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AEC RESEARCH AND DEVELOPMENT REPORT

**PREPARATION OF REACTOR-GRADE  $UO_2$   
FROM  $UO_3$  BY ARC FUSION**

C. B. GOODLETT

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*Savannah River Laboratory*

*Aiken, South Carolina*

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Technology - Feed Materials  
(TID-4500)

**PREPARATION OF REACTOR-GRADE  $UO_2$   
FROM  $UO_3$  BY ARC FUSION**

by

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Approved by

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August 1968

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**CONTRACT AT(07-2)-1 WITH THE  
UNITED STATES ATOMIC ENERGY COMMISSION**

## ABSTRACT

An arc-fusion process was developed that converts  $\text{UO}_3$  to reactor-grade  $\text{UO}_2$ .  $\text{UO}_3$  is fed to a carbon-arc furnace with internally insulated walls that maintain the temperature of the entire charge above the decomposition temperature of  $\text{UO}_3$  ( $\sim 650^\circ\text{C}$ ), and thereby eliminate diffusion of oxygen from  $\text{UO}_3$  at the walls to product nearer the center.

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## INTRODUCTION

A major production cycle at the Savannah River Plant (SRP) uses fuel elements made from natural or slightly enriched uranium metal. After irradiation, these elements are dissolved and the plutonium and uranium are separated from fission products. The recovered depleted uranium is converted to  $UO_3$ , and is stored in warehouses.

Recycle of this uranium within the Savannah River Plant was believed, at the time of this study, to offer cost savings and increased flexibility of production. Since the  $UO_3$  produced is not sufficiently stable for irradiation, it must be converted to a lower oxide such as  $U_3O_8$  or  $UO_2$  to give satisfactory operation in a reactor. In this mode of recycle, uranyl nitrate solution from SRP would be "sweetened" slightly in  $^{235}U$  before denitration to  $UO_3$ , the  $UO_3$  would be converted to reactor-grade  $UO_2$  (high density, low gas and impurity content), and the  $UO_2$  would be fabricated into fuel elements by vibratory compaction.

Reactor-grade  $UO_2$  has been produced from  $UO_3$  commercially by several processes. <sup>(1)</sup>

- High-fired  $UO_2$  produced from milled  $UO_2$  powder: Reduction of  $UO_3$  to  $UO_2$  in a hydrogen atmosphere, pulverizing to ~1 micron, production of "green" pellets using a binding agent, and sintering in a  $CO_2$  atmosphere followed by firing at  $1700^\circ C$  in a hydrogen atmosphere.
- High-fired  $UO_2$  produced from ammonium diuranate (ADU): Same as above, except the fine  $UO_2$  powder is formed by ADU precipitation from uranium hexafluoride.
- Arc fusion of "light"  $UO_2$  to dense  $UO_2$  by melting in an electric-arc furnace. <sup>(2)</sup>

A variety of other methods, including variations of the first two above, have been studied on an experimental scale, but none has been put into large-scale plant practice in the United States. Experimental work of a scouting nature was done at the Savannah River Laboratory (SRL) on three alternative processes aimed primarily at low capital expenditures.

- Reduction and sintering of pelletized  $UO_3$  with hydrogen in a resistance furnace.<sup>(3)</sup>
- Decomposition and sintering of large-granule  $UO_3$  in an induction furnace.
- Decomposition and fusion of  $UO_3$  with a plasma-arc or carbon-arc, skull-melting technique.

Preliminary experimental work on the first two processes indicated potential problems in obtaining the desired density, whereas the work with a carbon arc was encouraging. Therefore, a program was undertaken at SRL to develop a process for direct conversion of  $UO_3$  to reactor-grade  $UO_2$  by carbon-arc fusion. The results of the program are summarized in this report.

## SUMMARY

An arc-fusion process was developed that converts  $UO_3$  to reactor-grade  $UO_2$  with an O/U ratio between 2.00 and 2.05, a particle density >95% of theoretical, and impurity contents of <100 ppm  $N_2$  and <100 ppm carbon.  $UO_3$  is fed to a carbon-arc furnace with internally insulated walls that maintain the temperature of the entire charge above the decomposition temperature of  $UO_3$  (~650°C), and so eliminate diffusion of oxygen from  $UO_3$  at the walls to product nearer the center. Both melting and cooling are done under a flowing blanket of argon, as still another measure to control oxygen and nitrogen content of the product.  $UO_3$  powder is continuously added to the furnace by a screw feeder as fusion occurs; the product is removed as a batch after cooling. Temperatures in excess of 2850°C, the melting point of  $UO_2$ , are attained during the heating period.

## DISCUSSION

### PRIOR KNOWLEDGE

Nonreactor-grade  $UO_2$  or  $U_3O_8$  is fused by carbon arcs in water-cooled steel vessels by the Norton Company<sup>(2)</sup> after  $UO_3$  is reduced to the nonreactor-grade oxides in a separate facility. The  $UO_3$  or  $U_3O_8$  is fed into the vessels continuously, and the carbon electrodes are withdrawn as the liquid level rises. After the charge has been melted and allowed to cool, the product is removed as a central mass of fused material with a "skull" of unmelted material at the wall. The Norton Company was recently granted a patent<sup>(4)</sup> on their process for making reactor-grade  $UO_2$  by using a gas purge through the oxide during cooling to control impurities and stoichiometry.\*

### DESCRIPTION OF EQUIPMENT

#### 10-Inch Carbon-Arc Furnace

A 10-inch (ID) carbon-arc furnace with a 4-inch diameter electrode (Figure 1) was built entirely of carbon, with no special provision for cooling the crucible. The carbon pot itself was used as the anode; the carbon rod, as cathode. Power was supplied by a 40-kw, 55-volt DC welding machine. The rod was held stationary while the carbon pot was moved up and down with a scissors jack. A "blanket gas" line was also provided. The unit was later modified for addition of feed during a test.

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\* When SRL began this study on direct conversion of  $UO_3$  to reactor-grade  $UO_2$ , the Norton Company was not in a position to reveal their proprietary information; so much of the process had to be developed independently.

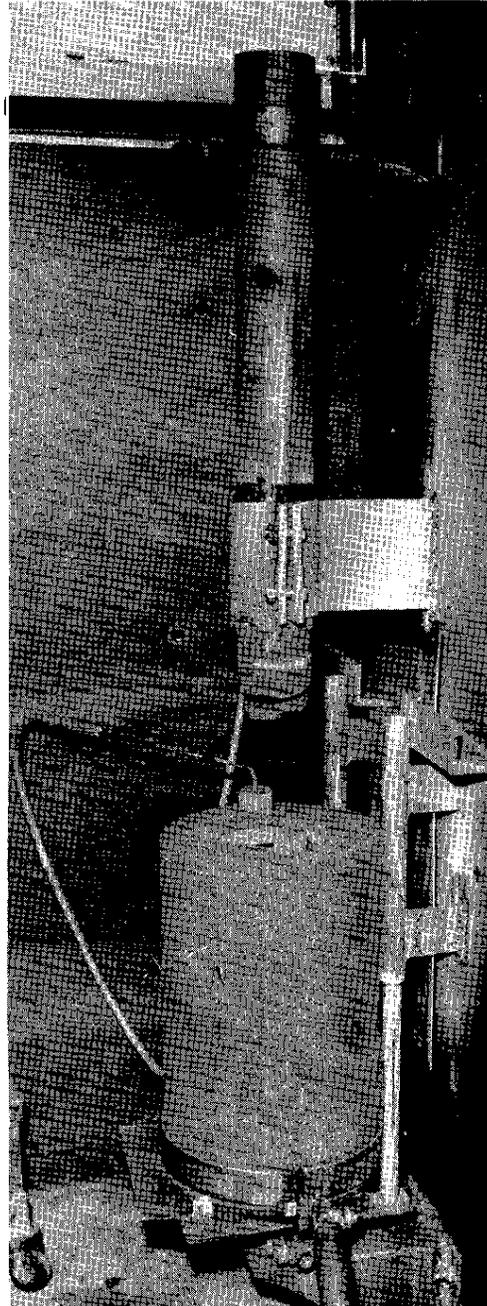
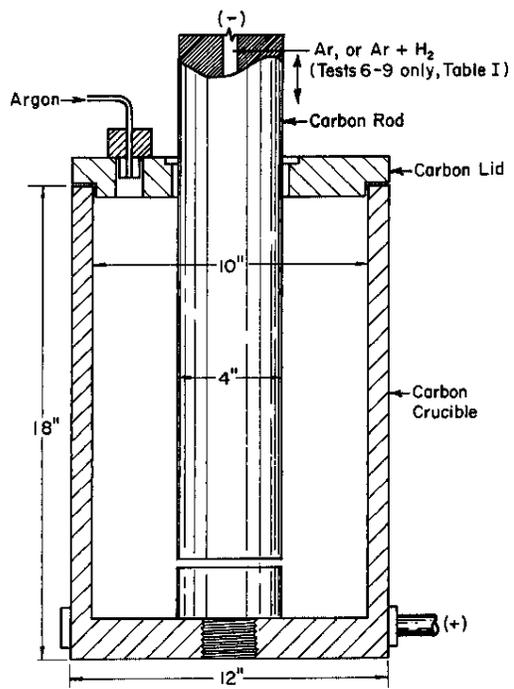


FIG. 1 10-INCH CARBON-ARC FURNACE

### 18-inch Carbon-Arc Furnace

In order to produce large batches of material and to obtain operating experience with equipment more suitable for plant operation, an arc furnace with an 18-inch-diameter steel crucible, a 6-inch-diameter movable electrode (initially), and an 80-kw power supply was fabricated (Figure 2). The steel crucible was surrounded by a water jacket, and had a stationary, but replaceable, carbon electrode projecting through the bottom. The movable electrode was positioned by a motor-driven screw. A vibrator was attached to the crucible to assist in moving the feed into the melt zone. The unit was later modified to use an 8-inch movable electrode.

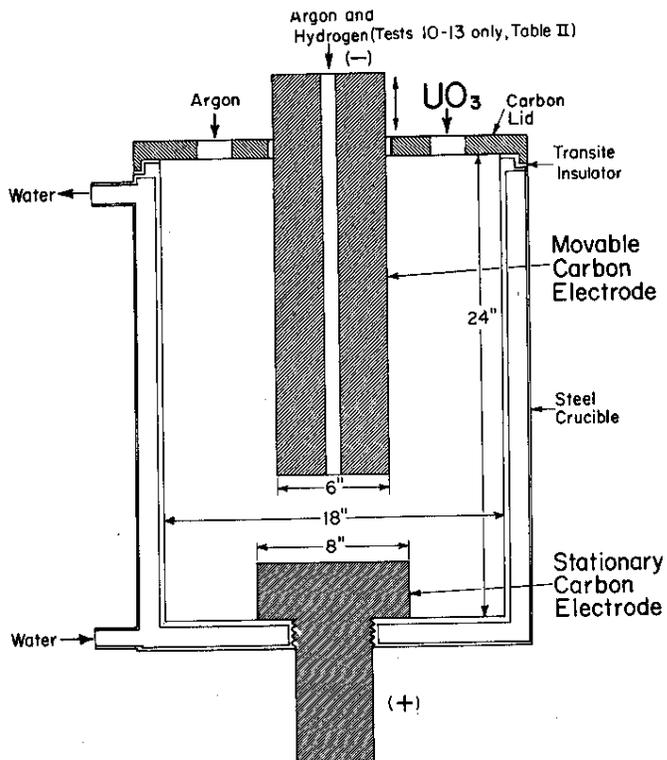
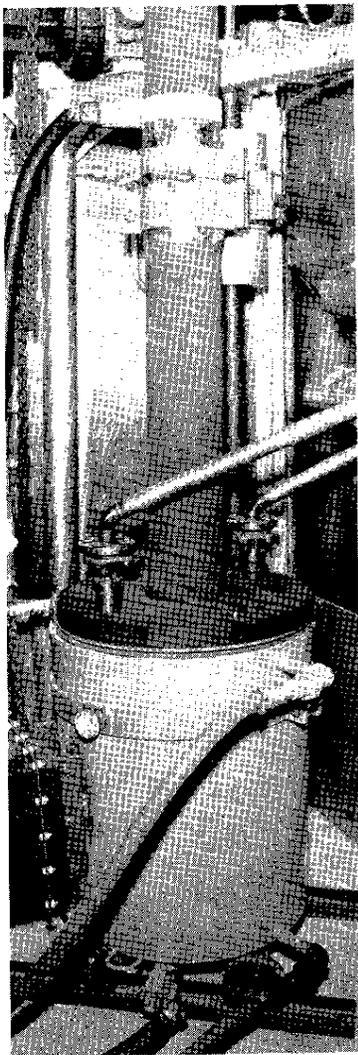


FIG. 2 18-INCH CARBON-ARC FURNACE

## TEST PROCEDURES AND RESULTS

### 10-Inch Carbon-Arc Furnace

#### *Mode of Operation*

In a typical fusion test, the crucible was raised until it touched the carbon rod, and was then filled with uranium oxide powder. Power was applied to the furnace, and the spacing between the carbon rod and the carbon crucible or melt surface (depending on condition of crucible contents) was adjusted to maintain the current at the 800-ampere capacity of the welding machine; the potential at this current was ~50 volts. Argon at 15 scfh was fed into the top of the furnace to exclude air.

Approximately one-half hour after a typical test was started, the top half of the furnace would glow at ~800°C, and a carbon monoxide flame issued from the annulus between the electrode and lid. The portion of the interior that was visible through an optical pyrometer sighted between the carbon rod and the carbon lid was at 1200 to 1400°C. When the electrode was withdrawn at the end of the test, the original full charge of granules had shrunk and the arc was no longer insulated thermally. The insulative layer apparently had been lost after one-half hour of operation, corresponding to glowing of the upper part of the vessel. Therefore, the furnace was modified to allow the addition of uranium oxide powder during fusion in order to maintain an insulating layer at the top surface of the melt.

#### *Effect of O/U Ratio on N<sub>2</sub> Content*

Nine arc-fusion tests were made in the 10-inch furnace: two with crushed UO<sub>2.00</sub> feed of ~88% theoretical density and seven with UO<sub>3</sub> prepared at SRP. Two of the UO<sub>3</sub> tests were made with an argon purge down the center of the electrode during the fusion, and a hydrogen-argon purge through the electrode during the cooling period. Two UO<sub>3</sub> tests were made with no purge during fusion, but with the hydrogen-argon purge through the electrode during cooling. The results of all the tests, summarized in Table I, show that when the O/U ratio of the product is slightly greater than 2.00, the nitrogen content is acceptably low (<50 ppm), but when

TABLE I  
Arc-Fused Uranium Oxide in 10-Inch Furnace<sup>a</sup>

| Test | Starting Material<br>Feed | Nitrogen, ppm         | Purge Gas Flow, scfh |                   |                        |                           | Fusion,<br>min | Mass,<br>lb | O/U<br>Ratio | Product                   |                            | Carbon,<br>ppm |
|------|---------------------------|-----------------------|----------------------|-------------------|------------------------|---------------------------|----------------|-------------|--------------|---------------------------|----------------------------|----------------|
|      |                           |                       | To Pot<br>Fusion     | To Pot<br>Cooling | To Electrode<br>Fusion | To Electrode<br>Cooling   |                |             |              | Nitrogen, ppm<br>Kjeldahl | ppm<br>Fusion <sup>b</sup> |                |
| 1    | UO <sub>2</sub> .00       | 20-70                 | 15 Ar                | 15 Ar             | None                   | None                      | 60             | 25          | 1.91         | 840                       | -                          | <25            |
| 2    | UO <sub>2</sub> .00       | 20-70                 | 15 Ar                | 15 Ar             | None                   | None                      | 120            | 10          | 1.91         | 820                       | -                          | <25            |
| 3    | UO <sub>3</sub>           | 5,000<br>to<br>10,000 | 15 Ar                | 15 Ar             | None                   | None                      | 30             | 35          | 1.99         | 210                       | -                          | <25            |
| 4    | UO <sub>3</sub>           |                       | 15 Ar                | 15 Ar             | None                   | None                      | 60             | 50          | 2.04         | 15                        | -                          | <25            |
| 5    | UO <sub>3</sub>           |                       | 15 Ar                | 15 Ar             | None                   | None                      | 60             | 75          | 2.12         | <20                       | -                          | <25            |
| 6    | UO <sub>3</sub>           |                       | 15 Ar                | 15 Ar             | 15 Ar                  | 29 Ar, 1.2 H <sub>2</sub> | 20             | 50          | 2.11         | -                         | -                          | -              |
| 7    | UO <sub>3</sub>           |                       | 15 Ar                | 15 Ar             | 15 Ar                  | 29 Ar, 1.2 H <sub>2</sub> | 85             | 100         | 2.10         | <10                       | 30                         | 155            |
| 8    | UO <sub>3</sub>           | 10,000                | 15 Ar                | 15 Ar             | None                   | 29 Ar, 1.2 H <sub>2</sub> | 210            | 71          | 2.05         | <10                       | 50                         | 70             |
| 9    | UO <sub>3</sub>           |                       | 15 Ar                | 33 Ar             | None                   | 14 Ar, 3.0 H <sub>2</sub> | 205            | 25          | 1.95         | 510                       | 660                        | 185            |

<sup>a</sup> UO<sub>3</sub> feed added during fusion starting with Test 5.

<sup>b</sup> Analytical technique reported in Reference 5, which includes both absorbed and combined nitrogen.

the ratio is slightly less than 2.00, the nitrogen content is high (up to 650 ppm). The latter relationship holds even when  $UO_2$  with low nitrogen content is used as the feed material. Apparently, substoichiometric  $UO_2$  picks up nitrogen to fill available sites in the oxygen-deficient uranium.

*Low Density  $UO_2$*

Two tests (6 and 7) made with argon (added through the electrode during the fusion) produced material that was porous and would not meet density specifications (>95% of theoretical); a column of unfired material was observed in the center of the ingot, apparently the result of cooling by the argon.

Photographs of typical  $UO_2$  product are shown in Figure 3, and a cross section of a typical product charge in place in the furnace is shown in Figure 4.

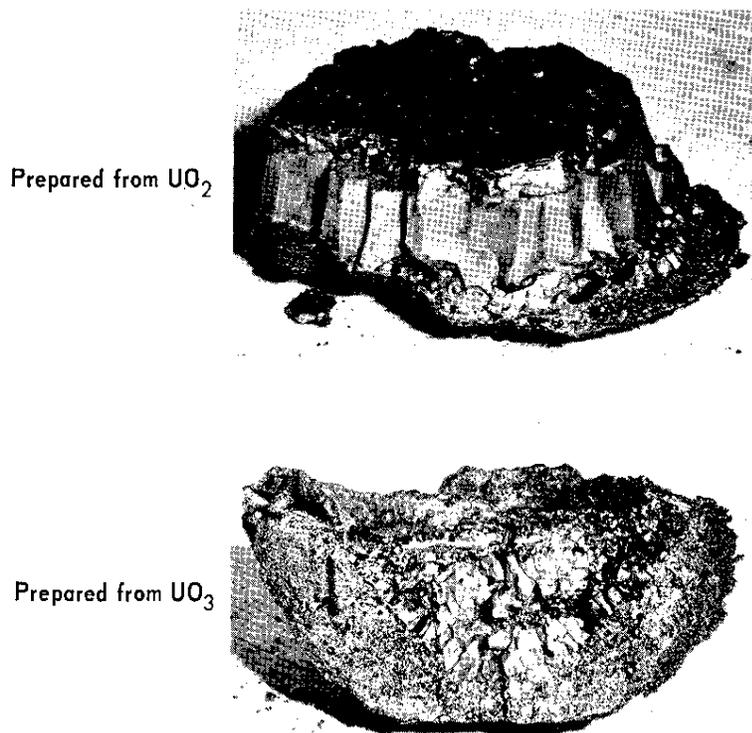


FIG. 3  $UO_2$  PRODUCED IN 10-INCH FURNACE

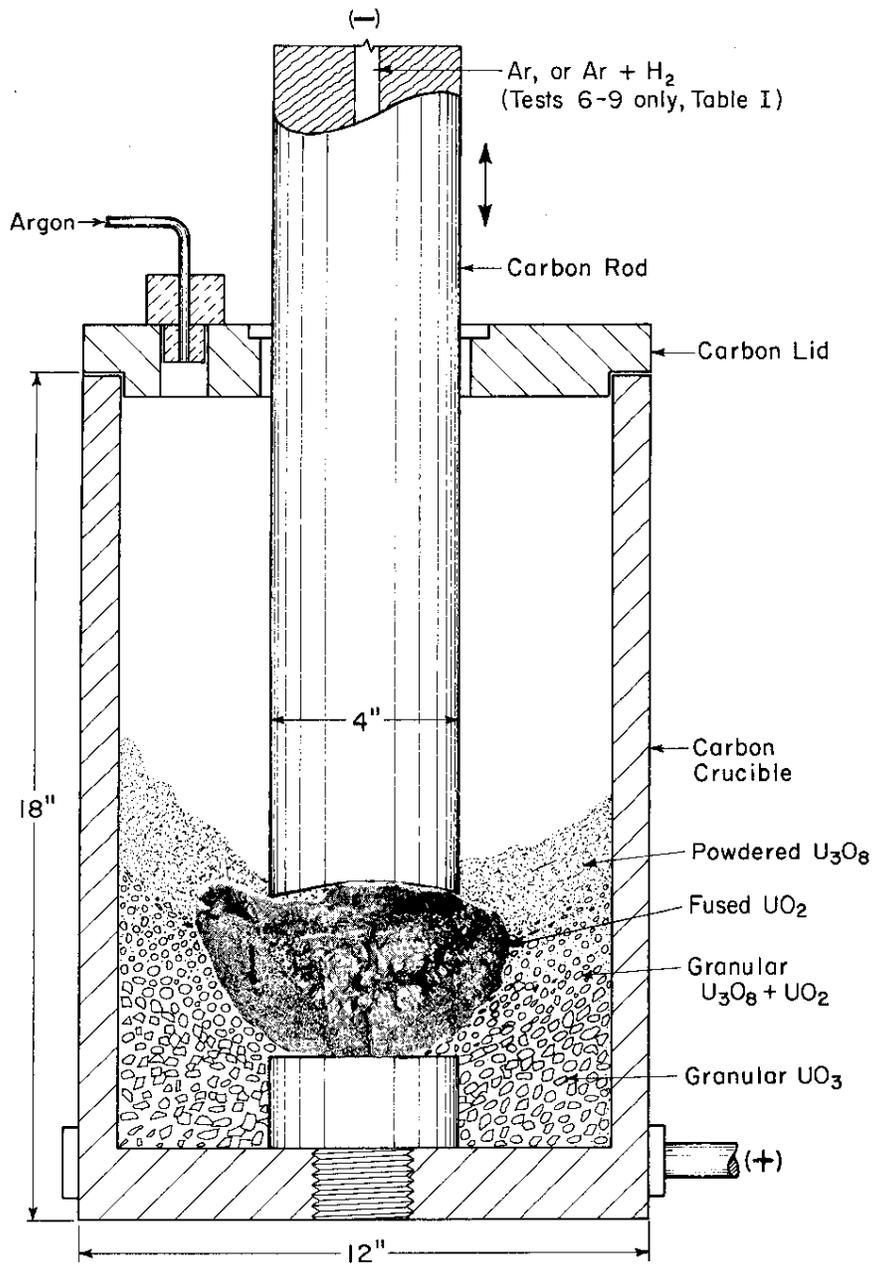


FIG. 4 TYPICAL PRODUCT CHARGE IN 10-INCH FURNACE

## 18-Inch Carbon-Arc Furnace

### *Mode of Operation*

Operation of the 18-inch furnace was basically the same as for the 10-inch furnace except that for each run the crucible initially contained uranium to a level only ~1 inch above the top of the stationary electrode. The current was maintained at 1000 amperes (limited by current carrying capacity of electrical connections) by adjusting the distance between the end of the movable electrode and the fixed electrode of melt. The feed rate of fresh oxide and the input power were controlled to maintain temperatures of 1100 to 1400°C at the top part of the furnace (measured by sighting through a hole in the furnace top with an optical pyrometer); temperatures above 1400°C at the top of the furnace resulted in rapid deterioration of the carbon lid and excessive electrode consumption. The temperature of the melt exceeded 2850°C.

During the initial part of each test the unit was operated at low feed rates (30% of feeder capacity) and full power (~70 kw), while near the end of the fusion the power had to be reduced to (~50 kw) even at maximum feed rate. The energy consumed in the actual reduction reaction is small; the energy required for heating is reduced as the quantity of material in the furnace increases and acts as an insulator. Typical feed rates and power requirements are shown in Figure 5. Inspection of the furnace after operating for 3 hours showed negligible product, indicating that until the furnace contains appreciable hot oxide no product is formed.

### *Effect of Temperature on O/U Ratio*

The data obtained from nine tests in the 18-inch furnace are summarized in Table II. The product from each of the first three tests was unacceptably high in oxygen (O/U from 2.09 to 2.20), even though a reducing atmosphere was maintained in the furnace during cooling. The high ratio of oxygen to uranium was attributed to diffusion of oxygen, during the cooling period, from

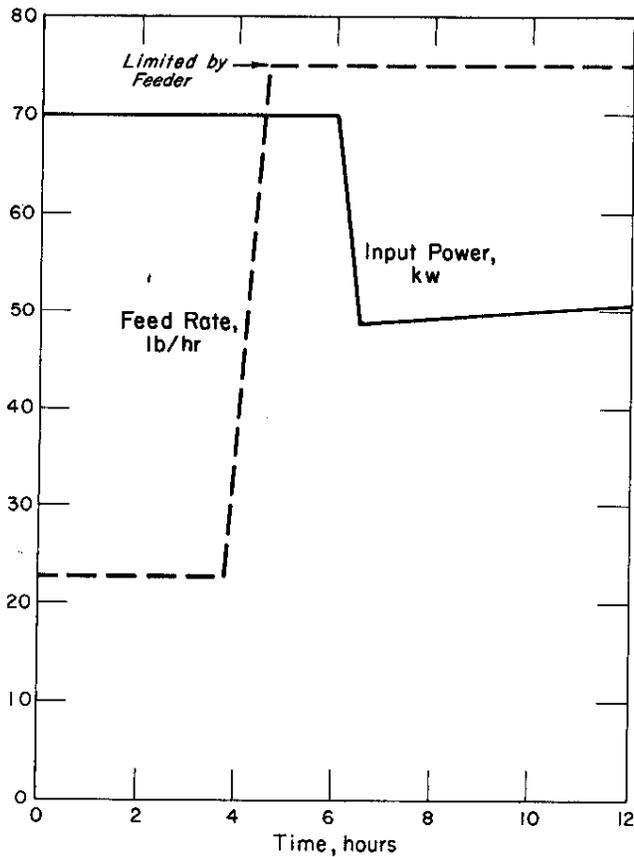


FIG. 5 TYPICAL INPUT POWER AND FEED RATE DURING ARC FUSION OF  $UO_3$  IN 18-INCH FURNACE

undecomposed  $UO_3$  found near the cold furnace walls to the relatively hot  $UO_2$ . Justification for this interpretation was found in the fact that lower O/U ratios were obtained in previous tests made with the uncooled graphite crucible (10-inch furnace) for which wall temperatures were at least  $500^\circ C$ . One test in the 18-inch furnace, which was stopped early because of equipment malfunction, had little  $UO_3$  present and also had a low O/U ratio (1.98 and 2.01).

The foregoing evidence indicated that maintaining the temperature in the crucible above the decomposition temperature of  $UO_3$  ( $UO_3 \xrightarrow{650^\circ C} U_2O_8 \xrightarrow{1125^\circ C} UO_2$ ) eliminates oxygen that can combine with the product during extended cooling periods. Consequently, an insu-

TABLE II

## Arc-Fused Uranium Oxide in 18-Inch Furnace

| Test | Equipment  | Purge Gas Flow, scfh |         |  | Weight,<br>lb | O/U<br>Ratio  | Product <sup>a</sup> |                   |
|------|--|----------------------|---------|--|---------------|---|----------------------|-------------------|
|      |  | To Pot               |         | To Electrode                           |               |   | Nitrogen,<br>ppm     | Carbon,<br>ppm    |
|      |  | Fusion               | Cooling | Cooling                                |               |   |                      |                   |
| 10   | Cold Wall, 6" Movable Electrode, Manual Feed                                 | 15 Ar                | 32 Ar   | 14 Ar, 4.0 H <sub>2</sub>              | 105           | 2.13<br>2.09  | 30<br>10             | 85<br>70          |
| 11   | "  | 15 Ar                | None    | 46 Ar, 4.0 H <sub>2</sub>              | 115           | 2.19<br>2.11  | 50<br>20             | 80<br>100         |
| 12   | "  | 15 Ar                | 32 Ar   | 14 Ar, 4.0 H <sub>2</sub>              | 180           | 2.12<br>2.15<br>2.20  | 55<br>40<br>65       | 80<br>80<br>130   |
| 13   | Insulated Wall, 8" Movable Electrode, Manual Feed                            | 17 Ar                | 32 Ar   | 14 Ar, 4.0 H <sub>2</sub>              | 130           | 2.04<br>2.05<br>2.02  | 40<br>30<br>50       | 25<br>30<br>-     |
| 14   | Insulated Wall, 8" Movable Electrode, Screw Feeder, Gas Purge Tube To Bottom | 17 Ar                | 17 Ar   | 14 Ar, 4.0 H <sub>2</sub> <sup>c</sup> | 160           | 1.93 <sup>d</sup><br>1.99 <sup>e</sup><br>2.02 <sup>f</sup> | 1000<br>690<br>40    | 100<br>800<br>840 |
| 15   | Insulated Wall, 8" Movable Electrode, Screw Feeder                           | 17 Ar                | 45 Ar   | None                                   | 280           | 2.05  | 10                   | 40                |
| 16   | "  | 17 Ar                | 38 Ar   | None                                   | 150           | 2.01  | 80                   | 90                |
| 17   | "  | 17 Ar                | 34 Ar   | None                                   | 340           | 2.02  | 230                  | 120               |
| 18   | "  | 17 Ar                | 34 Ar   | None                                   | 245           | 2.03  | 55                   | 35                |

a Analyses of Tests 14, 15, 16, 17, and 18 were on a crushed and blended composite sample; other analyses were made on grab samples.

b Analytical technique reported in Reference 5 which includes both absorbed and combined nitrogen.

c Hydrogen-argon purge in bottom of crucible instead of through electrode (see text).

d Average of analyses before crushing and blending.

e Analysis of material after crushing and blending.

f Analysis made ~8 weeks after e.

lating liner of 1/4 inch "Kaowool"\* impregnated with "Astrocram"\*\*\* or "Glasrock Slurry"\*\*\* was installed on the inside of the furnace to ensure a high enough temperature to decompose all of the UO<sub>3</sub>. At the same time, the movable electrode diameter was increased to 8 inches to lessen the frequency of replacement, the fixed electrode was increased to 12 inches, and a screw feeder was installed to

\* Trademark of Babcock and Wilcox Company for alumina-silica ceramic insulation.

\*\* Trademark of American Thermocatalytic Corporation for high temperature cement.

\*\*\* Trademark of Glasrock Products Corporation for high temperature silica cement.

provide a more reliable and uniform rate of addition of  $UO_3$ . A cross section of the modified furnace with typical charge is shown in Figure 6.

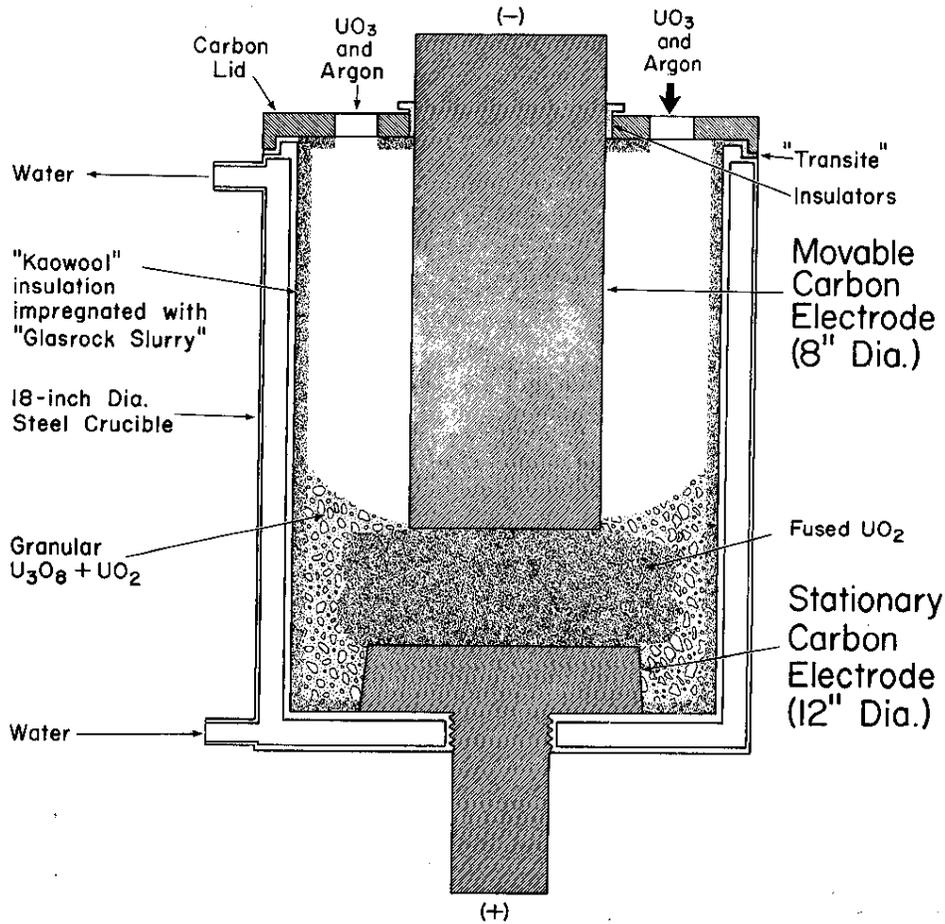


FIG. 6 TYPICAL PRODUCT CHARGE IN INSULATED 18-INCH FURNACE

*Obtaining Reactor-Grade UO<sub>2</sub>*

Four tests were made in the modified furnace using either purified argon (15, 16, 17) or argon-hydrogen (13) as a purge to prevent entry of air. Three of these tests (13, 15, 16) produced reactor-grade UO<sub>2</sub>: an O/U ratio between 2.00 and 2.05, a particle density >95% of theoretical, and impurities of <100 ppm N<sub>2</sub> and <100 ppm C. The product from Test 17 was high in nitrogen (230 ppm) even though the O/U ratio (2.02) was greater than 2.00: this contradicted previous data on nitrogen content versus O/U ratio. The only detectable difference between this run and the others was that the UO<sub>3</sub> feed was considerably older (produced 1/64 versus 12/65 and 8/66); the older feed may have had some additive, e.g., SO<sub>4</sub><sup>2-</sup>, which affected its characteristics. A final test (18) made with UO<sub>3</sub> feed representative of recent plant production (produced 9/67) also resulted in reactor-grade UO<sub>2</sub>. No additional studies were made to determine the reason for this anomaly. Figure 7 is a photograph of part of a fused ingot made in the 18-inch furnace.



FIG. 7 UO<sub>2</sub> PRODUCED IN 18-INCH FURNACE

### *Substoichiometric UO<sub>2</sub>*

Test 14 was made while purging a mixture of 20% H<sub>2</sub> - 80% Ar upward from the bottom of the crucible (the mixture was diluted further with argon before leaving the vessel) during 2 hours of reduced power and no feed, and during the cooling period. Initially the ingot product was low in oxygen (O/U ratio of 1.93) because of the reducing effect of the hydrogen, and the nitrogen content was high (1000 ppm); these results confirmed earlier observations in the 10-inch furnace of the inverse relation between oxygen content and nitrogen content. However, after crushing and blending of the fused ingot, the O/U ratio had increased to 1.99 and the nitrogen content had decreased to 690 ppm (also, surprisingly, the carbon content had increased from 100 to 800 ppm, probably because of accidentally crushing a piece of carbon from the electrode or top cover along with the product). Reanalysis of the crushed and blended sample after exposure to air for several months showed an acceptable O/U ratio (2.01) and nitrogen content (40 ppm), indicating that the oxygen-deficient UO<sub>2</sub> slowly picked up oxygen, and released nitrogen, until an O/U ratio of >2.00 was attained. Therefore, product that has a substoichiometric O/U ratio and high nitrogen content may be usable after crushing and contact with air.

### *Life of Insulating Liner*

The "Astrocram"- "Kaowool" or "Glasrock Slurry"- "Kaowool" liner installed inside the furnace to increase the temperature of the contents has a usable life of only one or two runs before it must be replaced. A cast ceramic liner or a high temperature metal liner backed with "Kaowool" for insulation may be more durable while providing the same temperature control, but tests of more durable liners were not made.

### *Material Balance*

A complete material balance (Table III) indicated that about 50% of the feed to the arc furnace must be recycled. The percent of material recycled should decrease for larger furnaces. About 2% of the UO<sub>2</sub> fed to the furnace was removed as dust through a vent from the hood containing the furnace.

TABLE III

Material Balance for Arc Fusion of  $UO_2$ 

|                  | O/U Ratio | Composition      |                | Weight,<br>lb | U, % |
|------------------|-----------|------------------|----------------|---------------|------|
|                  |           | Nitrogen,<br>ppm | Carbon,<br>ppm |               |      |
| Feed             | 3.0       | -                | -              | 685           | 100  |
| Product          | 2.02      | 230              | 120            | 342           | 53   |
| Recycle          |           |                  |                |               |      |
| Unfused Material | 2.14      | 297              | 700            | 298           | 45   |
| Dust             | 2.8       | 165              | 1400           | 12            | 2    |

*Electrode Consumption*

The movable carbon electrode was consumed at a rate of 0.054 lb per lb of uranium oxide in the crucible. This carbon usage rate is about 1.15 times that required to burn the oxygen to CO during the  $UO_3 \rightarrow UO_2$  reduction; the difference is attributed to inleakage of air. The stationary carbon electrode at the bottom of the crucible was not consumed appreciably during the run, since it was quickly covered with hot  $UO_2$  that then carried the electric discharge.

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