) = 16.1 , TANK LEVEL ~ 19'3"

POINT	TL DMA PRESS	TL DMA	TL LPH (VAM)	TL LPH (HIESE)	AVERAGE
2	7.3'	6.8'	7.3'	-	7.13'
3	8.5'	8.2'	9.0'	8.3'	8.50'
4	9.4'	9.2'	9.7'	-	9.43
5	10.4'	10.2'	10.9'	-	10.50'
6	-	11.0'	11.6'	11.1'	11.23'

LPH (HIESE) } DELTA WOULD INDICATE THAT
 THE DMA LEVEL IS CORRECT

PROCEED TO S.L.O.C. TEST DATA
 FOR FURTHER ANALYSIS

VAM HIESE

DATE	T	TIME	DMA	CPH	♀	CPH	♀	# OF PUMPS
10-22	28°	13:08	RX FINE -0.1"	32.23	23.02			6 AC
	65°	15:06	-0.1"	32.19	24.42			6 AC
	85°	16:14	-0.15"	32.12	25.88			6 AC
	94°	16:48	-0.30"	31.85	26.92			6 AC
	90°	16:51	—	32.52	27.05			6 DC

10-30 67° 11:11 RX FINE -1.8" 30.12 26.09
 RX CORSE 18.6'
 RX TANK BP 8.8 PSI/6

71° 11:30 -1.8" 30.14 26.32
 18.6'
 8.8 PSI/6

73.5° 11:45 -1.9" 30.03 26.53
 18.5'
 8.8 PSI/6

76° 12:00 -1.9" (26.73 30.11)
 18.5'
 8.8 PSI/6

(4075)

VAM

HESE

DATE	T	TIME	DMA	LPH	♀	LPH	♀	# AC's
10-16	~23°	MIDNIGHT		30.83	24.78			3 DC
10-17		10:30		30.18	24.77			6 AC
10-21			<10.7>	31.91	23.03			6 AC
10-21				32.57	22.97			6 DC
10-21		22:28	RX COARSE 19.0' RX FINE -1.3" RX TR BP 10.7PSG	31.90	23.10			6 AC
10-13	~23°	10:06	RX FINE -1.2" RX TR BP 8.8PSG	29.88	25.69			6 AC
		10:34	-1.1" 8.8PSG	29.96	25.71			6 AC
		11:30	-1.2" 8.8PSG	29.92	25.73			6 AC
		12:30	-1.1" 8.8	29.96	25.64			6 AC
10-13	~23°	16:04		30.57	25.73			NO AC/NO DC
		16:50		30.60	25.64			6 DC
		16:52		30.63	25.65			1 AC
		16:54		30.30	25.60			2 AC
		16:54½		30.30	25.61			3
		16:55		30.06	25.66			4
		16:56		29.98	25.68			5
		16:58		29.97	25.62			6
		17:15		29.92	25.62			6
	18:30			30.71	25.67			NO AC/NO DC

				VANA	HIESE			
DATE	T	TIME		DMA LPH	¢	LPH	¢	# OF PUMPS
(4065)	10-31	56.5°	01:00	EXT FINE 25.9'	24.41	27.19		6 AC
				EX CORSE 6.8'				
				EXTANK BP 3.3 psig				
		58°	01:45	6.8'	24.39	26.82		6 AC
				3.3 psig				
	62°	05:10	8.0'	24.93	26.64		6 AC	
			3.8 psig					
	75°	05:45	8.2'	25.08	27.02		6 AC	
			3.9 psig					
	80°	6:00	8.2'	25.19	27.25		6 AC	
			3.9 psig					
(4065)	10-31	84.5°	20:54	9.2'	25.53	28.21	11.38	6 AC
				4.4 psig				
		84°	21:20	9.2'	25.49	28.47	11.38	6 AC
				4.3 psig				
		85.5°	21:40	9.7'	25.75	28.80	11.55	6 AC
			4.6					
	81°	22:40	9.1'	25.46	29.05	11.30	6 AC	
			4.3 psig					
	80°	23:00	9.0'	25.44	29.25	11.30	6 AC	
			4.3 psig					
	84°	23:15	9.2'	25.55	29.42	11.40	6 AC	
			4.3 psig					
	89°	23:30	10.2'	26.03	29.59	11.90	6 AC	
			4.8 psig					

DATE	T	TIME	VAM		HIESE		# OF PUMPS
			DMA	LPH &	LPH &		
10-29	39°	16:15	RX FINE RT TANK P	-1.4"	30.19	23.40	3 AC
	50°	17:00		-1.5"	30.14	23.07	
	66°	18:00		-1.7"	30.14	23.54	
	80°	19:00		-1.9"	30.05	23.97	

XIITH TANK LEVEL ~ 0 i.e. TANK DRAINED

11-11 25°C 21.74 — 6.3 —

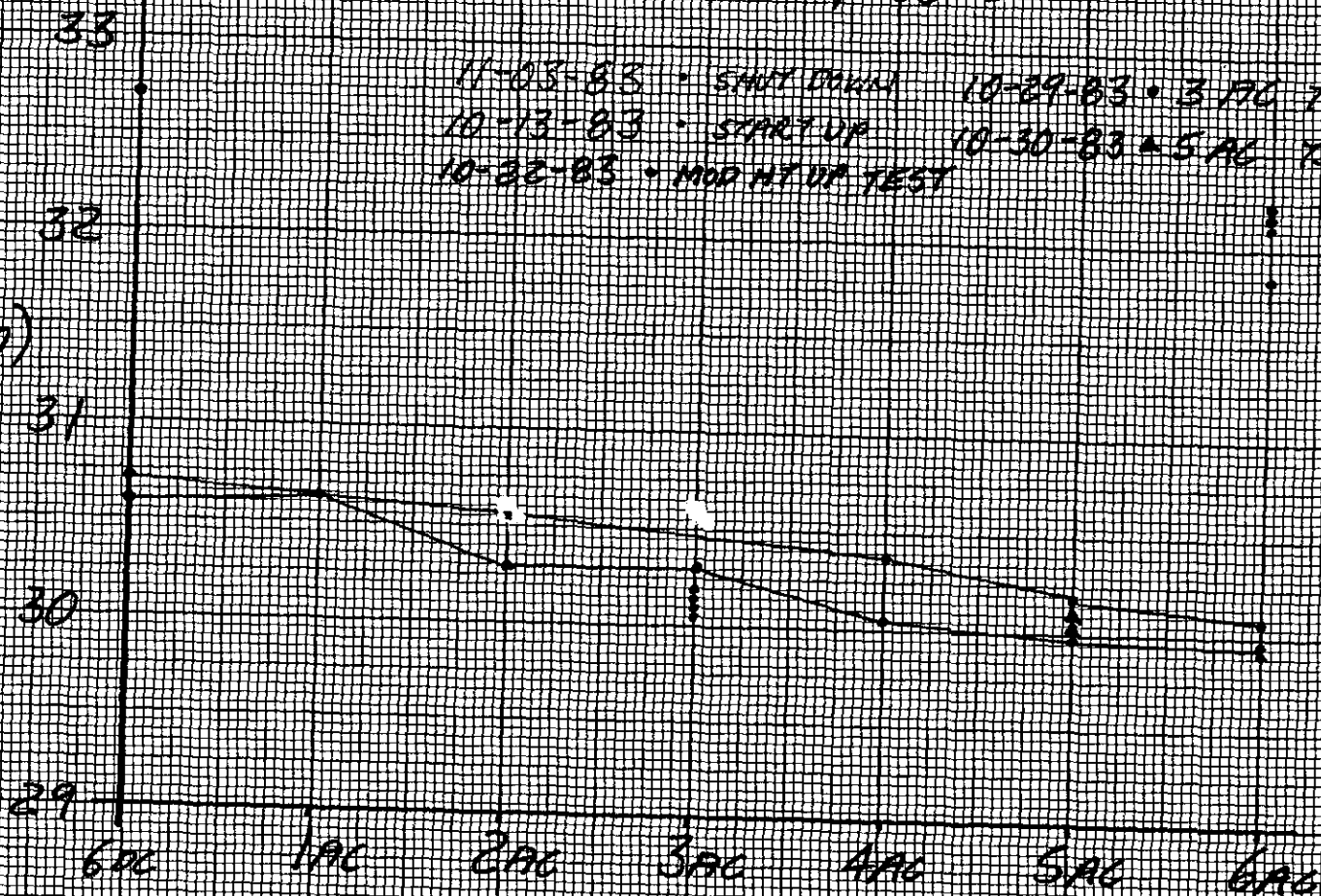
EFFECT OF PUMPS ON LPH (WAM)

10/30/83

TANK FULL & COLD

11-03-83 • SHUT DOWN
 10-13-83 • START UP
 10-22-83 • MOD HTUP TEST
 10-29-83 • 3.7G TEST 37°-80C
 10-30-83 • 5.4G TEST 67°-76C

LPH (WAM)
 PSIA



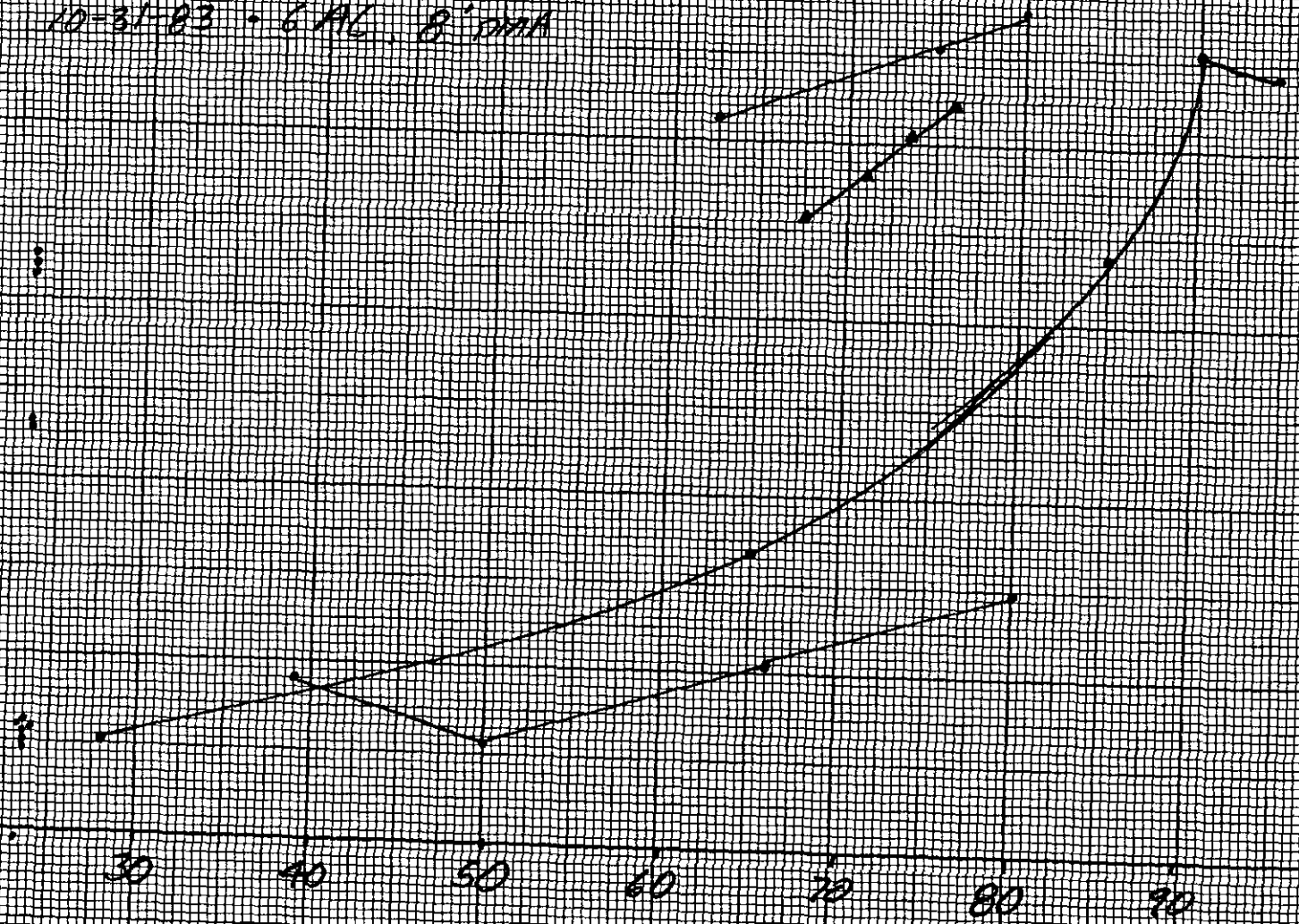
EFFECT OF TEMPERATURE ON ϕ (MAN)

10-22-83 - 1700 HY OF
 10-30-83 - 5 AC
 10-29-83 - 3 AC
 10-31-83 - 6 AC, 8° PHA

27.5
 26.5
 25.5
 24.5
 23.5
 22.5

20 30 40 50 60 70 80 90 100

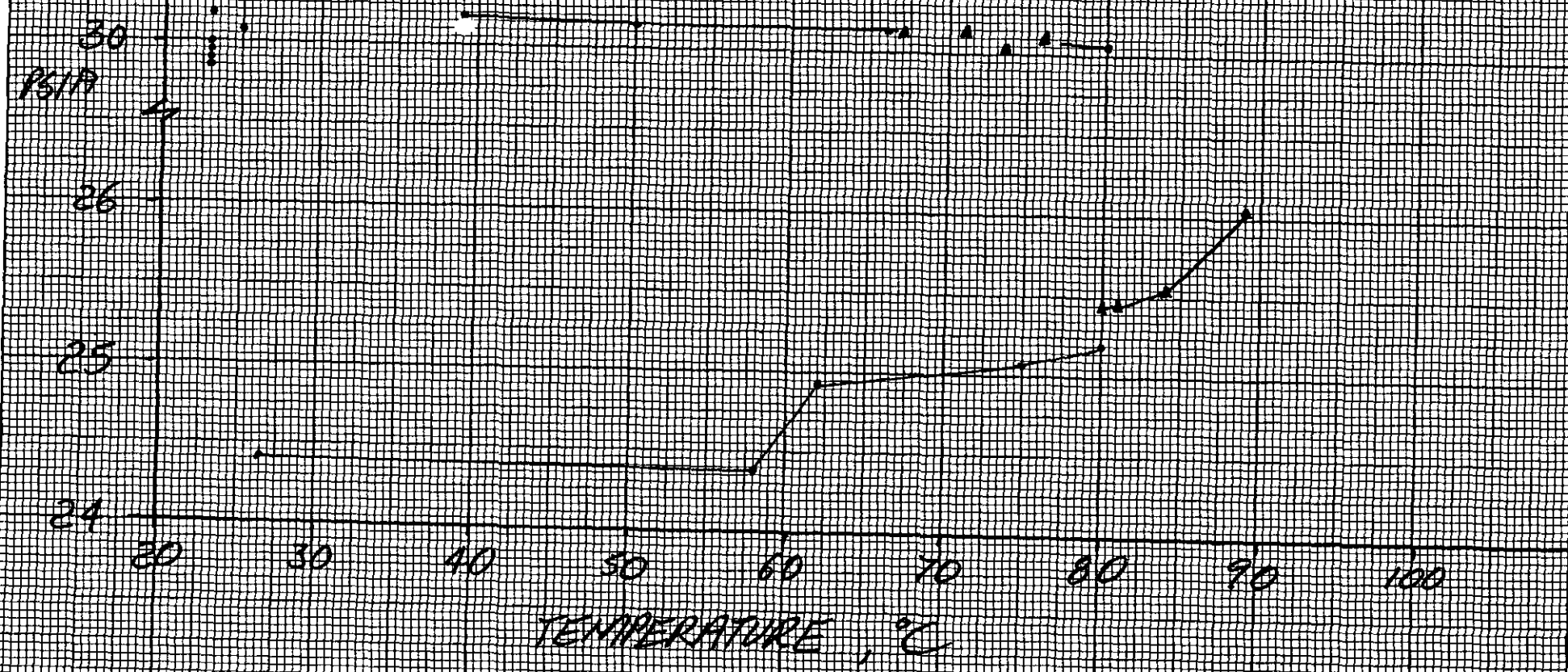
TEMPERATURE, °C



EFFECT OF TEMPERATURE ON LPH (VAM)

32 10-22-83 • WOOD HTUP
 10-30-83 • 5 AC ; 10-29-83 • 3 AC
 MISC • 6 AC FULL TANK
 31 10-31-83 • 6 AC 1/2 TANK ; 6 AC
 " " " " " "

LPH (VAM)



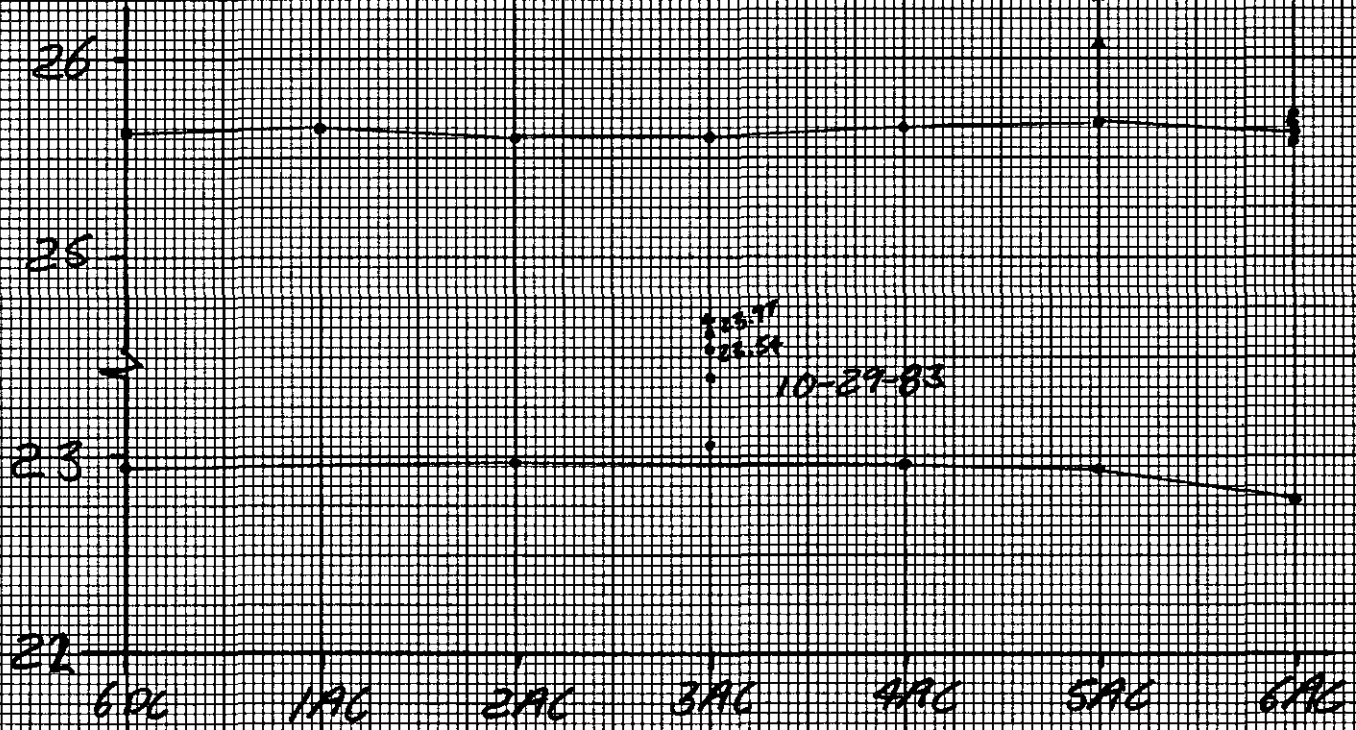
EFFECT OF RUMPS ON \dot{Q} WARM

TANK FULL & COLD

11-03-83 • SHUTDOWN
 10-13-83 • START UP

10-30-83

\dot{Q} (WARM)
 PSIA



S. L. O. C.
TANK LEVEL

0.20

ASSUME 30.89 PSIA = 19' 2"
 LPH (VAM)
 15.29 PSIA = 19' 2"
 LPH (HIESE)
 15.35 PSIA = 19' 2"
 ϕ (HIESE)

CALCULATE LEVELS $\rho \approx 1107 \text{ kg/m}^3 @ \sim 20^\circ\text{C}$

DMA	LPH VAM	LPH HIESE	ϕ
6.1'	5.4'	5.4'	
6.8'	6.2'	6.1'	
3.0'	2.4'	2.8'	
2.2'	1.5'	1.9'	
1.5'	0.92'	1.4'	
1.1'	0.63'	1.2'	
1.7'	0.77'	1.7'	
3.7'	2.9'	3.5'	
2.1'	1.4'	2.2'	
1.9'	1.1'	2.0'	
1.5'	0.86'	1.8'	
4.6'	3.75'		6.19'
2.1'	1.2'		2.96'
1.6'	0.75'		1.82'
1.4'	0.4'		1.46'

● CHECK CORRELATIONS

DMA TO LPH (VAM)

$$\text{ERROR AVG.} = 0.73'$$

$$\text{DMA} = 0.983 (\text{LPH}_{\text{VAM}}) + 0.777$$

$$\text{CORR} = 0.9932$$

DMA TO LPH (HEISE)

$$\text{ERROR AVG.} = -0.01'$$

$$\text{DMA} = 1.172 (\text{LPH}_{\text{HEISE}}) + -0.323$$

$$\text{CORR} = 0.9929$$

DRM DATA & ANALYSIS

SEE CURVE

$$\text{ABSOLUTE TANK LEVEL, FT} = 2.10 (\text{LPH}_{\text{HEISE}}) + -13.16$$

MY DATA 16 POINTS

$$\text{CORR.} = 0.9976$$

$$\text{ABSOLUTE TANK LEVEL} = 2.071 (\text{LPH}_{\text{HEISE}}) - 12.957$$

S.L.O.C. TEST TANK LEVEL DATA

DATE	TIME	DMA		VAM		HEISE	
		LEVEL	PRESSURE	LPH	¢	LPH	¢
TEMP ≈ 20°C							
11-5-83	23:36	20.1'	9.4 ^{PSIG}	30.92	21.37	15.30	15.36
11-6-83	1:20	20.1'	9.4	30.87	21.96	15.30	15.37
	2:36	19.9'	9.4	30.88	21.30	15.27	15.32
	4:30	6.1'	3.0	24.19	21.29	8.66	8.75
	5:30	6.1'	3.0	24.33	21.30	8.68	8.78
	7:00	6.8'	3.3	24.64	21.15	9.01	9.10
	10:26	3.0'	1.6	22.86		7.43	
	15:00	2.2'	1.2	22.90		6.98	
	23:00	1.5'	1.0	22.13		6.78	
11-7-83	7:45	1.1'	0.8	21.97		6.66	
	11:45	1.1'	0.7	22.01		6.70	
11-8-83	2:00	1.7'	1.0	22.06		6.88	
	7:00	3.7'	1.9	23.09		7.79	
	13:30	2.1'	1.3	22.38		7.14	
11-9-83	2:00	1.9'	1.2	22.20		7.07	
	7:00	1.5'	1.0	22.10		6.94	
11-10-83	5:00	4.6'	-	23.99			9.12
	8:26	2.1'	1.2	22.26			7.57

S.L.O.C. TEST TANK LEVEL DATA

DATE	TIME	DWA LEVEL PRESSURE	VAN LPH &	HISE LPH &
11-10-83	14:02	1.6'	22.05	7.02
	16:00	1.4'	21.88	6.85

Appendix F - Dissolved Gases

The concept of gas evolution and its effects on cavitation were not discussed in the results of previous cavitation studies at SRP. During the year long study of cavitation the following conclusions concerning dissolved gases and gas evolution were drawn.

- 1) The evolution of non-condensable dissolved gases; oxygen, nitrogen, helium, etc., takes place at a temperature below and pressure above the saturation point of the flowing fluid.
- 2) In the Georgia Iron Works Tests, it was determined that in the range of 0.7 - 2.0% dissolved gases, varying the dissolved gas content did not affect the increase in pressure drop that occurs when the gas evolves.
- 3) This increasing pressure drop occurs in the reactor effluent line and reduces the pump suction pressure forcing the pump into cavitation.
- 4) A sample of D₂O from P Area (while in operation) had a dissolved gas content of 1.4%. The L Area D₂O had a dissolved gas content of 0.8%.
5. The presence of evolved gases increase the compressibility of the flowing fluid and reduces flow noise and the cavitation damage potential.

G) Bingham Pump Company Data

The first curves are L Area data shown as NPSH vs. temperature. This can be used for comparison to the Bingham Pump Company data.

The data in this appendix is here for reference. It could not be found in the SRP records and was obtained from:

Bingham-Willamette Co.
2800 N.W. Front Avenue
P. O. Box 10247
Portland, Oregon 97210

(503) 226-5200

CAVITATION NPSH CURVES

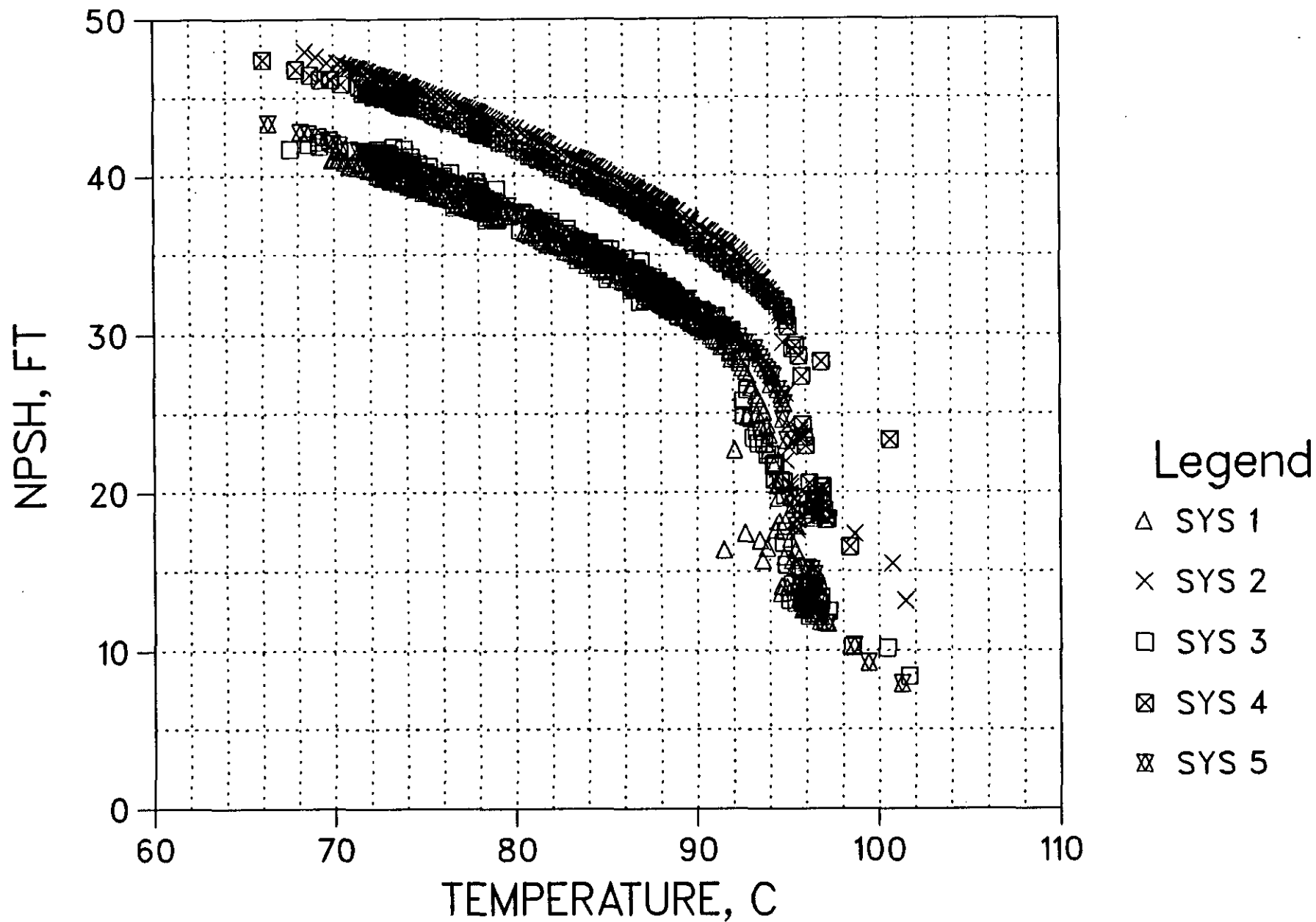
SYSTEM	FLOW	PUMP CUTOFF T PMP DP ; ACCEL	NPSH	(G.E.) NPSH BREAK	BINGHAM NPSH BREAK
1	27.3 KGPM	95.5°C	16'		AT 95°C
2	28.1	95.5	18.5'		
3	28.0	95.5	14'		17' @ 28.0
4	26.8	96	22.5' @ 96.5 = 18.5'		
5	26.2	96	14'		14' @ 25.0

THE ABOVE DATA IS $\pm 1.5'$ NPSH
AND FOR COMPARISON ONLY

PLEASED THAT NPSH NUMBERS ARE
SO CLOSE!

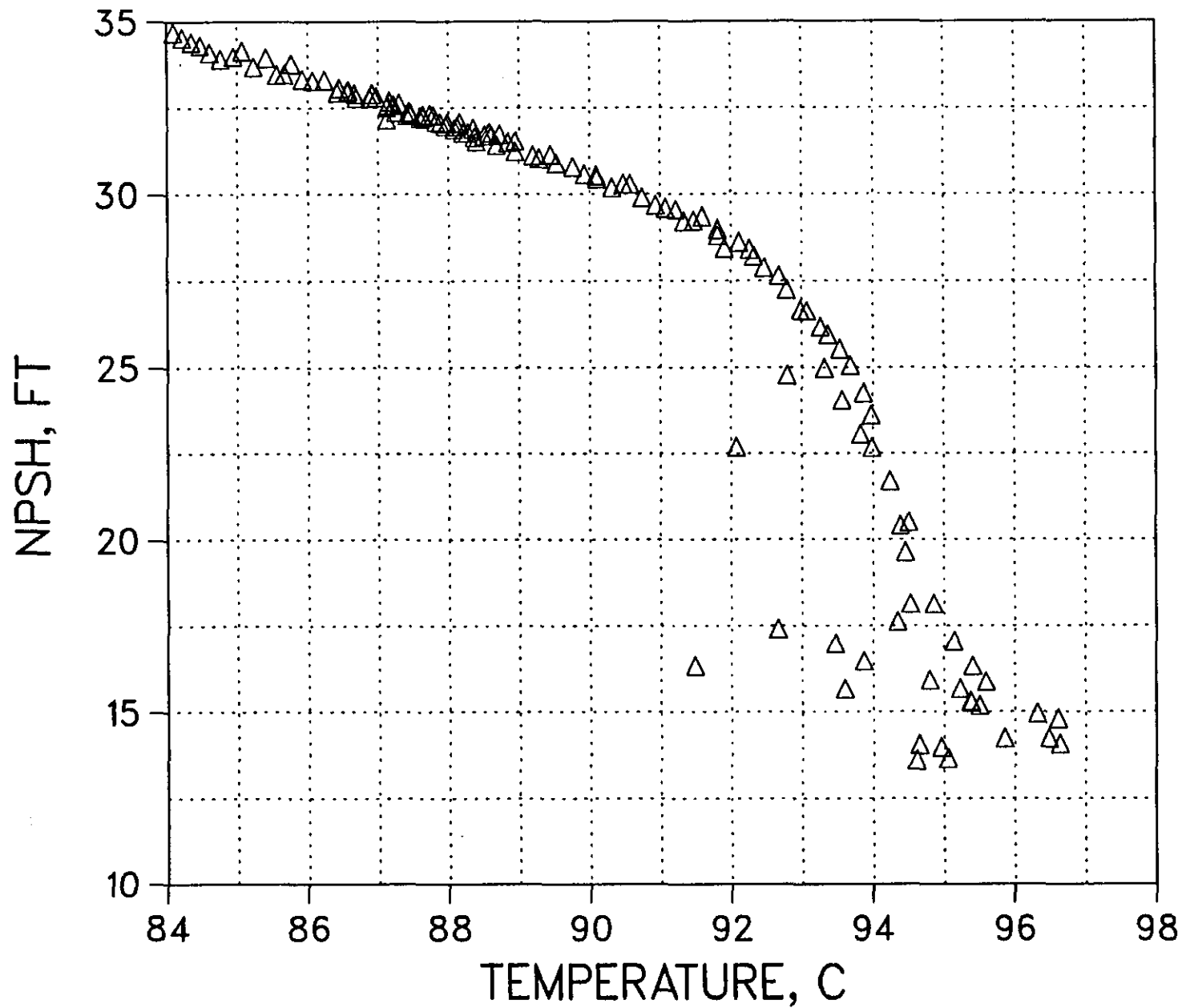
PUMP CAVITATION TESTS

UNADJ. TEMP. VS NPSH AT CL IMPELLER 5 pumps



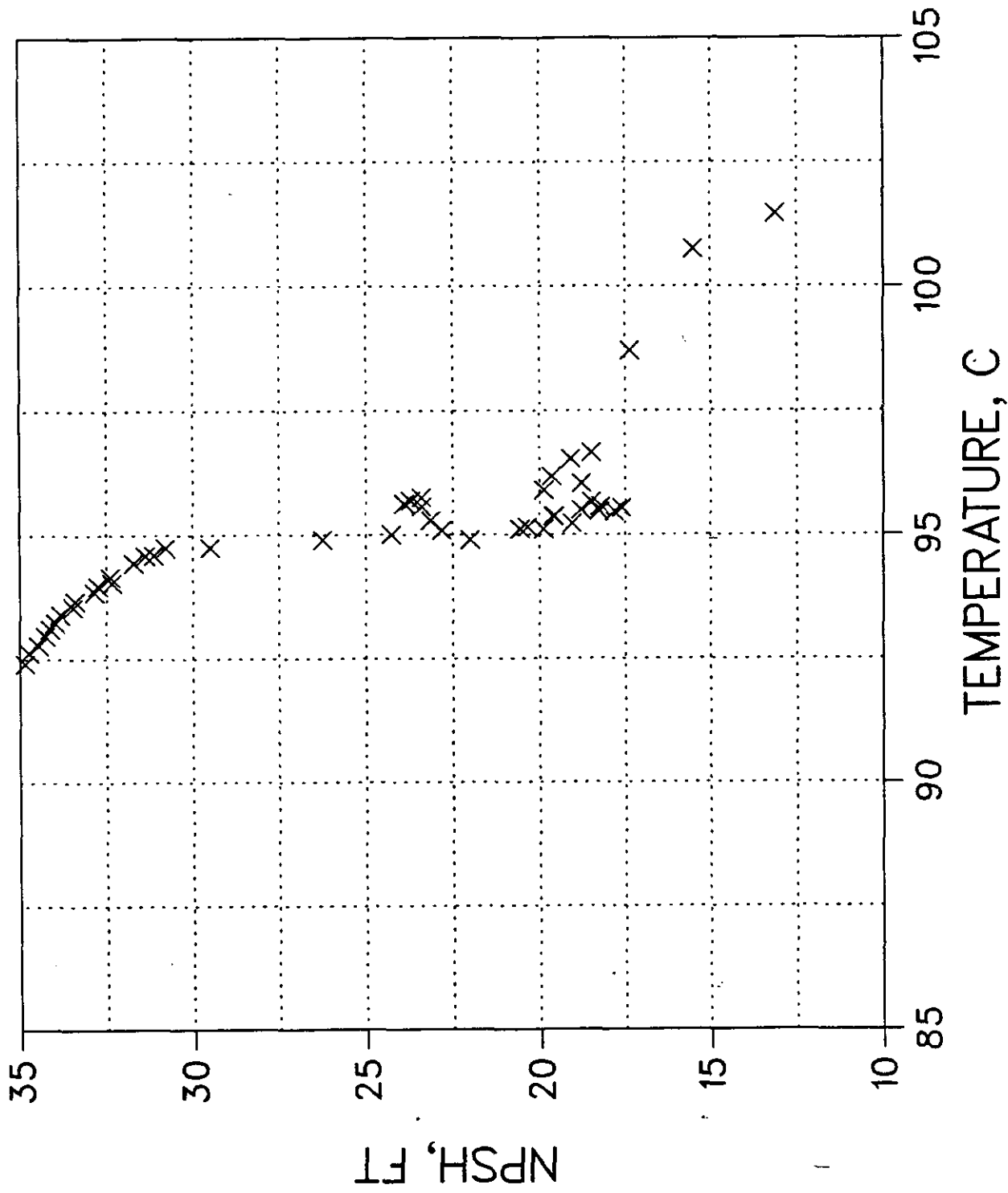
PUMP CAVITATION TESTS

UNADJ. TEMP. VS NPSH AT CL IMPELLER 5 pumps

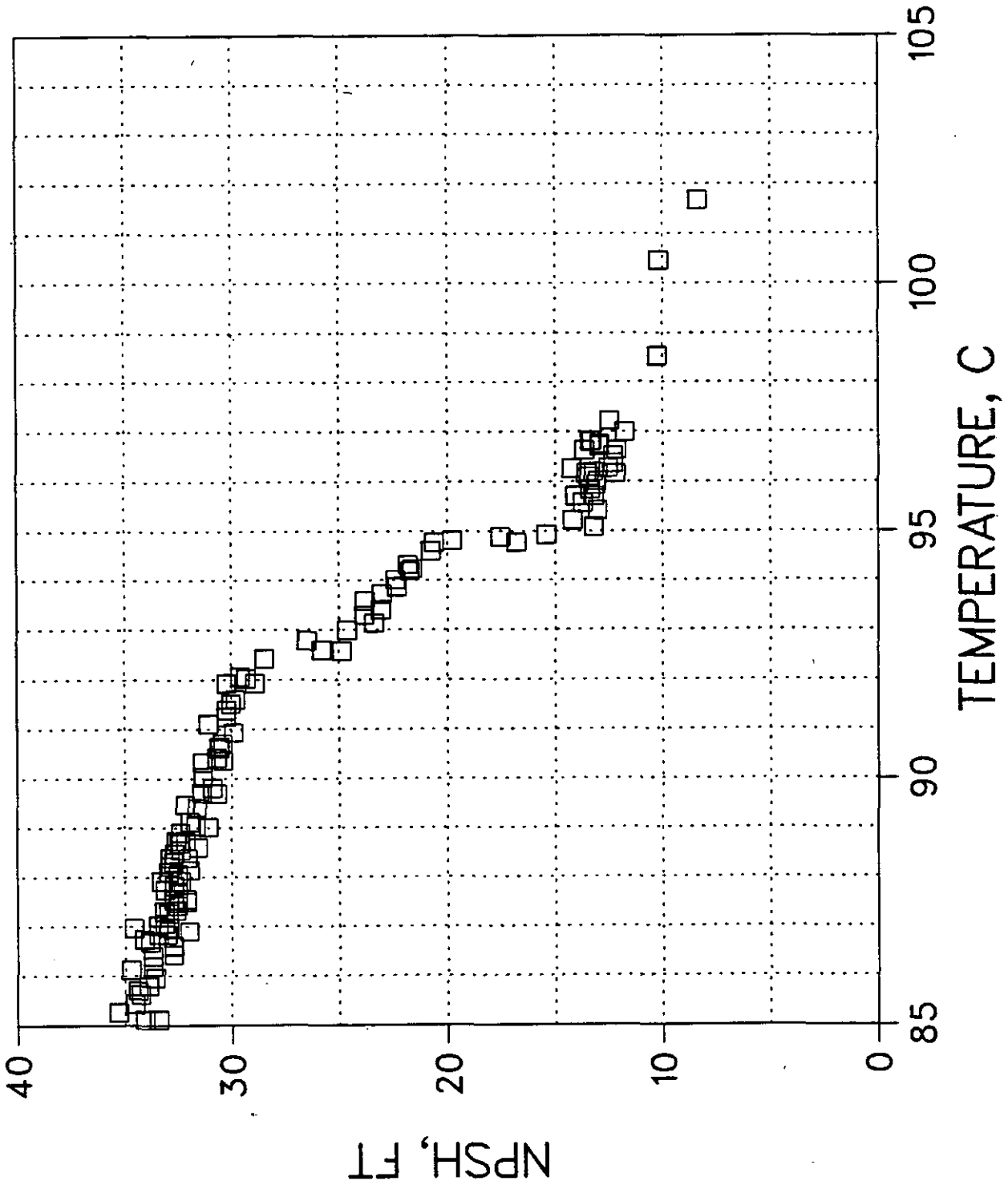


PUMP CAVITATION TESTS

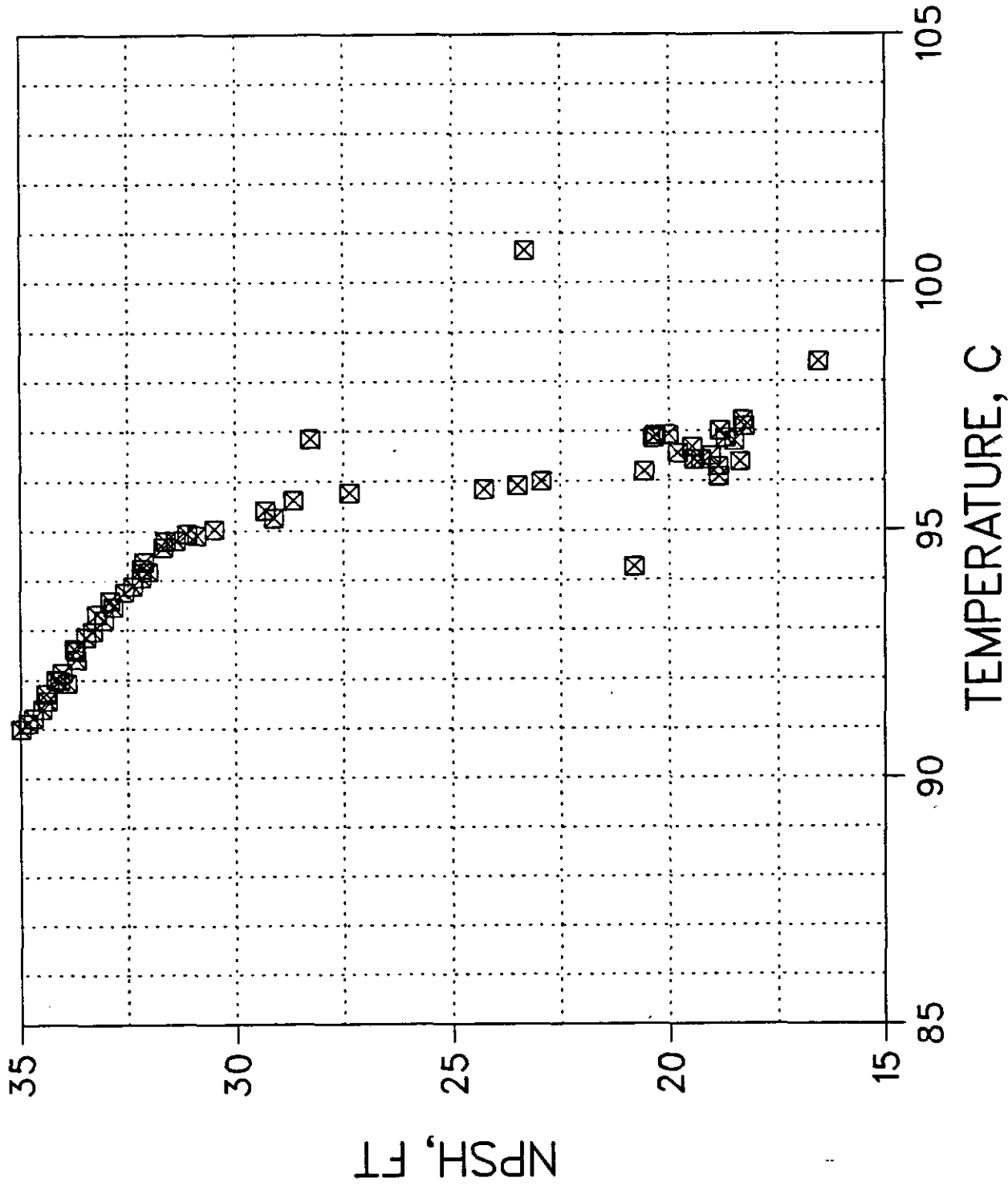
UNADJ. TEMP. VS NPSH AT CL IMPELLER 5 pumps



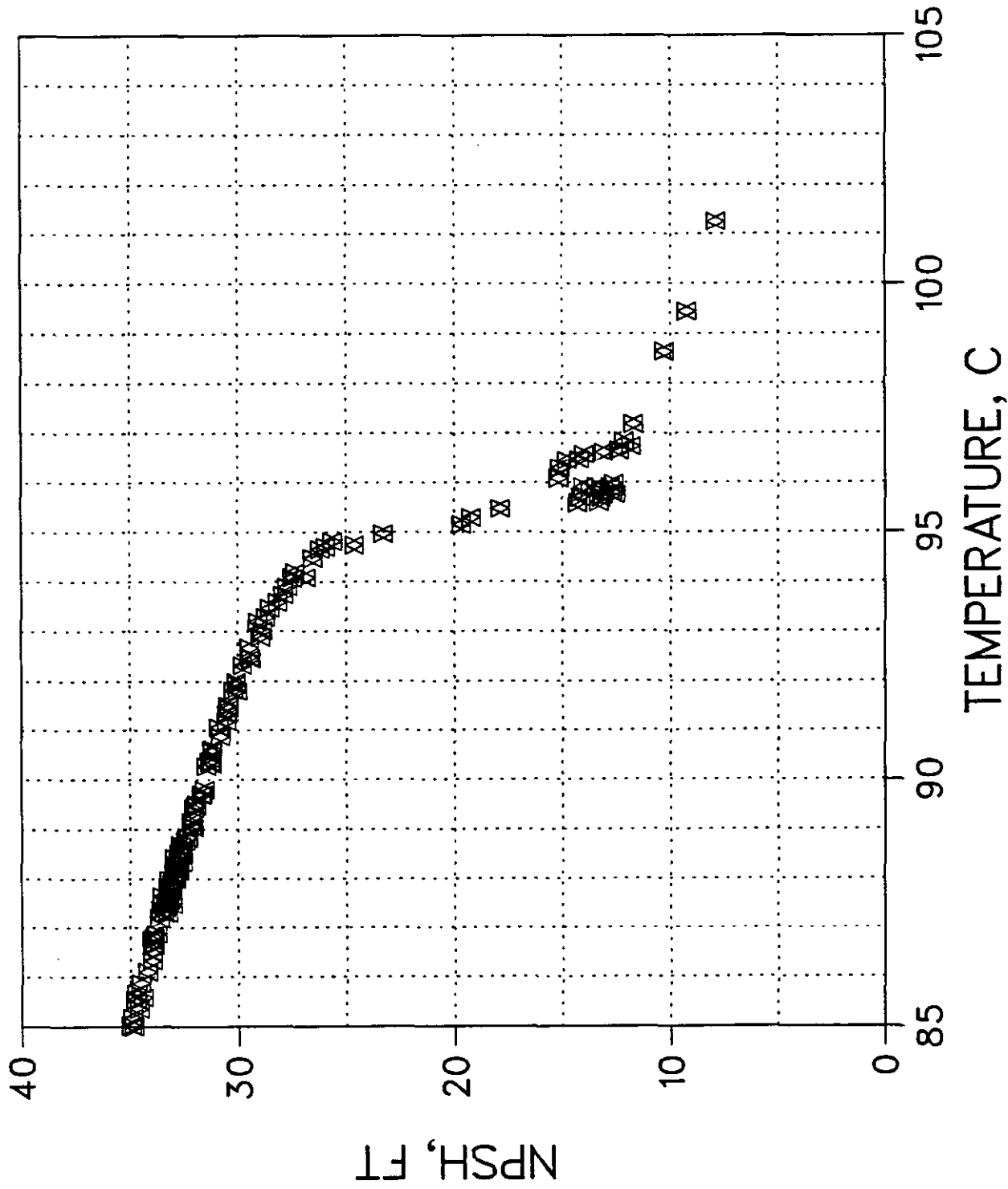
PUMP CAVITATION TESTS
UNADJ. TEMP. VS NPSH AT CL IMPELLER 5 pumps



PUMP CAVITATION TESTS
UNADJ. TEMP. VS NPSH AT CL IMPELLER 5 pumps



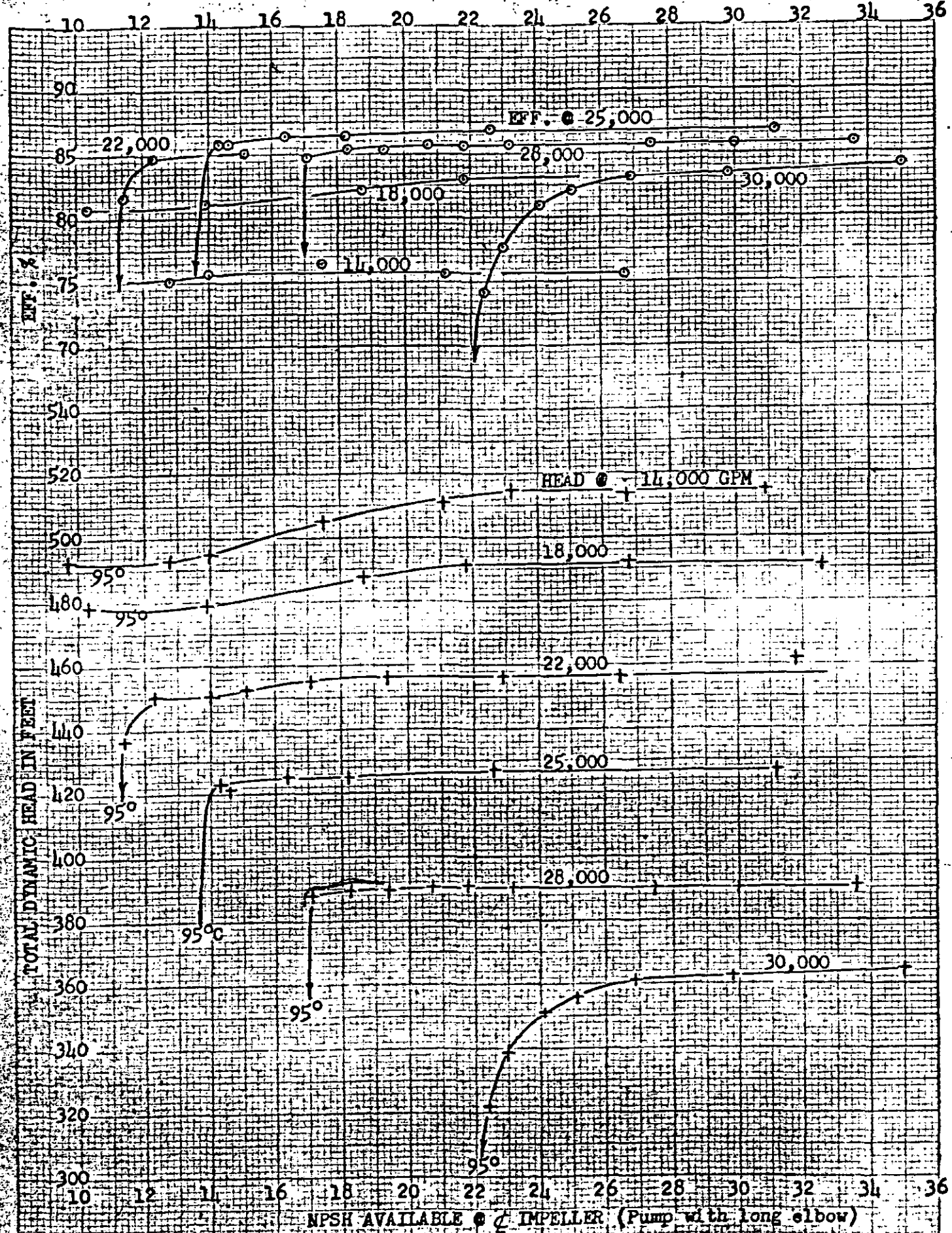
PUMP CAVITATION TESTS
UNADJ. TEMP. VS NPSH AT CL IMPELLER 5 pumps



T-6h160-K

APPROVED BY
BINGHAM PUMP COMPANY

T-6h160-K



Temp. 95°C
 Long Radius Suction elbow
 Approach No. 2
 ENR 11-17-56
 Bingham Pump Company

16 x 24 x 43 CD
 31799-1
 39-3/8 Diameter
 1000 RPM
 T-6h160-K

BINGHAM PUMP CO. PORTLAND, OREGON

PUMP SIZE & TYPE		CUSTOMER		CURT. ORDER NO.		PAGE		BINGHAM TEST NO.						
16 x 24 x 43 CD		E. I. DuPont de Nemours & Co.		AFC 22156 1/2 AX 2307		1 of 6		7-64160						
IMP. PART.	YANE	IMP. MAX DIA.	EYE AREA	ASSEMBLY	TEST MOTOR: CUSTOMER'S ALLIS-CHALMERS MOTOR	TEST MOTOR: 1000 RPM	TEST MOTOR: SERIAL NO. 74444	PUMP SERIAL NO.	TESTED BY					
1613 CD	4	42"	496 SQ IN	Z-2680	% EFF. @ LOAD: 72.8 @ 1/2, 54.3 @ 3/4, 34.1 @ 1, 22.8 @ 1 1/4			31799	ENR-MCL					
IMP. TEST DIA.	39-3/8 U.F. & O.F. to 1 1/2 x 6	CLASS B Cleared	DISCHARGE PIPE I. D.	SUCTION PIPE I. D.	TEST GEAR: CUSTOMER'S WESTERN GEAR, RATIO 1.73:1, 48 HP LOSS, SERIAL NO. 101									
NPWH CALC.			15"	23 1/4"										
NPWH = H _s + H _d + H _f			WATER TEMP. 95 °C		SUCTION APPROACH CASE No. 2 Center									
H _s = 5.3			VAPOR PRESS. H _v 29.5 FT. WATER		SUCTION ELBOW									
H _d = 11.3			BAR. H _a 30.08 IN HG		SUCTION GAGE ZERO, DWT G & IMP. G AT SAME ELEVATION									
H _f = 25.0														
NPWH = 41.6														
TIME FOR 10 REV. MOTOR SLIP SEC.	PUMP SPEED RPM	PUMP ONLY FEET OF WATER	PUMP WITH ELBOW FEET OF WATER	SUCTION IN. HG. @ A	DISCHARGE DWT. °C	BY 4-32 FT. PER 10,000 GPM	TOTAL DYNAMIC HEAD IN FEET OF WATER	24" VENTURI METER IN. HG. G.P.M.	POWER CURVE 14531 C.T. 40:1 P.T. 120:1 P = 4800	WATER HP	PUMP EFF. %	HEAD PROP. ACROSS ELBOW FROM B	AVG. S. G. FEET OF WATER	TEMP. °C
1	17.3	17.3	18.2	6.1	168.7	27.0	424.8	17.45	499	2580	86.4	2 2.3 3 4 5 6	0.9	
2	15.5	15.5	16.4	4.6	168	27.0	424.8	17.45	499	2580	86.4	5.1 2.4 0.5 0	0.9	
3	13.1	13.1	14.6	3.1	166	27.0	421.8	17.45	500	2565	85.8	5.0 2.5 0.6 0	0.9	
4	10.3	10.3	13.6	2.2	110	27.0	288.5	17.45	465	1755	63.8	5.5 3.5 1.0 0.4	1.2	
5	12.6	12.6	14.3	2.8	166.4	27.0	423.3	17.45	501	2570	85.8	5.0 4.5 2.7 2.2	3.0	
6	21.6	21.6	22.6	9.9	174.4	27.0	427.0	17.45	499	2600	87.0	5.3 4.0 0.7 0.3	0.6	
7	31.2	31.2	31.2	17.2	175	27.0	426.8	17.45	499	2595	86.8	4.6 2.8 0.5 0	0.7	
8	30.4	30.4	30.4	15.5	174	27.0	425.2	17.45	499	2585	86.4			
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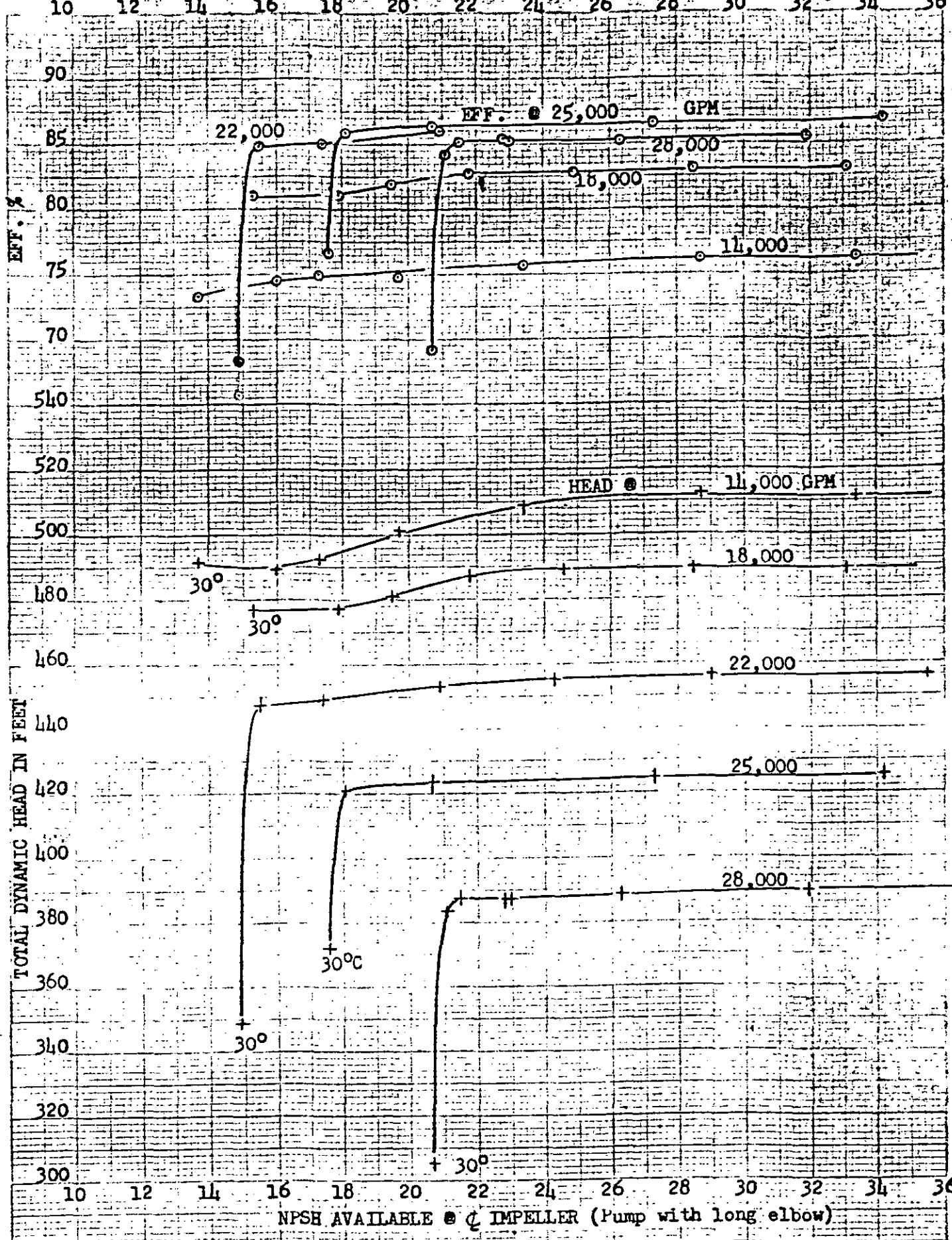
DATA CHECKED AND CERTIFIED CORRECT BY: *[Signature]*

TEST WITNESSED BY: *[Signature]*

S/S J.S. M... ..

T-64160-L

T-64160-L

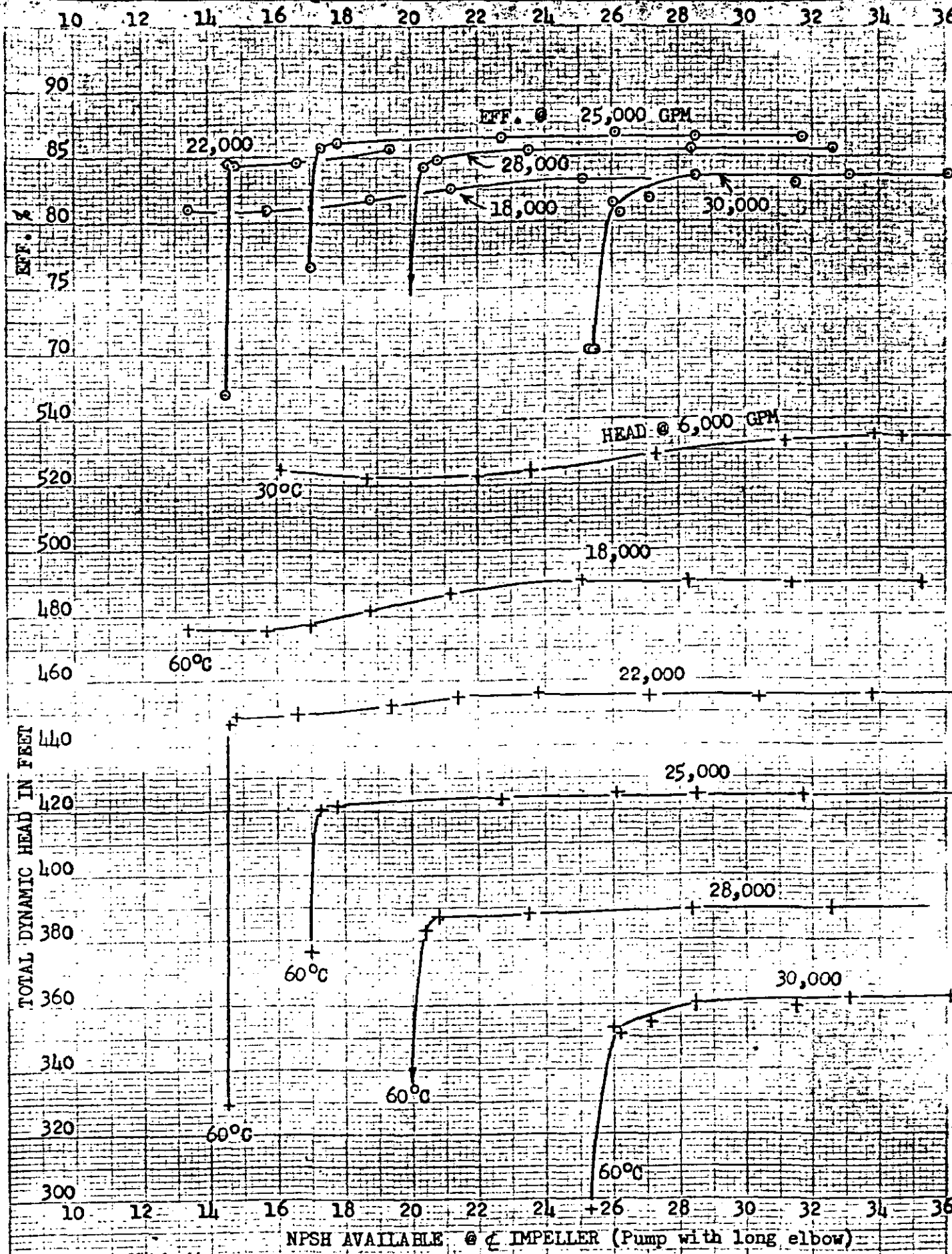


Temp. 30°C
 Long Radius Suction elbow
 Approach No. 2
 ENR 11-19-56
 Bingham Pump Company

16 x 24 x 43 CD
 31799-1
 39-3/8 Diameter
 1000 RPM
 T-64160-L

H-09179-1
 T-61160-M
 APPROVED FOR PUBLICATION
 FEBRUARY 1957
 ENGINEERING

H-09179-1



Temp. 30° ; 60°
 Long Radius Suction elbow
 Approach No. 2
 ENR 11-19-56
 Bingham Pump Company

16 x 24 x 43 CD
 31799-1
 39-3/8 Diameter
 1000 RPM
 T-61160-M

DINGHAM PUMP CO. PORTLAND, OREGON

PUMP SIZE & TYPE 16 x 24 x 43 CD		CUSTOMER E. I. DUPONT de NEMOURS & CO.		CUST. ORDER NO. AXC 22156 1/2 AX-2307		PAGE 1 OF 6		BINGHAM TEST NO. T-64160	
IMP. PATT. 1613 CD		EYE DIAMETER 19 1/2"		ASSEMBLY Z-2680		TEST MOTOR: CUSTOMER'S ALLIS-CHALMERS MOTOR 3000 HP, 1800 RPM, SERIAL NO. 134544		PUMP SERIAL NO. 31799	
IMP. TEST DIA. 39-3/8" U.F. & O.F. to 1-1/4 x 6 Class B Cleared		DISCHARGE PIPE I. D. 15"		SUCTION PIPE I. D. 23 1/4"		% EFF. @ LOAD, 92.8 @ 1/2, 94.3 @ 3/4, 94.5 @ 1 1/4		TESTED BY ENR:MKL	
DATE 9-6/7-56		WATER TEMP. 60 °C		SUCTION APPROACH CASE No. 2 Center		START 11:00 P.M.		STOP Page 5	
NPSH CALC. NPSH = H _s + $\frac{V^2}{2g}$ + H _f = H _s + 5.2 + 34.4 = H _s + 33.1 @ 25,000 GPM		VAPOR PRESS. H _{vp} 6.8 FT. WATER		SUCTION ELBOW LONG RADIUS		SUCTION GAGE ZERO, DWT & IMP. @ AT SAME ELEVATION		TEMPERATURE THERM. COUPLE °C. TANKS RECORDED & CONF. TROX °C.	

QZ	SPEED	PUMP ONLY FEET OF WATER	NPSH @ 1/2 IMP. FEET OF WATER	PUMP WITH L-R. ELBOW FEET OF WATER	SUCTION IN HG @ A	HG. COLUMN Before IN HG	DISCHARGE DWT. °C	H _v 4.32 FT. PER 10,000 GPM	TOTAL DYNAMIC HEAD IN FEET OF WATER	CAPACITY						PUMP EFF. %	AVG. 3, 4, 5, 6 FEET OF WATER	TEMPERATURE °C.
										24" VENTURI METER F	WATTS READ	BHP OUTPUT	WATER HP	IN. HG.	G.F.M.			
1		41.1	42.1	7.9	9.0	173 1/2	407.027.0	27.0	425.0	17.85	509	3045	4021	86.7	1.0	60		
2		35.7	36.7	3.2	3.6	171	401.227.0	27.0	424.6	17.85	509	3045	2638	86.5	1.0			
3		30.7	31.7	-1.1	-1.4	168-3/4	395.927.0	27.0	424.3	17.85	509	3045	2638	86.5	1.0			
4		25.1	26.1	-6.0	-7.0	167	391.827.0	27.0	425.8	17.85	509	3045	2645	86.8	1.0			
5		21.6	22.7	-9.8	-10.4	164-3/4	386.527.0	27.0	423.9	17.85	509	3045	2635	86.5	1.1			
6		16.8	17.8	-13.2	-15.3	161-3/4	379.527.0	27.0	421.8	17.85	510	3050	2625	86.1	1.0			
7		16.3	17.3	-13.7	-15.8	161	377.727.0	27.0	420.5	17.85	510	3050	2615	85.7	1.0			
8		13.5	17.0	-13.9	-16.1	142	333.127.0	27.0	376.2	17.85	510	3050	2340	76.7	3.5			
9			28.5	-3.9	-4.6	167-1/2	393.027.0	27.0	424.6	17.85	509	3045	2638	86.5				
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DATA CHECKED AND
CORRECTED BY:

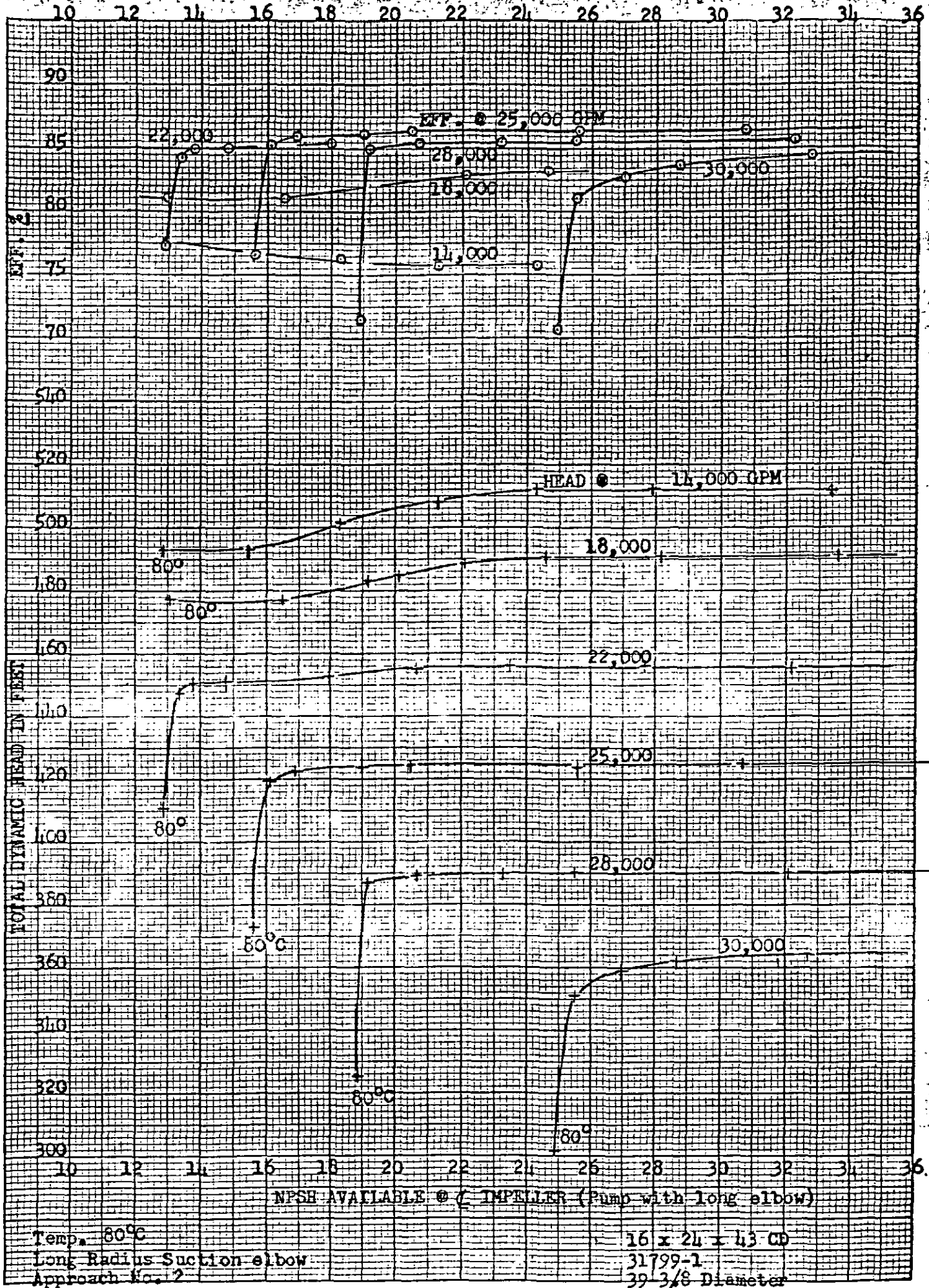
E. A. Lem

TEST WITNESSED BY
E. I. DUPONT de NEMOURS & CO.

Not witnessed

T-64160-

T-64160-N



KEUFFEL & ESSER CO. ALBANY, N.Y.

ALBANY, N.Y.

Temp. 80°C
 Long Radius Suction elbow
 Approach No. 2

16 x 24 x 4.3 CD
 31799-1
 39 3/8 Diameter
 1000 RPM
 T-64160-N

ENR 11-19-56
 Bingham Pump Company

YMR

BINGHAM PUMP CO. PORTLAND, OREGON

PUMP SIZE & FITS 16 x 24 x 43 CD			CUSTOMER E. I. DuPONT de NEMOURS & CO.			CUST. ORDER NO. AXC 22156 1/2 / AE2307			PAGE 1 OF 6		BINGHAM TEST No. T-64160-N	
IMP. PAT. 1613 CD	VALE 4	IMP. MAX DIA. 42"	EYE DIAMETER 19 1/2"	EYE AREA 496 SQ. IN.	ASSEMBLY Z-2680	TEST MOTOR, CUSTOMER'S ALLIS-CHALMERS MOTOR 3000 HP. 1800 RPM SERIAL No. 134344 % EFF. @ LOAD: 92.8 @ 1/2, 94.3 @ 3/4, 94.5 @ 1, 94.5 @ 1 1/4			PUMP SERIAL No. 31799-1			
IMP. TEST DIA. 39-3/8 U.F. & O.F. to 1 1/4 x 6 Class B Cleanup			DISCHARGE PIPE I. D. 15"		SUCTION PIPE I. D. 23 1/4"		TEST GEAR: CUSTOMER'S WESTERN GEAR, RATIO 1.783:1, 45 HP LOSS, SERIAL No. 101			TESTED BY ENR-MKL		DATE 9-12/13

NPSH CALC. NPSH = H _s + $\frac{V^2}{2g}$ + H _A - H _{Vp} = H _s + 5.5 + 34.9 - 16.1 = H _s + 24.3 @ 25000 GPM			WATER TEMP. 80 °C VAPOR PRESS. H _{Vp} 16.1 FT. WATER BAR. H _{29.95} IN HG. 34.9 FT. WATER			SUCTION APPROACH CASE No. 2 Center SUCTION ELBOW Long Radius SUCTION GAGE ZERO, DWT & IMP. & AT SAME ELEVATION						START 11:00
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RUN NO.	SPEED		NPSH @ IMP.		SUCTION		DISCHARGE		H _v 4.32 FT. PER 10,000 GPM	TOTAL DYNAMIC HEAD IN FEET OF WATER	CAPACITY		POWER		WATER HP F =	PUMP EFF. %	HEAD DROP ACROSS ELBOW FROM 3						AVG. 3, 4, 5, 6 1.07 FEET OF WATER	THERMO COUPLE #6 °C		
	TIME FOR 10 REV. MOTOR SLIP SEC.	PUMP SPEED RPM	PUMP ONLY FEET OF WATER	PUMP WITH L.R. ELBOW FEET OF WATER	HG. COLUMN Before ELBOW		DWT. "C"				24" VENTURI METER F = 5958	CURVE 14531 C.T. 40:1 P.T. 120:1 F = 4800	IN. HG.	G.P.M.			WATTS READ	BHP OUTPUT	IN. HG.							
					IN. HG. @ A	FEET OF WATER	PSI	FEET OF WATER											2	3	4	5			6	
1			29.6	30.7	+5.7	6.4	170 1/2	104.2	27.0	421.8	17.6	25000	504	3015	2605	86.5	5.1	2.4	0.5	0	-	1.1	79 1/2	80		
2			24.5	25.6	+1.3	+1.3	167 7/8	398.2	27.0	423.9	17.6	25000	504	3015	2600	86.3	5.2	2.5	0.7	0	-	1.1	80	80		
3			19.4	20.5	-3.1	-3.8	165 7/8	393.5	27.0	424.3	17.6	25000	504	3015	2604	86.4	5.1	2.5	0.6	0	-	1.1	79	75		
4			15.7	16.9	-6.2	-7.4	163 1/2	388.1	27.0	422.5	17.6	25000	505	3020	2595	86.0	5.5	2.6	0.7	0	-	1.2	79	80		
5			13.8	16.1	-6.9	-8.2	162	384.6	27.0	419.8	17.6	25000	505	3020	2575	85.2	5.1	3.4	1.9	1.2	-	2.3	79	75		
6			12.1	15.6	-7.3	-8.7	142	337.1	27.0	372.8	17.6	25000	500	2490	2290	76.6	4.8	5.7	2.5	1.6	-	3.5	78	75		
7				19.0	-4.4	-5.3	165	391.7	27.0	424.0	17.6	25000	504	3015	2600	86.2							79 1/2	75		
8				37.2	+11.3	+12.9	173 1/2	411.9	27.0	426.0	17.6	25000	503	3010	2620	87.0							80	80		
9				42.3	+15.7	+18.0	175 1/2	416.6	27.0	425.6	17.6	25000	503	3010	2618	86.9							80	80		
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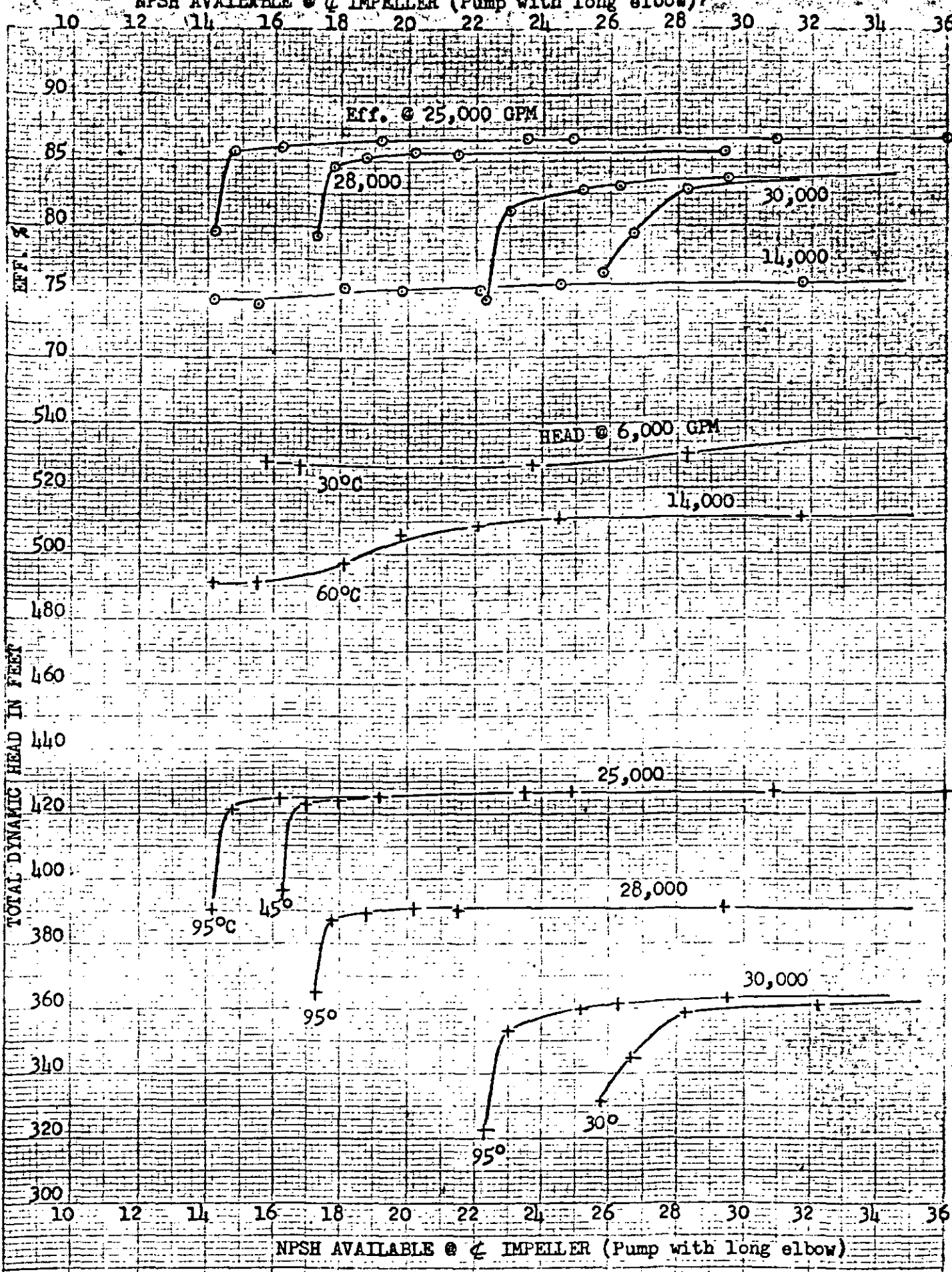
DATA CHECKED AND
CORRECTED BY

TEST WITNESSED BY
E. I. DuPONT de NEMOURS & CO.

NOT WITNESSED

0-001170-1
 KENNEDY & SONS CO.
 WILMINGTON, DE.
 4001101

T-64160-0

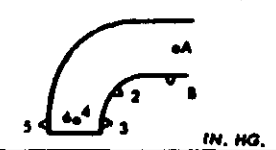


Temp. 30°, 45°, & 60°C
 Long Radius Suction elbow
 Approach No. 2
 ENR 11-29-56
 Bingham Pump Company

16 x 24 x 43 CD
 31799-1
 39-3/8 Diameter
 1000 RPM
 T-64160-0

DINGHAM PUMP CO. PORTLAND, OREGON

PUMP SIZE & T.P. 16 x 24 x 43 CD			CUSTOMER E. I. DuPONT de NEMOURS & CO.			CUST. ORDER NO. AXC 22156 1/2 AX-2307			PAGE 3 OF 7		BINGHAM TEST No. T-64160- 0	
IMP. PATT. 1613 CD		VANE 4	IMP. MAX DIA. 42"		EYE DIAMETER 19 1/2"	EYE AREA 496 SQ. IN.	ASSEMBLY Z-2680		TEST MOTOR: CUSTOMER'S ALLIS-CHALMERS MOTOR 3000 HP. 1800 RPM SERIAL No. 154544 % EFF. @ LOAD: 92.8 @ 1/4, 94.3 @ 3/4, 94.5 @ 1, 94.5 @ 1 1/4			PUMP SERIAL No. 31799- 1
IMP. TEST DIA. 39-3/8" U.F. & O.F. to 1 1/4 x 6 Class B Cleanup			DISCHARGE PIPE I. D. 15"		SUCTION PIPE I. D. 23 1/4"		TEST GEAR: CUSTOMER'S WESTERN GEAR, RATIO 1.783:1, 45 HP LOSS, SERIAL No. 101			TESTED BY GMR:MKL	DATE 9-14-56	
NPSH CALC. NPSH = H _s + $\frac{V^2}{2g}$ + H _A - H _{vp} = H _s + 6.9 + 35.2 - 29.5 = H _s + 12.6 @ 28,000 GPM			WATER TEMP. 95 °C VAPOR PRESS. H _{vp} 29.5 FT. WATER BAR. H _A 29.97 IN HG 35.2 FT. WATER			SUCTION APPROACH CASE No. 2 Center SUCTION ELBOW Long Radius SUCTION GAGE ZERO, DWT C & IMP. C AT SAME ELEVATION			START 12:30 A.M.		STOP Page 7	

RUN NO.	SPEED		NPSH @ C IMP.		SUCTION		DISCHARGE		H _v 4.32 FT. PER 10,000 GPM	TOTAL DYNAMIC HEAD IN FEET OF WATER	CAPACITY		POWER		WATER HP F = 4110	PUMP EFF. %	HEAD DROP ACROSS ELBOW FROM B						AVG. 3, 4, 5, 6 FEET OF WATER	THERMO COUPLE #6 °C	FAST REC'D & CORRECTED °C		
	TIME FOR 10 REV. MOTOR SLIP SEC.	PUMP SPEED RPM	PUMP ONLY FEET OF WATER	PUMP WITH L.R. ELBOW FEET OF WATER	HG. COLUMN Before ELBOW F = 1.174-0.3		DWT. "C" F = 2.398				24" VENTURI METER F = 5989		CURVE 14531 C.T. 40:1 P.T. 120:1 F = 4800				WATTS READ	BHP OUTPUT									
					IN. HG. @ A	FEET OF WATER	PSI	FEET OF WATER			IN. HG.	G.P.M.	IN. HG.	G.P.M.					2	3	4	5				6	
1			43.1	26.2	30.5	161 1/2	387.3	33.9	390.7	21.9	28000	518	3100	2660	85.8								1.09	95	95 1/2		
2			29.4	14.6	16.8	156	374.1	33.9	391.2	21.9	28000	519	3105	2660	85.7									95	95		
3			21.5	7.8	8.9	152 1/4	365.1	33.9	390.1	21.9	28000	519	3105	2655	85.5									94 1/2	95		
4			20.2	6.7	7.6	152	364.5	33.9	390.8	21.9	28000	519	3105	2660	85.7									95	95		
5			17.6	5.5	6.2	151	362.1	33.9	389.8	21.9	28000	519	3105	2650	85.3	7.0	2.8	0.9	0	-	1.2	95	95				
6			14.4	4.3	4.7	140	335.7	33.9	364.9	21.9	28000	523	3130	2480	79.3	6.0	4.5	2.6	1.1	-	2.9	95	95				
7			16.3	4.7	5.2	149 1/4	358.5	33.9	387.2	21.9	28000	520	3110	2635	84.6	6.8	2.9	1.2	0.3	-	1.5	95	95				
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DATA CHECKED AND
CORRECTED BY: *E. I. DuPont*

TEST WITNESSED BY
E. I. DuPONT de NEMOURS & CO. Not witnessed

BINGHAM PUMP CO. PORTLAND, OREGON

PUMP SIZE & TYPE 16x24x43 CD			CUSTOMER E. I. DuPONT de NEMOURS & CO.			CUST. ORDER NO. AXC 22156 1/2 AX-2307			PAGE 4 OF 7		BINGHAM TEST No. T-64162-0			
IMP. PATT. 1613 CD	VAPE 4	IMP. MAX DIA. 42"	EYE DIAMETER 19 1/2"		EYE AREA 496 SQ. IN.	ASSEMBLY Z-2680		TEST MOTOR: CUSTOMER'S ALLIS-CHALMERS MOTOR 3000 HP. 1000 RPM SERIAL No. 154564 % EFF. @ LOAD: 92.8 @ 1/2, 94.3 @ 3/4, 94.5 @ 1, 94.5 @ 1 1/4				PUMP SERIAL No. 31799-1		
IMP. TEST DATA 39-3/8" U.F. & O.F. to 1 1/4 x 6 Class B Cleanup			DISCHARGE PIPE I. D. 15"		SUCTION PIPE I. D. 23 1/4"		TEST GEAR: CUSTOMER'S WESTERN GEAR, RATIO 1.783:1, 45 HP LOSS, SERIAL No. 101				TESTED BY ENR:MLL	DATE 9-14-56		
NPSH CALC. NPSH = H _s + $\frac{V^2}{2g}$ + H _A - H _{Vp} = H _s + 3.7 + 34.4 - 6.8 = H _s + 29.3 @ 14,000 GPM			WATER TEMP. 60 °C			VAPOR PRESS. H_{Vp} 6.8 FT. WATER			SUCTION APPROACH CASE No. 2 Center				START Page 3	
			BAR. H_A 29.97 IN HG 34.4 FT. WATER			SUCTION ELBOW Long Radius			SUCTION GAGE ZERO, DWT & IMP. & AT SAME ELEVATION				STOP Page 7	

RUN NO.	SPEED		NPSH @ 1 IMP.		SUCTION		DISCHARGE		H _v 4.32 FT. PER 10,000 GPM	TOTAL DYNAMIC HEAD IN FEET OF WATER	CAPACITY		POWER		WATER HP F = 4021	PUMP EFF. %	HEAD DROP ACROSS ELBOW FROM B						AVG. 3, 4, 5, 6 FEET OF WATER	THERMO COUPLE #6 °C	TEMP. °C
	TIME FOR 10 REV. MOTOR SLIP SEC.	PUMP SPEED RPM	PUMP ONLY FEET OF WATER	PUMP WITH L.R. ELBOW FEET OF WATER	HG. COLUMN Before ELBOW		DWT. "C"				24" VENTURI METER		CURVE 14531				IN. HG.								
					IN. HG. @ A	FEET OF WATER	PSI	FEET OF WATER			IN. HG.	G.P.M.	WATTS READ	BHP OUTPUT			2	3	4	5	6				
1			39.8	40.2	+9.6	+10.9	219	513.8	8.5	511.4	5.6	14000	396	2350	1782	75.8	1.6	0.9	0.2	0	-	0.4	60	60	
2			31.3	31.7	+2.2	+2.4	215 1/2	505.6	8.5	511.7	5.6	14000	397	2355	1782	75.7	1.7	0.9	0.2	0	-	0.4	60	60	
3			24.1	24.5	-4.1	-4.8	212	497.4	8.5	510.7	5.6	14000	397	2355	1780	75.6	1.6	0.9	0.3	0	-	0.4	60	60	
4			19.4	19.8	-8.2	-9.5	208	488.0	8.5	506.0	5.6	14000	396	2350	1765	75.1	1.7	0.8	0.2	0	-	0.4	60	60	
5			15.1	15.5	-11.9	-13.8	200	469.2	8.5	491.5	5.6	14000	390	2315	1712	74.1	1.7	0.9	0.2	0	-	0.4	60	60	
6			13.8	14.2	-13.2	-15.1	199 1/2	468.0	8.5	491.6	5.6	14000	388	2300	1712	74.5	1.7	0.8	0.2	0	-	0.4	60	60	
7			17.6	18.1	-9.7	-11.2	203 1/2	477.4	8.5	497.1	5.6	14000	387	2295	1730	75.4	1.6	1.1	0.4	0	-	0.5	60	60	
8			22.1		-6.2	-7.2	210	492.7	8.5	508.4	5.6	14000	396	2350	1768	75.2							60	60	
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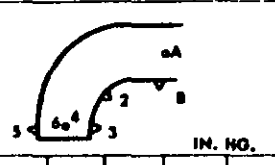
E. I. DuPont

DINGHAM PUMP CO. PORTLAND, OREGON

PUMP SIZE & TYPE 16 x 24 x 43 CD		CUSTOMER E. I. DuPONT de NEMOURS & CO.			CUST. ORDER NO. AXC 22156 1/2 AX-2307		PAGE 5 OF 7	BINGHAM TEST No. T-64160-0
IMP. PATT. 1613 5D	VANE 4	IMP. MAX DIA. 42"	EYE DIAMETER, 19 1/2"	EYE AREA 496 SQ. IN.	ASSEMBLY Z-2680	TEST MOTOR: CUSTOMER'S ALLIS-CHALMERS MOTOR 3000 HP. 1800 RPM SERIAL No. 154544 % EFF. @ LOAD: 92.8 @ 1/2, 94.3 @ 3/4, 94.5 @ 1, 94.5 @ 1 1/2		PUMP SERIAL No. 31799-1

IMP. TEST DIA. 39-3/8" U.F. & O.F. to 1 1/4 x 6 Class B Cleanup		DISCHARGE PIPE I. D. 15"	SUCTION PIPE I. D. 23 1/4"	TEST GEAR: CUSTOMER'S WESTERN GEAR, RATIO 1.783:1, 45 HP LOSS, SERIAL No. 101	TESTED BY ENR SKKL	DATE 9-11-56
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NPSH CALC. NPSH = H _s + $\frac{V^2}{2g}$ + H _A - H _{vp} = H _s + $\frac{7.9^2}{2 \times 32.2}$ + $\frac{34.0}{2.31}$ - $\frac{1.4}{2.31}$ = H _s + 10.5 @ 30,000 GPM		WATER TEMP. 30 °C VAPOR PRESS. H _{vp} 1.4 FT. WATER BAR. H _a 29.97 IN HG 34.0 FT. WATER	SUCTION APPROACH CASE No. 2 Center SUCTION ELBOW Long Radius SUCTION GAGE ZERO, DWT ϕ & IMP. ϕ AT SAME ELEVATION	START Page 3 STOP Page 7
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RUN NO.	SPEED		NPSH @ ϕ IMP.		SUCTION		DISCHARGE		H _v 4.32 FT. PER 10,000 GPM	TOTAL DYNAMIC HEAD IN FEET OF WATER	CAPACITY		POWER		WATER HP P =	PUMP EFF. %	HEAD DROP ACROSS ELBOW FROM B						TEMPERATURE			
	TIME FOR 10 REV. MOTOR SLIP SEC.	PUMP SPEED RPM	PUMP ONLY FEET OF WATER	PUMP WITH L.R. ELBOW FEET OF WATER	HG. COLUMN Before Elbow F = 1.134		DWT. "C"				24" VENTURI METER F = 5885		CURVE 14531 C.T. 40.1 P.T. 120.1 P. 4800	WATTS READ			BHP OUTPUT							AVG. 3, 4, 5, 6 1.05 FEET OF WATER	THERMO COUPLE #6 °C	TANK TEMP. & CORR. TEST °C
					IN. HG. @ A	FEET OF WATER	PSI	FEET OF WATER			IN. HG.	G.P.M.						2	3	4	5	6				
1			44.2	45.7	+4.6	+5.2	143	331.3	38.0	364.9	26.0	30000	544	3260	2755	84.5	7.3	3.5	0.9	0	-	1.5	31	31		
2			30.7	32.3	-7.2	-8.2	135 1/2	314.0	38.0	361.0	26.0	30000	543	3250	2725	83.8	7.4	3.5	1.0	0	-	1.6	30	30		
3			26.7	28.3	-10.8	-12.2	132-3/4	307.6	38.0	358.6	26.0	30000	546	3270	2710	82.8	7.5	3.5	1.0	0	-	1.6	30	30		
4			24.2	25.8	-13.0	-14.7	120	278.0	38.0	331.5	26.0	30000	546	3270	2500	76.5	7.5	3.6	1.0	0	-	1.6	30	30		
5			25.1	26.7	-12.2	-13.8	126	291.9	38.0	344.5	26.0	30000	547	3275	2600	79.5	7.5	3.5	1.0	0	-	1.6	30	30		
6																										
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DATA CHECKED AND
CERTIFIED CORRECT BY:

E. I. DuPont
CHIEF TEST ENGINEER

TEST WITNESSED BY
E. I. DuPONT de NEMOURS & CO.

Not witnessed

DINGHAM PUMP CO. PORTLAND, OREGON

PUMP SIZE & TYPE 16 x 24 x 43 CD			CUSTOMER E. I. DuPONT de NEMOURS & CO.			CUST. ORDER NO. AXC 22156 1/2 AX-2307		PAGE 6 OF 7		BINDER & TEST No. T-64160- 2		
IMP. PATT. 1613 CD	VANE 4	IMP. MAX DIA. 42"	EYE DIAMETER 19 1/2"	EYE AREA 496 SQ. IN.	ASSEMBLY Z-2680	TEST MOTOR: CUSTOMER'S ALLIS-CHALMERS MOTOR 3000 HP. 1800 RPM SERIAL No. 154544 % EFF. @ LOAD: 92.8 @ 1/2, 94.3 @ 3/4, 94.3 @ 1, 94.5 @ 1 1/4				PUMP SERIAL No. 21799- 92		
IMP. TEST DIA. 39-3/16" U.F. & O.F. to 1 1/4 x 6 Class B Cleanup			DISCHARGE PIPE I. D. 15"		SUCTION PIPE I. D. 23 1/4"		TEST GEAR: CUSTOMER'S WESTERN GEAR, RATIO 1.783:1, 45 HP LOSS, SERIAL No. 101				TESTED BY ENR:MKL	DATE 9-14-56

NPSH CALC. NPSH = H _s + $\frac{v^2}{2g}$ + H _A - H _{vp} = H _s + 0.3 + 34.0 - 1.4 = H _s + 32.9 @ 6000 GPM			WATER TEMP. 30 °C VAPOR PRESS. H _{vp} 1.4 FT. WATER BAR. H _A 29.97 IN HG 34.0 FT. WATER			SUCTION APPROACH CASE No. 2 Center SUCTION ELBOW Long Radius SUCTION GAGE ZERO, DWT & IMP. & AT SAME ELEVATION						START Page 3 STOP Page 7	
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QUI NO.	SPEED		NPSH @ IMP.		SUCTION		DISCHARGE		H _v 4.32 FT. PER 10,000 GPM	TOTAL DYNAMIC HEAD IN FEET OF WATER	CAPACITY		POWER		WATER HP F =	PUMP EFF. %	HEAD DROP ACROSS ELBOW FROM B						AVG. 3, 4, 5, 6 1.05 FEET OF WATER	THERMO COUPLE #6 °C	TASER REC'D & COIL TEMP °C		
	TIME FOR 10 REV. MOTOR SLIP SEC.	PUMP SPEED RPM	PUMP ONLY FEET OF WATER	PUMP WITH L.R. ELBOW FEET OF WATER	HG. COLUMN Before ELBOW		DWT. "C"				24" VENTURI METER		CURVE 14531 C.T. 40:1 P.T. 120:1 F = 4800				WATTS READ	BHP OUTPUT	IN. 1								
					IN. HG. @ A	FEET OF WATER	PSI	FEET OF WATER			IN. HG.	G.P.M.	2	3					4	5	6						
1			39.6	39.7	+6.0	+6.8	233 1/2	541.0	1.6	535.8	1.04	6000	302	1770	810	45.7	0.3	0.2	0.2	0	-	0.1	29	29			
2			28.2	28.3	-4.1	-4.6	226 1/2	524.2	1.6	530.4	1.04	6000	305	1790	801	44.7	0.3	0.2	0.2	0	-	0.1	29	29			
3			23.6	23.7	-8.1	+9.2	223	516.7	1.6	527.5	1.04	6000	310	1820	797	43.8	0.3	0.2	0.2	0	-	0.1	29	29			
4			16.7	16.8	-14.2	-16.1	220	509.7	1.6	527.4	1.04	6000	305	1790	797	44.5	0.3	0.2	0.2	0	-	0.1	30	30			
5			15.7	15.8	-15.1	-17.1	220	509.7	1.6	528.4	1.04	6000	305	1790	799	44.6											
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DATA CHECKED AND CERTIFIED CORRECT BY: <u><i>E. J. Klein</i></u> CHIEF TEST ENGINEER	TEST WITNESSED BY: <u>Not witnessed</u> E. I. DuPONT de NEMOURS & CO.
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PUMP SIZE & FT.

16 x 24 x 43 CD

CUSTOMER

E. I. DuPONT de NEMOURS & CO.

CUST. ORDER NO.

AXC 22156 1/2 AX-2307

PAGE

7 OF 7

TEST No.

64169

IMP. PATT. 1613 CD

VANE 4

IMP. MAX DIA. 42"

EYE DIAMETER 19 1/2"

EYE AREA 496 SQ. IN.

ASSEMBLY Z-2680

TEST MOTOR: CUSTOMER'S ALLIS-CHALMERS MOTOR
3000 HP, 1800 RPM SERIAL No. 154564
% EFF. @ LOAD: 92.8 @ 1/2, 94.3 @ 3/4, 94.5 @ 1, 94.5 @ 1 1/4

PUMP SERIAL No. 31799

IMP. TEST DIA. 39 3/8" U.F. & O.F. to 1 1/2 x 6
Class B Cleanup

DISCHARGE PIPE I. D. 15"

SUCTION PIPE I. D. 23 1/4"

TEST GEAR: CUSTOMER'S WESTERN GEAR,
RATIO 1.783:1, 45 HP LOSS, SERIAL No. 101

TESTED BY
EMR:MKL

DATE
9-16-5

NPSH CALC.

$$\begin{aligned} NPSH &= H_s + \frac{V_s^2}{2g} + H_a - H_{vp} \\ &= H_s + 5.5 + 34.2 - 3.3 \\ &= H_s + 36.4 @ 25,000 \text{ GPM} \end{aligned}$$

WATER TEMP. 45 °C

VAPOR PRESS. H_{vp} 3.3 FT. WATER

BAR. H_a 29.97 IN HG 34.2 FT. WATER

SUCTION APPROACH CASE No. 2 Center

SUCTION ELBOW Long Radius

SUCTION GAGE ZERO, DWT & IMP. @ SAME ELEVATION

START
PAGE 3

STOP
6:40 A

RUN NO.	FEED		NPSH @ C. IMP.		SUCTION		DISCHARGE		TOTAL DYNAMIC HEAD IN FEET OF WATER	CAPACITY		POWER		WATER HP	PUMP EFF. %	HEAD DROP ACROSS ELBOW FROM B						AVG. 3, 4, 5, 6, 1.05 FEET OF WATER	THERMO COUPLE °C	
	TIME FOR 10 REV. MOTOR SLIP SEC.	PUMP SPEED RPM	PUMP ONLY FEET OF WATER	PUMP WITH L.R. ELBOW FEET OF WATER	HG. COLUMN Before ELBOW		DWT. "C"			Hv 4.32 FT. PER 10,000 GPM	24" VENTURI METER	CURVE 14531 C.T. 40:1 P.T. 170:1 F = 4800	WATTS READ			BHP OUTPUT	IN. HG.							
					IN. HG. @ A	FEET OF WATER	PSI	FEET OF WATER									2	3	4	5	6			
1			44.6	45.8	+8.3	+9.4	175	407.8	27.0	425.4	17.95	25000	512	3060	2665	87.2	5.1	2.6	0.8	0	-	1.2	45	
2			34.1	35.3	-0.8	-0.9	171	398.4	27.0	426.3	17.95	25000	512	3060	2670	87.2	5.2	2.4	0.9	0	-	1.2	45	
3			23.5	24.6	-10.3	-11.8	165-3/4	386.2	27.0	425.0	17.95	25000	511	3055	2665	87.2	5.5	2.4	0.8	0	-	1.1	45	
4			18.0	19.2	-15.1	-17.2	163-3/4	381.9	27.0	425.7	17.95	25000	513	3070	2668	87.0	5.6	2.6	0.9	0	-	1.2	45	
5			16.7	18.0	-16.1	-18.4	162 1/2	378.6	27.0	424.0	17.95	25000	512	3060	2658	86.8	5.8	2.7	1.0	0	-	1.3	45	
6			15.7	17.0	-17.0	-19.4	161 1/2	376.3	27.0	422.7	17.95	25000	512	3060	2645	86.4	5.4	2.8	1.0	0	-	1.3	45	
7			12.5	16.3	-17.6	-20.1	150	349.5	27.0	396.6	17.95	25000	516	3085	2480	80.4	4.9	5.0	3.8	2.0	-	3.8	45	
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DATA CHECKED AND CERTIFIED CORRECT BY:

E. I. Rein
CHIEF TEST ENGINEER

TEST WITNESSED BY

E. I. DuPONT de NEMOURS & CO. Not witnessed