

**Key Words:**

Rotary Filter

Filtration

Hanford

# Testing of a Rotary Microfilter to Support Hanford Applications

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## SUMMARY

Savannah River National Laboratory (SRNL) researchers are investigating and developing a rotary microfilter for solid-liquid separation applications at the Savannah River Site (SRS). Because of the success of that work, the Hanford Site is evaluating the use of the rotary microfilter for its Supplemental Pretreatment process. The authors performed rotary filter testing with a full-scale, 25-disk unit with 0.5  $\mu$  filter media manufactured by Pall Corporation using a Hanford AN-105 simulant at solids loadings of 0.06, 0.29, and 1.29 wt %.

The conclusions from this testing follow.

- The filter flux at 0.06 wt % solids reached a near constant value at an average of 0.26 gpm/ft<sup>2</sup> (6.25 gpm total).
- The filter flux at 0.29 wt % solids reached a near constant value at an average of 0.17 gpm/ft<sup>2</sup> (4 gpm total).
- The filter flux at 1.29 wt % solids reached a near constant value at an average of 0.10 gpm/ft<sup>2</sup> (2.4 gpm total).
- Because of differences in solids loadings, a direct comparison between crossflow filter flux and rotary filter flux is not possible. The data show the rotary filter produces a higher flux than the crossflow filter, but the improvement is not as large as seen in previous testing.
- Filtrate turbidity measured < 4 NTU in all samples collected.
- During production, the filter should be rinsed with filtrate or dilute caustic and drained prior to an extended shutdown to prevent the formation of a layer of settled solids on top of the filter disks.
- Inspection of the seal faces after ~ 140 hours of operation showed an expected amount of initial wear, no passing of process fluid through the seal faces, and very little change in the air channeling grooves on the stationary face.
- Some polishing was observed at the bottom of the shaft bushing. The authors recommend improving the shaft bushing by holding it in place with a locking ring and incorporated grooves to provide additional cooling.
- The authors recommend that CH2MHill Hanford test other pore size media to determine the optimum pore size for Hanford waste.

## INTRODUCTION

SRNL researchers identified and tested the rotary microfilter as a technology to increase solid-liquid separation throughput.<sup>1,2,3,4</sup> The testing showed significant improvement in filter flux with the rotary microfilter over the baseline crossflow filter (i.e., 2.5 – 6.5X during the scoping tests, as much as 10X in actual waste tests, and approximately 2X in pilot-scale tests).

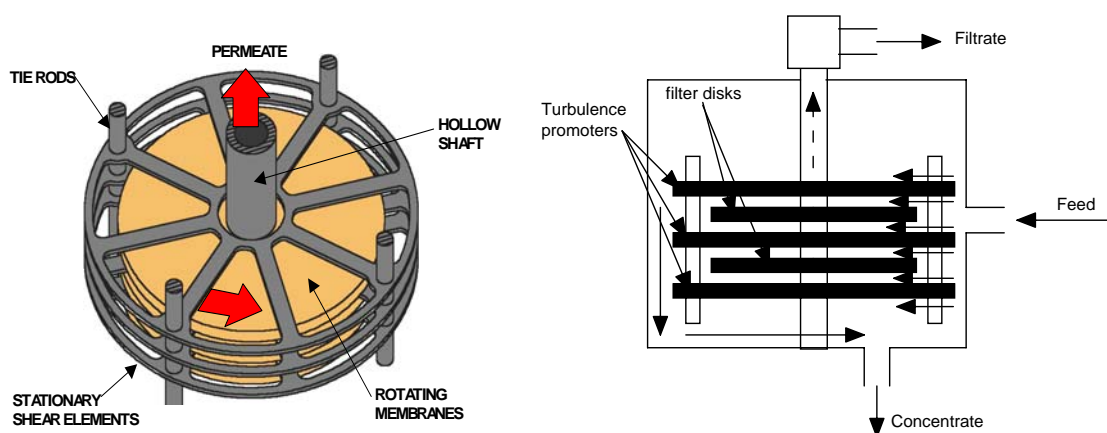
SRNL received funding from DOE EM-21, Office of Waste Processing (formerly Office of Cleanup Technologies), to develop the rotary microfilter for high level radioactive service. The work focused on evaluating alternative rotary microfilter vendors, redesigning the equipment for radioactive service, engineering studies to evaluate the risks, determining downstream impacts, assessing costs and benefits of deploying this technology, performing actual waste and pilot-

scale testing of the technology, and evaluating alternative filter media. The work led to the decision to design, fabricate and perform testing on a full-scale rotary microfilter for potential SRS Tank Farm applications.

SRNL performed the following work to evaluate the rotary microfilter. They demonstrated flushing of the filter housing and effective removal of soluble and insoluble contaminants. They tested the rotary microfilter performance with simulated small column ion exchange feed and observed ~ 6X improvement in filter flux of a crossflow filter with similar feed. They conducted simulated sludge washing and found the rotary filter unit behaved as a continuous stirred tank reactor. They concentrated the feed to 20 wt % solids, and the filter flux was ~ 6X the flux measured with a crossflow filter at similar solids loadings.<sup>5</sup>

Because of the success of that testing, the Hanford Site is evaluating the use of the rotary microfilter for its Supplemental Pretreatment process.<sup>6</sup> The authors received funding from DOE EM-21 to continue the development of the rotary microfilter and to evaluate its suitability for being the solid-liquid separation technology for Supplemental Pretreatment.<sup>7,8</sup>

The SpinTek high shear rotary filter used in this testing has 25 filter disks covered with 0.5  $\mu$  pore size (nominal) sheet membranes (0.007 inch thick) manufactured by Pall Corporation. The filter area of each disk is 0.96 ft<sup>2</sup>. The disks are physically mounted on and are hydraulically connected to a common hollow rotating shaft. The entire stack of membrane disks is enclosed within a vessel. Feed is fed into the filter vessel through the inlet on the side of the vessel wall. A pressure is set in the tank by restricting the outlet flow typically using a gate valve on the concentrate piping. This applied pressure forces liquid through the filters on the filter disk. Between each disk is a set of baffles or turbulence promoters. These turbulence promoters cause strong currents and eddies at the surface of the membrane inhibiting the formation of a filter cake. Filtrate flows through the media and along a mesh inside the disk into the hollow shaft. The filtrate then flows through the shaft to the rotary joint which allows the spinning shaft to couple to stationary piping. The concentrated slurry exits the vessel through an outlet on the bottom. Figure 1 illustrates the flow paths across the filter disks during filtration.

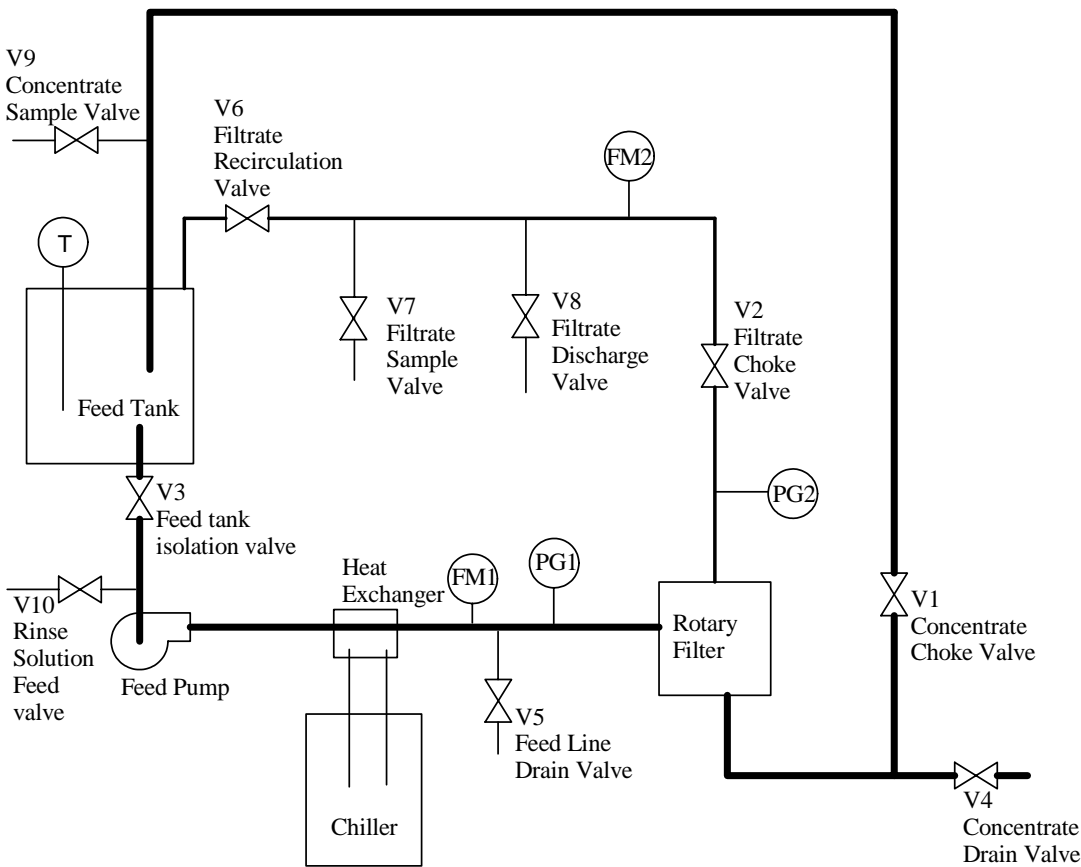


**Figure 1. Diagram of Rotary Filter Principle of Operation**

The advantage of the rotary microfilter compared to other membrane processes results from the high shear acting on the boundary layer next to the membrane. This shear greatly reduces fouling of the membrane surface and increases fluid flow through the membrane. Pressure is decoupled from the feed flow rate, allowing more control over the driving force pressure and independent control of the shear applied to the filter cake. This feature allows the direct application of shear force with a magnitude significantly greater than that available in conventional membrane systems. The membranes rotate at a tip speed of 60 ft/s in close proximity to the turbulence promoters. For comparison, previous cross-flow filter testing used axial velocities ranging from 3 to 25 ft/s.<sup>1-4</sup> This creates high speed currents and eddies near the membrane surface. These eddies create a great deal of turbulence at the membrane surface decreasing the buildup of filter cake on the membrane. The SpinTek rotary filter unit uses 11-inch diameter disks and typically operates with a rotational speed of 1170 rpm.

**TESTING**

The authors performed the rotary filter testing with a full-scale, 25-disk unit that had been used in previous testing to support the small column ion exchange and sludge washing applications for SRS.<sup>5</sup> Figure 2 shows a schematic of the test system.



**Figure 2. Schematic of Filter Test System**

The pump used in testing was a six stage centrifugal booster pump that had been used in previous testing.<sup>5</sup> It produced a flow rate of 18 – 25 gpm with a feed pressure of 60 – 100 psi. The Concentrate and Filtrate Choke valves, V1 and V2 respectively, were PVC gate valves which allowed a fine control of the pressure in the system. All isolation valves, V3 through V9, were PVC ball valves with the exception of V7, the filtrate sample valve, which was stainless steel. Pressure was measured using manual dial pressure gages, which are labeled PG1 and PG2 in Figure 2. Feed and filtrate flow were measured using Fischer Porter Magnetic flow meters and are labeled FM1 and FM2 respectively. The temperature of the process fluid was measured in the feed tank with a Type K thermocouple, indicated in the sketch as “T”. All data taken during testing was recorded by hand on data sheets. To minimize the amount of feed slurry needed, the concentrate and filtrate streams are recombined in the feed tank. The feed tank is mixed by recirculation of the concentrate and filtrate streams and by a 1 hp agitator.

Prior to the tests conducted here, the filter unit was modified by replacing the silicon carbide/silicon carbide faced John Crane Type 1 mechanical seal with a John Crane Type 28LD air cooled seal. The material of the bottom shaft bushing was changed from graphite to silicon-carbide. To prevent excessive wear on the shaft, an additional silicon carbide sleeve was added so that the contact wear surfaces at the bottom of the shaft are both silicon carbide.

The filter disks used in testing were a set of 25 un-used disks.

Personnel prepared a simulated Hanford AN-105 feed slurry containing 5 M sodium. The recipe is based on the simulant developed in 2000, but it eliminates trace RCRA metals.<sup>9</sup> Table 1 shows the composition of the supernate and Table 2 shows the solids fractions of the slurry. Personnel prepared 100 gallons of supernate as follows. They added 75.6 kg of de-ionized water to a tank. Next, they added sodium aluminate, sodium hydroxide (50 wt % solution), boric acid, calcium nitrate, cesium nitrate, magnesium nitrate, potassium nitrate, zinc nitrate, sodium chloride, sodium fluoride, sodium sulfate, and potassium molybdate. They mixed the solution until all of the compounds dissolved. Next, they added sodium silicate, sodium acetate, sodium formate, sodium glycolate, sodium oxalate, and sodium phosphate, mixing the solution after the addition of each compound. They added an additional 113.4 kg of de-ionized water, and mixed the solution thoroughly. They added the sodium carbonate, and mixed thoroughly. They added the sodium nitrate and sodium nitrite, and mixed the solution thoroughly. They added an additional 146.7 kg of de-ionized water, and mixed the solution overnight.

Personnel prepared the solids fraction of the slurry as follows. They procured all of the compounds, except for sodium oxalate, with particle size less than 10  $\mu$ . The sodium oxalate was not available as less than 10  $\mu$ , so SRNL personnel ground the sodium oxalate particles using a Union Process SG-1 Attritor Mill and measured the particle size of the product with a scanning electron microscope. The analysis showed the particles to be less than 10  $\mu$ . They mixed the compounds together in the ratios shown in Table 2.

**Table 1. Hanford AN-105 Supernate**

<u>Compound</u>	<u>Target Concentration</u> (g/L)
NaAlO <sub>2</sub>	56.661
NaOH	64.461
H <sub>3</sub> BO <sub>3</sub>	0.137
Ca(NO <sub>3</sub> ) <sub>2</sub> ·4H <sub>2</sub> O	0.111
CsNO <sub>3</sub>	0.114
Mg(NO <sub>3</sub> ) <sub>2</sub> ·6H <sub>2</sub> O	0.027
KNO <sub>3</sub>	9.030
Zn(NO <sub>3</sub> ) <sub>2</sub> ·6H <sub>2</sub> O	0.022
NaCl	7.039
NaF	0.197
Na <sub>2</sub> SO <sub>4</sub>	0.536
K <sub>2</sub> MoO <sub>4</sub>	0.096
Na <sub>2</sub> SiO <sub>3</sub> ·9H <sub>2</sub> O	1.003
NaCH <sub>3</sub> COO·3H <sub>2</sub> O	2.241
HCOONa	2.044
HOCH <sub>2</sub> COONa	0.706
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	0.436
Na <sub>3</sub> PO <sub>4</sub> ·12H <sub>2</sub> O	1.072
Na <sub>2</sub> CO <sub>3</sub>	10.405
NaNO <sub>3</sub>	98.500
NaNO <sub>2</sub>	78.211

**Table 2. Hanford AN-105 Solids**

<u>Compound</u>	<u>Solids Fraction (%)</u>
Al <sub>2</sub> O <sub>3</sub>	9.2
CaOxalate	5.0
Cr <sub>2</sub> O <sub>3</sub>	26.0
Fe <sub>2</sub> O <sub>3</sub>	1.1
MnO <sub>2</sub>	0.3
NaOxalate	52.5
NiO	0.5
SiO <sub>2</sub>	5.4

Personnel prepared the slurry as follows. They added 80 gallons of supernate and 226.04 g of solids to the filter feed tank to produce a 0.06 wt % solids slurry. They fed the slurry to the filter at a feed flow rate of ~25 gpm, a feed pressure of ~70 psi, and a feed temperature of ~35 °C. The filtrate pressure was ~30 psi, producing a transmembrane pressure of ~40 psi. They set the rotor speed to 1170 rpm. The filter operated for ~40 hours on day shift (i.e., ~ 8 hours per day, 5 times per week), and personnel recorded the operating parameters and filtrate flow rate during the test. The operating parameters recorded were feed flow rate, filtrate flow rate, feed pressure, concentrate pressure, filtrate pressure, temperature, and rotor speed. Motor current and output power, along with the surface temperatures of the rotary joint and mechanical seal housing were



measured at random intervals. Appendix A contains the data. They collected filtrate samples twice each day of operation to measure turbidity.

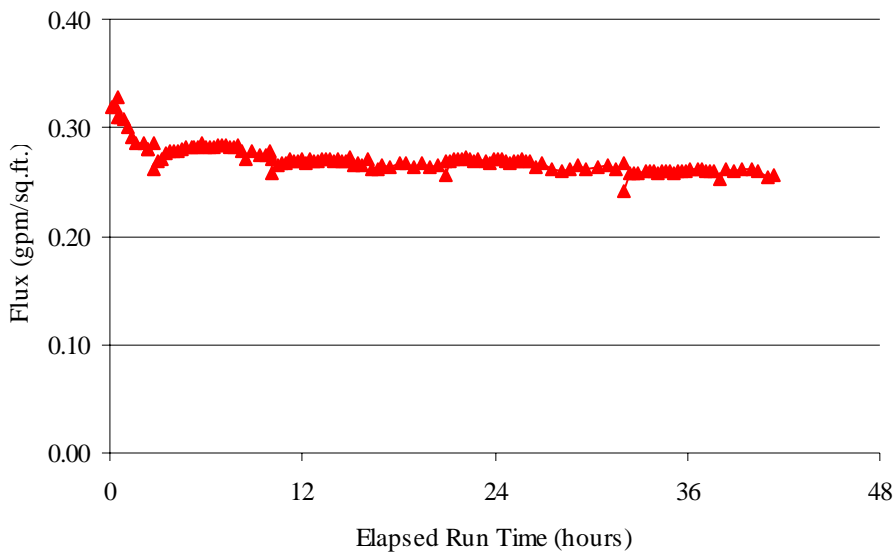
After operating for 40 hours, they added an additional 866.5 g of solids to the feed tank to produce a 0.29 wt % solids slurry. They fed the slurry to the filter at a feed flow rate of ~25 gpm, a feed pressure of ~70 psi, and a feed temperature of ~35 °C. The filtrate pressure was ~30 psi, producing a transmembrane pressure of ~40 psi. They set the rotor speed to 1170 rpm. The filter operated for ~40 hours on day shift, and personnel recorded the operating parameters and filtrate flow rate during the test. They collected filtrate samples daily to measure turbidity.

After operating for 40 hours, they added an additional 3767.38 g of solids to the feed tank to produce a 1.29 wt % solids slurry. They fed the slurry to the filter at a feed flow rate of ~25 gpm, a feed pressure of ~70 psi, and a feed temperature of ~35 °C. The filtrate pressure was ~30 psi, producing a transmembrane pressure of ~40 psi. They set the rotor speed to 1170 rpm. The filter operated for ~40 hours on day shift, and personnel recorded the operating parameters and filtrate flow rate during the test. They collected filtrate samples daily to measure turbidity.

## RESULTS

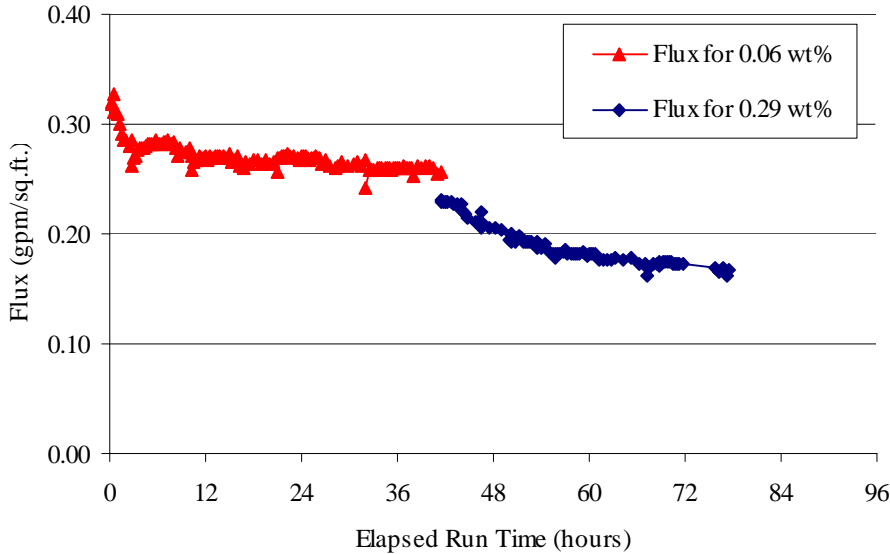
### Mechanical Performance and Flux

**Figure 3** shows the flux with the 0.06 wt % slurry. After reaching near constant value, the filter flux averaged 0.26 gpm/ft<sup>2</sup> (6.25 gpm total). The filter reached near constant value in approximately 10 hours.



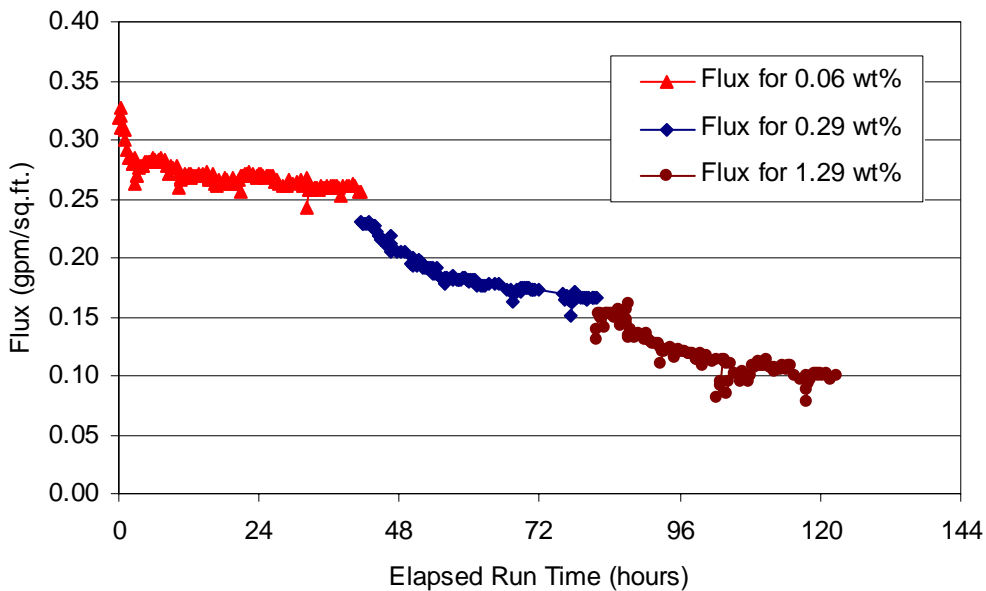
**Figure 3 Flux for 0.06 wt% Insoluble Solids at TMP of 40 psi**

Additional solids were added to the feed to raise the insoluble solids concentration to 0.29 wt %. **Figure 4** shows the flux with the 0.29 wt % slurry. After reaching a near constant value, the filter flux averaged 0.17 gpm/ft<sup>2</sup> (4 gpm total). The filter reached a near constant value after approximately 15 hours.



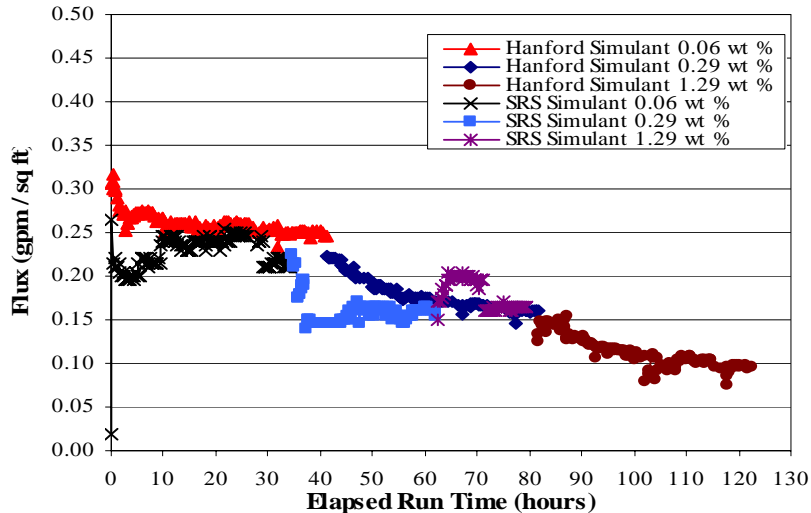
**Figure 4 Flux for 0.06 wt % and 0.29 wt % Insoluble Solids at TMP of 40 psi**

**Figure 5** shows the flux with the 1.29 wt % slurry added. After reaching a near constant value, the filter flux averaged approximately 0.10 gpm/ft<sup>2</sup> (2.4 gpm total). The filter flux reached a near constant value after approximately 25 hours.



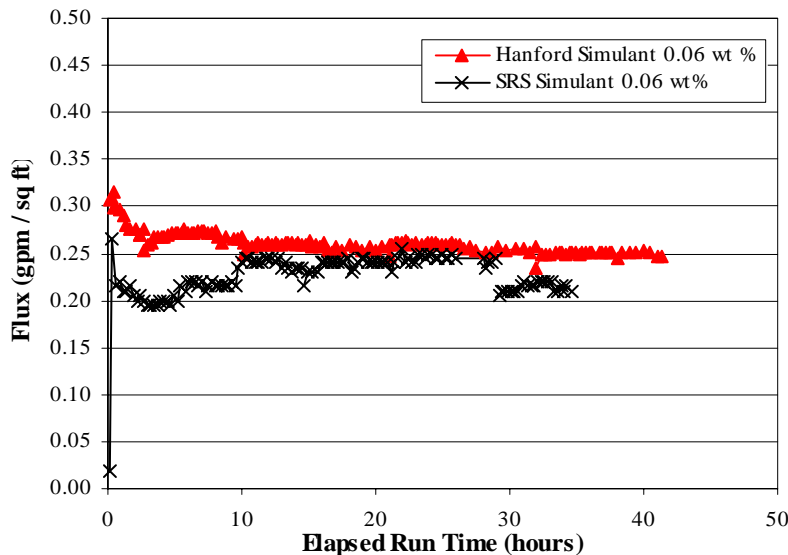
**Figure 5 Flux for 0.06 wt %, 0.29 wt % and 1.29 wt % Insoluble Solids at TMP of 40 psi**

Figure 6 compares the flux of the AN-105 simulant to the flux measured during a prior test with simulated SRS sludge. The comparison is made since both sludges contain similar compounds (e.g., metal oxides) and have relatively similar particle size (mean 1 – 5  $\mu$ ). At the start of the testing with 0.06 wt % solids, the AN-105 simulant had a higher flux than the SRS sludge simulant. When we increased the solids loading to 0.29 wt %, the flux with the AN-105 simulant was initially higher. By the end of that test, the flux was approximately the same for both feed slurries. When we increased the solids loading to 1.29 wt %, the flux with SRS simulant remained approximately the same, while the flux with AN-105 decreased further.



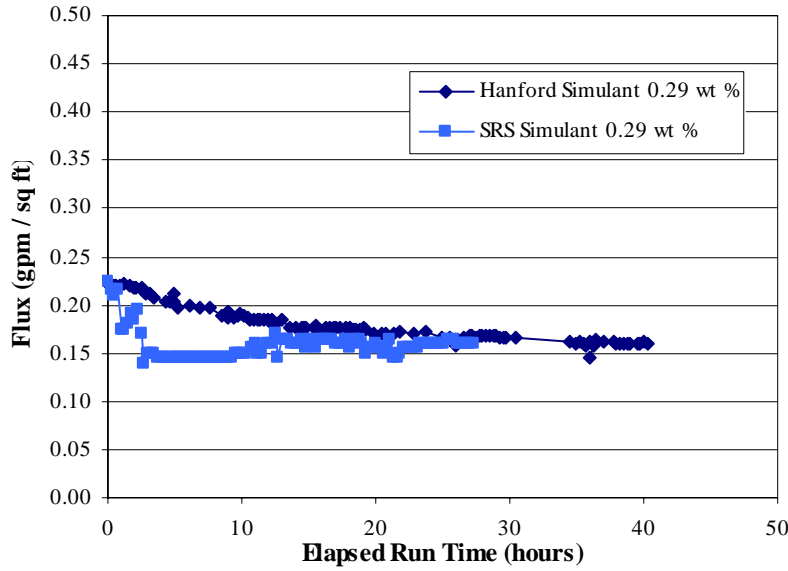
**Figure 6 Comparison of SRS and Hanford Simulant Flux Rates**

Figure 7 shows a comparison of the 0.06 wt % insoluble solids loadings for the Hanford simulant and the SRS simulant.<sup>5</sup>



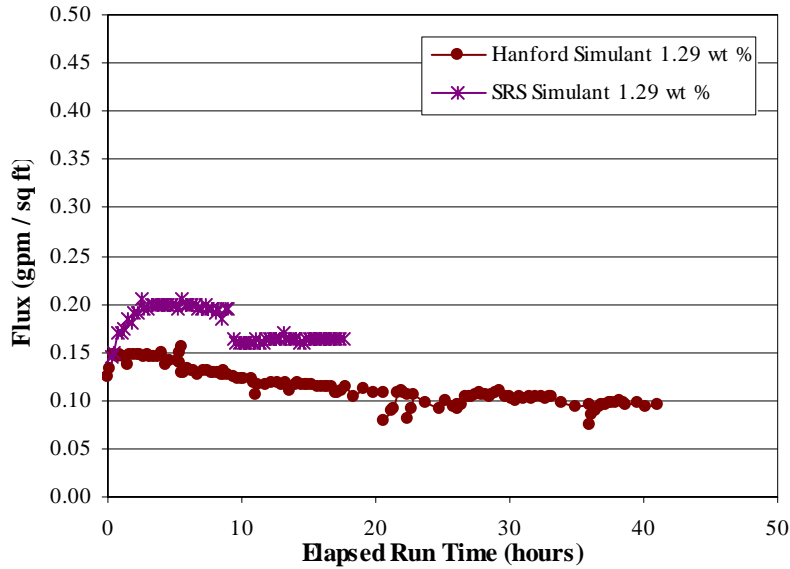
**Figure 7 Comparison of Hanford and SRS Simulant Flux Rates at 0.06 wt % Insoluble Solids**

Figure 8 compares the testing with the AN-105 simulant with the SRS simulant at 0.29 wt % insoluble solids.<sup>5</sup> Over the course of testing both simulants reached approximately the same state-state flux of approximately 0.17 gpm per square foot of media. Total filtration rate for the filter unit was approximately 4 gpm at this solids loading.



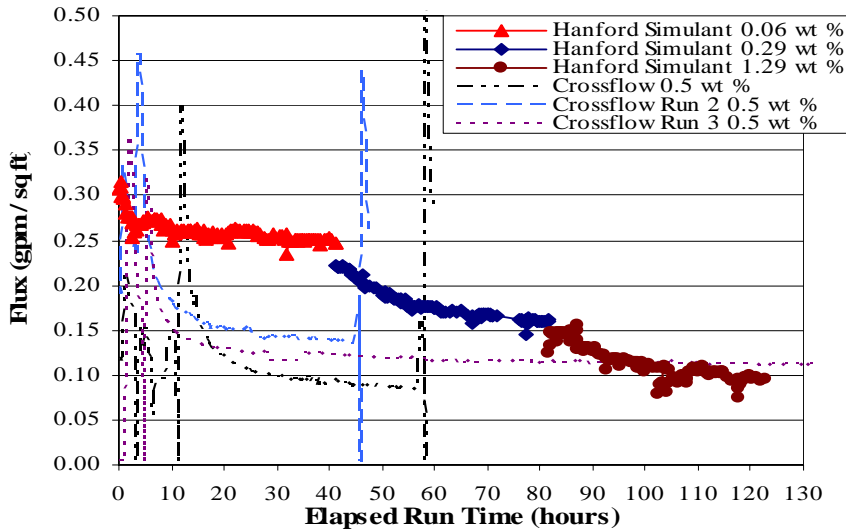
**Figure 8 Comparison of Hanford and SRS Simulant Flux Rates at 0.29 wt % Insoluble Solids**

Figure 9 compares the flux of the AN-105 simulant with the SRS simulant at 1.29 wt % insoluble solids.<sup>5</sup> Both simulants had approximately the same starting flux of 0.15 gpm per square foot. The flux with the AN-105 simulant continued to decay until reaching approximately 0.10 gpm per disk or 2.4 gpm of filtrate for the entire unit.



**Figure 9 Comparison of Hanford and SRS Simulant Flux Rates at 1.29 wt % Insoluble Solids**

Figure 10 compares the flux in this test with the flux measured during a crossflow filter test with an AN-105 simulant.<sup>10</sup> Because the tests used different solids loadings, different filter pore size, and differences in simulant recipe, a direct comparison is not available. Comparing the rotary filter flux at 0.06 wt % solids with the crossflow filter flux at 0.5 wt % solids shows the rotary filter flux is 1.8 – 3.0 X higher. Comparing the rotary filter flux at 0.29 wt % solids with the crossflow filter flux at 0.5 wt % solids shows the rotary filter flux is 1.15 – 2.0 X higher. Comparing the rotary filter flux at 1.29 wt % solids with the crossflow filter flux at 0.5 wt % solids shows the rotary filter flux is 0.7 – 1.25 X of the flux with a crossflow filter.

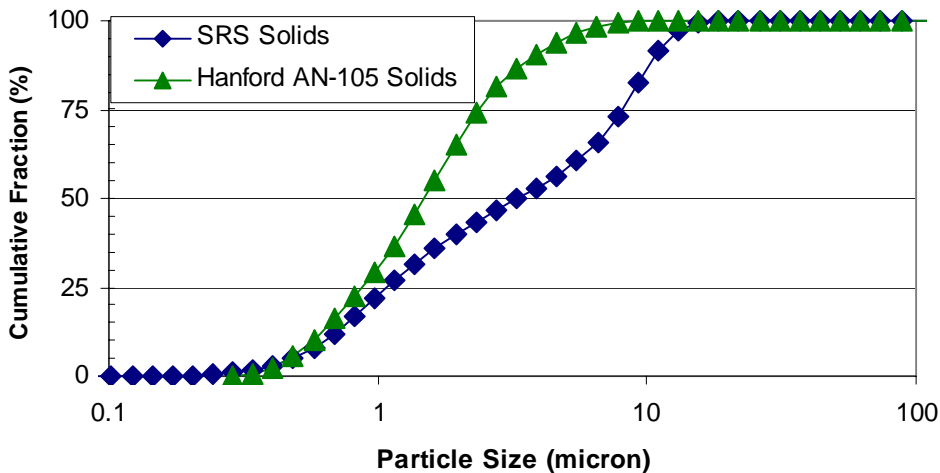


**Figure 10 Comparison of Flux with Rotary Filter and Crossflow Filter**

Figure 11 shows the particle size distribution of the solids in the current test and in the rotary filter test using SRS sludge. Particle size was measured with a Microtrac SRA-150. The carrier fluid for the measurement was simulated salt solution (SRS salt solution for SRS sludge and AN-105 salt solution for AN-105 solids). The median particle size of the AN-105 solids was 1.49  $\mu$ . The median particle size of the SRS solids was 3.32  $\mu$ . In addition, the AN-105 solids had a larger fraction of particles less than 1  $\mu$ . According to different filtration theories, filter flux increases with increasing particle size. The relationship is described by equation [1]

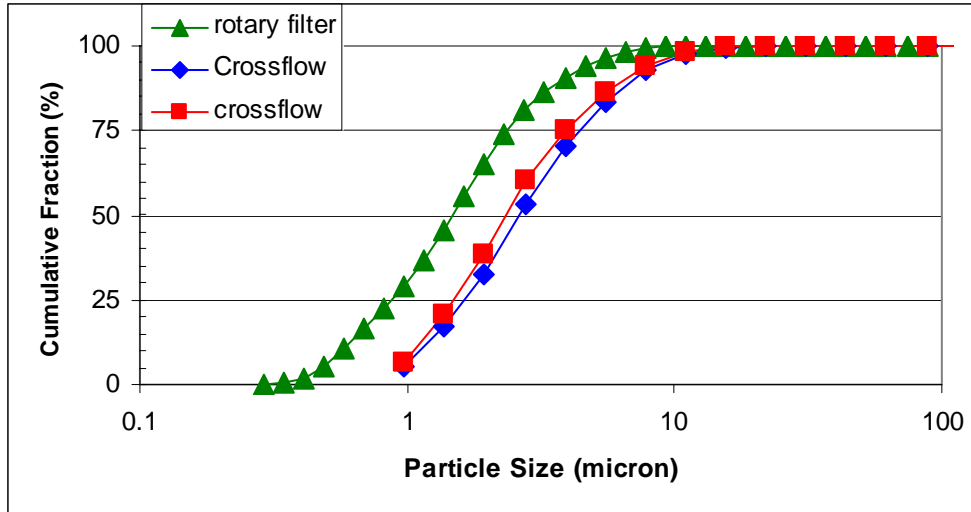
$$J = K d_p^n \tag{1}$$

where J is filter flux, K is a constant,  $d_p$  is particle size, and n is an exponent. Various filtration models have n equal to 4/3, 2, and 3.<sup>11</sup> In addition, the increase in fine particles (<1  $\mu$ ) would provide more particles that could penetrate the filter membrane to foul the filter pores.



**Figure 11. Comparison of Particle Size Data for Hanford and SRS Simulants**

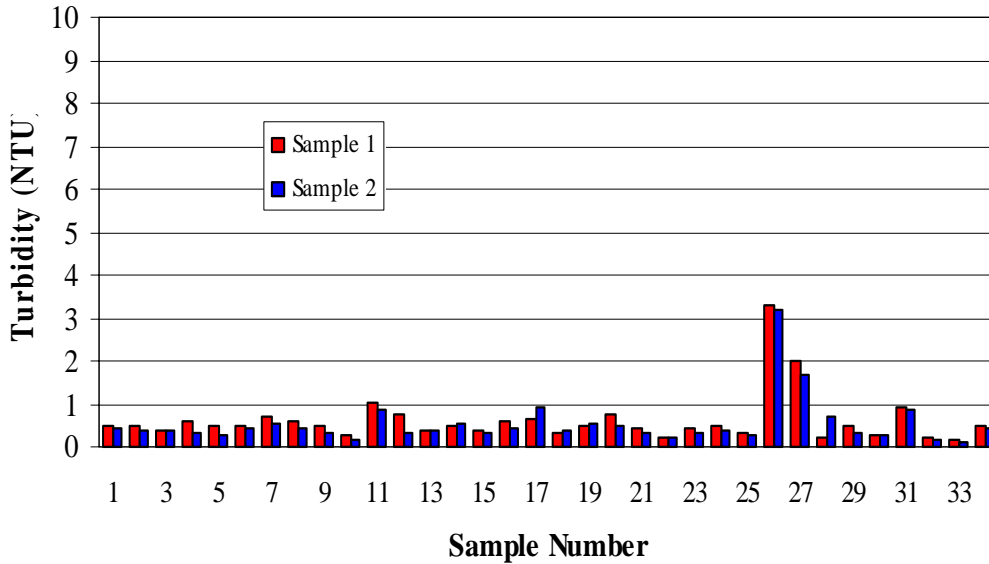
Figure 12 shows the particle size of the AN-105 solids from the rotary filter test and the crossflow filter test. The median particle size of the AN-105 solids in the rotary filter test was 1.49  $\mu$ . The median particle size of the solids during the crossflow filter tests was 2.32 and 2.59  $\mu$ . As described above, this larger particle size would produce higher filter flux, and may explain why the rotary filter did not show as big of an improvement in filter flux as has been observed in other rotary filter versus crossflow filter tests. In addition, the feed for the rotary filter test had a larger fraction of particles less than 1  $\mu$  than the feed for the crossflow filter tests.



**Figure 12. Particle Size Comparison of Hanford Simulant used in Rotary and Crossflow Filters**

**Filtrate Clarity**

Figure 13 shows the turbidity of the filtrate samples collected. All filtrate samples had turbidity less than 4 NTU.

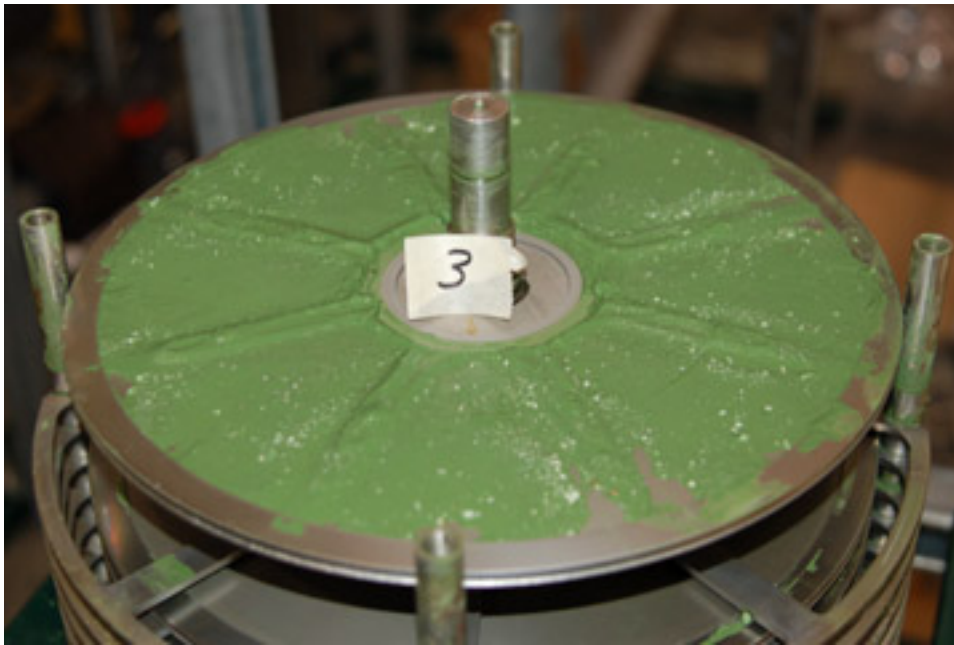


**Figure 13. Filtrate Turbidity from Rotary Filter Testing of Hanford Simulant**

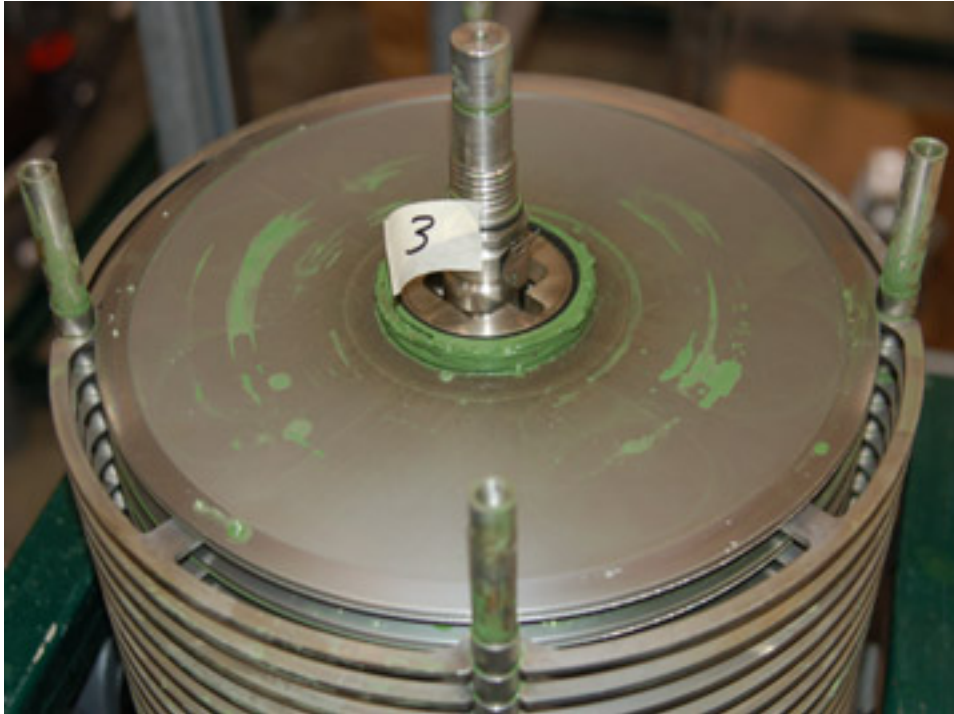


## Disassembly and Inspection

After completion of the operational testing, personnel disassembled the filter disk stack. The disk stack was not flushed because the feed pump failed due to the packing of large (up to 2 cm) solids in the suction side of the pump (see Appendix B). A significant difference in the filter cake between the top side of the disks and the bottom side was observed. Figure 14 shows the top of a representative filter disk and Figure 15 shows the bottom side of the same filter disk (third from the bottom in the stack). The filter-cake buildup on the top side of the disk is due to the settling of the feed material when operation is complete. During testing, the filter was simply shut down at the end of the day. No draining or flushing was done. Additionally, no attempt was made to clean in the disk in-situ by dropping the TMP while maintaining the rotor speed. In previous testing, this approach was shown to improve filter flux by a small amount. The condition of the filter disks is consistent with previous observations with the top side of the disks showing a greater buildup of solids. This leads to the conclusion that the filter is better at preventing the buildup of filter cake than breaking up a filter cake that has already formed. To prevent the buildup of similar filter-cake in deployment, it is recommended that the filter be drained and flushed with filtrate or dilute caustic after shutdown.



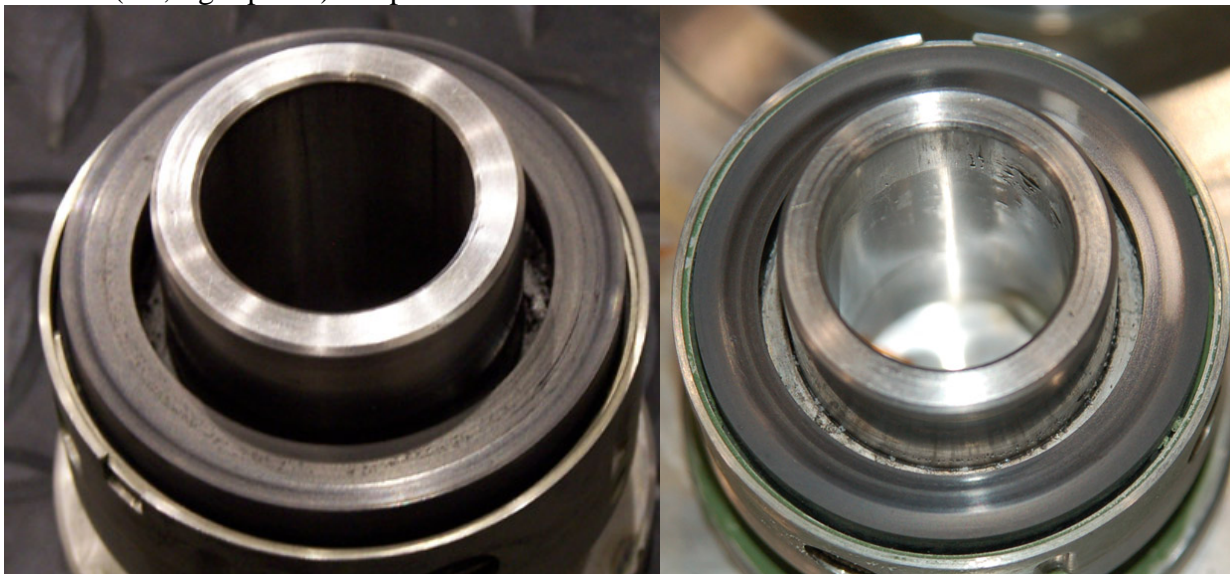
**Figure 14 Top Side of Filter Disk**



**Figure 15 Bottom Side of Filter Disk**

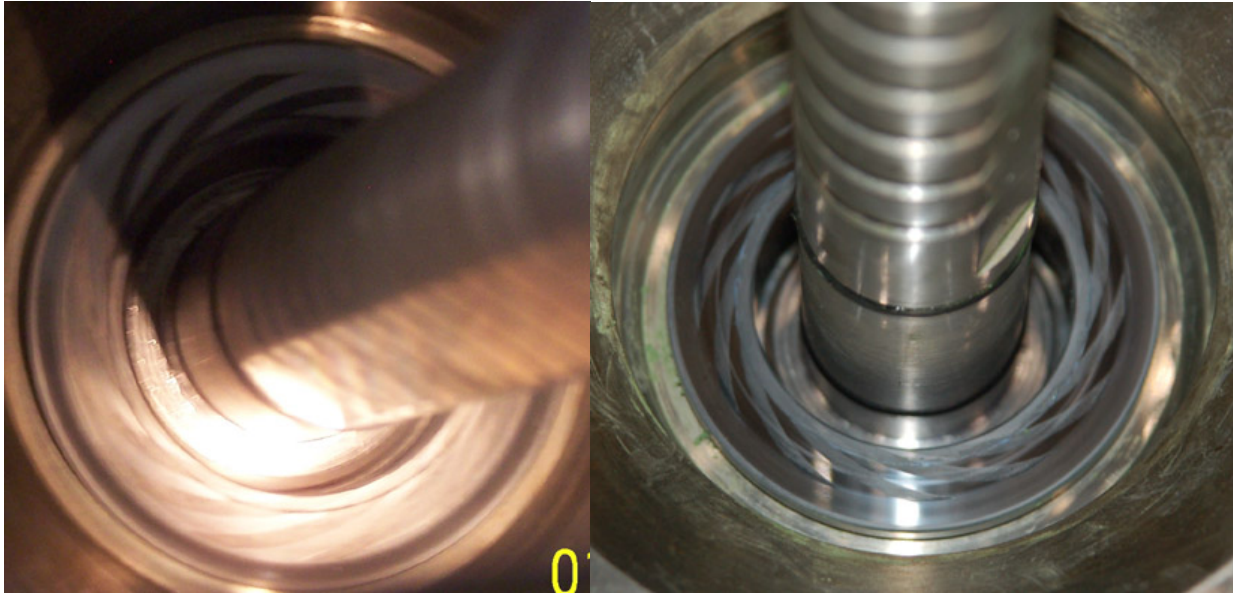
### Seal Wear Inspection

After disassembly was completed, the shaft seal was removed and inspected. There was no indication that any of the process fluid passed the seal. Figure 16 shows the seal rotor after the first 20 hours and 44 minutes (i.e., left photo) of operation and then after 143 hours and 28 minutes (i.e., right photo) of operation



**Figure 16 Rotor Portion of Air Seal after 20  $\frac{3}{4}$  Hours (left photo) and 143  $\frac{1}{2}$  hours (right photo) of Operation**

Figure 17 shows the stationary part of the seal after the first 20 hours and 44 minutes of operation and then after 143 hours and 28 minutes of operation.



**Figure 17 Stationary Portion of Air Seal after 20 <sup>3</sup>/<sub>4</sub> hours (left photo) and 143 <sup>1</sup>/<sub>2</sub> hours (right photo) of Operation**

The carbon face of the rotor is showing polishing in the area indicative of initial wear. This polishing is due to contact of the seal faces, primarily at startup and shutdown, when there is not enough velocity to cause liftoff for the faces. No evidence of the passing of process fluid was observed. Very little change to the air channeling grooves on the stationary was observed, though no depth measurements were obtained since these measurements would have required the removal of the seal stationary.

Figure 18 and Figure 19 show the condition of the bushing set at the bottom of the filter after 143 hours and 28 minutes of operation. Some polishing can be observed on the bottom of the shaft bushing as well as the receiver bushing. The shaft bushing is not supported and is held in place by a sealant. This sealant was compromised by the process fluid allowing the shaft bushing to contact the bottom of the receiver bushing. It is recommended that the shaft bushing be updated to allow it to be held in place by a retaining ring as well as incorporated grooves to allow for additional cooling flow.



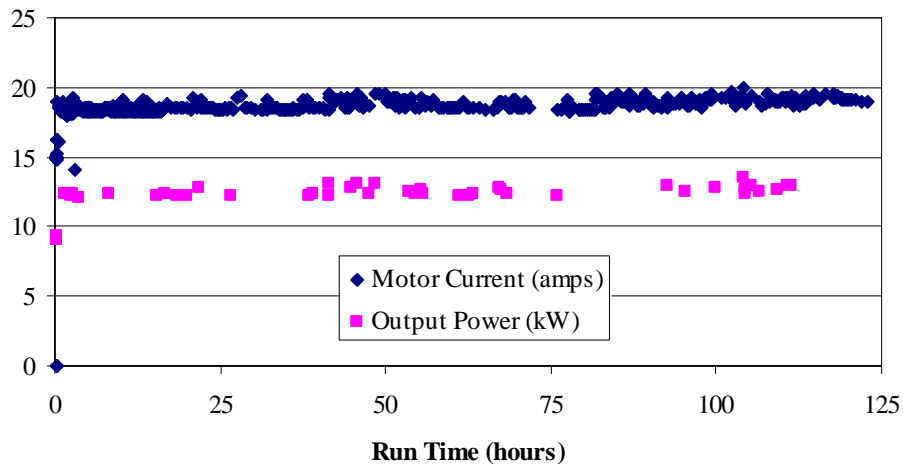
**Figure 18. Shaft Bushing after 143 ½ hours of Operation**



**Figure 19. Receiver Bushing after 143 ½ hours of Operation**



Figure 20 shows the current and power draw by the filter motor during operation.



**Figure 20. Filter Motor Power and Current Draw**

The maximum current rating on the motor is 24.1 amps at 460 volts. No dramatic power or current increases were required as the insoluble solids loadings were increased in the process fluid.

## CONCLUSIONS

The conclusions from this testing follow.

- The filter flux at 0.06 wt % solids reached a near constant value at an average of 0.26 gpm/ft<sup>2</sup> (6.25 gpm total).
- The filter flux at 0.29 wt % solids reached a near constant value at an average of 0.17 gpm/ft<sup>2</sup> (4 gpm total).
- The filter flux at 1.29 wt % solids reached a near constant value at an average of 0.10 gpm/ft<sup>2</sup> (2.4 gpm total).
- Because of differences in solids loadings, a direct comparison between crossflow filter flux and rotary filter flux is not possible. The data show the rotary filter produces a higher flux than the crossflow filter, but the improvement is not as large as seen in previous testing.
- Filtrate turbidity measured < 4 NTU in all samples collected.
- During production, the filter should be rinsed with filtrate or dilute caustic and drained prior to an extended shutdown to prevent the formation of a layer of settled solids on top of the filter disks.
- Inspection of the seal faces after ~ 140 hours of operation showed an expected amount of initial wear, no passing of process fluid through the seal faces, and very little change in the air channeling grooves on the stationary face.
- Some polishing was observed at the bottom of the shaft bushing. The authors recommend improving the shaft bushing by holding it in place with a locking ring and incorporated grooves to provide additional cooling.
- The authors recommend that CH2MHill Hanford test other pore size media to determine the optimum pore size for Hanford waste.

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Appendix A: Test Data

Rotary Microfilter Data Sheet

Date: 10/24/02

Time (hh:mm)	Tank Level (gal)	Temp (°F)	Conc. Press (psi)	Filtrate Press (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Insol Solids (wt %)	Comments	Observer
9:50	28	90	46	26	9.50	6.4	60	lock	12.3-amp 1st cycle count	YHF
10:00	"	96.7	46	15	9.51	7.2	60	"	12.0-amp	
10:10	"	96.0	47	15	9.71	7.15	60	"	12.0-amp	
10:20	"	99.8	48	17	9.65	7.05	60	"	11.9-amp	





Rotary Microfilter Data Sheet

Date: 12/10/07

P6J P52

Time (hh:mm)	Tank Level (gal)	Temp (°F)	Conc. Press (psi)	Filtrate Press (psi)	Feed Flow (m³/h)	Filtrate Flow (m³/h)	Rotar Speed (RPM)	Insol Solids (wt %)	Comments	Observer
10:05	20	81.2	45	2.2	12.30	5.61	600	40%	Rotar Joint 77.3°F	
10:16	30	91.0	43	2.2	12.30	5.40	600	40%	Seal - 95.5°F	
									10:14 Seal - 91.5°F Joint - 97.8°F	
									STOPPED	
11:32	30	94.0	41.5	2.1	11.23	3.04	600	40%	Joint - 93.0 Seal - 97.0	
11:38	30	85.6	41.0	2.1	11.03	6.07	600	40%	Seal - 15.3 Joint - 83.0 Seal - 93.5	
									Stopped	
15:07	30	91.8	38.0	15.5	10.16	5.23	60.0	40%	water 94.5°F Temp @ Rotar Joint	MP
15:30	30	98.1	50.0	19.5	11.95	6.30	60.0	40%	water 95.9°F Temp @ Seal	MP
									96.0°F Rotar - Joint 119.5°F	MP
10:50	30	80.0	50.0	20.0	11.91	5.82	60.0	40%	Rotar Joint 79.9°F	MP
11:07	30.0	101.3	50.0	18.0	11.52	6.47	60.0	40%	151 Amps	MP
11:15	30.0	92.0	70.0	35.0	11.69	6.22	60.0	40%	Joint 96.5 Seal 93.5	MP
11:34	30.0	94.6	70.0	33.0	11.01	6.40	60.0	40%	Joint 91.5 Seal 94.5	MP
11:59	30.0	94.6	70.0	33.0	11.01	6.40	60.0	40%	Joint 91.5 Seal 91.5	MP
									Seal 91.5	MP
									Seal 91.5	MP

12.11





25 Dext Rotary Filter Data Sheet													
Date	Tank Level	Solids Loading (wt %)	Temp (F)	Conc PG-1 (PSI)	Filterate PG-2 (psi)	Feed Flow (mA)	Filterate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments	Recorded by
12-19-07													
13:10	70	0.06	81.6	70	3.0	148	4.71	60.0	69.5	73.0	19.5	Final light level of 80 gal. sample - 29% solids	SWP
13:25	70	0.06	81.2	70	3.0	149	4.90	60.0	71.5	73.0	19.0		SWP
13:40	70	0.06	81.9	71	3.1	148	5.03	60.0	71.5	73.0	18.7		SWP
13:50													
14:00													
14:03	70	0.06	81.6	72	3.1	149	4.30	60	118.5	105	18.5	Polled about 30 seconds	SWP
14:10	70	0.06	81.6	72	3.1	149	4.30	60	118.5	105	18.5	Added 0.1% water to seeds	SWP
14:18	70	0.06	81.6	71	3.0	148	5.04	60	118.5	105	18.3		SWP
14:25	70	0.06	81.6	71	3.0	148	5.04	60	118.5	105	18.3		SWP
14:30	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
14:37	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
14:40	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
14:47	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
14:50	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
14:53	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
14:57	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
14:59	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:00	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:07	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:07	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:10	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:13	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:16	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:19	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:22	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:25	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:28	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:31	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:34	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:37	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:40	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:43	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:46	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:49	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:52	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:55	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
15:58	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:01	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:04	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:07	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:10	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:13	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:16	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:19	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:22	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:25	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:28	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:31	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:34	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:37	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:40	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:43	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:46	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:49	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:52	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:55	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
16:58	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:01	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:04	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:07	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:10	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:13	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:16	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:19	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:22	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:25	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:28	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:31	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:34	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:37	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:40	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:43	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:46	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:49	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:52	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:55	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
17:58	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:01	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:04	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:07	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:10	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:13	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:16	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:19	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:22	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:25	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:28	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:31	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:34	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:37	70	0.06	81.2	72	3.0	148	5.32	60	118.5	105	18.0		SWP
18:40	70	0.06	81.2	72	3.0	148	5.32</						

25 Disk Rotary Filter Data Sheet												
Date:	12-20-07											
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. PG-1 (PSI)	Filtrate PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
0800	70.0	0.06	81.1	70.0	30.0	1220	520	60.0	78.5	82.0	18.7	Mixer Speed = 40
0810	70.0	0.06	81.1	70.0	30.0	1220	520	60.0	78.5	82.0	18.7	Mixer Speed = 40
0815	70.0	0.06	81.1	70.0	30.0	1220	520	60.0	78.5	82.0	18.7	Mixer Speed = 40
0830	70.0	0.06	81.1	70.0	30.0	1175	547	60.0	78.5	82.0	18.7	Mixer Speed = 40
0845	70.0	0.06	81.1	70.0	30.0	1191	547	60.0	78.5	82.0	18.7	Mixer Speed = 40
0900	70.0	0.06	81.1	70.0	30.0	1182	547	60.0	78.5	82.0	18.7	Mixer Speed = 40
0915	70.0	0.06	81.1	70.0	30.0	1173	543	60.0	78.5	82.0	18.7	Mixer Speed = 40
0930	70.0	0.06	81.1	70.0	30.0	1172	543	60.0	78.5	82.0	18.7	Mixer Speed = 40
0945	70.0	0.06	81.1	70.0	30.0	1202	535	60.0	78.5	82.0	18.7	Mixer Speed = 40
1000	70.0	0.06	81.1	70.0	30.0	1183	534	60.0	78.5	82.0	18.7	Mixer Speed = 40
1015	70.0	0.06	81.1	70.0	30.0	1201	536	60.0	78.5	82.0	18.7	Mixer Speed = 40
1030	70.0	0.06	81.1	70.0	30.0	1187	542	60.0	78.5	82.0	18.7	Mixer Speed = 40
1045	70.0	0.06	81.1	70.0	30.0	1201	545	60.0	78.5	82.0	18.7	Mixer Speed = 40
1100	70.0	0.06	81.1	70.0	30.0	1199	541	60.0	78.5	82.0	18.7	Mixer Speed = 40
1115	70.0	0.06	81.1	70.0	30.0	1203	544	60.0	78.5	82.0	18.7	Mixer Speed = 40



25 Disk Rotary Filter Data Sheet												
Date:	1-2-08											
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc Press PG-1 (PSI)	Filtrate Press PG-2 (PSI)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
11:35	760	0.06	617	08	30	1161	492	60	67.0	71.0	19.7	Mixer found up pulled Sample 511 make
11:40	760	0.06	603	70	30	1161	547	60	67	84.5	18.8	
12:00	760	0.06	613	70	30	1137	541	60.0	62.5	82.0	18.4	
12:15	760	0.06	624	70	32	1141	534	60.0	62.5	82.5	18.4	
12:30	760	0.06	624	72	32	1141	535	60.0	65.5	85.0	18.4	
12:45	760	0.06	645	70	30	1182	541	60.0	73.5	94.8	18.8	
13:00	760	0.06	645	70	30	1187	541	60.0	93.5	94.3	19.2	
13:15	760	0.06	650	91	30	1187	542	60.0	95.0	95.0	18.2	
13:30	760	0.06	651	70	30	1173	541	60.0	95.0	95.0	18.2	
13:45	760	0.06	645	70	30	1182	535	60.0	95.5	95.5	18.2	
14:00	760	0.06	649	71	31	1183	534	60.0	94.5	93.5	18.2	
14:15	760	0.06	645	70	30	1198	535	60.0	65	95.5	18.2	
14:30	760	0.06	65.1	70	30	1176	532	60.0	66.0	96.0	18.2	
14:45	760	0.06	649	70	31	1183	537	60.0	65.0	93.0	18.2	
15:00	760	0.06	649	71	32	1174	547	60.0	76.5	96.5	17.7	
15:15	760	0.06	646	71	30	1185	541	60.0	96.5	96.0	18.2	
15:30	760	0.06	646	71	31	1190	534	60.0	92.0	95.5	18.3	
15:45	760	0.06	650	71	31	1193	536	60.0	96.0	97.5	18.3	
16:01	760	0.06	65.1	71	31	1179	539	60.0	92.5	96.5	18.4	

15:05 Effluent sample pulled

Recorded by

25 Disk Rotary Filter Data Sheet													
Date:	1-3-08												
Time	Tank Level	Solids Loading (wt %)	Temp (F)	Conc. Press PG-1 (psi)	Filtrate Press PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (rpm)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments	Recorded by
7:35	70	0.06	90.6	70	30	18.1	3.34	60.0	94.5	90.5	18.2	HY @ 67°F	Soren
7:45	70	0.06	90.6	70	30	17.9	3.24	60.0	94.5	18.2			
8:00	70	0.06	91.9	70	30	17.9	3.24	60.0	94.5	18.2			
8:15	70	0.06	93.3	70	30	18.1	3.24	60.0	94.5	18.2			
8:30	70	0.06	94.2	70	30	18.1	3.24	60.0	94.5	18.2			
8:45	70	0.06	94.2	70	30	18.1	3.24	60.0	94.5	18.2			
9:00	70	0.06	95.3	70	30	18.1	3.24	60.0	94.5	18.2			
9:15	70	0.06	95.3	70	30	18.1	3.24	60.0	94.5	18.2			
9:30	70	0.06	95.3	70	30	18.1	3.24	60.0	94.5	18.2			
9:45	70	0.06	95.3	70	30	18.1	3.24	60.0	94.5	18.2			
10:00	70	0.06	95.3	70	30	18.1	3.24	60.0	94.5	18.2	Pulverized Sulfate Sample	Soren	
10:15	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
10:30	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
10:45	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
11:00	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
11:15	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
11:30	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
11:45	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
12:00	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
12:15	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
12:30	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
12:45	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
13:00	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
13:15	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
13:30	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
13:45	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
14:00	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
14:15	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
14:30	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
14:45	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
15:00	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
15:15	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
15:30	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
15:45	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			
16:00	70	0.06	95.0	70	30	18.1	3.24	60.0	94.5	18.2			



25 Disk Rotary Filter Data Sheet													
Date:	1	25	02										
Time (hr:min)	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. Press PG-1 (PSI)	Filtrate Press PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments	Recorded by
10:32	68	0.06	84	63	22	12.10	10.04	55.0	87.0	95.5	16.5		
10:42	68	0.06	87	66	24	12.17	10.14	54.8	87.0	96.0	16.3		
10:52	68	0.06	95	67	24	12.23	10.16	54.9	92.5	96.0	16.2		
11:02	67	0.06	99	68	25	12.24	10.32	54.8	96.5	100	16.1		
STOPPED RUN													
14:30	68	0.06	95	69	20	12.21	9.79	60	87.5	94.5	13.6		
14:40	68	0.06	96	69	21	12.22	9.79	60	87.5	94.0	13.5		
14:50	69	0.06	94	68	20	12.24	9.79	60	87.5	94.0	13.5		
15:15	69	0.06	95	69	21	12.10	9.79	60	87.5	94.0	13.7		
15:30	68	0.06	83	41	30	11.8	9.62	60	98.5	95.0	18.7		
15:46	68	0.06	93	71	30	11.7	9.5	60	95.5	95.5	18.7		
16:12	68	0.06	94	70	30	11.94	9.5	60	96	96.5	18.6		
16:30	68	0.06	95	70	30	11.9	9.4	60	95	96	18.5		
17:00	68	0.06	93	71	31	11.9	9.4	60	92	95.5	18.8		
18:00	68	0.06	93	71	31	11.9	9.5	60	95.5	97	18.6		
<p>Over 12.4 MW temp const 158.0°</p> <p>Power 12.4 MW</p> <p>12.32 MW</p> <p>9' head to 1010'</p>													
													D74
													D74
													D74
													D74

25 Disk Rotary Filter Data Sheet														
Date:	1-28-2005													
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. Press PG-1 (PSI)	Filtrate Press PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Joint Temp (F)	Motor Current (amps)	Comments	Recorded by	
0730	67	0.06	74	70	30	11.96	9.25	60	94.5	93.5	18.8	Start UP Comments add more to wash pan Pulled Filtrate Sample	DTH	
0749	67	0.06	73	70	31	11.94	9.20	60	94.5	93.5	18.6			
0800	68	0.06	74	70	30	11.76	9.21	60	94.5	93.0	18.5			
0815	68	0.06	74	70	30	11.93	9.34	60	94.5	93.5	18.8			
0830	67	0.06	75	70	30	11.90	9.35	60	94.5	93.5	18.8			
0849	67	0.06	75	71	30	11.90	9.37	60	94.5	93.5	18.8			
0900	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
0915	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
0930	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
0949	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1000	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1015	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1030	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1049	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1100	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1115	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1130	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1149	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1200	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1215	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1230	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1249	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1300	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1318	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1338	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1400	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1431	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
1445	67	0.06	75	70	30	11.90	9.37	60	94.5	93.5	18.8			
0835	65	0.06	71	70	30	11.85	9.35	60	87	91	18.8			
1415	68	0.06	72	71	31	11.85	9.24	60	71.5	91.5	18.7			



25 Disk Rotary Filter Data Sheet													
Date:	1-29-08												
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. Press PG-1 (PSI)	Filtrate Press PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Recorded by	
0741	63	0.06	78	30	30	11.94	5.94	60	69	95.3	19.1	Sum	
0800	63	0.06	79	30	30	11.79	5.13	60	80.3	99	14.5	Sum	
0815	63	0.06	94	30	30	11.71	5.16	60	91.0	98.5	19.7	Sum	
0830	63	0.06	94	30	30	11.33	5.17	60	92.5	92.5	19.6	Sum	
0845	63	0.06	94	30	30	11.32	5.13	60	93.5	91.5	19.6	Sum	
0900	63	0.06	93	30	30	11.30	5.13	60	94.5	91.5	19.5	Sum	
0915	63	0.06	93	30	30	11.29	5.13	60	94.5	93.0	19.4	Sum	
0930	63	0.06	93	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1000	63	0.06	93	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1015	63	0.06	93	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1030	63	0.06	93	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1045	63	0.06	93	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1100	63	0.06	93	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1115	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1130	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1145	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1200	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1215	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1230	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1245	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1300	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1315	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1330	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1345	63	0.06	92	30	30	11.29	5.17	60	94.0	93.0	19.3	Sum	
1418	63	0.06	95	30	30	11.53	5.05	60	96	96	18.4	Sum	
1432	63	0.06	95	30	30	11.88	5.03	60	98	97	18.5	Sum	
1500	63	0.06	95	30	30	11.75	5.13	60	96.5	97.5	18.8	Sum	
1534	63	0.06	95	30	30	11.66	5.07	60	97.5	98.5	18.5	Sum	
1600	63	0.06	95	30	30	11.35	5.12	60	97.5	98.5	18.5	Sum	
1631	63	0.06	95	30	30	11.76	5.14	60	97.5	97.5	18.5	Sum	
1701	63	0.06	95	30	30	11.85	5.08	60	96.5	97.5	18.5	Sum	
1730	63	0.06	95	30	30	11.85	5.16	60	97.5	97.5	18.5	Sum	
1800	63	0.06	96	30	30	11.83	5.02	60	97.5	96	18.5	Sum	
1831	63	0.06	96	30	30	11.76	5.13	60	96	97.5	18.5	Sum	
1851	63	0.06	96	30	30	11.87	5.18	60	96.5	97.5	18.5	Sum	

12.33 kW  
175.4 lbs  
17.26 kW  
175.4 lbs  
17.26 kW

Pulled Filtrate Sample

Pulled Filtrate Sample

Start UP  
Comments

25 Disk Rotary Filter Data Sheet												
Date:	1/31/08											
Time (hr:min)	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. Press PG-1 (PSI)	Filtrate Press PG-2 (psf)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
07:33	65	0.06	80	70	30	11.56	8.94	60	72	78.5	17.2	Recorded by DNY
07:48			82	70	30	11.57	9.19		86.9	93.9	18.7	
08:15			82	70	30	11.86	9.24		86.5	97.5	18.5	
08:30			82	70	30	11.87	9.24		87	96.5	18.7	
08:45			82	70	30	11.88	9.25		87	96.5	18.7	
09:00			82	70	30	11.88	9.25		87	96.5	18.7	
09:15			82	70	30	11.88	9.25		87	96.5	18.7	
09:30			82	70	30	11.88	9.25		87	96.5	18.7	
09:45			82	70	30	11.88	9.25		87	96.5	18.7	
10:00			82	70	30	11.88	9.25		87	96.5	18.7	
10:15			82	70	30	11.88	9.25		87	96.5	18.7	
10:30			82	70	30	11.88	9.25		87	96.5	18.7	
10:45			82	70	30	11.88	9.25		87	96.5	18.7	
11:00			82	70	30	11.88	9.25		87	96.5	18.7	
11:15			82	70	30	11.88	9.25		87	96.5	18.7	
11:30			82	70	30	11.88	9.25		87	96.5	18.7	
11:45			82	70	30	11.88	9.25		87	96.5	18.7	
12:00			82	70	30	11.88	9.25		87	96.5	18.7	
12:15			82	70	30	11.88	9.25		87	96.5	18.7	
12:30			82	70	30	11.88	9.25		87	96.5	18.7	
12:45			82	70	30	11.88	9.25		87	96.5	18.7	
13:00			82	70	30	11.88	9.25		87	96.5	18.7	
13:15			82	70	30	11.88	9.25		87	96.5	18.7	
13:30			82	70	30	11.88	9.25		87	96.5	18.7	
13:45			82	70	30	11.88	9.25		87	96.5	18.7	
14:00			82	70	30	11.88	9.25		87	96.5	18.7	
14:15			82	70	30	11.88	9.25		87	96.5	18.7	
14:30			82	70	30	11.88	9.25		87	96.5	18.7	
14:45			82	70	30	11.88	9.25		87	96.5	18.7	
15:00			82	70	30	11.88	9.25		87	96.5	18.7	
15:15			82	70	30	11.88	9.25		87	96.5	18.7	
15:30			82	70	30	11.88	9.25		87	96.5	18.7	
15:45			82	70	30	11.88	9.25		87	96.5	18.7	
16:00			82	70	30	11.88	9.25		87	96.5	18.7	
16:15			82	70	30	11.88	9.25		87	96.5	18.7	
16:30			82	70	30	11.88	9.25		87	96.5	18.7	
16:45			82	70	30	11.88	9.25		87	96.5	18.7	
17:00			82	70	30	11.88	9.25		87	96.5	18.7	
17:15			82	70	30	11.88	9.25		87	96.5	18.7	
17:30			82	70	30	11.88	9.25		87	96.5	18.7	
17:45			82	70	30	11.88	9.25		87	96.5	18.7	
18:00			82	70	30	11.88	9.25		87	96.5	18.7	
18:15			82	70	30	11.88	9.25		87	96.5	18.7	
18:30			82	70	30	11.88	9.25		87	96.5	18.7	

12.22 KC  
12.91 KC  
run at medium flow rate  
DME sample 18:20



25 Disk Rotary Filter Data Sheet													
Date:	1-31-08												
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc PG-1 (PSI)	Filtrate PG-2 (gal)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments	Recorded by
0800	68	206	77	70	30	1190	867	60	87.5	72.5	19.1	Started Run	Soren
0815			91	70	30	1190	897		87.5	73.0	18.7		Soren
0830			93	70	30	1190	917		87.5	74.0	18.6		Soren
0845			93	70	30	1190	917		87.5	74.0	18.6		Soren
0900			93	70	30	1190	917		87.5	74.0	18.6		Soren
0915			93	70	30	1190	917		87.5	74.0	18.6		Soren
0930			93	70	30	1190	917		87.5	74.0	18.6		Soren
0945			93	70	30	1190	917		87.5	74.0	18.6		Soren
1000			93	70	30	1190	917		87.5	74.0	18.6		Soren
1015			93	70	30	1190	917		87.5	74.0	18.6		Soren
1030			93	70	30	1190	917		87.5	74.0	18.6		Soren
1045			93	70	30	1190	917		87.5	74.0	18.6		Soren
1100			93	70	30	1190	917		87.5	74.0	18.6		Soren
1115			93	70	30	1190	917		87.5	74.0	18.6		Soren
1130			93	70	30	1190	917		87.5	74.0	18.6		Soren
1145			93	70	30	1190	917		87.5	74.0	18.6		Soren
1213			93	70	30	1190	917		87.5	74.0	18.6		Soren
1230			93	70	30	1190	917		87.5	74.0	18.6		Soren
1245			93	70	30	1190	917		87.5	74.0	18.6		Soren
1300			93	70	30	1190	917		87.5	74.0	18.6		Soren
1315			93	70	30	1190	917		87.5	74.0	18.6		Soren
1330			93	70	30	1190	917		87.5	74.0	18.6		Soren
1345			93	70	30	1190	917		87.5	74.0	18.6		Soren
1400			93	70	30	1190	917		87.5	74.0	18.6		Soren
1415			93	70	30	1190	917		87.5	74.0	18.6		Soren
1430			93	70	30	1190	917		87.5	74.0	18.6		Soren
1445			93	70	30	1190	917		87.5	74.0	18.6		Soren
1500			93	70	30	1190	917		87.5	74.0	18.6		Soren
1515			93	70	30	1190	917		87.5	74.0	18.6		Soren
1530			93	70	30	1190	917		87.5	74.0	18.6		Soren
1545			93	70	30	1190	917		87.5	74.0	18.6		Soren
1600			93	70	30	1190	917		87.5	74.0	18.6		Soren
1615			93	70	30	1190	917		87.5	74.0	18.6		Soren
1630			93	70	30	1190	917		87.5	74.0	18.6		Soren
1645			93	70	30	1190	917		87.5	74.0	18.6		Soren
1700			93	70	30	1190	917		87.5	74.0	18.6		Soren

6

25 Disk Rotary Filter Data Sheet												
Date:	2/1/08											
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. PG-1 (PSI)	Filtrate PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Recorded by
0945	68	0.24	73	30	30	11.91	8.95	6.0	71.5	33.5	14.6	13.11 kW Added solids to 0.25% DTH
0946			71	31	31	11.91	8.95		71.5	33.5	14.6	Comments
0948			70	30	30	11.80	8.91		71.5	33.5	14.6	
0949			70	30	30	11.80	8.91		71.5	33.5	14.6	Pullled Filtrate Sample Vibration measurements being taken
0950			70	30	30	11.80	8.91		71.5	33.5	14.6	
0952			70	30	30	11.80	8.91		71.5	33.5	14.6	Subst
0953			70	30	30	11.80	8.91		71.5	33.5	14.6	
1038			70	30	30	11.80	8.91		71.5	33.5	14.6	Subst
1048			70	30	30	11.80	8.91		71.5	33.5	14.6	
1107			70	30	30	11.80	8.91		71.5	33.5	14.6	Subst
1113			70	30	30	11.80	8.91		71.5	33.5	14.6	
1145			70	30	30	11.80	8.91		71.5	33.5	14.6	Subst
1201			70	30	30	11.80	8.91		71.5	33.5	14.6	
1258			70	30	30	11.80	8.91		71.5	33.5	14.6	Subst
1315			70	30	30	11.80	8.91		71.5	33.5	14.6	
1335			70	30	30	11.80	8.91		71.5	33.5	14.6	Subst
1427			70	30	30	11.80	8.91		71.5	33.5	14.6	
1500			70	30	30	11.80	8.91		71.5	33.5	14.6	Subst
1558			70	30	30	11.80	8.91		71.5	33.5	14.6	
1640			70	30	30	11.80	8.91		71.5	33.5	14.6	Subst
1725			70	30	30	11.80	8.91		71.5	33.5	14.6	
1820			70	30	30	11.80	8.91		71.5	33.5	14.6	Subst
1844			70	30	30	11.80	8.91		71.5	33.5	14.6	

25 Disk Rotary Filter Data Sheet												
Date:	2-5-07											
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc PG-1 (PSI)	Filtrate PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (rpm)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
0746	68	0.29	53	70	30	1152	717	60	76	93.5	18.9	Started run
0800			53	70	30	1143	715		76	92.8	19.0	
0813			53	70	30	1151	717		76	93.2	19.0	
0830			53	70	30	1151	717		76	93.5	19.3	
0849			53	70	30	1151	718		76	94.0	19.2	
0900			53	70	30	1151	718		76	94.0	19.2	
0913			53	70	30	1151	718		76	94.0	19.2	
0930			53	70	30	1151	718		76	94.0	19.2	
0949			53	70	30	1151	718		76	94.0	19.2	
1000			53	70	30	1151	718		76	94.0	19.2	
1015			53	70	30	1151	718		76	94.0	19.2	
1030			53	70	30	1151	718		76	94.0	19.2	
1045			53	70	30	1151	718		76	94.0	19.2	
1100			53	70	30	1151	718		76	94.0	19.2	STOPPED RUN
1525			90	70	30	1185	761		90.5	90.5	18.8	12.7L KW
1545			93	70	30	1177	761		91.5	91.5	18.2	
1615			15	72	31	1171	769		99	98.5	18.6	12.35 KW
1650			92	70	30	1163	754		95.5	102	18.5	
1720			93	70	30	1172	751		100	100.5	19.2	12.63 KW
1740			95	70	30	1180	752		95	100.5	18.9	12.38 KW



25 Desk Rotary Filter Data Sheet													
Date	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. PG-1 (PSI)	Filterate PG-2 (gal)	Feed Flow (mA)	Filterate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments	Recorded by
0706	68	0.29	95	70	30	1187	7145	60	94.5	72.6	17.8	Started filter	Susan
0719			92	70	30	1173	7161		94.3	73.0	18.2		Susan
0730			93	70	30	1191	7153		94.5	94.0	19.0		Susan
0742			95	70	30	1178	7153		96.5	94.0	19.8		Susan
0743			95	70	30	1179	7159		99.0	96.5	19.9		Susan
0730			93	70	30	1150	7156		90.5	96.5	19.1		Susan
0740			93	70	30	1163	7181		90.5	96.0	19.1		Susan
0719			94	70	30	1152	7151		92.5	95.5	19.3		Susan
0730			93	70	30	1190	7151		96.8	94.3	19.6		Susan
0745			93	70	30	1191	7151		91.5	95.0	19.5		Susan
1000			94	70	30	1180	7152		91.0	95.5	19.5		Susan
1030			94	70	30	1178	7153		91.5	95.0	19.3		Susan
1049			93	70	30	1191	7151		96.5	95.0	19.3		Susan
1100			93	70	30	1191	7148		92.0	95.0	19.3		Susan
1115			95	70	30	1180	7150		96.0	94.5	19.3		Susan
1130			95	70	30	1183	7150		95.5	94.0	19.5		Susan
1145			95	70	30	1181	7151		96.5	94.5	19.5		Susan
1200			93	70	30	1191	7140		96.5	94.5	18.3		Susan
1210			95	70	30	1180	7141		96.5	94.5	18.3	17.25 KL	Susan
1304			95	70	30	1181	7141		96.5	94.5	18.0		Susan
1330			95	70	30	1186	7141		96	94	18.5		Susan
1400			95	70	30	1173	7140		96	94	18.5		Susan
1530			95	70	30	1177	7143		97.5	102	18.5		Susan
1725			95	70	30	1173	7143		98	98.5	18.7		Susan
1734			95	70	30	1171	7151		95.5	97.5	18.3		Susan
1815			95	70	30	1172	7152		98	100.5	18.5		Susan
1835			95	70	30	1174	7148		97	97.5	18.8		Susan



25 Disk Rotary Filter Data Sheet													
Date:	2/2/08												
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. PG-1 (PSI)	Filtrate PG-2 (gal)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments	Recorded by
8:50	64	0.74	82	70	30	11.78	2.14	60	77	52.5	19.0	12.37 K U	By DWT
8:55			81	70	30	11.76	2.18		91	43.5	19.0	12.55 K U	By DWT
8:58			85	70	30	11.81	2.34		99	39.5	19.0		By DWT
9:00			96	70	30	11.71	2.35		100	101	18.8	12.32 K U	By DWT
9:05			95	70	30	11.67	2.30		97	97	18.5		By DWT
9:10													
9:15													
9:20													
9:25													
9:30													
9:35													
9:40													
9:45													
9:50													
9:55													
10:00													
10:05													
10:10													
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13:20													
13:25													
13:30													
13:35													
13:40													
13:45													
13:50													
13:55													
14:00													

25 D-Sk Rotary Filter Data Sheet												
Date	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Comp. Press (PSI)	Filtrate Press (PSI)	Feed Flow (mA)	Filter Flow (mA)	Rotar Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
10/5	69	0.29	91	70	30	1191	721	60	960	945	18.4	Sum Zoran
10/30			91	70	30	1191	719		930	945	18.4	Sum Zoran
10/26			91	70	30	1191	720		935	945	18.4	Sum Zoran
11/02			91	70	30	1181	720		935	945	18.4	Sum Zoran
11/30			91	70	30	1190	724		930	945	18.4	Sum Zoran
11/45			91	70	30	1191	722		930	945	18.4	Sum Zoran
13/02			91	70	30	1191	721		935	945	18.4	Sum Zoran
12/13			91	70	30	1191	721		935	945	18.4	Sum Zoran

25 Disk Rotary Filter Data Sheet												
Date:	2-11-08											
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. Press PG-1 (PSI)	Filtrate Press PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
0718	6.5	1.29	72	70	70	1193	6.81	60	60.0	72.0	19.6	Started run 12.52 KW
0831			73	70	70	1191	6.69		60.0	72.0	19.6	
0845			ET	70	70	1196	6.95		90.5	92.5	15.5	
0900			91	70	70	1195	6.89		93	95	14.2	
0914			93	70	70	1189	6.93		96.0	93.5	19.2	
0930			93	70	70	1191	6.92		96.0	94.5	18.6	
0949			95	70	70	1198	6.73		95.3	94.0	18.5	Pulled Feed Filter to Sample
1000			95	70	70	1190	6.56		95.2	94.5	18.6	
1013			93	70	70	1192	6.96		96.5	94.0	18.7	
1030			96	70	70	1192	6.96		96.5	94.5	18.6	
1043			93	70	70	1193	6.94		97.0	95.0	19.7	
1100			93	70	70	1194	6.92		101.3	96.3	19.8	
1115			96	70	70	1193	6.93		101.5	96.3	19.8	
1130			96	70	70	1190	6.89		100.8	96.5	19.0	
1145			96	70	70	1190	6.70		101.4	96.5	19.5	
1200			96	70	70	1190	6.91		100.8	92.0	19.1	
1213			97	70	70	1190	6.43		100.5	92.0	19.1	STOPPED RUN
1229			91	70	70	1196	7.00		80	90.5	19.0	Restarted 17.71KW
1517			91	70	70	1186	6.75		55.5	58.5	18.9	
1605			95	70	70	1198	6.89		95.5	85.0	18.9	Working - measurement
1640			96	70	70	1185	6.81				13.6	"
1647			95	70	70	1174	6.97				14.4	Shutdown
1836			93	70	70	1154	7.00				15.2	
1845			95	70	70	1193	7.10					



25 Disk Rotary Filter Data Sheet												
Date:	2-12-08											
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. PG-1 (PSI)	Filtrate PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
0930	6.5	1.29	90	90	30	1191.656	600	92	94	19.1		Started run
0945			90	90	30	1191.657		93.5	90.5	19.0	Comments	
0950			92	90	30	1191.661		91.5	92.5	19.4		Started run
0955			94	90	30	1191.660		93	93.0	19.6	Started run	
0930			94	90	30	1191.660		93.0	93.5	19.7		Started run
0945			93	90	30	1191.659		93.0	94.0	19.7	Started run	
1013			93	90	30	1191.663		93.5	94.0	19.5		Started run
1030			95	90	30	1191.660		94.5	94.5	19.5	Started run	
1045			95	90	30	1191.659		94.5	94.5	19.5		Started run
1100			95	90	30	1191.659		94.5	94.5	19.5	Started run	
1115			93	90	30	1191.659		92.5	94.5	19.4		Started run
1130			93	90	30	1191.653		92.5	94.5	19.3	Started run	
1145			93	90	30	1191.653		92.5	94.5	19.1		Started run
1300			94	90	30	1191.663		93.0	94.5	19.6	Started run	
1315			94	90	30	1191.653		93.0	94.5	19.6		Started run
1345			94	90	30	1191.648		93.0	94.5	19.9	Started run	
1400			94	90	30	1191.646		93.0	94.5	19.7		Started run
1415			94	90	30	1191.644		93.0	94.5	19.7	Started run	
1430			93	90	30	1191.646		93.0	94.5	19.6		Started run
1440			93	90	30	1191.644		93.0	94.5	19.7	Started run	
1515			93	90	30	1191.631		93.0	94.5	18.4		Started run
1530			93	90	30	1191.631		93.0	94.5	18.4	Started run	

25 Disk Rotary Filter Data Sheet												
Date:	2/13/08											
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc PG-1 (PSI)	Filtrate Press PG-2 (psi)	Feed Flow (mA)	Filtrate Flow (mA)	Rotary Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
8:14	65	1.77	80	70	30	1173	614	60	78.5	80.5	15.3	detached coupling alignment 12.96 KW
9:30			93	70	30	1181	633	60	86	83	18.8	
10:00			94	70	30	1180	637	60	87	83.5	18.8	
10:30			95	70	30	1179	638	60	87	83.5	18.8	
10:45			93	70	30	1178	639	60	87	83.5	18.8	
11:00			96	70	30	1181	635	60	88	84.5	19.2	
11:10			96	70	30	1181	632	60	88	84.5	19.2	
11:45			93	70	30	1178	634	60	87	83.5	19.1	
12:00			93	70	30	1178	635	60	87.5	83.0	19.1	
12:15			96	70	30	1180	631	60	89.0	84.5	19.3	
13:00			96	70	30	1180	633	60	89.0	84.5	19.3	
13:45			96	70	30	1180	634	60	89.0	84.5	19.3	
13:50			96	70	30	1180	631	60	89.0	84.5	19.3	
13:55			96	70	30	1180	631	60	89.0	84.5	19.3	
14:00			96	70	30	1180	633	60	89.0	84.5	19.4	
14:15			96	70	30	1179	633	60	89.5	84.5	19.1	
14:30			96	70	30	1179	637	60	89.5	84.5	19.2	
14:45			96	70	30	1180	637	60	89.5	84.5	19.2	
14:50			96	70	30	1180	638	60	89.5	84.5	19.2	
15:00			96	70	30	1180	638	60	89.5	84.5	19.1	
15:15			96	70	30	1180	638	60	89.5	84.5	19.1	
15:30			96	70	30	1180	638	60	89.5	84.5	19.1	
16:07			95	70	30	1180	638	60	89.5	84.5	19.1	
16:50			95	70	30	1180	638	60	89.5	84.5	19.1	
17:31			95	70	30	1179	635	60	89.5	84.5	19.3	
19:18			95	70	30	1177	638	60	89.5	84.5	19.1	

25 Disk Rotary Filter Data Sheet												
Date:	8-15-08											
Time	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Conc. Press (PSI)	Filtrate PG-2 (cst)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
1325	127	12.7	90	30	30	1172.557	650	715	73.5	19.7		Started run
1330			90	30	1172.377		99.0	96.0	19.7			
1335			90	30	1171.513		100.5	96.0	19.7			
1345			90	30	1172.613		100.5	96.0	19.1			
1400			90	30	1174.613		100.5	93.5	19.3			
1415			95	30	1173.613		97.5	94.5	19.3		Pulled 5 Litrate Sample	
												Shut down



25 Disk Rotary Filter Data Sheet													
Date:	Tank Level (gal)	Solids Loading (wt %)	Temp (F)	Core Press PG-1 (PSI)	Filtrate Press PG-2 (PSI)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments	Recorded by
2/19	65	1.29	67	70	30	145	5.63	60	68	70.5	20.0	13.46 kW	BYE
1420			66	70	30	146	5.89	60	68	70.5	19.1	13.67 kW	BYE
1521			69	70	30	148	5.95	60	69	70.5	18.8	13.90 kW	BYE
1619			69	70	30	146	5.88	60	68	70.5	19.1	13.93 kW	BYE
1692			69	70	30	149	6.01	60	68	70.5	18.7	13.55 kW	BYE
1715			65	70	30	140	5.84	60	68	70.5	18.8	13.94 kW	BYE
1738			62	70	30	148	5.93	60	68	70.5	18.5	13.50 kW	BYE

25 Disk Rotary Filter Data Sheet																
Date:	Tank Solids			Conc.			Filtrate		Rotor		Rotary		Motor		Comments	Recorded by
Time	Level (gal)	Loading (wt %)	Temp (F)	PG-1 (psi)	PG-2 (psi)	Flow (mA)	Filtrate Flow (mA)	Speed (Hz)	Temp (F)	Temp (F)	Current (amps)					
08:13	60	1.29	99	70	30	11.975.38	60	63	72.5	19.5						
08:30			93	70	30	11.875.97		71.5	83.0	19.9						
08:42			94	70	30	11.836.10		71.0	82.9	19.7						
09:13			94	70	30	11.826.10		73.6	83.5	19.1						
09:30			94	70	38	11.8316.09		74.9	83.3	19.1						
09:45			94	70	30	11.826.11		76.5	88	19.0						
10:00			94	71	30	11.826.11		78.5	88.5	19.0						
10:15			93	70	30	11.786.11		78.0	87.8	19.2						
10:30			93	70	30	11.826.09		78.0	88.0	19.2						
10:45			93	70	30	11.826.11		78.5	88.0	19.2						
11:00			93	70	30	11.796.15		78.5	88.0	19.9						
11:15			95	70	30	11.796.15		79	88.9	19.3						
11:30			95	70	30	11.796.15		79	88.9	19.3						
11:45			95	72	30	11.796.15		79	88.9	19.3						
12:00			95	70	30	11.796.15		79	88.9	19.3						
12:15			95	70	30	11.796.15		79	88.9	19.3						
12:30			95	70	30	11.796.15		79	88.9	19.3						
12:45			95	70	30	11.796.15		79	88.9	19.3						
13:00			95	70	30	11.796.15		79	88.9	19.3						
13:15			95	70	30	11.796.15		79	88.9	19.3						
13:30			95	70	30	11.796.15		79	88.9	19.3						
13:45			95	70	30	11.796.15		79	88.9	19.3						
14:00			95	70	30	11.796.15		79	88.9	19.3						
14:15			95	70	30	11.796.15		79	88.9	19.3						
14:30			95	70	30	11.796.15		79	88.9	19.3						
14:45			95	70	30	11.796.15		79	88.9	19.3						
15:00			95	70	30	11.796.15		79	88.9	19.3						
15:15			95	70	30	11.796.15		79	88.9	19.3						
15:30			95	70	30	11.796.15		79	88.9	19.3						
15:45			95	70	30	11.796.15		79	88.9	19.3						
16:00			95	70	30	11.796.15		79	88.9	19.3						



25 Disk Rotary Filter Data Sheet												
Date:	2-21-08											
Time (h:mm)	Tank Level (gal)	Solids Loading (wt %)	Tamp (F)	Conc. Press PG-1 (PSI)	Filtrate Press PG-2 (PSI)	Feed Flow (mA)	Filtrate Flow (mA)	Rotor Speed (Hz)	Seal Temp (F)	Rotary Joint Temp (F)	Motor Current (amps)	Comments
1435	60	1.79	96	70	30	11.83	5.52	60	66.8	72.5	19.6	Started Run
1443						11.83	5.71		77.5	86.5	19.9	
1448						11.79	5.51		84.3	90.8	19.9	
1450						11.77	5.56		94.0	91.5	19.9	
1453						11.79	5.99		93.0	92.3	19.8	
1454						11.70	5.95		96.5	95.0	19.8	
1456						11.51	5.55		95.4	94.0	19.1	
1458						11.90	5.59		95.0	96.0	19.1	
1459						11.54	5.58		94.0	94.9	19.1	
1459						11.54	5.58		96.5	94.9	19.1	
1500						11.73	5.97		97.5	95.0	19.1	Pulled Filtrate Sample
1505						11.73	5.97		97.3	94.5	19.1	
1515						11.73	5.97		97.3	94.5	19.1	
1525						11.73	5.97		97.3	94.5	19.1	
1535						11.73	5.97		97.3	94.5	19.1	
1545						11.73	5.97		97.3	94.5	19.1	
1555						11.73	5.97		97.3	94.5	19.1	
1605						11.73	5.97		97.3	94.5	19.1	
1615						11.73	5.97		97.3	94.5	19.1	
1625						11.73	5.97		97.3	94.5	19.1	
1635						11.73	5.97		97.3	94.5	19.0	sh. h.d.u.

25 Disk Rotary Filter Data Sheet																									
Date:	7/77	Tank Level (gal)	60	Solids Loading (wt %)	12.5	Temp (F)	71	Conc PG-1 (PSI)	70	Fitrate PG-2 (psi)	30	Feed Flow (mA)	4.78	Filtrate Flow (mA)	5.72	Rotor Speed (Hz)	60	Seal Temp (F)	86	Rotary Joint Temp (F)	71	Motor Current (amps)	4.3	Comments	Disc's for disk
Time (hh:mm)	11:25																								
	11:45																								
	12:05																								
	12:25																								
<p>Recorded by: <i>[Signature]</i></p>																									

Appendix B: Solid Particles

